

~~The Paperwork Reduction Act of 1995, no persons are required to respond to a collection of information unless it displays a valid OMB control number.~~

UTILITY PATENT APPLICATION TRANSMITTAL

(Only for new nonprovisional applications under 37 CFR § 1.53(b))

Attorney Docket No	1606.0020001
First Inventor or Application Identifier	Peter G BROWN
Title	System and Method for Simulation, Modeling and Scheduling of Solution Preparation in Biopharmaceutical Batch Process Manufacturing Facilities
Express Mail Label No	

APPLICATION ELEMENTS

See MPEP chapter 600 concerning utility patent application contents

ADDRESS TO
Assistant Commissioner for Patents
Box Patent Application
Washington, DC 20231

1. * Fee Transmittal Form (e.g., PTO/SB/17)
(Submit an original, and a duplicate for fee processing)
2. Specification [Total Pages 99]
(preferred arrangement set forth below)
 - Descriptive title of the Invention
 - Cross References to Related Applications
 - Background of the Invention
 - Brief Summary of the Invention
 - Brief Description of the Drawings *(if filed)*
 - Detailed Description
 - Claims
 - Abstract of the Disclosure
3. Drawings (35 U.S.C. 113) [Total Sheets 105]
4. Oath or Declaration [Total Pages 2]
 a. Newly executed (original)
 b. Copy from a prior application (37 CFR 1.63(d)) *(for continuation/divisional with Box 17 completed)*
[Note Box 5 below]
1. **DELETION OF INVENTOR(S)**
 Signed statement attached deleting inventor(s) named in the prior application, see 37 CFR §§ 1.63(d)(2) and 1.33(b)
5. Incorporation By Reference *(useable if Box 4b is checked)*
 The entire disclosure of the prior application, from which a copy of the oath or declaration is supplied under Box 4b, is considered as being part of the disclosure of the accompanying application and is hereby incorporated by reference therein
17. If a CONTINUING APPLICATION, check appropriate box, and supply the requisite information below and in a preliminary amendment
 Continuation Divisional Continuation-in-Part (CIP) of prior application No. /

Prior application information: Examiner _____ Group/Art Unit: _____

18. CORRESPONDENCE ADDRESS

 Customer Number
or Bar Code Label

(Insert Customer No. or Attach bar code label here)

or Correspondence address below

NAME	STERNE, KESSLER, GOLDSTEIN & FOX PLLC Attorneys at Law				
ADDRESS	Suite 600, 1100 New York Avenue, N.W.				
CITY	Washington	STATE	DC	ZIP CODE	20005-3934
COUNTRY	USA	TELEPHONE	(202) 371-2600	FAX	(202) 371-2540

NAME (Print/Type)	Robert Sokohl	Registration No. (Attorney/Agent)	36,013
SIGNATURE			
Date	6/19/98		

Burden Hour Statement: This form is estimated to take 0.2 hours to complete. Time will vary depending upon the needs of the individual case. Any comments on the amount of time you are required to complete this form should be sent to the Chief Information Officer, Patent and Trademark Office, Washington, DC 20231. DO NOT SEND FEES OR COMPLETED FORMS TO THIS ADDRESS. SEND TO: Assistant Commissioner for Patents, Washington, DC 20231.

Under the Paperwork Reduction Act of 1995, no persons are required to respond to a collection of information unless it displays a valid OMB control number.

FEE TRANSMITTAL*Patent fees are subject to annual revision on October 1.**These are the fees effective October 1, 1997**Small Entity payments must be supported by a small entity statement,
otherwise large entity fees must be paid. See Forms PTO/SB/09-12.
See 37 C.F.R. §§ 1.27 and 1.28***TOTAL AMOUNT OF PAYMENT****(\$ 395.00)****Complete if Known**

Application Number	To be assigned
Filing Date	June 19, 1998
First Named Inventor	Peter G. BROWN
Examiner Name	To be assigned
Group / Art Unit	To be assigned
Attorney Docket Number	1606.0020001/RES/RVM

METHOD OF PAYMENT (check one)**FEE CALCULATION (continued)**

1. The Commissioner is hereby authorized to charge indicated fees and credit any overpayment to

Deposit Account Number	19-0036
Deposit Account Name	Sterne, Kessler, Goldstein & Fox P L I. C

- Charge Any Additional Fee Required Under 37 CFR 1.16 and 1.17 Charge the Issue Fee Set in 37 CFR 1.18 at the Mailing of the Notice of Allowance

2. Payment Enclosed. Check No. _____

- Money Order

- Other*

*Charge any deficiencies or credit any overpayments in the fees or fee calculations of Parts 1, 2 and 3 below to Deposit Account No 19-0036

FEE CALCULATION**1. BASIC FILING FEE**

Large Fee Code	Entity Fee (\$)	Small Fee Code	Entity Fee (\$)	Fee Description	Fee Paid
101	790	201	395	Utility filing fee	<u>395.00</u>
106	330	206	165	Design filing fee	_____
107	540	207	270	Plant filing fee	_____
108	790	208	395	Reissue filing fee	_____
114	150	214	75	Provisional filing fee	_____

SUBTOTAL (1) (\$ 395.00) _____

2. EXTRA CLAIM FEES

Extra	Fee from below	Fee Paid
Total Claims 3 - 20** = 0	X 0	= 0
Indep. Claims 1 - 3** = 0	X 0	= 0

Multiple Dependent Claims _____ = 0

** or number previously paid, if greater. For Reissues see below

Large Fee Code	Entity Fee (\$)	Small Fee Code	Entity Fee (\$)	Fee Description
103	22	203	11	Claims in excess of 20
102	82	202	41	Independent claims in excess of 3
104	270	204	135	Multiple dependent claim
108	82	209	41	**Reissue independent claims over original patent
110	22	210	11	**Reissue claims in excess of 20 and over original patent

SUBTOTAL (2) (\$ 0) _____

3 ADDITIONAL FEES

Large Fee Code	Entity Fee (\$)	Small Fee Code	Entity Fee (\$)	Fee Description	Fee Paid
105	130	205	65	Surcharge - late filing fee or oath	_____
127	50	227	25	Surcharge - late provisional filing fee or cover sheet	_____
139	130	139	130	Non-English specification	_____
147	2,520	147	2,520	For filing a request for reexamination	_____
112	920*	112	920*	Requesting publication of SIR prior to Examiner action	_____
113	1,840*	113	1,840*	Requesting publication of SIR after Examiner action	_____
115	110	215	55	Extension for reply within first month	_____
116	400	216	200	Extension for reply within second month	_____
117	950	217	475	Extension for reply within third month	_____
118	1,510	218	755	Extension for reply within fourth month	_____
128	2,060	228	1,030	Extension for reply within fifth month	_____
119	310	219	155	Notice of Appeal	_____
120	310	220	155	Filing a brief in support of an appeal	_____
121	270	221	135	Request for oral hearing	_____
138	1,510	138	1,510	Petition to institute a public use proceeding	_____
140	110	240	55	Petition to revive - unavoidable	_____
141	1,320	241	660	Petition to revive - unintentional	_____
142	1,320	242	660	Utility issue fee (or reissue)	_____
143	450	243	225	Design issue fee	_____
144	670	244	335	Plant issue fee	_____
122	130	122	130	Petitions to the Commissioner	_____
123	50	123	50	Petitions related to provisional applications	_____
126	240	126	240	Submission of Information Disclosure Stmt	_____
581	40	581	40	Recording each patent assignment per property (times number of properties)	_____
146	790	246	395	Filing a submission after final rejection (37 CFR 1.129(a))	_____
149	790	249	395	For each additional invention to be examined (37 CFR 1.129(b))	_____

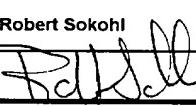
Other fee (specify) .

Other fee (specify) .

*Reduced by Basic Filing Fee Paid

SUBTOTAL (3) (\$ 0) _____

SUBMITTED BY**Complete (if applicable)**

Typed or Printed Name	Robert Sokohl	Reg. Number	36,013
Signature		Date	6/19/98
		Deposit Acct. User ID	

Burden Hour Statement. This form is estimated to take 0.2 hours to complete. Time will vary depending upon the needs of the individual case. Any comments on the amount of time you are required to complete this form should be sent to the Chief Information Officer, Patent and Trademark Office, Washington, DC 20231. DO NOT SEND FEES OR COMPLETED FORMS TO THIS ADDRESS. SEND TO: Assistant Commissioner for Patents, Washington, DC 20231

STERNE, KESSLER, GOLDSTEIN & FOX P.L.L.C.

ATTORNEYS AT LAW

SUITE 600

1100 NEW YORK AVENUE, N W
WASHINGTON, D.C. 20005-3934

(202) 371-2600

FACSIMILE (202) 371-2540, (202) 371-6566

jc408 U.S.
96/61/98

ROBERT GREENE STERNE
EDWARD J KESSLER
GEORGE A GOLDSTEIN
SAMUEL L FOX
DAVID K S CORNWELL
ROBERT W ESMOND
TRACY-GENE G DURKIN
MICHELE A CIMBALA
MICHAEL B RAY
ROBERT E SOKOHL
ERIC K STEFFE
MICHAEL Q LEE

JOHN M COVERT*
LINDA E ALCORN
RAZ E FLESHNER
ROBERT C MILLONIG
STEVEN R LUDWIG
MICHAEL V MESSINGER
JUDITH U KIM*
KEITH KIND
TIMOTHY J SHEA, JR
DONALD R MCPHAIL
PATRICK E GARRETT
BARBARA A PARVIS
MICHAEL A RAHMAN*

STEPHEN G WHITESIDE*
NOEL B WHITLEY*
JEFFREY T HELVEY*
RICHARD A DUNNING, JR
KIMBERLIN M TOOHEY
RALPH P ALBRECHT
HEIDI L KRAUS*
JEFFREY R KURIN*
CARL B MASSEY, JR.*
RAYMOND MILLIEN*
PATRICK D O'BRIEN*
BRIAN S ROSENBLUM*

DONALD J FEATHERSTONE**
LAWRENCE B BUGAISKY**
KAREN R MARKOWICZ**
GRANT E REED**
VICTOR E JOHNSON**
SERGE SIRA**

*BAR OTHER THAN D C
**REGISTERED PATENT AGENTS

WRITER'S DIRECT NUMBER

June 19, 1998

INTERNET ADDRESS

Assistant Commissioner for Patents
Washington, D.C. 20231

Box Patent Application

Re: U.S. Non-Provisional Utility Patent Application under 37 C.F.R. § 1.53(b)
Appl. No. To be assigned; Filed: June 19, 1998
(From Provisional Appl No. 60/050,294, Filed. June 20, 1997)
For: **System and Method for Simulation, Modeling and Scheduling of
Solution Preparation in Biopharmaceutical Batch Process
Manufacturing Facilities**
Inventor Peter G. BROWN
Our Ref: 1606 0020001

Sir.

The following documents are forwarded herewith for appropriate action by the U.S.
Patent and Trademark Office:

1. PTO Utility Patent Application Transmittal Form (PTO/SB/05),
2. U.S. Utility Patent Application entitled:

**System and Method for Simulation, Modeling and Scheduling of Solution
Preparation in Biopharmaceutical Batch Process Manufacturing Facilities**

and naming as inventor

Peter G. Brown

Assistant Commissioner for Patents
June 19, 1998
Page 2

the application comprising:

a. A specification containing:

- (i) 90 pages of description prior to the claims;
- (ii) 1 page of claims (3 claims),
- (iii) a one (1) page abstract;
- (iv) 7 pages of Appendices A1-A7;

b. One-Hundred and Five (105) sheets of drawings (Figures 1-11, 12A-H, 13-35, 36A-H, 37A-B, 38-41, 42A-D, 43-44, 45A-I, 46-63, 64A-Z, 64AA-64AB),

c. An original executed combined Declaration and Power of Attorney for Patent Application;

3 PTO Fee Transmittal Form PTO/SB/17 (in duplicate);

4. Authorization to Treat a Reply As Incorporating An Extension of Time Under 37 C.F.R. § 1.136(a)(3) (in duplicate),

5 Our check No 22125 for \$395 00 to cover:

\$395.00 Filing fee for patent application; and

6 Two (2) return postcards.

It is respectfully requested that, of the two attached postcards, one be stamped with the filing date of these documents and returned to our courier, and the other, prepaid postcard, be stamped with the filing date and unofficial application number and returned as soon as possible.

Assistant Commissioner for Patents
June 19, 1998
Page 3

The U.S. Patent and Trademark Office is hereby authorized to charge any fee deficiency, or credit any overpayment, to our Deposit Account No. 19-0036. A duplicate copy of this letter is enclosed

This patent application claims priority, under 35 U.S.C. § 119(e), to U.S. Provisional Application No. 60/050,294, filed June 20, 1997.

Respectfully submitted,

STERNE, KESSLER, GOLDSTEIN & FOX P.L.L.C.



Robert Sokohl
Attorney for Applicant
Registration No 36,013

0020001 pto

**System and Method for Simulation, Modeling and Scheduling
of Solution Preparation in Biopharmaceutical Batch Process
Manufacturing Facilities**

Inventor: Peter G. Brown

5

Cross-Reference to Related Applications

This application claims priority to U.S. Provisional Patent Application No. 60/050,294, filed June 20, 1997, Attorney Docket No. 1606.0020000.

This application is related to the following commonly-owned, co-pending applications:

- 10 • "System and Method for Simulation and Modeling of Biopharmaceutical Batch Process Manufacturing Facilities", by Brown, having application number 09/019,777 (Attorney Docket No. 1606.0010001), filed February 6, 1998;
- 15 • "System and Method for Simulation, Modeling and Scheduling of Equipment Preparation in Biopharmaceutical Batch Process Manufacturing Facilities", by Brown, having application number TBA (Attorney Docket No. 1606.0030001), filed concurrently herewith,
- 20 • "System and Method for Simulation, Modeling and Scheduling of Equipment Maintenance and Calibration in Biopharmaceutical Batch Process Manufacturing Facilities", by Brown, having application number TBA (Attorney Docket No. 1606.0040001), filed concurrently herewith; and
- 25 • "System and Method for Simulation, Modeling and Scheduling of Quality Control Sampling in Biopharmaceutical Batch Process Manufacturing Facilities", by Brown, having application number TBA (Attorney Docket No. 1606.0050001), filed concurrently herewith.

Each of the above applications are incorporated herein by reference in their entirety.

Background of the Invention

Field of the Invention

The present invention relates generally to the design of large scale batch manufacturing facilities, and specifically to the design of biopharmaceutical drug manufacturing processes.

5

Related Art

Biopharmaceutical plants produce biopharmaceutical products through biological methods. Typical biopharmaceutical synthesis methods are mammalian cell culture, microbial fermentation and insect cell culture. Occasionally biopharmaceutical products are produced from natural animal or plant sources or by a synthetic technique called solid phase synthesis. Mammalian cell culture, microbial fermentation and insect cell culture involve the growth of living cells and the extraction of biopharmaceutical products from the cells or the medium surrounding the cells. Solid phase synthesis and crude tissue extraction are processes by which biopharmaceuticals are synthesized from chemicals or extracted from natural plant or animal tissues, respectively.

The process for producing biopharmaceuticals is complex. In addition to basic synthesis, additional processing steps of separation, purification, conditioning and formulation are required to produce the end product biopharmaceutical. Each of these processing steps includes additional unit operations. For example, the step of purification may include the step of Product Adsorption Chromatography, which may further include the unit operations of High Pressure Liquid Chromatography (HPLC), Medium Pressure Liquid Chromatography (MPLC), Low Pressure Liquid Chromatography (LPLC), etc. The production of biopharmaceuticals is complex because of the number,

complexity and combinations of synthesis methods and processing steps possible. Consequently, the design of a biopharmaceutical plant is expensive.

Tens of millions of dollars can be misspent during the design and construction phases of biopharmaceutical plants due to inadequacies in the design process. Errors and inefficiencies are introduced in the initial design of the biopharmaceutical production process because no effective tools for modeling and simulating a biopharmaceutical production process exists. The inadequacies in the initial process design carry through to all phases of the biopharmaceutical plant design and construction. Errors in the basic production process design propagate through all of the design and construction phases, resulting in increased cost due to change orders late in the facility development project. For example, detailed piping and instrumentation diagrams (P&IS) normally cost thousands of dollars per diagram. Problems in the biopharmaceutical production process design frequently necessitate the re-working of these detailed P&IS. This adds substantially to the overall cost of design and construction of a biopharmaceutical plant

There are generally three phases of biopharmaceutical plants which coincide with the different levels of drug approval by the FDA. A Clinical Phase I/II biopharmaceutical plant produces enough biopharmaceutical product to support both phase I and phase II clinical testing of the product which may involve up to a few hundred patients. A Clinical Phase III biopharmaceutical plant produces enough biopharmaceutical product to support two to three-thousand patients during phase III clinical testing. A Clinical Phase III plant will also produce enough of the biopharmaceutical drug to support an initial commercial offering upon the licensing of the drug by the FDA for commercial sale. The successive phases represent successively larger biopharmaceutical facilities to support full scale commercial production after product licensing. Often the production process design is repeated for each phase, resulting in increased costs to each phase of plant development.

The design, architecture and engineering of biopharmaceutical plants is a several hundred million dollars a year industry because of the complex nature of biopharmaceutical production. Design of biopharmaceutical plants occurs in discrete phases. The first phase is the conceptual design phase. The first step in the conceptual design phase is identifying the high-level steps of the process that will produce the desired biopharmaceutical. Examples of high-level steps are synthesis, separation, purification and conditioning. After the high-level process steps have been identified, the unit operations associated with each of the high-level steps are identified. Unit operations are discrete process steps that make up the high-level process steps. In a microbial fermentation process, for example, the high-level step of synthesis may include the unit operations of inoculum preparation, flask growth, seed fermentation and production fermentation.

The unit operation level production process is typically designed by hand and is prone to errors and inefficiencies. Often, in the conceptual design phase, the specifications for the final production process are not complete. Therefore some of the equipment design parameters, unit operation yields and actual production rates for the various unit operations must be estimated. These factors introduce errors into the initial design base of the production process. Additionally, since the production process is designed by hand, attempting to optimize the process for efficiency and production of biopharmaceutical products is impractically time consuming.

Scale calculations for each of the unit operations are performed to determine the size and capacity of the equipment necessary to produce the desired amount of product per batch. Included in the scale calculations is the number of batches per year needed to produce the required amount of biopharmaceutical product. A batch is a single run of the biopharmaceutical process that produces the product. Increasing the size and capacity of the equipment increases the amount of product produced per batch. The batch cycle time is the amount of time required to produce one batch of product. The amount of product produced in a given amount of time, therefore, is dependent upon the amount produced per

batch, and the batch cycle time. The scale calculations are usually executed by hand to determine the size and capacity of the equipment that will be required in each of the unit operations. Since the scale calculations are developed from the original conceptual design parameters, they are also subject to the same errors inherent in the initial conceptual design base.

Typically a process flow diagram is generated after the scale calculations for the unit operations have been performed. The process flow diagram graphically illustrates the process equipment such as tanks and pumps necessary to accommodate the process for a given batch scale. The process flow diagram illustrates the different streams of product and materials through the different unit operations. Generally associated with the process flow diagram is a material balance table which shows the quantities of materials consumed and produced in each step of the biopharmaceutical production process. The material balance table typically includes rate information of consumption of raw materials and production of product. The process flow diagram and material balance table provides much of the information necessary to develop a preliminary equipment list. The preliminary equipment list shows the equipment necessary to carry out all of the unit operations in the manufacturing procedure. Since the process flow diagram, material balance table and preliminary equipment list are determined from the original conceptual design parameters, they are subject to the same errors inherent in the initial conceptual design base.

A preliminary facility layout for the plant is developed from the process flow diagram, material balance table and preliminary equipment list. The preliminary facility layout usually begins with a bubble or block diagram of the plant that illustrates the adjacencies of rooms housing different high-level steps, as well as a space program which dimensions out the space and square footage of the building. From this information a preliminary equipment layout for the plant is prepared. The preliminary equipment layout attempts to show all the rooms in the plant, including corridors, staircases, etc. Mechanical, electrical and plumbing engineers estimate the mechanical, electrical and plumbing needs of the facility

based on the facility design layout and the utility requirements of the manufacturing equipment. Since the preliminary facility layout is developed from the original conceptual design parameters, they are subject to the same errors inherent in the initial conceptual design base.

5 Typically the next phase of biopharmaceutical plant design is preliminary piping and instrumentation diagram (P&ID) design. Preliminary P&IS are based on the process flow diagram from the conceptual design phase. Often the calculations on the process design are re-run and incorporated into the preliminary P&ID. The preliminary P&IS incorporate the information from the material balance table with the preliminary equipment list to show the basic piping and instrumentation required to run the manufacturing process

10 Detailed design is the next phase of biopharmaceutical plant design. Plans and specifications which allow vendors and contractors to bid on portions of the biopharmaceutical plant are developed during the detailed design. Detailed P&IS are developed which schematically represent every detail of the process systems for the biopharmaceutical plant. The detailed P&IS include for example, the size and components of process piping, mechanical, electrical and plumbing systems; all tanks, instrumentation, controls and hardware. A bill of materials and detailed specification sheets on all of the equipment and systems are developed from the P&IS. Detailed facility architecture diagrams are developed that coincide with the detailed P&IS and equipment specifications. The detailed P&IS and facility construction diagrams allow builders and engineering companies to bid on the biopharmaceutical plant project. Since the preliminary and detailed P&IS are developed from the original conceptual design parameters, they are subject to the same errors inherent in the initial conceptual design base. Reworking the preliminary and detailed P&IS due to errors in the conceptual design phase can cost thousands of dollars per diagram.

15 The inability to accurately model and simulate the biopharmaceutical production process drives inaccurate initial design. Often, these inaccuracies result in changes to the design and construction diagrams at the plant construction

site, or repair and reconstruction of the plant during the construction phase resulting in millions of dollars in additional cost.

Solution preparation is one of the primary consumers of capital and utility resources in the construction and operation of a biopharmaceutical facility. Often, the facility and process designers specify equipment that is many times what is required to support their solution preparation needs in order to ensure that all of the processes in the facility can be supported. Equipment, utility and cleaning equipment costs are a function by the preparation and use of solutions. The excess capacity, therefore, results in wasted construction capital and continuous losses during the operation of the plant.

What is needed, therefore, is a system and method for accurately simulating, modeling and scheduling solution preparation in the biopharmaceutical production process. A method and system for simulating, modeling and scheduling solution preparation in the biopharmaceutical production process would allow designers to reduce the number of errors introduced into plant design at the earliest stages. Such a system and method would also allow an engineer to validate the production process design and maximize the efficiency of the plant by finding optimum equipment configurations. Such a system and method would allow the generation of detailed specifications for the equipment and solution preparation scheduling that would smooth the transition throughout all of the design phases and fix the cost of design and construction of a biopharmaceutical facility.

Summary of the Invention

The present invention satisfies the above-stated needs by providing a method and system for simulating, modeling and scheduling solution preparation in the biopharmaceutical production process. The system and method includes the steps of identifying a solution for preparation and its associated volume. After the solution for preparation is identified, a predetermined start date and one successive

start date for solution preparation for the solution are identified. After the solution, start and successive start dates are identified, the solution is assigned to a preparation vessel. After the solution has been assigned to a preparation vessel, the duration of the solution preparation procedure is determined and assigned to
5 the solution preparation vessel.

Brief Description of the Figures

FIG. 1 illustrates a flow diagram of the process to generate a block flow
diagram and a process time line according to the present invention.

10 FIG. 2 illustrates a flow diagram of the process for determining the necessary reactor volume according to the present invention

FIG. 3 illustrates a unit operation list for a microbial fermentation process.

FIG. 4 illustrates a unit operation list for a mammalian cell culture process.

15 FIG. 5 illustrates a flow diagram for cross-referencing a unit operation list with a process parameters table according to the present invention.

FIG. 6 illustrates an exemplary process parameters table.

FIG. 7 illustrates the process for generating a block flow diagram according to the present invention.

FIG. 8 illustrates an exemplary block flow diagram according to the present invention.

FIG. 9 illustrates a block flow diagram for the process of generating a process time line according to the present invention.

FIGS. 10-11 illustrate a high-level process time line according to the present invention.

5 FIGS 12A-12H illustrate a detailed process time line according to the present invention.

FIG. 13 is a block flow diagram illustrating an overview of the process for scheduling and simulating solution preparation in a biopharmaceutical production process.

10 FIG. 14 is a block flow diagram illustrating the step of determining the solution preparation time associated with each solution preparation vessel.

FIG. 15 illustrates an exemplary list of solution preparation parameters.

15 FIG. 16 is a block flow diagram illustrating the step of assigning the solutions required by the biopharmaceutical production process to particular solution preparation vessels.

FIG. 17 illustrates an exemplary list of solution preparation procedure parameters.

FIG. 18 illustrates an exemplary preparation vessel to solution assignment list.

20 FIG. 19 illustrates an exemplary computer according to an embodiment of the present invention.

FIG. 20 is a block flow diagram illustrating the step of determining the calculated preparation start date and next solution preparation date for each solution

FIG. 21 illustrates an exemplary master quality control protocol table.

5 FIG. 22 is a block flow diagram illustrating the step of generating a solution preparation equipment quality control time line.

FIG. 23 is a block flow diagram illustrating the step of generating a preparation equipment quality control time line

10 FIG. 24 is a block flow diagram illustrating the step of determining the earliest solution preparation start date for each solution preparation vessel.

FIG. 25 is a block flow diagram illustrating the step of determining the latest solution preparation start date for each solution preparation vessel.

FIG. 26 is a block flow diagram illustrating the step of calculating solution preparation vessel utilization time.

15 FIG. 27 is a block flow diagram illustrating the step of calculating the cumulative solution preparation time for each solution preparation vessel.

FIG. 28 is a block flow diagram illustrating the step of determining the percentage utilization of each solution preparation vessel.

20 FIG. 29 is a block flow diagram illustrating the step of generating an initial solution prep shift schedule.

FIG. 30 is a block flow diagram illustrating the step of back scheduling solution preparation in the initial solution prep shift schedule.

FIG. 31 illustrates an exemplary initial solution preparation shift schedule.

5 FIG. 32 is a block flow diagram illustrating the process for generating a solution preparation schedule.

FIG. 33 is a block flow diagram illustrating an overview of the process for scheduling and simulating solution preparation in a biopharmaceutical production process.

10 FIG. 34 is a block flow diagram illustrating the step of generating the preparation equipment protocol table.

FIG. 35 is a block flow diagram illustrating the step of generating the equipment preparation procedure table.

FIGS. 36A-36H illustrate exemplary preparation equipment protocol tables.

15 FIGS. 37A-37B illustrate an exemplary equipment preparation procedure table

FIG. 38 is a block flow diagram illustrating the step of generating the equipment dimension table.

FIG. 39 illustrates an exemplary equipment dimension table.

FIG. 40 is a block flow diagram illustrating the step of generating the master list of equipment requiring preparation.

FIG. 41 is a block flow diagram illustrating the step of generating the equipment preparation load table.

5 FIGS. 42A-42D illustrate an exemplary equipment preparation load table.

FIG. 43 is a block flow diagram illustrating the step of generating the equipment preparation load summary table.

FIG 44 is a block flow diagram illustrating the step of determining the capacities of the preparation equipment.

10 FIGS. 45A-45I illustrate an exemplary process equipment quality control assay sample time line.

FIG. 46 is a block flow diagram illustrating the step of generating the equipment preparation time line

15 FIG. 47 is a block flow diagram illustrating the step of generating the preparation equipment list with functional specification and costs.

FIG. 48 is a block flow diagram illustrating the step of generating the preparation equipment utility time line.

FIG 49 is a block flow diagram illustrating the step of generating a process equipment maintenance table.

FIG. 50 is a block flow diagram illustrating the step of generating a process equipment maintenance time line.

FIG. 51 is a block flow diagram illustrating the step of generating a solution preparation equipment maintenance table.

5 FIG 52 is a block flow diagram illustrating the step of generating a solution preparation equipment maintenance time line

FIG. 53 is a block flow diagram illustrating the step of generating a preparation equipment maintenance table.

10 FIG. 54 is a block flow diagram illustrating the step of generating a preparation equipment maintenance time line.

FIG. 55 is a block flow diagram illustrating the step of generating a process equipment calibration table.

FIG. 56 is a block flow diagram illustrating the step of generating a process equipment calibration time line.

15 FIG. 57 is a block flow diagram illustrating the step of generating a solution preparation equipment calibration table

FIG. 58 is a block flow diagram illustrating the step of generating a solution preparation equipment calibration time line.

20 FIG. 59 is a block flow diagram illustrating the step of generating a preparation equipment calibration table.

FIG 60 is a block flow diagram illustrating the step of generating a preparation equipment calibration time line.

FIG. 61 is a block flow diagram illustrating the step of generating a master quality control protocol table

5 FIG 62 is a block flow diagram illustrating the step of generating a master quality control sample table.

FIG. 63 is a block flow diagram illustrating the step of generating a process equipment quality control time line.

10 FIGS. 64A-64AB illustrate an exemplary process equipment maintenance time line

Appendix A1-A7 is a detailed example of a process parameters table showing a list of unit operations and their associated parameters

Detailed Description of the Preferred Embodiments

1.0 Biopharmaceutical Batch Process Simulator

15 FIG. 1 illustrates a high-level flow diagram of the preferred embodiment. The process begins by determining the necessary reactor vessel capacity at step 102. The reactor vessel is the container in which the crude product is first synthesized. For example, in mammalian cell culture processes, the reactor vessel houses the mammalian cells suspended in growth media. Next, the unit operation sequence for production of the biopharmaceutical product is determined at step 104. The unit operation sequence is the series of unit operations that are required to produce the biopharmaceutical product. Each unit operation is an individual

step in the biopharmaceutical manufacturing process with an associated set of manufacturing equipment. The unit operation list is the list of unit operations that make up the unit operation sequence and their associated sequence information. The unit operation sequence information is the information that defines the scheduling cycles for each of the unit operations in the unit operation list. Scheduling cycles are iterations ((the default being one (1)) of unit operations in the unit operation sequence. Together, the unit operation list and the unit operation sequence information define the unit operation sequence. The desired biopharmaceutical product dictates the particular unit operations and their order in the biopharmaceutical production process. Some examples of unit operations are: inoculum preparation, initial seeding of the reactor vessel, solids harvest by centrifugation, high-pressure homogenization, dilution, etc.

Scheduling cycles and cycle offset duration for each of the unit operations in the biopharmaceutical production process are determined at step 106. Scheduling cycles are iterations of unit operations in the unit operation sequence, and occur in three levels. Additionally, each level of scheduling cycle has an associated offset duration that dictates the time period between the beginnings successive scheduling cycles.

"Cycles per unit operation" is the first level of scheduling cycles. Cycles per unit operation are defined as the number of iterations a unit operation is repeated in a process by itself before proceeding to the next operation. For example, the harvest and feed unit operation in a mammalian cell culture process has multiple cycles per unit operation. Product-rich media is drawn from the reactor vessel and nutrient-rich media is fed into the reactor vessel multiple times during one harvest and feed unit operation. The multiple draws of product-rich reactor media are pooled for processing in the next unit operation.

The second level of scheduling cycles is "cycles per batch." Cycles per batch are defined as the number of iterations a set of consecutive unit operations are repeated as a group before proceeding to the next unit operation after the set of consecutive unit operations. The set of consecutive unit operations repeated

as a group are also referred to as a subprocess. For example, the set of unit operations including inoculum preparation, flask growth, seed fermentation, production fermentation, heat exchange, and continuous centrifugation/whole-cell harvest in a microbial fermentation process are often cycled together. Running through each of the six steps results in a single harvest from the microbial fermentation reactor vessel. Multiple harvests from a reactor vessel may be needed to achieve a batch of sufficient quantity. Each additional harvest is pooled with the previous harvest, resulting in a single batch of cell culture for the process.

The third level of scheduling cycles is "cycles per process." Cycles per process are defined as the number of iterations a batch cycle is repeated for a process that employs continuous or semi-continuous product synthesis. In such a case, a single biopharmaceutical production process may result in multiple batches of product. For example, in a mammalian cell-culture process a single cell culture is typically in continuous production for 60-90 days. During this period multiple harvests of crude product are collected and pooled on a batch basis to be processed into the end product biopharmaceutical. The pooling of multiple harvests into a batch of material will occur several times during the cell culture period resulting in multiple batch cycles per process.

In step 108, a process parameters table master list is referenced to obtain all operational parameters for each unit operation in the unit operation list. The process parameters table contains a list of all unit operations and operational parameters necessary to simulate a particular unit operation. Examples of operational parameters are the solutions involved in a particular unit operation, temperature, pressure, duration, agitation, scaling volume, etc. Additionally, the process parameters table supplies all of the individual tasks and task durations involved in a particular unit operation. For example, the unit operation of inoculum preparation includes the individual tasks of setup, pre-incubation, incubation, and cleanup. Examples of unit operations for biopharmaceutical manufacturing and their associated operational parameters are included in this application as Appendix A1-A7.

A block flow diagram is generated at step 110 after unit operation list has obtained the operational parameters from the process parameters table at step 108. The block flow diagram illustrates each unit operation in the manufacturing process as a block with inputs for both incoming product and new material, as well as outputs for both processed product and waste. The block flow diagram is a simple yet convenient tool for quantifying material flows through the process in a way that allows the sizing of many key pieces of equipment relative to a given process scale.

The information in each block of the block flow diagram is generated from the parameters and sizing ratios from the process parameters table in the unit operation list, and block flow diagram calculation sets. A calculation set is a set of algebraic equations. The parameters and calculation sets are used to calculate the quantities of material inputs, product and waste outputs required for that unit operation based on the quantity of product material being received from the previous unit operation. Likewise, a given block flow diagram block calculates the quantity of product to be transferred to the next unit operation block in the manufacturing procedure. These calculations take into account the unit operation scheduling cycles identified at step 106, as further explained below.

A process time line is generated at step 112 after the block flow diagram is generated at step 110. The process time line is a very useful feature of the present invention. The process time line is generated from the unit operation list, the tasks associated with each of the unit operations, the scheduling cycles for each of the unit operations in the process, the process parameters from the master process parameters table and the volume of the material as calculated from the block flow diagram. The process time line is a relative time line in hours and minutes from the start date of the production process. The relative time is converted into days and hours to provide a time line for the beginning and ending times of each unit operation and its associated tasks for the entire biopharmaceutical drug production process.

The process time line is a very powerful tool for process design. The process time line can be used to accurately size pumps, filters and heat exchangers used in unit operations, by calculating the flow rate from the known transfer time and the volume of the material to be transferred, filtered or cooled. The process
5 time line accurately predicts loads for labor, solution preparation, equipment cleaning, reagent, process utilities, preventative maintenance, quality control testing, etc.

FIG. 2 further illustrates step 102 of determining the necessary reactor vessel capacity. The amount of biopharmaceutical product to be produced in a given amount of time is determined in step 202. Normally, the amount of biopharmaceutical product required is expressed in terms of mass produced per year. The number of reactor vessel runs for a particular biopharmaceutical product per year is determined at step 204. Factors considered when determining the number of reactor vessel cycles for a particular biopharmaceutical product are, for example, the number of biopharmaceutical products produced in the reactor vessel (i.e., the reactor vessel is shared to produce different products), the reaction time for each cycle of the reactor vessel and the percentage of up-time for the reactor vessel over the year.
10
15

The yield of each batch or reactor cycle is calculated at step 206. The yield from each batch or a reactor cycle is process-dependent and is usually expressed in grams of crude product per liter of broth. Given the required amount of biopharmaceutical product per year from step 202, the number of reactor cycles available to produce the required biopharmaceutical product from step 204, and the yield of each reactor cycle from step 206, the necessary reactor volume to produce the required amount of biopharmaceutical product is calculated at step
20
25
30 208

FIG. 3 illustrates a unit operation list for an exemplary microbial fermentation biopharmaceutical production process. The far left-hand column, column 302, lists the unit operation sequence numbers for each of the unit operations in the process. The exemplary microbial fermentation unit operation

list includes 23 unit operations. The unit operation sequence number defines the order in which the unit operations occur. For example, unit operation sequence number 1, inoculum preparation, occurs first, before unit operation sequence number 2, flask growth. Column 304 shows the unit operation identifier codes associated with each of the unit operations in the unit operation list (see step 108).
5 The unit operation identifier codes are used to bring operational parameters from the process parameters table into the unit operation list. For example, heat exchange, unit operation list numbers 5, 8 and 10, has a unit operation identifier code 51.

As described above with reference to FIG. 1, after the unit operation sequence for a particular biopharmaceutical production process has been determined at step 104, the scheduling cycles associated with each unit operation is determined at step 106. Columns 306, 310 and 318 list the number of scheduling cycles for the microbial fermentation process of FIG. 3. Scheduling cycles are iterations of unit operations in the unit operation sequence, and occur in three levels. Additionally, each level of scheduling cycle has an associated offset duration that dictates the time period between the beginnings of successive scheduling cycles, shown in columns 308, 316 and 324.
10
15

Column 306 lists the number of cycles per unit operation for each of the unit operations in the microbial fermentation unit operation sequence. In the exemplary microbial fermentation unit operation sequence, each of the unit operations has only one cycle per unit operation. Again, cycles per unit operation define the number of iterations a unit operation is repeated in a process by itself before proceeding to the next unit operation
20

Column 308 lists the cycle offset duration in hours for the cycles per unit operation. Since each of the unit operations in the microbial fermentation example of FIG. 3 has only one cycle per unit operation, there is no cycle offset duration for any of the unit operations. Cycle offset duration defines the time period between the beginnings of successive scheduling cycles.
25

Column 310 lists the cycles per batch for each of the unit operations in the microbial fermentation unit operation sequence. Unit operation sequence numbers 1-6 are defined as having three cycles per batch. Cycles per batch defines the number of iterations a set of consecutive unit operations are repeated as a group before proceeding to the next unit operation. In FIG. 3, for example, the set of unit operations 1-6, as defined in unit operation start column 312 and unit operation end column 314, cycle together as a group (e.g., the sequence of unit operations for the exemplary microbial fermentation process is 1, 2, 3, 4, 5, 6, 1, 2, 3, 4, 5, 6, 1, 2, 3, 4, 5, 6 and 7). Unit operations 1-6 cycle together as a group three times before the process continues to unit operation 7, as defined in column 310.

After unit operation sequence numbers 1-6 have cycled consecutively three times, the microbial fermentation production process continues at unit operation sequence number 7, resuspension of cell paste. After unit operation sequence number 7, the process continues with three cycles per batch of unit operation sequence numbers 8-10. The unit operations of heat exchange, cell disruption and heat exchange are cycled consecutively three times, as defined in columns 310, 312 and 314. After unit operation sequence numbers 8-10 have cycled three times, the microbial fermentation production process continues at resuspension/surfactant, unit operation sequence number 11.

Unit operation sequence numbers 11 and 12 cycle together two times, as defined by columns 310, 312 and 314. After unit operation sequence numbers 11 and 12 have been cycled two times, the microbial fermentation production process continues without cycling from unit operation sequence number 13 through unit operation sequence number 23 to conclude the microbial fermentation production process.

Columns 326-332 of FIG. 3 represent the step wise recover (SWR) and overall recovery (OAR) percentages of the product and total proteins. SWR is the recovery of protein for the individual unit operation for which it is listed. OAR is the recovery of protein for the overall process up to and including the unit

operation for which it is listed. The product recovery columns represent the recovery of the desired product protein from the solution in the process. The protein recovery columns represent the recovery of contaminant proteins from the solution which result in higher purity of the product solution.

5 FIG. 4 illustrates a unit operation list for an exemplary mammalian cell culture production process. Column 402 lists unit operation sequence numbers 1-19. Unit operation sequence numbers 1-19 define the order in which the unit operations of the mammalian cell culture production process occur. The most notable differences between the microbial fermentation process of FIG. 3 and the mammalian cell culture process of FIG. 4 are the multiple cycles per unit operation of unit operation sequence number 8 and the multiple cycles per process of unit operation sequence numbers 8-18

10 Unit operation sequence number 8 of FIG. 4 illustrates the concept of multiple cycles per unit operation. Unit operation sequence number 8 is the unit operation of harvesting product rich growth media from and feeding fresh growth media into the mammalian cell reactor vessel. In most mammalian cell culture processes, the product is secreted by the cells into the surrounding growth media in the reactor vessel. To harvest the product, some of the product rich growth media is harvested from the reactor vessel to be processed to remove the product, and an equal amount of fresh growth media is fed into the reactor vessel to sustain production in the reactor vessel. The process of harvesting and feeding the reactor vessel can continue for many weeks for a single biopharmaceutical production process. Unit operation sequence number 8 is repeated seven times, or 7 cycles per unit operation (e.g., the unit operation sequence is 7, 8, 8, 8, 8, 8, 8, 9). Note that the offset duration for unit operation sequence number 8 is 24 hours. The offset duration defines the time period between the cycles per unit operation. In the example of FIG. 4, unit operation sequence number 8 is repeated 7 times (7 cycles per unit operation) and each cycle is separated from the next by 24 hours, or one day. This corresponds to unit operation sequence number 8 having a duration of one week, with a harvest/feed step occurring each day.

FIG. 4 also illustrates the feature of multiple cycles per process. Cycles per process is defined as the number of iterations a batch cycle is repeated in a given process that employs continuous or semi-continuous product synthesis. Each batch cycle results in a batch of product. A single biopharmaceutical production process, therefore, may result in multiple batches of product. In the mammalian cell culture process example of FIG. 4, unit operation sequence numbers 8-18 are repeated together as a group eight times (column 418). Each of these cycles of unit operation sequence numbers 8-18 produce one batch of product (columns 420-422). The offset between each cycle of unit operation sequence numbers 8-18 is 168 hours, or one week (column 424).

In the example of FIG. 4, unit operation sequence numbers 8-18 proceed as follows: the reactor vessel is harvested and fed once each day for seven days; the results of the harvest/feed operation are pooled in unit operation sequence number 9 at the end of the seven days; unit operations 9-18 are then executed to process the pooled harvested growth media from unit operation sequence number 8. Unit operation sequence numbers 8-18 are cycled sequentially once each week to process an additional seven day batch of harvested growth media from unit operation sequence number 8. At the end of eight weeks, the mammalian cell culture process is completed.

FIG. 5 further illustrates step 108, cross referencing the unit operation sequence with the master process parameters table. The operational parameters in the process parameters table are those parameters necessary to simulate a particular unit operation. The parameters from the process parameters table define the key operational parameters and equipment sizing ratios for each unit operation in the unit operation sequence. The values for these parameters and ratios are variables which can be easily manipulated and ordered to model and evaluate alternative design scenarios for a given process scale. Examples of the process parameters associated with each unit operation are listed in Appendix A1-A7. It should be noted, however, that the list of unit operations, parameters, values, and scaling ratios is not exhaustive. One of ordinary skill in the art could

expand the process parameters table to encompass additional unit operations and production processes for other batch process industries such as chemical pharmaceutical, specialty chemical, food, beverage and cosmetics. Such expansion would allow the present invention to simulate and schedule additional batch production processes for other such batch processes.

FIG. 5 illustrates the files necessary to cross-reference the unit operation list with the process parameters table in step 108. Exemplary unit operation list 502 for the biopharmaceutical production process and process parameters table 504 are input into processing step 506. Step 506 cross-references the unit operation list and process parameters table based on unit operation identification code (see FIG. 3). The parameters are copied from the process parameters table 504 into the unit operation list 502 to generate unit operation list 508.

FIG. 6 further illustrates exemplary process parameters table, 504. The operational parameters in the process parameters table are those parameters necessary to simulate a particular unit operation. The unit operation identification codes of process parameters table 504 are used in the cross-reference step 506 to assign the parameters from the process parameters table 504 to the unit operation list 502. Examples of operational parameters are the solutions involved in a particular unit operation, temperature, pressure, duration, agitation, scaling volume, etc. Additionally, the process parameters table defines all of the individual tasks and task durations involved in each unit operation. It should be noted, however, one of ordinary skill in the art could expand the process parameters table to encompass additional unit operations and production processes for other batch process industries such as chemical pharmaceutical, specialty chemical, food, beverage and cosmetics. Such expansion would allow the present invention to simulate and schedule additional batch production processes for other such batch processes.

FIG. 7 further illustrates step 110, generating a block flow diagram. A block flow diagram depicts each unit operation in the biopharmaceutical production process as a block with inputs for both incoming product and new

material, as well as outputs for both processed product and waste. The material that flows through each of the unit operation blocks is quantified by calculation sets in each of the block flow diagram blocks. A unit operation block in a block flow diagram is a graphical representation of a unit operation. A calculation set is a set of algebraic equations describing a unit operation. Some examples of outputs of the calculation sets are: required process materials for that unit operation, equipment performance specifications and process data outputs to be used for the next unit operation. Some examples of inputs to the calculation sets are: product quantity (mass) or volume (liters) from a previous unit operation, other parameters and/or multipliers derived from the process parameters table, as well as the design cycles defined in the unit operation list.

Block flow diagram 708 is generated from unit operation list 508 and block flow diagram calculation set 704. Block flow diagram calculation set 704 is an exhaustive list of unit operation identifier codes and the calculation sets associated with each unit operation identifier. Unit operation list 508 and block flow diagram calculation set 704 are linked together based on unit operation identifier code.

Step 706 calculates the block flow diagram material flow requirements and basic equipment sizing requirements from unit operation list 508 which includes all of the associated operational parameters from the process parameters table, and the block flow diagram calculation set 704. Block flow diagram 708 allows the sizing of many key pieces of equipment relative to a given process scale. Since the material flow quantities into and out of each unit operation is determined at step 706, the capacity of many equipment items involved in each unit operation can be determined. The block flow diagram also manages important information in the unit operation list 502 such as the percent recovery, percent purity and purification factor of the product in each unit operation. This information helps identify the steps in the process that may need optimization.

The following is an example calculation set for a tangential flow micro-filtration (TFMF) system unit operation. Tangential flow micro-filtration is an

important process technology in biopharmaceutical manufacturing. This technology significantly extends the life of the filtration media and reduces the replacement cost of expensive filters.

TFMF generically requires the same steps to prepare the membrane for each use as well as for storage after use. The design parameters for each unit operation such as TFMF have been developed around these generic design requirements.

Generic Parameters (Variables) from the Process Parameters Table

5	Equipment Design Type	Plate & Frame
10	Membrane Porosity	0.2 micron
15	Membrane Flux rate	125 Liters/square meter/hour
20	Process Time	2 Hours
	Retentate/Filtrate Rate	20 to 1
	Flush volume	21.5 Liters/square meter
	Prime volume	21.5 Liters/square meter
	Wash Volume	0.5 % of Process Volume
	Regenerate Volume	10.8 Liters/square meter
	Storage Volume	21.5 Liters/square meter
	% Recovery of Product	95%
	% Recovery of Total Protein	80%
	Clean In Place (CIP)	Yes
	Steam In Place (CIP)	Yes

Input Values from Previous Unit Operation

Product Volume	1,000 Liters
Product Quantity	1.5 Kg
Total Protein Quantity	3 0 Kg

- 5 The calculation set for this unit operation first takes the incoming process volume and uses it as a basis of sizing the filtration membrane for the filtration system based on the above flux rate and required processing time.

$$1,000 \text{ Liters} / 125 \text{ L/SM/Hr} / 2 \text{ Hours} = 4.0 \text{ SM of 0.2 micron membrane}$$

- 10 After calculating the square meter (SM) of membrane required by this unit operation, the volumes of each of the support solutions can be calculated based on the above volume ratios.

Flush volume	21.5 Liters/SM x 4.0 SM = 86 Liters
Prime volume	21.5 Liters/SM x 4.0 SM = 86 Liters
Wash Volume	5 % of 1,000 Liters = 50 Liters
Regenerate	21.5 Liters/SM x 4.0 SM = 86 Liters
Storage	10.8 Liters /SM x 4.0 SM = 42 Liters

The flow rate of the filtrate is calculated from the volume to be filtered and the required process time

$$1,000 \text{ Liters} / 2 \text{ Hours} = 8.3 \text{ Liters/minute}$$

- 20 The flow rate of the retentate is calculated based on the above retentate/filtrate ratio.

$$8.3 \text{ Liters per minute} \times 20 = 167 \text{ Liters/minute}$$

Based on the input of the process volume to this unit operation and the above parameters, the equipment size, the filtration apparatus, the retentate pump, the support linkage and associated systems can be designed.

In addition, the input values for the quantity of product and contaminant protein received from the previous unit operation together with the recovery factors listed in the parameters allow the calculation of the cumulative recovery of product through this step, as well the percent purity of the product and the product purification factor for this step. This information is helpful for identifying steps in the manufacturing process which require optimization.

FIG. 8 illustrates an exemplary block flow diagram for the first five unit operations of the microbial fermentation process unit operation list of FIG. 3. Unit operations 1 through 5 are shown as blocks 802, 804, 806, 808 and 810. The input solutions to each of the steps are shown as arrows tagged with solution identifier information from the unit operation list 508. The process streams to which these solutions are added at each unit operation are also shown as arrows tagged with process stream identifier information. Working from the initial process stream characteristics (P-101) in unit operation 1, inoculum prep, the volumes of input materials (solutions) and subsequent process streams in each of the unit operations is determined using scale-up ratios which are included in the information from the unit operation list 508 for each respective unit operation. For example, the volume of solutions and process streams flowing into and out of each of unit operation blocks 802-810 in FIG. 8 is determined by the initial starting characteristics of the process stream P-101 and the volume of its associated input material S-101 in the first unit operation, block 802 and the scale up ratio in each of the successive unit operations, blocks 804-810. The solutions involved in each of unit operation blocks 802-810 are likewise part of the information for each respective unit operation in the unit operation list 508.

FIG. 9 further illustrates step 112, generating the process time line. The process time line is generated (steps 904-906) from unit operation list 508 and block flow diagram calculation set 704. Unit operation list 508 contains enough input information to generate a detailed process time line which includes the start and stop times for most of the tasks associated with each unit operation. The durations of some unit operation tasks are not scale dependent. The durations of other unit operation tasks are, however, scale dependent. In the latter case, as a process is scaled up, the amount of time required to complete a unit operation task increases. In such cases, where duration of a unit operation task is scale dependent, block flow diagram calculation set 704 is required to calculate the quantity of material handled by the unit operation task. After the quantity of material handled by a unit operation task is determined, its duration can be determined. Examples of scale dependent task durations are the time required to pump solutions from one storage tank to another, the amount of time required to heat or cool solutions in a heat exchanger, the amount of time required to filter product or contaminants from solution

FIG. 10 is an example of a high-level process time line for a microbial fermentation process. The unit operation sequence of the process time line of FIG. 10 corresponds to the unit operation list of FIG. 3. The high-level process time line shown in FIG. 10 illustrates two process cycles of the microbial fermentation unit operation sequence, labeled "First Process Cycle" and "Second Process Cycle." A process cycle is a complete run of the biopharmaceutical production process, as defined by the unit operation sequence for the process.

The first two columns of the process time line of FIG. 10 identify the unit operation sequence number and unit operation description of the unit operation being performed, respectively. The first three sets of unit operations correspond to the three cycles per batch of unit operation sequence numbers 1-6 of FIG. 3. Three cycles of unit operations 1-6 are performed and the results are pooled into unit operation 7, pool harvests. The two columns to the right of the duration

column identify the week and day that the particular unit operation is occurring in the first process cycle.

The day and the week each unit operation is performed is calculated from the start time of the process, as well as the cumulative duration of each of the previous unit operations. In the example of FIG. 10, Sunday is defined as the first day of the week. In the example of FIG. 10, the process sequence begins at unit operation 1, inoculum prep, on Friday of the first week. After unit operation 1 has completed (24 hours later, since unit operation 1 has a 24 hour duration) unit operation 2 is performed on Saturday. The begin and end times for each successive unit operation are calculated from the duration of the unit operation and end time of the previous unit operation. Note that FIG. 10 is calculated to the day and week only for the purposes of explanation. Usually the process time line is determined for each of the tasks associated with a unit operation to the minute.

As illustrated in FIG. 10, unit operation 7 occurs on Monday of the third week in the first process cycle. The third column from the left is the duration of each of the unit operations. After the three cycles of unit operations 1 through 6 have been pooled in unit operation 7, the process continues at unit operations 8 through 10, heat exchange, cell disruption and heat exchange. Each of unit operations 8 through 10 are cycled three times and the associated scheduling information is contained in column to the right of the unit operation duration. Since each cycle of unit operations 8 through 10 have a duration of .5 hours, as shown in column 3, each cycle occurs on Monday of the third week in the process.

FIG. 11 illustrates the final unit operations of the process time line for the microbial fermentation process. After 3 cycles of unit operations 8 through 10 have been completed, unit operation sequence numbers 11 and 12 cycle together two times on Monday, week 3 of the first process cycle. After unit operation sequence numbers 11 and 12 have been cycled twice, the microbial fermentation production process continues without cycling from unit operation sequence number 13 through unit operation sequence number 22 to conclude the microbial

fermentation production process. The durations and associated start times are listed for each of the unit operations 13-22.

FIGS. 12A-12H illustrate the preferred embodiment of a detailed process time line. The unit operation sequence of the process time line of FIGS. 12A-12H correspond to the unit operation list of FIG. 3. The process time line of FIGS. 12A-12H illustrates a single process cycle of the microbial fermentation unit operation sequence. The individual tasks associated with each unit operation are included after the unit operation. For example, in FIG. 12A, unit operation 1A, inoculum prep, consists of the individual tasks of set up, pre-incubation, incubation, and clean up. Columns 11-14 show the start date and time and finish date and time for each of the tasks in each unit operation. Since setup and clean up are not part of the critical path of the process, they do not directly affect the start and end times of following unit operations. The start and finish date and times for the set up and clean up operations of each of the unit operations are valuable because they ensure that the equipment will be available for each unit operation if the process time line is followed.

The process time line of FIGS. 12A-12H includes examples of unit operation task duration calculations. Row 20, column 15 of FIG. 12A, which corresponds to the harvest task of unit operation 3A, seed fermentation, is an example of a duration calculation. As stated above, the duration of some unit operations is process scale dependent (i.e., the duration is dependent upon the volume processed). The harvest task in the seed fermentation unit operation is an example of a task whose duration is process scale dependent. In column 15, the calculations column, information listed for the harvest task is 50 liters, 1.7 liters/minute (LPM), and 0.5 hours. Fifty liters represents the volume of material that is harvested during a harvest task. 1.7 liters/minute represents the rate at which the solution is harvested. Given the volume to be harvested and the flow rate of the harvest, the duration of the harvest task is calculated to be 0.5 hours. Each task in a unit operation that is volume dependent has its duration calculated in order to generate the process time line of FIGS 12A-12H.

The process time line of FIGS. 12A-12H can be resolved to minutes and seconds, if necessary. The accuracy of the process time line allows the precise planning and scheduling of many aspects of the batch manufacturing process. The process time line scheduling information can be used to schedule manufacturing resources such as labor, reagents, reusables, disposables, etc., required directly by the manufacturing process. Pre-process support activities such as solution preparation, and equipment prep and sterilization, required to support the core process, including the labor, reagents, etc. can be scheduled, cost forecasted and provided for. Post-process support activities such as product formulation, aseptic fill, freeze drying, vial capping, vial labeling and packaging required to ship the purified product in a form ready for use may be added to the process time line and managed. Based on the process time line, labor, reagents, etc., required to support these post-process support functions can be acquired and managed. One of the most important aspects of the present invention is the determination of process utility loads such as USP Purified Water, Water For Injection, Pure Steam, etc., for all of the manufacturing equipment. The process time line can be used to determine the peak utility loading, and utility requirements for the facility. Building utility loads such as building steam, heating, ventilation, air conditioning, plumbing, etc., for all manufacturing equipment, process areas and facility equipment can be determined based on the process time line and the equipment associated with each of the unit operations. The process time line can be used to measure the time that the equipment has been in service to schedule preventative maintenance of all plant equipment, Quality Assurance activities including instrument calibration, automated batch documentation, etc. and Quality Control activities including process system maintenance, raw material testing, in process testing and final product testing, etc.

2.0 Solution Preparation Scheduling Module

The preferred embodiment of the present invention is a computer based system and method for the simulation, modeling and scheduling of batch process solution preparation. The preferred embodiment is based on a method for generating scheduling information which accurately defines the complex manufacturing operations of solution preparation in batch manufacturing processes. This scheduling capability system allows the definition of manufacturing costs and systems in a more detailed and accurate manner than previously possible. As a result, this invention allows the rapid and accurate evaluation of numerous batch manufacturing alternatives in order to arrive at an optimal process design early in a facility development project. In so doing the invention minimizes project cost over runs which result from inaccuracies that can carry forward from the early stages of design into construction. The invention also allows the accurate scheduling of solution preparation activities in an operating manufacturing plant, including the scheduling of resources required by solution preparation such as labor, reagents, disposables, reuseables, utilities, equipment maintenance & calibration, etc..

The object of the solution preparation scheduling module is to assign each solution to a solution preparation vessel and to generate a solution preparation schedule for each solution preparation vessel. Scheduling solution preparation in each solution preparation vessel allows the biopharmaceutical production process designer to manage, predict and optimize solution preparation vessel inventory, equipment cost, utility requirements, clean and preparation and other solution preparation associated activities

FIG. 13 is a flow chart providing an overview of the process for scheduling and simulating solution preparation in a biopharmaceutical production process. Step 1302 determines the solution preparation time for each solution preparation vessel. A solution preparation vessel is a vessel used for the preparation of solution used in the biopharmaceutical production process. In the preferred

embodiment, each type of solution preparation vessel used in the biopharmaceutical production process has an associated solution preparation time. The solution preparation time is the amount of time it takes to prepare solution in the solution preparation vessel. Preparation of one solution preparation vessel's volume of solution is called a solution preparation cycle. Each solution preparation vessel has associated solution preparation parameters. Solution preparation parameters describe the amount of time necessary to complete various steps in the solution preparation process.

Step 1304 assigns the solutions in the biopharmaceutical production process to particular solution preparation vessels. Solutions are assigned to particular vessels in order to schedule and determine the load on the solution preparation vessels. Step 1304 includes the procedure of determining the total volume of each solution needed for the biopharmaceutical production process and assigning it to a preparation vessel of the appropriate size. Large volume solutions can be prepared in smaller multiple solution preparation cycles and pooled to yield a higher volume batch of solution. Conversely, smaller volume solutions can be batch prepared in larger preparation volumes to accommodate multiple process cycles provided the shelf life of these solutions allow longer storage times.

Step 1306 determines the calculated start date and the next preparation date of each solution. The calculated start date for the preparation of a solution is the date which solution preparation should begin in order to have the solution ready for use in the biopharmaceutical process. The calculated start date takes into account the amount of time necessary to prepare the solution, and other lead time factors necessary for preparation of solution. The next preparation date is the earliest date that a solution will be prepared after its calculated start date. The next preparation date is determined by adding the periodicity of solution preparation to the calculated start date. The periodicity of solution preparation is how often each solution must be prepared in order to sustain the biopharmaceutical production process.

Step 1308 determines the earliest solution preparation date for each solution preparation vessel for a given process cycle. Since each solution has been assigned to a solution preparation vessel, and the calculated start dates for each solution have been determined, step 1308 determines the earliest calculated start date for each solution preparation vessel. The earliest calculated start date associated with a solution preparation vessel is the date which the first solution is prepared in the vessel for a given process cycle. The earliest calculated start date associated with a solution preparation vessel identifies the point in the process cycle by which the preparation vessel must be available.

Step 1310 determines the latest next preparation date for each solution preparation vessel. The latest next preparation date for each solution preparation vessel is the date that a solution preparation vessel is last used for solution preparation to support a given process cycle. Based on the solution to solution preparation vessel assignments determined in step 1304, the earliest calculated start date for each solution and the next preparation dates for each of the solutions determined in step 1306, step 1310 determines the latest next preparation date for each solution preparation vessel. The earliest calculated start date and the latest next preparation date associated with a solution preparation vessel define the usage boundaries of the solution preparation vessel in the process cycle. The loading of a solution prep vessel can be evaluated during the time between the earliest calculated start date and the latest next preparation date. In the case where the usage boundary is set by a solution which is batch prepared to accommodate multiple process cycles, the usage boundary of a tank includes these multiple process cycles. Therefore the loading on a solution preparation vessel in this instance will also account for solutions from multiple process cycles.

The duration of time between the first biopharmaceutical production process activity related to a given process and the last biopharmaceutical production process activity related to that process may be called a manufacturing cycle (i.e., multiple process cycles define a manufacturing cycle). In the case where an activity, such as the preparation of a solution, accommodates multiple

process cycles, a manufacturing cycle consists of multiple process cycles. In the case where all the activities associated with a process only accommodate one process cycle a manufacturing cycle consists of only one process cycle. Therefore manufacturing cycles may consist of one or more process cycles with their related support activities.

5

Step 1311 calculates the use duration for each solution preparation vessel. The use duration for each solution preparation vessel is the time that a solution preparation vessel is occupied with the preparation of solution for a manufacturing cycle. For example, when multiple solutions are assigned to a single solution preparation vessel, the use duration for the solution preparation vessel is determined based on the earliest calculated start date and the latest next preparation date for all of the solutions assigned to the solution preparation vessel. The total number of hours the solution preparation vessel is occupied can be calculated from the use duration (days) and the number of shift hours per day for the particular manufacturing cycle (e.g., single shift operation would normally be 8 hours per day).

10

Step 1312 calculates the cumulative solution preparation time for each solution preparation vessel. The cumulative solution preparation time is the amount of time a solution preparation vessel is occupied with the preparation of solutions in a biopharmaceutical manufacturing cycle. Step 1312 calculates the cumulative solution preparation time for each solution preparation vessel based on:

15

- 1) the solutions assigned to a particular vessel;
- 2) the prep vessel use duration;
- 3) the duration of a process cycle;
- 4) the number of preps of a solution per process cycle; and
- 5) solution preparation times.

20

For example, if five solutions are to be prepared in a particular solution preparation vessel each requiring two preparations per process cycle, process

25

cycle durations of seven days, solution preparation times of three hours, during a use duration of fourteen days, the cumulative solution preparation time for the solution preparation vessel would be sixty hours over a two week period.

Step 1314 determines the percent utilization of each solution preparation vessel. The percent utilization of each solution preparation vessel is the fraction of the use duration that the solution preparation vessel is actually engaged in the preparation of solution, or the cumulative solution preparation time. The percent utilization is determined based on the use duration, cumulative solution preparation time and the number of hours per solution prep shift for the process cycle. For example, if the use duration for a solution preparation vessel is fourteen days, and there are eight shift hours per day, then the solution preparation vessel has a total availability of one hundred twelve hours. If, as calculated above, the cumulative solution preparation time for the solution preparation vessel is sixty hours, then the percent utilization of the solution preparation vessel is approximately fifty-four percent. The percent utilization of each solution preparation vessel is determined in step 1314 so that the biopharmaceutical production process planner is able to gauge the level of utilization of the solution preparation equipment and make any adjustments in the solution preparation equipment pool or production cycles.

Step 1316 generates the initial shift schedule for each solution preparation vessel. The initial shift schedule is a daily schedule of solutions to be prepared in a particular solution preparation vessel. Step 1316 generates the initial shift schedule based on the calculated start date for each solution, the periodicity of solution preparation for each solution and the solution to solution preparation vessel assignment.

Step 1318 back schedules solution preparation procedures that do not fit in the shift schedule and checks for system capacity problems. Back scheduling is the process of rescheduling solution preparation cycles for previous days or time slots. The initial shift schedule is generated regardless of the number of hours a solution preparation vessel is occupied for a particular day. For example, the

initial shift schedule may have a particular solution preparation vessel scheduled for fourteen hours of solution preparation. In a biopharmaceutical production process that operates sixteen hours a day, all of the solutions scheduled for the solution preparation vessel can be accommodated. If, however, the
5 biopharmaceutical production process operates only eight hours a day, not all of the required solutions may be prepared on the scheduled date Step 1318 back schedules to earlier days those solution preparation cycles that cannot be completed on the initially scheduled day. The scheduling of a back scheduled solution preparation cycle into an available shift is performed according to the priority of the oldest back scheduled date for all available back scheduled solutions. The end result of step 1318 is to generate a final shift schedule for each prep vessel which assigns the appropriate solutions to that vessel and schedules out the preparation of each solution according to shift capacity, the duration of each prep assigned to that shift.

10
15 Step 1320 generates a time line for the operation of each solution prep vessel and its associated equipment according to the shift assignments in the final shift schedule and the durations associated with each solution prep step in the solution prep procedure table. Based on this time line resources requirements for labor, reagents, disposables, reusables, utilities, maintenance, etc., can be
20 accurately scheduled

25 FIG. 14 further illustrates step 1302, determining the solution preparation time for each solution preparation vessel. Step 1302 begins at step 1420 determining the setup time for a solution preparation vessel. Step 1420 compares a list of solution preparation vessels 1402 that are available for use in the biopharmaceutical production process and their associated solution preparation vessel identifiers with a master list of solution preparation vessel identifiers and their associated set up times 1410. Solution identifiers and solution preparation vessel identifiers are keys or tags that identify individual solution preparation vessel and solution types. Examples of solution preparation vessel set up times
30 are illustrated in FIG. 15, column 1410. List of solution preparation vessels 1402

includes the minimum/maximum working volumes for each vessel, as well as the particular tasks associated with the solution preparation vessel and any process equipment necessary to complete solution preparation. The solution preparation tasks and equipment may be included in the total solution preparation time 1428
5 for use in equipment preparation and scheduling.

Next, step 1408 determines the water collection time for each preparation vessel. The water collection time is the amount of time necessary to fill the maximum working volume 1406 of the solution preparation vessel at the water collection rate 1404. Water collection rate 1404 is the rate at which the solution preparation vessel can be filled. Different solution preparation vessels have different water collection rates, depending on their specific water collection hardware. Step 1408 estimates the water collection time for each solution preparation vessel based on its maximum working volume 1410 and the water collection rate 1404. In the preferred embodiment, the volume of water to be collected is assumed to be the preparation vessel maximum working volume 1406.
10 In alternative embodiments, the volume of water to be collected can be the actual volume of solution prepared in the solution preparation cycle. Examples of water collection rate 1404, maximum working volume 1406 and water collection time 1502 are illustrated in FIG. 15, columns 1404, 1406 and 1502, respectively.
15

Step 1414 defines the weigh and mix times associated with each solution preparation vessel. Weigh and mix time 1416 is the time required to weigh, mix and adjust the components of a solution. Preparation vessel identifiers 1402 are matched with the associated preparation vessel weigh and mix time 1416. The weigh and mix time 1416 associated with each solution preparation vessel in the biopharmaceutical process is thereby assigned to the associated solution preparation vessel identifier 1402. The default weigh and mix time variables can be manipulated by the process designer. Examples of weigh and mix time 1416 are illustrated in FIG 15, column 1416.
20
25

Next, step 1418 determines the time required to filter the solution in a preparation vessel. The time required to filter the solution in a preparation vessel
30

is the amount of time post-preparation filtering and transfer of the prepared solution out of the solution preparation vessel requires. Step 1418 calculates the time required to filter the solution in a preparation vessel based on preparation vessel identifier 1402, preparation vessel maximum working volume 1406, filtration flux rate 1424 and surface area of filtration media 1412. In the preferred embodiment, the volume of solution to be filtered is assumed to be the preparation vessel maximum working volume 1406. In alternative embodiments, the volume of solution to be filtered can be the actual volume of solution prepared in the solution preparation cycle. The surface area of the filtration media 1412 is the area of the filtration media used to filter the solution as it is transferred out of the solution preparation vessel. Filtration flux rate 1424 is the rate per unit area that the solution is can be filtered through the filtration media. Examples of filtration flux rate 1424 and surface area of filtration media 1412 are illustrated in FIG. 15, columns 1424 and 1412, respectively

Step 1426 calculates the adjusted filtration time. The adjusted filtration time is the filtration time as determined in step 1418 multiplied by the filtration delay factor 1430. Filtration delay factor 1430 is based on the additional filtration time typically required to manipulate solution storage vessels on a fill line. Step 1426 calculates the adjusted filtration time by multiplying the filtration time calculated in step 1418 by the filtration delay factor 1430. FIG. 15, column 1430 shows exemplary values for filtration delay factor 1430.

Step 1432 determines clean in place and steam in place durations associated with each solution preparation vessel. Clean in place duration 1422 and steam in place duration 1434 are the durations of the cleaning procedures necessary to prepare a solution preparation vessel for use in the next solution preparation cycle. Step 1432 matches preparation vessel identifiers 1402 with clean in place duration 1422 and steam in place duration 1434 to determine the clean in place duration 1422 and steam in place duration 1434 times associated with each of the solution preparation vessel used in the biopharmaceutical

production process. FIG. 15, columns 1422 and 1434 illustrate exemplary values for clean in place duration 1422 and steam in place duration 1434, respectively.

Step 1436 calculates total solution preparation time 1428 for each preparation vessel by summing the time values calculated in steps 1420, 1408, 1414, 1418, 1426 and 1432. Total solution preparation time 1428 represents the amount of time required to prepare the maximum working volume 1406 of solution in a particular solution preparation vessel. It should be noted, however, that one of ordinary skill could expand the calculation of total solution preparation time 1428 to include additional steps, factors or parameters other than those described herein. Such expansion would allow the present invention to calculate the total solution preparation time 1428 for a solution preparation vessel more accurately, or to include additional factors in the calculation. In addition, the calculation of total solution preparation time 1428 for a solution preparation vessel could also be adjusted to accommodate solution preparation working volumes which are less than the maximum solution preparation working volumes for a given solution prep vessel. Column 1428 of FIG 15 provides exemplary values for total solution preparation time 1428.

FIG. 15 shows an exemplary list of solution preparation parameters. Examples of such parameters are minimum working volume 1402, maximum working volume 1406, set up time 1410, water collection rate 1404, water collection time 1502, weigh and mix time 1416, square area of filter media 1412, volume per unit of filter area per hour 1424 and post-solution preparation and cleaning procedure duration 1422, 1434.

Minimum working volume 1402 and maximum working volume 1406 are the minimum and maximum volumes of solution a solution preparation vessel can prepare. Set up time 1410 is the amount of time necessary to prepare a solution preparation vessel for the solution preparation process. Water collection time 1404 is the time necessary to fill the solution preparation vessel with the maximum working volume 1406 of water. Weigh and mix time 1416 is the time necessary to weigh and mix the ingredients of a solution in a particular solution preparation

vessel. Square area of filter medium 1412 is the area of the filter associated with a particular solution preparation vessel. Volume per unit of filter area per hour 1424 is the flux rate per unit of filter area associated with a particular solution preparation vessel. Post solution preparation and cleaning procedure duration 1422 and 1434 are the times associated with preparing the solution preparation vessel after the preparation of a batch of solution.

FIG. 16 further illustrates step 1304, assigning the solutions required by the biopharmaceutical production process to particular solution preparation vessels. In order to schedule solution preparation cycles, each solution must be assigned to a solution preparation vessel. Step 1304 begins with step 1602. Step 1602 sets the preparation cycles per batch for a solution to be prepared. Preparation cycles per batch 1608 are the number of times a solution is prepared in a solution preparation vessel to support one product batch cycle. For example, if one-hundred and fifty liters of solution 101 is required to make a batch of product in a biopharmaceutical production process and the solution is to be prepared in a fifty liter solution preparation vessel, solution 101 may be prepared in three preparation cycles per batch of fifty liters each, yielding a 150 liter batch of solution 101. Alternatively, solution 101 may be prepared in four preparation cycles per batch of thirty-seven and one-half liters each in a solution preparation vessel of at least thirty-seven and one-half liters. In the preferred embodiment, preparation cycles per batch 1608 of solution is initially set by the designer. Preparation cycles per batch 1608 will affect values throughout the solution preparation scheduling module and the solution preparation procedure as a whole. The number of preparation cycles per batch 1608 for each solution will dictate the size of a solution preparation vessel and the time required to prepare a batch of solution.

Step 1606 determines the number of days per solution preparation cycle 1610 for each of the solutions involved in the biopharmaceutical production process. The number of days per solution preparation cycle 1610 is determined from preparation cycles per batch 1608 and days per batch cycle 1604. The batch

cycle time is the amount of time required to produce one batch of product. Days per batch cycle 1604 is the number of days between successive batches of product. The number of days per preparation cycle 1610 is the number of days between the beginnings of each solution preparation. Dividing the number of days per batch cycle by the preparation cycles per batch 1608 yields the number of days per preparation cycle 1610. For example, if one-hundred and fifty (150) liters of solution per batch of product is to be prepared in a solution preparation vessel with a working volume of fifty liters, the preparation cycles per batch 1608 is three. If one batch of biopharmaceutical product is produced every 6 days, the days per batch cycle 1604 is six. Given that there are three preparation cycles per batch for a particular solution, and there are six days per batch cycle, the number of days per preparation cycle 1610 is determined to be two. That is, there are two days between the beginnings of each fifty liter preparation cycle of solution.

Decision step 1612 checks the shelf life of the solution against the number of days per preparation cycle 1610. In the preparation of solutions, it is possible that the number of days per preparation cycle 1610 may exceed the shelf life of the solution. In such a situation, it is possible to have "stale" solution available for use in the biopharmaceutical production process because it has been held too long. If decision step 1612 determines that number of days per preparation cycle 1610 is greater than the shelf life, step 1304 continues at step 1602 where the number of preparation cycles per batch 1608 is adjusted (preferably increased). Adjusting the preparation cycles per batch 1608 of the solution will allow the solution preparation process designer to decrease the number of days per preparation cycle 1610 as determined in step 1606. If decision step 1612 determines that the number of days per preparation cycle 1610 is less than the shelf life of the instant solution, step 1304 continues at step 1616.

Step 1616 calculates the liters per preparation cycle of solution 1620 for each solution. Liters per preparation cycle of solution 1620 is calculated by dividing the total liters per batch for each solution 1618 by the number of preparation cycles per batch 1608 as determined in step 1602. Total liters per

batch for each solution 1618 is the quantity of each solution type needed to produce a batch of product in the biopharmaceutical production process and is stored in the material balance table.

Step 1624 determines the solution preparation vessel type for the preparation of each solution. Step 1624 assigns each solution to a solution preparation vessel in step 1624, generating preparation vessel to solution assignment list 1626. Step 1624 assigns each solution to a solution preparation vessel based on the number of liters per preparation cycle of solution 1620 and preparation vessel identifier and associated volume list 1402. Solution preparation vessels are chosen from preparation vessel identifier and associated volume list 1402 in order to place liters per preparation cycle of solution 1620 within the minimum working volume 1402 and the maximum working volume 1406 range of a solution preparation vessel. Preparation vessel to solution assignment list 1626 is a list of solutions to be prepared in the biopharmaceutical production process, and their associated solution preparation vessel.

Fig. 17 illustrates exemplary values of data for the present invention. Column 1618 illustrates exemplary values for the total liters per batch for each solution 1618. Column 1608 illustrates exemplary values for number of preparation cycles per batch 1608. In the instant example, all of the solutions as shown in column 1608 are prepared in one preparation cycle per batch. Column 1604 illustrates exemplary values for days per batch cycle 1604. Column 1610 illustrates exemplary values of number of days per preparation cycle 1610 as determined in step 1606. In the instant example, since the number of preparation cycles per batch 1608 of solution is equal to one for all of the solutions in the solution production process, the number of days per preparation cycle 1610 equals the number of days per batch cycle 1604. Column 1614 illustrates exemplary values of shelf life of solution 1614. Column 1706 illustrates exemplary values for the outcome of decision step 1612 where number of days per preparation cycle 1610 is compared to shelf life of solution 1614. Column 1618 of FIG. 17 illustrates exemplary values for total number of liters per batch for each solution

1618. Since the number of preparation cycles per batch 1608 for each of the solutions is one in the instant example, the number of liters per preparation cycle of solution 1620 is equal to total liters per batch for each solution 1618.

5 Columns 1708-1728 of FIGS. 17 and 18 illustrate an exemplary solution to solution preparation vessel assignment list 1626. The tank identifiers run along the top of column 1708-1728 and the solution identifiers run along the vertical axis on the far left hand side of the tables in FIGS. 17 and 18. In FIG. 18, exemplary solution preparation vessel identifiers are placed in the columns horizontally opposed from the solution identifiers indicating that the preparation vessel is assigned to that solution.

10 FIG. 18 illustrates exemplary preparation vessel to solution assignment list 1626. Columns 1626 illustrates preparation vessel to solution assignments. Column 1722 illustrates solution preparation vessel #108 is associated with solutions S-0107, S-0108, S-0112, S-0115, S-0117, and S-0120. Similarly, column 1724 illustrates solution preparation vessel #109 is associated with solutions S-0116, S-0118, and S-0119. Column 1726 illustrates solution preparation vessel #110 is associated with solutions S-0106 and S-0114. Column 1728 illustrates solution preparation vessel #111 is associated with solutions S-0101 and S-0113.

15 FIG. 20 further illustrates step 1306, determining the calculated start date for preparation of each solution 2010 and the next preparation date for each solution 2022. The next preparation date 2022 is based on the calculated start date 2010 and the number of days per solution preparation cycle 1610. Step 1306 begins at step 2004, determining the calculated start date for the preparation of each solution (“calculated start date”) 2010. Calculated start date 2010 is the date by which the preparation of a solution should begin in order to prepare the solution in time for use in the biopharmaceutical production process. The calculated start date 2010 is determined by calculating back from the earliest date a solution is needed 2006 in the biopharmaceutical production process and the “lead time” needed to prepare and test a batch of solution before use. In the

preferred embodiment, the back calculated values are the total solution preparation time for a solution preparation vessel 1428, the number of back days to allow for a failed lot of solution 2002 and the number of hold days for solution quality assurance and quality control (QA/QC) testing 2008. If a batch of
5 solution fails QA/QC testing, the solution will have to be prepared again, and this lead time is expressed as the number of back days to allow for a failed lot of solution 2002. The earliest date a solution is required 2006 comes directly from the process time line via the material balance table. The material balance is a list 10 of solution formulation reagents and calculation sets, each of which is associated with a unit operation. The material balance table includes the volumes of all the process streams in the block flow diagram 704 and their constituent solution components according to the formulation of the solution. The material balance table also identifies the time that a solution is required in the manufacturing process according to the task scheduling data in the process time line 906.

15 After the calculated start date for solution preparation 2010 is determined, it is assigned to the associated solution and prep vessel solution assignment list 1626 resulting in a calculated start date 2010 for the preparation of each solution and its associated solution preparation vessel.

Step 2018 calculates the next solution preparation date for each solution
20 after the calculated start date 2010 has been determined for each solution by selecting the greater of days for batch or days for preparation. Step 2018 calculates the next solution preparation date for each solution by. The next solution date is calculated in step 2018 by adding the number of days per preparation cycle 1610 to the calculated start date for preparation of each solution
25 assigned to a preparation vessel 2010.

FIG. 24 further illustrates step 1308, determining the earliest solution preparation start date for each solution preparation vessel in a process cycle. Step 1308 begins by determining and assigning the calculated solution preparation start dates 2010 to each solution preparation vessel in step 2402. Solution preparation vessel (“prep vessel”) to solution assignment list 1626 and calculated solution
30

preparation start date for all solutions 2010 are cross-referenced to generate calculated and assigned solution prep start dates to prep vessels 2404. Step 2406 generates the earliest solution preparation start date for each solution preparation vessel (“earliest start date”) 2408. Calculated and assigned solution prep start dates to prep vessels 2404 is processed in step 2406 to determine the earliest solution preparation start date associated with each preparation vessel. Step 2406 results the earliest preparation start dates assigned to each preparation vessel 2408. This list provides the solution preparation vessels necessary for the biopharmaceutical production process, as well as the earliest date each solution preparation vessel is needed for preparation of solution in the process cycle.

FIG. 25 further illustrates step 1310, determining the latest solution preparation start date for each solution preparation vessel. Step 1310 begins by determining and assigning the next solution preparation dates to each solution preparation vessel at step 2502. A next solution preparation date is the date that a solution preparation vessel will be needed for the preparation of solution next after the earliest start date 2408. The solution preparation vessel to solution assignment list 1626 and next solution preparation date for each solution 2022, as determined in step 2018, are matched to generate a list of next solution preparation dates to each preparation vessel at step 2502. Next, step 2504 determines the latest next solution preparation start date associated with each preparation vessel 2506. The latest next solution preparation start dates are those dates associated with preparation vessels which signify the last preparation of solution procedure to occur in a particular solution preparation vessel during a process cycle.

FIG. 26 further illustrates step 1311, calculating solution preparation vessel utilization time for each solution preparation vessel 2604. Solution preparation vessel utilization time 2604 for each preparation vessel is that time during which the vessel is occupied with the preparation of solution(s) for a particular manufacturing cycle. Solution preparation vessel utilization time 2604 is the duration between the earliest preparation start date 2408 and the end of

latest next solution preparation cycle. The end of latest next solution preparation cycle is calculated by adding the total solution preparation time for a solution preparation vessel 1428 to the latest next solution preparation start date for each solution preparation vessel 2506, which results in the date when the solution preparation vessel has completed preparing solution in a process cycle. Solution preparation vessel utilization time for each solution preparation vessel 2604 is determined by comparing the earliest solution preparation start date 2408 with the sum of the latest next solution preparation start date 2506 and the total solution preparation time for each solution preparation vessel 1428.

FIG. 27 further illustrates step 1312, calculating the cumulative solution preparation time for each solution preparation vessel 2708. Cumulative solution preparation time for each solution preparation vessel 2708 is the amount of time that each preparation vessel is actually occupied with the preparation of solution. Essentially, cumulative solution preparation time is the product of the total solution preparation time for a solution preparation vessel 1428 and the number of solution preparation cycles that the solution preparation vessel is used for in the manufacturing cycle. For example, if the total solution preparation time for a solution preparation vessel is six hours per cycle, and the solution preparation vessel is used in the preparation of six cycles of solution, the cumulative solution preparation time 2708 is thirty-six hours.

Step 1312 begins by assigning a solution preparation total time for each solution preparation vessel to each preparation vessel at step 2702. Total solution preparation time for each preparation vessel 1428 from step 1302 is matched to preparation vessel to solution assignment list 1626. The lists of preparation vessels, the solutions associated therewith and their total solution preparation times are input into step 2704. Step 2704 determines the cumulative solution preparation time for each solution by multiplying the total solution preparation time 1428 for the solution preparation vessel by a solution's respective number of preparation cycles per batch 1608. Step 2704 results in the amount of time each solution preparation vessel is occupied with the preparation each particular

solution. Step 2706 determines the cumulative solution preparation time for each solution preparation vessel 2708 by summing the amount of time each solution preparation vessel is actually occupied with the preparation of solution. Steps 2704 and 2706 result in the list of cumulative solution preparation times for each preparation vessel 2708.

FIG. 28 further illustrates step 1314, determining the percentage utilization of each solution preparation vessel. The percentage utilization of a solution preparation vessel is the ratio of the cumulative total solution preparation time for each solution preparation vessel 2708 to the total time that a solution preparation vessel is available for solution preparation 2802 expressed as a percentage. Determining the percentage utilization of each solution preparation vessel 2808 allows the process designer to tailor the preparation cycles per batch 1602 of each solution to maximize the utilization of the solution preparation equipment, thereby minimizing cost and maximizing efficiency. Step 1314 begins by calculating the total number of hours a solution preparation vessel is available at step 2802. The total number of hours a preparation vessel is available is the product of the solution preparation vessel utilization time 2604, as determined in step 2602, and the hours per solution preparation shift 2804. The hours per solution preparation shift 2804 is provided from in the original process design parameters for the biopharmaceutical production process. For example, if the process is designed as a two shift process, the plant would normally run sixteen hours a day, and the number of hours per solution prep shift 2804 would be sixteen.

Step 2802 multiplies the solution preparation vessel utilization time 2604 by the hours per solution preparation shift per day 2804. Step 2802 results in the number of raw hours that a solution preparation vessel is available to the biopharmaceutical production process. For example, if the solution preparation vessel utilization time 2604 is six days, and the biopharmaceutical production process is run one shift a day (eight hours), the number of hours the solution preparation vessel is available for use in the biopharmaceutical production process is forty-eight. Forty-eight is the maximum number of hours that the solution

preparation vessel is available for use. If such a solution preparation vessel is actually occupied with the preparation of solution for twenty-four hours, the percentage utilization of the solution preparation vessel during its period of availability 2808 would be fifty percent.

5 Step 2806 calculates the percentage utilization of each solution preparation vessel. The percentage utilization 2808 is determined by comparing the total number hours a solution preparation vessel is available as calculated in step 2802 with the cumulative total solution preparation time for each solution preparation vessel 2708. By dividing cumulative total solution preparation time for each solution preparation vessel 2708 by the total number of hours a preparation vessel is available as calculated in step 2802, percentage utilization of each preparation vessel during its period of availability 2808 is calculated, as explained in the example above.

10 FIG. 29 further illustrates step 1316, generating the initial shift schedule 2910. The initial shift schedule 2910 is a table of dates scheduling the preparation of solutions for use in the biopharmaceutical production process. Initial shift schedules 2910 are generated for each of the solution preparation vessels. An initial shift schedule for a solution preparation vessel contains the solutions to be prepared and their associated preparation dates, as well as the days per prep cycle.

15 FIG. 31 is an example of an initial shift schedule. Step 1316 begins with step 2902, generating a time-line starting from the earliest start prep date of all the solutions required by the biopharmaceutical production process at step 2902. In the preferred embodiment, the time-line is incremented one day at a time, out to a date predetermined by the system designer. In alternative embodiments, the time-line and shift schedule are incremented or delimited in whichever time intervals are most convenient.

20

25

Step 2904 determines and matches solution preparation dates for each solution 2404 with the dates in the shift schedule time-line from step 2902. Matched solution preparation dates to solution preparation vessels 2404 are entered into the shift schedule time-lines for each of the solution preparation

vessels. Starting from the calculated start date 2404, step 2904 enters successive preparation start dates for each solution associated with a preparation vessel based on the number of days per preparation cycle 1610. For example, if a particular solution assigned to solution preparation vessel has two days per preparation cycle, the solution is scheduled for preparation in its solution preparation vessel every two days after its calculated start date 2010. Step 2904 results in a list of solutions and associated preparation dates for each solution preparation vessel 2906.

Step 2908 enters the total number of solution preparation hours for each solution into each initial shift schedule time-line. The result is the number of preparation hours each day associated with every solution preparation in the initial shift schedule. Step 2908 matches solution preparation times for each solution preparation vessel 1428 with the dates assigned in each of the shift schedule time-lines to generate the initial shift schedule 2910. The total number of hours each solution preparation vessel is occupied with the preparation of solution each day can then be determined by adding the number of solution preparation hours associated with each day on an initial shift schedule time-line 2910. In the preferred embodiment, the number of hours of solution preparation per day per solution preparation vessel is essentially the product of the number of solution preparation cycles and the total solution preparation time for the solution preparation vessel 1428. For example, if a solution preparation vessel has a total solution preparation time for the solution preparation vessel 1428 of five hours, and is scheduled for four solution preparation cycles, the solution preparation vessel is scheduled for twenty hours of solution preparation that day. Step 2910 results in the initial shift schedule with solution identifiers and their solution preparation times assigned to their respective shifts 2910.

FIG. 31 is an example of an initial shift schedule for solution preparation vessel 101. Exemplary solution identifiers are shown in column 3102. Column 3102 illustrates exemplary solution identifiers for the solutions used in the biopharmaceutical production process. Solution identifiers 3102 with date entries

in corresponding An exemplary value for hours per solution prep shift is given in box 2804. Exemplary values for number of days per preparation cycle is given in column 1610. Exemplary values of solution prep dates of each solution is given in column 2906.

5 FIG. 30 further illustrates step 1318, back scheduling solution preparation in the initial shift schedule. Solution preparation is initially scheduled in steps 1302-1316 without considering the possibility of scheduling conflict. Back scheduling solution preparation is done in order to avoid conflicts in the solution preparation process. Scheduling conflicts result from scheduling more solution preparation cycles for a solution preparation vessel than can be accommodated in the amount of time available. For example, a scheduling conflict will occur if a particular solution preparation vessel is scheduled for twenty hours of solution preparation on one sixteen hour day. The present invention back schedules those solution preparation cycles that do not fit into their scheduled shift or day. For example, if a solution preparation vessel is scheduled for three solution preparation cycles of three hours each, the solution preparation vessel is scheduled for nine hours of preparation activity. If the production facility runs on an eight hour day, not all of the solutions can be prepared as scheduled. The present invention back schedules one of the solution preparation cycles, leaving six hours of solution preparation to be completed in one day. The back scheduled solution preparation cycle is rescheduled to the first previous available shift so that the solution is prepared in time for use in the biopharmaceutical production process as scheduled in the process time line. After step 1318 is completed, the solution preparation time line is in proper form for use as a solution preparation and scheduling and management tool.

10

15

20

25

Step 1318 begins at step 3002, successively summing the solution preparation times for each of the days or shifts in the initial shift schedule 2910 the solution preparation times are summed in order to determine the total solution preparation time for each solution preparation vessel on each shift. For the purpose of summing the solution preparation times, a shift is the number of hours

30

in one biopharmaceutical production process day (e.g., eight hours for a single shift plant, sixteen hours for a double shift plant, etc.). Step 2002 results in a list for each solution preparation vessel of summed solution preparation times for each shift 3004. Summed solution preparation times 3004 are compared with the available shift hours/day 2804 in step 3006. If the sum of the scheduled solution preparation times 3004 exceeds the number of shift hours available 2804, solutions are marked as “back scheduled” and are rescheduled for the first previously available shift. From the previous example, one of the three hour solution preparation cycles is to be rescheduled for the first previously available shift, leaving six hours of solution preparation in the eight hour shift. If the originally scheduled day for the nine hours of solution preparation was Wednesday, the three hour solution preparation would be back scheduled to Tuesday. After a solution that doesn't fit into the current day has been back scheduled, it is removed from the current day schedule.

If step 3006 determines that the number of shift hours 2804 available exceeds the sum of the scheduled solution preparation times 3004, step 3010 determines if any solution is scheduled for preparation on the current shift. If step 3010 determines that a solution is scheduled for preparation in the current shift, step 3012 leaves the solution scheduled for preparation in the shift schedule.

If step 3010 determines that no solutions are assigned to the solution preparation vessel for the shift that is being evaluated, step 1318 continues to step 3014. Step 3014 determines if any solutions have been back scheduled to the current shift for preparation for a later shift. If no solution preparation cycles have been back scheduled to the current shift, the process continues to step 3002 where the next shift is analyzed for back scheduling. If step 3014 determines that solution preparation cycles have been back scheduled, the process continues at step 3016. Step 3016 checks the original scheduling date on the back scheduled solution preparation cycle to determine if the back scheduled date is earlier than the original scheduling date minus the periodicity of the back scheduled solution. For example, if the solution has been successively back scheduled for four days

(i.e., the preparation cycle of the solution had to be scheduled back four days in order to fit into a shift), and its periodicity was two days, the back scheduled prep would be potentially interfering the previously scheduled prep of the same solution thereby indicating a shift schedule capacity error.

5 If step 3016 determines that the solution is back scheduled beyond its periodicity, an alarm is raised indicating that a system capacity issue exists at step 3020. If step 3016 determines that the back scheduled solution preparation cycle not earlier than its orbitally scheduled date minus its periodicity, the solution preparation cycle is scheduled for the current shift at step 3018.

10 FIG. 32 further illustrates step 1320, generating solution preparation schedule 3210. Solution preparation schedule 3210 schedules each task associated with solution preparation for the biopharmaceutical process based on the back-scheduled shift schedule 3202 and the solution preparation procedure 3212. Solution preparation schedules 3210 are generated for each solution preparation vessel that has an assigned solution. Back-scheduled initial shift schedule 3202, as generated in Step 1318, contains the solution preparation vessel to solution preparation assignment for each of the shifts in the initial shift schedule 2910. Step 1320 is performed for each of the shifts in the initial shift schedule 2910, thereby scheduling all of the solution preparation tasks for each solution preparation vessel on each shift.

15 Step 1320 begins at Step 3206, determining the number of solution preparation that are scheduled for the current shift in the back-scheduled initial shift schedule 3202. If no solutions are scheduled for preparation, step 1320 continues to step 3204 which moves to the next shift in the back-scheduled initial shift schedule 3202. If there are solution preparations scheduled for the current shift, step 1320 continues to step 3208. Step 3208 generates the solution preparation schedule 3210 from the solution preparation procedure data 3212 for each solution preparation scheduled in the shift. For example, if two solutions are scheduled to be prepared in solution preparation vessel 101, each task in each solution preparation procedure is scheduled out in solution preparation schedule

3210. An exemplary solution preparation procedure 3212 is illustrated in FIG. 14
(steps 1420, 1408, 1414, 1418, 1426, 1432, and 1436).

FIG. 15 illustrates exemplary solution preparation procedure data, as described above, used to generate solution preparation schedule 3210. Step 3208 schedules out each task for each solution preparation assigned to the current shift. After step 3208, and if there are additional shifts in the back-scheduled initial shift schedule 3202, step 1320 continues at step 3204 proceeding to the next shift in back-scheduled initial shift schedule 3202. Step 1320 repeats to schedule all of the solution preparations in the back-scheduled initial shift schedule. Step 1320 results in, therefore, solution preparation schedule 3210 which is a time line, by shift, for each solution preparation task for each solution preparation assigned to a solution preparation vessel.

3.0 Equipment Preparation Scheduling Module

The object of the equipment preparation module is to simulate, schedule and model equipment preparation and loading in the biopharmaceutical production process. Equipment used in the biopharmaceutical production becomes soiled and must be cleaned, wrapped and sterilized in order to be used again. The process of cleaning, wrapping and sterilizing is known as equipment preparation. A piece of equipment that has been used in the biopharmaceutical production process and requires preparation before it can be used again is called a soiled process component. Equipment preparation is performed in order to sustain the biopharmaceutical production process.

Current methods for the design equipment preparation procedures typically fall short of accurately defining the relatively complex procedures that are executed in an equipment prep area. As a result the equipment and work areas associated with equipment prep are usually inefficiently designed. Since the cleaning and sterilizing (prep) equipment associated with equipment prep activities are capital and utility intensive, an improved method for accurately modeling and

optimizing these areas of a biopharmaceutical production facility is needed. The preferred embodiment provides a computer simulation method for the design and scheduling of equipment prep operations which is more accurate and efficient than conventional design methods.

FIG. 33 is a flowchart illustrating an overview of the process for scheduling and simulating equipment preparation in a biopharmaceutical production process. Step 3302 generates a preparation equipment protocol table. A preparation equipment protocol is a protocol for the operation of a piece of preparation equipment. Preparation equipment protocols usually include a plurality of equipment preparation tasks. A preparation task is a step in the equipment preparation process. For example, in a glassware dryer, a task may be loading the dryer, preheating the dryer, drying the glassware, unloading the dryer, etc. A preparation equipment protocol table is a set of standard preparation equipment protocols to clean soiled process components. Preparation equipment protocols are usually developed through experimentation and quality assurance testing. The preparation equipment protocols that prepare the soiled process components for reuse most effectively and to the required levels of cleanliness become the preparation equipment protocols.

Preparation equipment protocols are associated with specific pieces of preparation equipment. Examples of preparation equipment are bench sinks, wash stations, glassware washers, glassware dryers, carboy washers, carboy dryers, autoclaves, steam sterilizers, etc. Furthermore, there may be multiple preparation equipment protocols per piece of preparation equipment. For example, there may be four preparation protocols associated with each type of bench sink, each having different combinations of bench sink cleaning tasks and durations. Although the preferred embodiment describes a finite set of preparation equipment, soiled process components and preparation equipment protocols, one of ordinary skill could easily expand the process described herein to any preparation equipment or soiled process components.

Step 3304 generates an equipment preparation procedure table. An equipment preparation procedure is a standard procedure comprising a plurality of preparation equipment protocols by which a soiled process component is cleaned and sterilized for reuse in the biopharmaceutical production process. For example, an equipment preparation procedure for a carboy may include the preparation equipment protocols of bench sink rinsing, bench sink cleaning, carboy washing, carboy drying, wrapping and sterilization in an autoclave. Different types of soiled process components require different combinations of preparation equipment protocols in order to be readied for reuse in the biopharmaceutical production process, thereby defining different equipment preparation procedures. As with preparation equipment protocols, equipment preparation procedures are determined through experimentation, quality assurance and quality control. Each type of equipment used in the biopharmaceutical production process has an associated equipment preparation procedure.

An equipment preparation procedure table is a list of preparation equipment protocols and their associated information that define an equipment preparation procedure for each of the soiled process component types. In a preferred embodiment, there are equipment preparation categories for each piece of soiled process components. Instead of an equipment preparation procedure associated with each type of soiled process component, there is a an equipment preparation procedure associated with each equipment preparation category. Preparation equipment protocols associated with each of the different equipment preparation categories are placed together in a table format to provide the preparation procedures for each piece of soiled process components assigned to an equipment preparation category.

Step 3306 generates the equipment dimension table. Equipment dimensions are the length, height and depth of a piece of process equipment requiring cleaning and sterilization (e.g., beaker, flask, carboy, stainless steel fittings, etc.). The equipment dimension table defines the dimensions of all process equipment potentially requiring cleaning after use in the biopharmaceutical

5 production process. The equipment dimension table is determined directly from the list of equipment used in the biopharmaceutical production process. The equipment dimension list provides a means for determining the volume of the equipment to be cleaned in the biopharmaceutical production process, thereby
allowing the calculation of the capacity of the preparation equipment

10 Step 3308 generates a master list of equipment that may require preparation. Each unit operation in the biopharmaceutical production process is associated with preparation equipment. Step 3308 generates a master list of equipment associated with the biopharmaceutical production process and solution preparation process. In the preferred embodiment, the preparation equipment associated with each unit operation for both the biopharmaceutical production process and solution preparation process is defined when the unit operations for these activities are defined. As described above, the process equipment associated with unit operations of a biopharmaceutical production process are incorporated into a production process time line. Likewise the activities associated with each step of solution preparation is identified in step 1302 and incorporated into total solution preparation time for the solution preparation vessels 1428.

15

20 Step 3310 generates the equipment preparation load table. The equipment preparation load table includes data describing when particular soiled process components from the equipment dimension table are available for preparation. For example, some information comes from the finish times for the tasks in process time line 906 that define when the soiled process components from the biopharmaceutical production process will be available for cleaning. Step 3310 generates the equipment preparation load table by comparing the process time line schedule with the equipment preparation master list.

25

30 Step 3312 generates the equipment preparation load summary table. The equipment preparation load summary table is the sum of all equipment preparation load tables from each of the biopharmaceutical production processes active in the biopharmaceutical facility. For example, a facility may be producing multiple biopharmaceutical products in multiple processes. In such a case, the preparation

equipment handles equipment preparation for multiple biopharmaceutical production processes. Likewise, a facility may have multiple solution preparation suites. In such a case, the preparation equipment handles equipment preparation for multiple solution prep suites. Step 3312 generates the equipment preparation load summary table for the sum of all biopharmaceutical production processes by combining the equipment preparation load tables for all of the biopharmaceutical production processes.

Step 3314 estimates the preparation equipment capacity. The capacity of the preparation equipment is determined in order to provide sufficient capacity to handle the load of soiled process components in the biopharmaceutical facility. Preparation capacity is the flow rate of soiled process components that the preparation equipment can accommodate. Preparation capacity is estimated based on the flow rate of equipment from the preparation load summary table. The rate at which soiled process components are generated in the biopharmaceutical production facility is a good estimate of the capacity of the preparation equipment.

Step 3316 determines the equipment preparation time line. The equipment preparation time line includes scheduling each soiled process component through each piece of preparation equipment in each of the equipment preparation procedures. Functional specifications for the preparation equipment and the utility load requirements for the preparation equipment can be generated from the equipment preparation time line. Functional specifications describe a piece of equipment with particularity. For example, functional specifications for a pump include pump type, flow rate, maximum and minimum input and output pressures, input and output fitting sizes, electrical requirement, temperature range and type and frequency of required maintenance.

FIG. 34 further illustrates step 3302, generating the preparation equipment protocol table. Step 3302 begins with step 3404, generating the preparation equipment protocol identifiers 3408. Preparation equipment protocol identifiers 3408 are keys or codes which identify each preparation equipment protocol. Preparation equipment protocol identifiers 3408 allow each preparation equipment

protocol to be identified in the equipment preparation module and are used to generate the preparation equipment protocol table. Step 3404 assigns unique preparation equipment identifiers 3408 to each of the preparation equipment protocols 3402. Preparation equipment protocol table 3402 also includes the task and duration information associated with each preparation equipment protocol.

5 Next, step 3406 generates preparation equipment protocol table 3410. Preparation equipment protocol table 3410 is generated by assigning preparation equipment protocol identifiers 3408 to each preparation equipment protocol in preparation equipment protocol table 3402.

10 FIGS. 36A-36H are exemplary preparation equipment protocol tables 3410. Column 3408 in FIGS. 36A-36H illustrate exemplary preparation equipment protocol identifiers 3408. Preparation equipment protocol table 3410 contains information describing each preparation protocol. Preparation equipment protocol identifiers BS-1 through BS-5 identify individual bench sink preparation protocols. For example, FIG. 36A illustrates protocol task durations for the bench sink preparation equipment. Protocol task duration is the amount of time associated with a task in a preparation equipment protocol. For example, protocol BS-1 in FIG. 36A has a loading task duration of 5 minutes. Bench sink protocol BS-1, therefore, includes the step of loading the bench sink, which requires 5 minutes. Protocol task durations of prewash rinse with non-potable hot water (NPHW), prewash rinse with non-potable cold water (NPCW), detergent wash with reagent, post wash rinse with NPHW and NPCW, final rinse and hold dry are illustrated in FIG. 36A. Columns 3602 and 3604 are examples of protocol parameters. Protocol parameters are data elements that describe particular facets of a preparation equipment protocol. In the example of FIG. 36A, protocol parameters detergent wash reagent and grams of reagent per cubic foot are used to describe the detergent in the bench sink wash process.

15

20

25

30 FIG. 36B illustrates an exemplary preparation equipment protocol table for a wash station. Column 3408 of FIG. 36B illustrates exemplary preparation equipment protocol identifiers 3408 for a wash station. FIG. 36C illustrates an

exemplary preparation equipment protocol table for a glassware washer. Column 3408 in FIG. 36C illustrates exemplary preparation equipment protocol identifiers 3408 for a glassware washer. FIG. 36D illustrates an exemplary preparation equipment protocol table 3410 for a glassware dryer. Column 3408 in FIG. 36D illustrates exemplary preparation equipment protocol identifiers 3408 for a glassware dryer. FIG. 36D illustrates exemplary task durations for tasks associated with the glassware dryer protocols. Some examples of task durations are loading 3618, heat up 3620, drying 3624, cooling 3626 and unloading 3628, as shown by their respective columns. Column 3622 illustrates the drying temperature protocol parameter. FIG. 36E illustrates an exemplary preparation equipment protocol table 3410 for a carboy washer. FIG. 36F illustrates an exemplary preparation equipment protocol table 3410 for a carboy dryer.

FIG. 36G illustrates an exemplary preparation equipment protocol table for a steam sterilizer. Due to the multiple protocol parameters and task durations associated with steam sterilizer preparation equipment protocols, the preparation equipment protocol table of FIG. 36G is two-dimensional. Row 3608 illustrates exemplary preparation equipment protocol identifiers 3408 for the steam sterilizer. The steam sterilizer preparation equipment protocol table 3410 includes multiple protocol tasks 1-33 as illustrated in column 3606. Each of the tasks in the steam sterilizer protocol has associated protocol parameters and protocol durations as illustrated in columns 3608, 3610, 3612, 3614 and 3616. Row 32 in column 3606 of FIG. 36G illustrates exemplary values for the total time in minutes required for each of the different steam sterilizer protocols (protocol identifiers SS-1, SS-2 and SS-3). FIG. 36H illustrates an exemplary preparation equipment protocol table 3410 for a dry heat stabilizer.

FIG. 35 further illustrates step 3304 generating equipment preparation procedure table 3512. Equipment preparation procedure table 3512 includes data associated with each equipment preparation procedure, including the sequence of preparation equipment protocols and their individual durations as well as their cumulative duration over the entire procedure. Step 3304 begins at step 3506,

generating equipment preparation procedure identifiers 3510. Equipment preparation procedure identifiers are tags or codes which identify equipment preparation procedures. FIGS. 37A and 37B illustrate an exemplary equipment preparation procedure table 3512. Row 3702 illustrates exemplary equipment preparation procedure identifiers 3510. EPC-1, EPC-2, EPC-3, EPC-4, EPC-5, EPC-6 and EPC-7 are examples of codes which identify equipment preparation procedures.

Step 3508 generates equipment preparation procedure table 3512. Step 3508 generates equipment preparation procedure table 3512 from preparation equipment protocol tables 3502, equipment preparation procedures 3504 and equipment preparation procedure identifiers 3510. Equipment preparation procedures 3504 provides the list of preparation equipment protocols that identify a particular equipment preparation procedure and equipment assignment. FIG. 37A, for example, shows equipment preparation procedure EPC-1 includes (as shown in column EPC-1) preparation equipment protocols BS-1, BS-3, GD-1, and SS-1 in FIG. 37B. Equipment preparation procedures 3504 also include the equipment assignments for each of the equipment preparation procedures. Equipment assignments define the soiled process components associated with, or prepared by, each equipment preparation procedure. For example, a particular equipment preparation procedure may only be used to clean carboys. Step 3508 compares the preparation equipment protocols in the equipment preparation procedures 3504 with the preparation equipment protocol tables 3502. The protocol durations and protocol parameters provide the information in equipment preparation procedures table 3512. Equipment preparation procedure identifiers 3510 are assigned to each individual equipment preparation procedure in equipment preparation procedure table 3512.

FIGS. 37A and 37B illustrate exemplary equipment preparation procedure tables 3512. Row 3702 illustrates exemplary equipment preparation procedure identifiers EPC-1, EPC-2, EPC-3, EPC-4, EPC-5, EPC-6, and EPC-7. Equipment preparation procedure identifiers 3510 identify equipment preparation procedures

for different categories of equipment. Exemplary equipment preparation procedure identifier EPC-5 includes the preparation equipment protocols of wash station (WS-1), carboy washer (CW-1), carboy dryer (CD-1), and steam sterilization autoclave 1 (SS-2). Associated with each of the preparation equipment protocols are task durations. Column 3704 illustrates task durations for equipment preparation procedure EPC-5. The task durations for each of the preparation equipment protocols are totaled to yield the equipment preparation procedure duration for EPC-5. Cumulative totals for the equipment preparation procedure duration are given in column 3706, rows 8, 15, 24, 31, 38, 45, 52, 66, 75 and 82. The cumulative durations are the sum of all the previous preparation equipment protocol durations in the equipment preparation procedure.

FIG. 38 further illustrates step 3306, generating equipment dimension table 3816. Step 3306 begins at step 3806, generating the master equipment dimension list 3808. Step 3806 uses the list of equipment requiring preparation 3802 and the equipment dimensions list 3804 to generate master equipment list 3806 which defines the dimensions of all process equipment that may cleaned by the equipment preparation procedure. List of equipment requiring preparation 3802 is a complete list of all the equipment used in the biopharmaceutical production process. List of equipment requiring preparation 3802 may be generated from the unit operations that define the process time line 906 or solution preparation schedule. Alternatively, list of equipment requiring preparation 3802 may be provided by the system designer as the equipment used in the biopharmaceutical production process by design. List 3802 identifies those pieces of equipment that will need to be prepared in order to complete the biopharmaceutical production process. Equipment dimensions list 3804 is a master list of equipment dimensions for all of the equipment available for use in the biopharmaceutical production process. Often, equipment dimensions list 3804 will be provided by the vender or manufacturer of the process equipment. List of equipment requiring preparation 3802 is compared to the equipment dimensions list 3804 in order to assign the

equipment dimensions to the equipment used in the biopharmaceutical production process, resulting in master equipment dimension list 3808.

Next, step 3812 generates the equipment dimension table with segregated equipment preparation procedure identifiers. Step 3812 segregates the equipment dimension list into equipment preparation procedures as defined in the equipment preparation procedures and equipment assignment list 3504. The master equipment dimension list 3808 is segregated based on the equipment preparation procedure identifiers 3510 in order to generate equipment dimension table 3816 according to equipment preparation procedure identifiers. The resultant equipment dimension table 3816 includes a list of specific process equipment and their associated equipment preparation procedure identifiers. Each particular equipment preparation procedure (e.g., EPC-1, EPC-2, EPC-3, etc.) is assigned to particular equipment types. Equipment dimension table 3816 also includes the dimensions of equipment to be prepared.

FIG. 39 illustrates an exemplary equipment dimension table 3816. Row 3902 illustrates exemplary equipment preparation procedure identifiers 3510. Rows 3904 identify the dimensions of each particular type of equipment involved in the equipment preparation process. Rows 3904 illustrates exemplary values for the dimensions of soiled process components to be cleaned in the equipment preparation procedure. Row 1 of rows 3904 illustrates exemplary values for the right-to-left dimension (R/L) in inches. Row 2 of rows 3904 illustrates exemplary values for the front-to-back dimension (F/B) in inches. Row 3 of rows 3904 illustrates exemplary values for top-to-bottom dimensions (T/B) in inches. Row 5 of rows 3904 illustrates exemplary values for volume in cubic inches (CI). Row 6 of rows 3904 illustrates exemplary values for volume in cubic feet (CF). CI and CF are computed directly from the rectilinear dimensional values in rows 1-3 of rows 3904.

Column 3906 illustrates exemplary dimensional values for siphon tube equipment in equipment preparation procedure EPC-1. Column 3908 illustrates exemplary dimensional values for instruments including pressure indicators (PI),

optical density probe and pH probe Column 3910 illustrates exemplary dimensional values for fittings including tees, elbows, crosses, reducers, hose barbs and clamps. Column 3912 illustrates exemplary dimensional values for small and medium plasticware Column 3914 illustrates exemplary dimensional values for silicone and butyl rubber stoppers. Column 3916 illustrates exemplary dimensional values for small and large flexible tubing. Column 3918 illustrates exemplary dimensional values for small and medium glassware. Column 3920 illustrates exemplary dimensional values for one, twenty and forty-five liter polypropylene carboys. Column 3922 illustrates exemplary dimensional values for ten, twenty and forty-five liter borosilicate glass carboys.

FIG. 40 further illustrates step 3308, generating equipment preparation master list 4004. Equipment preparation master list 4004 includes the process equipment that may be soiled by unit operation tasks and the solution preparation procedure tasks in the biopharmaceutical production process As described above, each task in unit operation master list 508 has associated process equipment The process equipment associated with each unit operation task is added to the equipment preparation master list 4004 in step 4002. Step 4002 uses unit operation master list 508 to generate a master list of equipment that may require preparation after use in the biopharmaceutical production process. Each piece of equipment has an associated dimension as defined in equipment dimension table 3816. Step 4002 compares unit operation master list 508 with equipment dimension table 3816 to assign the equipment dimensions to the equipment in unit operation master list 508 when generating equipment preparation master list 4004. Step 4002 compares solution preparation task list 4006 with equipment dimension table 3816 to assign the equipment dimensions to the solution preparation task list 4006 when generating equipment preparation master list 4004. After step 4002, equipment preparation master list 4004 contains the list of process equipment used in the biopharmaceutical production process that may become soiled process components requiring cleaning by the equipment preparation procedures.

FIG. 41 further illustrates step 3310, generating equipment preparation load table 4104. Equipment preparation load table 4104 includes data indicating when soiled process components from the equipment preparation master list 4004 will be available from the biopharmaceutical production process. Step 4102 generates equipment preparation load table 4104 by combining solution preparation schedule 3210 and process time line 906 with equipment preparation master list 4004. Cumulative flow of equipment out of the biopharmaceutical production process as represented by solution preparation schedule 3210 and process time line 906 is compared with equipment preparation master list 4004 in order to provide the equipment dimensional information in equipment preparation load table 4104. Equipment preparation load table 4104 includes soiled process components, the schedule for when the soiled process components are available for equipment preparation procedures, the dimensional information associated with each soiled process component and which task in the biopharmaceutical production process or solution preparation process generated the soiled process components. Equipment preparation load table 4104 represents the volumetric flow rate of equipment out of the biopharmaceutical production process that needs to be prepared for later use in order to sustain continuous biopharmaceutical production.

FIGS. 42A-42E illustrate an exemplary equipment preparation load table 4104. Column 4202 illustrates exemplary task titles. Task titles 4202 may originate from solution preparation procedure tasks or the titles of tasks in unit operations. Column 4204 illustrates exemplary task end times. The values in columns 4204 represent the date and time various soiled process components will be available for cleaning and preparation in equipment preparation procedures. Columns 4206-4216 of FIGS. 42A and 42B illustrate exemplary values for soiled process components available for preparation in equipment preparation procedures. In each of the columns, each of the soiled process components contains the number and cubic footage with which it is associated. FIGS. 42C-42D illustrate additional tasks in the biopharmaceutical production process.

As before, columns 4218-4228 of FIGS. 42C-42D illustrate exemplary values for soiled process components available for preparation in equipment preparation procedures.

FIG. 43 further illustrates step 3312, generating equipment preparation load summary table 4304. Equipment preparation load table 4104 defines when soiled process components from the equipment preparation master list 4004 will be available from all biopharmaceutical production processes active in the biopharmaceutical facility. Because single equipment preparation facilities may be shared across multiple biopharmaceutical production processes, the equipment load tables 4104 are combined to create equipment preparation load summary table 4304. Equipment preparation load summary table 4304 allows the scheduling and simulation of equipment preparation procedures for the entire biopharmaceutical production facility

FIG 44 further illustrates step 3314, determining the capacities of the preparation equipment 4416. Step 3314 begins with step 4404, generating an initial equipment preparation schedule 4408 An initial equipment preparation schedule 4408 is generated for each equipment preparation procedure (EPC-1, EPC-2, EPC-3, etc.). As stated above, each equipment preparation procedure is associated with specific soiled process components. The initial equipment preparation schedule 4408 begins prior to the earliest date that soiled process components are available, as provided by the equipment preparation load summary table 4304

The initial equipment preparation schedule 4408 is an initial schedule for the arrival of soiled process components at each piece of preparation equipment. Since the duration of each task in each of the equipment preparation procedures is known, the time at which soiled process components arrive at various preparation equipment is calculated directly by adding the duration of each task from the preparation equipment protocol table 3410 to the equipment preparation load summary table 4304. The time at which each soiled process component arrives at a particular step in a preparation equipment protocol is the sum of

5 previous equipment preparation procedure tasks and the time which the soiled process component became available, as indicated in the equipment preparation load summary table 4304. Scheduling the soiled process components that arrive at each piece of preparation equipment allows the peak loading on the preparation equipment to be determined. The peak loading of the preparation equipment can then be used to determine the size and capacity of the preparation equipment.

10 Step 4412 compares the peak cubic footage load, as determined in step 4410, with the cubic footage of the largest soiled process component from the equipment dimension table 3816. Step 4412 selects the larger of the peak cubic foot load and the cubic footage of the largest equipment item from the equipment dimension table.

15 Step 4414 uses the larger peak CF value as determined in step 4412 to generate the capacities for the preparation equipment 4416. Capacities for the preparation equipment 4416 will need to be high enough to handle the peak cubic footage of soiled process components that need to be prepared in the equipment preparation procedure. The capacities determined in step 4414 and stored in table 4416, therefore, are the maximum capacities for the preparation equipment. Once the necessary capacity for the preparation equipment has been determined, an equipment prep time line can be generated.

20 FIG 46 further illustrates step 3316, generating the equipment preparation time lines 4610. Equipment preparation time lines 4610 include scheduling information for each soiled process component through each piece of preparation equipment in equipment preparation procedures. Equipment preparation time line 4610 includes the schedule of operation for each piece of preparation equipment. Equipment preparation time lines 4610 also include scheduling information for each particular facet of preparation equipment operation including resource loads for labor, utilities, disposables, reusables, maintenance, calibration, etc. Together with the capacity data determined in step 4414, equipment preparation time line 4610 allows the determination of functional specifications for preparation equipment to which cost and other data can be matched.

Step 3316 begins with step 4606, generating the final equipment preparation shift schedules for each piece of preparation equipment. As stated above, after the preparation equipment capacities have been determined in step 3314, the maximum load capacities for the preparation equipment 4602 are known. Capacities for preparation equipment 4416 define the maximum load capacities for preparation equipment 4602. Minimum load capacity for preparation equipment 4604 is a value set by the biopharmaceutical production process designer in order to maximize efficiency or for the validation of equipment preparation procedure. For example, a biopharmaceutical production process designer may determine that sterilizer equipment should not be operated at less than fifty percent of its load capacity. The sterilizer equipment, therefore, would be operated only when sufficient volume of soiled process components have been accumulated. Step 4606 generates the final equipment preparation shift schedules for each piece of equipment based on the maximum load capacities for preparation equipment 4602, the minimum load capacities for preparation equipment 4604, and equipment preparation procedure table 3512. The final equipment preparation shift schedules include the load cycling through the preparation equipment dictated by the minimum load capacities 4604 and the maximum load capacities 4602. Maximum load capacities 4602 and minimum load capacities 4604 define when each particular protocol in the equipment preparation procedure table 3512 is executed. The final equipment preparation shift schedules contain accurate scheduling of the operation of each

Step 4608 generates the equipment preparation time lines 4610. The equipment preparation time lines 4608 differ from the final equipment preparation shift schedules, as determined in step 4606, by providing detailed scheduling of the tasks associated the prep equipment protocols in equipment prep procedure table 3512. Equipment preparation time lines 4610 are generated by comparing equipment preparation procedure table 3512 with the final equipment preparation shift schedules for each piece of preparation equipment. Equipment preparation

time lines 4610 contain the time data for specific tasks and operation of preparation equipment.

FIG. 47 illustrates the process of generating preparation equipment functional specifications 4706. Preparation equipment functional specifications list 4706 contains functional specifications and costs associated with each piece of preparation equipment used in the equipment preparation procedure. Maximum load capacities for preparation equipment 4602 is used with equipment preparation time lines 4610 to provide the necessary specifications for the preparation equipment in the preparation equipment procedure. Step 4704 compares the specifications of maximum load capacities 4602 and equipment preparation time lines 4610 to determine which preparation equipment units from master equipment and cost list 4702 are required for the equipment preparation procedures. Master equipment and cost list 4702 contains the functional specifications of all of the available preparation equipment and their associated costs. Preparation equipment is selected from master equipment and cost list 4702 based on functional specification matching with equipment preparation time lines 4610 and maximum load capacities for the preparation equipment 4602. The result of step 4704 is preparation equipment list with functional specifications and cost 4706, which is a subset of master equipment and cost list 4702. Preparation equipment list with functional specifications and costs 4706 provides a means to more accurately match required preparation equipment with detailed cost and other data such as loads for utilities maintenance, calibration, quality assurance and quality control testing, etc.

FIG. 48 illustrates a process of generating preparation equipment utility time line 4810. The preparation equipment utility time line 4810 provides the utility requirements for the equipment preparation process. The preparation equipment utility time line 4810 includes the utility requirements for each piece of preparation equipment and the associated date and time for the requirements. The preparation equipment utility time line 4810 allows the calculation of utility costs associated with each piece of preparation equipment and allows a

biopharmaceutical facilities designer to determine the necessary utility supply to the preparation equipment. The process of generating preparation equipment utility time line 4810 begins with step 4804, generating the preparation equipment utility table. The preparation equipment utility table includes a list of the preparation equipment functional specifications from preparation equipment list 4706 matched with the utility data for each piece of preparation equipment as given by preparation equipment utility data 4802 Preparation equipment utility data 4802 includes the requirements for each piece preparation equipment during each task in a preparation equipment protocol. Examples of utility data are electrical power requirements, potable and nonpotable hot and cold water requirements, waste water requirements, steam requirements, etc. Step 4804 generates preparation equipment utility table 4806 by matching the data from equipment preparation equipment list 4706 with preparation equipment utility data 4802 on a preparation equipment by preparation equipment basis.

Step 4808 generates preparation equipment utility time line 4810. Step 4808 matches the data in preparation equipment utility table 4806 with equipment preparation time line 4610 to generate preparation equipment utility time line 4810. Preparation equipment utility time line 4810 schedules out the utility requirements for each piece of preparation equipment on a for each task in the preparation equipment protocols. Each of the tasks in equipment preparation time line 4610 is matched to the data in preparation equipment utility table 4806. Based on equipment preparation time line 4610 and the utility requirements for each piece of preparation equipment as described in preparation equipment utility table 4806, the utility requirements for each of preparation equipment is scheduled out in preparation equipment utility time line 4810. The utility time line 4810 when combined with the utility time lines from other manufacturing operations such as biopharmaceutical production, solution preparation, etc. provides peak loading data for the accurate sizing of utilities. The detailed data of the equipment time lines allows for the identification and optimization of utility peak loads and cost through the analysis of well documented operations schedules

4.0 Equipment Maintenance Scheduling Module

Equipment maintenance in a biopharmaceutical production facility is necessary to sustain the biopharmaceutical production process. The types and frequency of maintenance required is a function of the particular equipment used in the facility, as well as the frequency and nature of use. The equipment involved in the production process, solution preparation process, and equipment preparation all require regular maintenance during sustained operation. Often, maintenance frequency and cost are not considered in the design of a biopharmaceutical production facility. Maintenance costs, however, are a significant fraction of the cost of operating the biopharmaceutical facility and producing the biopharmaceutical product. Since maintenance is a significant cost of operating a biopharmaceutical production facility, a system and method for scheduling and modeling the maintenance of process equipment, solution preparation equipment and preparation equipment would allow the biopharmaceutical facility designer to predict and minimize the cost of maintenance. Additionally, scheduling and modeling maintenance of a biopharmaceutical production process would allow for more complete modeling of a biopharmaceutical production facility.

Modeling and scheduling biopharmaceutical production facility maintenance is based on the functional specifications and usage of the biopharmaceutical production process equipment. Each piece of equipment has associated maintenance parameters. For example, a particular pump may require a new drive belt, seals and lubrication after a predetermined number of hours of operation. Filtration media in filters must be changed after a predetermined number of hours of use. Given equipment functional specifications, equipment maintenance requirements and production schedules for biopharmaceutical production process equipment, equipment maintenance can be modeled and scheduled.

FIG. 49 illustrates the process of generating process equipment maintenance table 4906. Process equipment maintenance table 4906 includes maintenance procedures, maintenance duration (i.e., the amount of time required to perform the maintenance), reusables (i.e., those maintenance items that must be replaced periodically), disposables (i.e., those maintenance items that must be replaced after every use), the maintenance period (i.e., the amount of use before the equipment must be serviced), and the number of hours required to complete the maintenance tasks for the equipment.

Step 4904 generates process equipment maintenance tables 4906 from the process equipment list and functional specifications 4908 and process equipment maintenance data 4902. Process equipment list 4908 is generated from unit operation list 508. Unit operation list 508 includes the process equipment associated with each task in a unit operation. The process equipment list 4908, therefore, includes a list of process equipment form unit operation list 508. Process equipment list 4908 also includes functional specifications associated with each piece of process equipment in process equipment list 4908. Functional specifications describe a piece of equipment with particularity. For example, functional specifications for a pump include pump type, flow rate, maximum and minimum input and output pressures, input and output fitting sizes, electrical requirement, temperature range and type and frequency of required maintenance.

Functional specifications associated with each piece of process equipment are determined from the block flow diagram 704, process time line 906 and equipment data sheets. Equipment data sheets, usually vendor or manufacturer provided, are equipment specifications that provide the capacity and functional specifications for equipment available for use in the biopharmaceutical production processes. Each unit operation has associated process equipment. The functional specifications of the equipment, however, are rate- and time-dependent. Block flow diagram 704 defines the volume of solution and biopharmaceutical product handled by each unit operation. The process time line 906 defines the rate at which solutions and biopharmaceutical product are handled in each unit operation

The volume and rate information from the block flow diagram and process time line, therefore, define the operational parameters of the process equipment. The functional specifications of the process equipment are determined directly by matching the volume and rate parameters for the equipment with the volume and rate parameters in equipment data sheets. The functional specifications of the equipment from the equipment data sheet are then added to the process equipment list to form process equipment list with functional specifications 4908.

Step 4904 generates process equipment maintenance table 4906 from process equipment list with functional specifications 4908 and process equipment maintenance data 4902. Process equipment maintenance data 4902 includes functional specifications for each piece of process equipment and their associated maintenance information. Process equipment maintenance data 4902 includes replaceables, reusables, labor, cycle life and the cost of the associated maintenance item. Some examples of replaceables and reusables are: filters, gaskets, bearings, seals, belts, crank-shafts, lubricants and thermal media. Associated with each maintenance item is the number and identifier for the item, the quantity, the cycle life (i.e., the amount of time or use before replacement), and the cost per cycle. Also included in process equipment maintenance data 4902 is the amount of labor associated with each maintenance item and the number of dollars per cycle for the labor

Step 4904 matches process equipment list with functional specifications 4908 with process equipment maintenance data 4902, to generate process equipment maintenance table 4906. Process equipment list with functional specifications 4908 is matched with process equipment maintenance data 4902 based on a comparison of functional specifications in the process equipment list 4908 and the process equipment maintenance data 4902. Step 4904 copies the process equipment maintenance data 4902 for each piece of process equipment in the process equipment list 4908, thereby creating process equipment maintenance table 4906.

FIGS. 64A-64AB illustrate an exemplary process equipment maintenance table 4906. Column 6402 illustrates exemplary unit operations and their associated process equipment, as determined from process equipment list 4908. FIGS. 64A-64E illustrate the process equipment maintenance data for unit operations 1-6, as illustrated in column 6402.

Column 6404 of FIG. 64A illustrates exemplary maintenance data values for the filter maintenance items. Included in column 6404 are item number, quantity, cycle life of the filter materials, unit cost of the filter materials, dollars per cycle of the filter material, the labor of hours required to service the filter media, and the dollars per cycle for the labor. Item number identifies the stock number or part number of the item used in the maintenance procedure. Cycle life of the materials identifies the useful life the maintenance item. Quantity identifies the quantity of the maintenance item used in the maintenance procedure. Unit cost is the per unit cost of the maintenance item. Dollars per cycle is the quotient of the cost of the maintenance items and the cycle life of the maintenance items.

Column 6406 illustrates exemplary maintenance data for gasket maintenance items. Column 6408 of FIGS. 64A and 64B illustrates exemplary maintenance data for bearing maintenance items. Column 6410 of FIG. 64B illustrates exemplary maintenance data for seal maintenance items. Column 6412 of FIGS. 64B and 64D illustrate exemplary maintenance data for belt maintenance items. Column 6416 of FIG. 64C illustrates exemplary maintenance data for crank shaft maintenance items. Column 6418 of FIGS. 64C and 64D illustrates exemplary maintenance data for lubricant maintenance items. Column 6420 of FIG. 64D illustrates exemplary maintenance data for thermal media maintenance items. FIGS. 64E-64AB illustrate the same maintenance items as described in column 6404-6420, as associated with unit operations 7-22.

FIG 50 illustrates the process of generating the process equipment maintenance time line 5004. Process equipment maintenance time line 5004 is a schedule maintenance items or procedures for process equipment in the biopharmaceutical production process. Step 5002 generates process equipment

maintenance time line 5004 by applying the equipment scheduling data from the process equipment time line 906 data to the process equipment maintenance table 4906. Step 5002 calculates the accumulated usage time for each piece of equipment and schedules maintenance on the equipment at the times specified by the process equipment maintenance table 4906. Process equipment maintenance time line 5004 includes process equipment maintenance data from process maintenance data 4906 and the specific time and date when each piece of process equipment should be serviced. Step 5002, therefore, determines the number of unit operations or process cycles required to attain the cycle life rating on the maintenance item in order to trigger the maintenance processes.

FIG. 51 illustrates the process of generating solution preparation equipment maintenance table 5106. Solution preparation equipment maintenance table 5106 includes maintenance procedures, maintenance duration (i.e., the amount of time required to perform the maintenance), reusables (i.e., those maintenance items that must be replaced periodically), disposables (i.e., those maintenance items that must be replaced after every use), the maintenance period (i.e., the amount of use before the equipment must be serviced), and the number of hours required to complete the maintenance tasks for the equipment.

Step 5104 generates solution preparation equipment maintenance table 5106 from the solution preparation equipment list and functional specifications 5108 and solution preparation equipment maintenance data 5102. Solution preparation equipment list 5108 is generated from preparation vessel identifier and associated volume list 1402. Preparation vessel identifier and associated volume list 1402 includes the solution preparation equipment associated with each solution preparation vessel. The solution preparation equipment list 5108, therefore, includes a list of solution preparation equipment from preparation vessel identifier and associated volume list 1402. Solution preparation equipment list 5108 also includes functional specifications associated with each piece of solution preparation equipment in solution preparation equipment list 4809. The functional specifications for each solution preparation vessel and its associated solution

preparation equipment are included in preparation vessel identifier and associated volume list 1402 when it is defined.

Step 5104 generates solution preparation equipment maintenance table 5106 from solution preparation equipment list with functional specifications 5108 and solution preparation equipment maintenance data 5102. Solution preparation equipment maintenance data 5102 includes functional specifications for each piece of solution preparation equipment and their associated maintenance information. Solution preparation equipment maintenance data 5102 includes replaceables, reusables, labor, cycle life and the cost of the associated maintenance item. Some examples of replaceables and reusables are: filters, gaskets, bearings, seals, belts, crank-shafts, lubricants and thermal media. Associated with each maintenance item is the number and identifier for the item, the quantity, the cycle life (i.e., the amount of time or use before replacement), and the cost per cycle. Also included in solution preparation equipment maintenance data 5102 are the amount of labor associated with each maintenance item and the number of dollars per cycle for the labor.

Step 5104 matches solution preparation equipment list with functional specifications 5108 with solution preparation equipment maintenance data 5102, to generate solution preparation equipment maintenance table 5106. Solution preparation equipment list with functional specifications 5108 is matched with solution preparation equipment maintenance data 5102 based on a comparison of functional specifications in the solution preparation equipment list 5108 and the solution preparation equipment maintenance data 5102. Step 5104 copies the solution preparation equipment maintenance data 5102 for each piece of solution preparation equipment in the solution preparation equipment list 5108, thereby creating solution preparation equipment maintenance table 5106.

FIG. 52 illustrates the process of generating the solution preparation equipment maintenance time line 5204. Solution preparation equipment maintenance time line 5204 is a schedule maintenance items or procedures for solution preparation equipment in the biopharmaceutical production process. Step

5202 generates process equipment maintenance time line 5204 by applying the equipment scheduling data from the solution preparation equipment time line 3210 data to the solution preparation equipment maintenance table 5106. Step 5202 calculates the accumulated usage time for each piece of equipment and schedules 5 maintenance on the equipment at the times specified by the solution preparation equipment maintenance table 5106. Solution preparation equipment maintenance time line 5204 includes solution preparation equipment maintenance data from process maintenance data 5106 and the specific time and date when each piece of solution preparation equipment should be serviced. Step 5202, therefore, determines the number of unit operations or process cycles required to attain the cycle life rating on the maintenance item in order to trigger the maintenance processes.

FIG 53 illustrates the process of generating preparation equipment maintenance table 5306. Preparation equipment maintenance table 5306 includes maintenance procedures, maintenance duration (i.e., the amount of time required to perform the maintenance), reusables (i.e., those maintenance items that must be replaced periodically), disposables (i.e., those maintenance items that must be replaced after every use), the maintenance period (i.e., the amount of use before the equipment must be serviced), and the number of hours required to complete 10 the maintenance tasks for the equipment.

Step 5304 generates preparation equipment maintenance table 5306 from preparation equipment list with functional specifications 4706 and preparation equipment maintenance data 5302. Preparation equipment list 4706 also includes functional specifications associated with each piece of preparation equipment as determined in step 3314. Preparation equipment maintenance data 5302 includes functional specifications for each piece of preparation equipment and their associated maintenance information. Preparation equipment maintenance data 20 25 5302 includes replaceables, reusables, labor, cycle life and the cost of the associated maintenance item.

Step 5304 matches preparation equipment list with functional specifications 4706 with preparation equipment maintenance data 5302, to generate preparation equipment maintenance table 5306. Preparation equipment list with functional specifications 4706 is matched with preparation equipment maintenance data 5302 based on a comparison of functional specifications in the preparation equipment list 4706 and the preparation equipment maintenance data 5302. Step 5304 copies the preparation equipment maintenance data 5302 for each piece of preparation equipment in the preparation equipment list 4706, thereby creating preparation equipment maintenance table 5306.

FIG. 54 illustrates the process of generating the preparation equipment maintenance time line 5404. Preparation equipment maintenance time line 5404 is a schedule maintenance items or procedures for preparation equipment in the biopharmaceutical production process. Step 5402 generates process equipment maintenance time line 5404 by applying the equipment scheduling data from the preparation equipment time line 4610 data to the preparation equipment maintenance table 5306. Step 5402 calculates the accumulated usage time for each piece of equipment and schedules maintenance on the equipment at the times specified by the preparation equipment maintenance table 5306. Preparation equipment maintenance time line 5404 includes preparation equipment maintenance data from process maintenance data 5306 and the specific time and date when each piece of preparation equipment should be serviced. Step 5402, therefore, determines the number of unit operations or process cycles required to attain the cycle life rating on the maintenance item in order to trigger the maintenance processes.

5.0 *Equipment Calibration Module*

Equipment calibration in a biopharmaceutical production facility is necessary to sustain the biopharmaceutical production process. Equipment calibration is essential to the accurate measurement and control of all key

manufacturing operations. Instruments such as pressure indicators, temperature indicators, flow meters, load cells etc. are at the core of most manufacturing systems. The reliability of these instruments and the processes they serve is dependent on punctual and consistent calibration programs. The types and frequency of calibration required is a function of the particular equipment used in the facility, as well as the frequency and nature of use. The equipment involved in the production process, solution preparation process and equipment preparation all require regular calibration during sustained operation. Often, calibration frequency and cost are not considered in the design of a biopharmaceutical production facility. Calibration costs and scheduling, however, are a significant fraction of the cost of operating the biopharmaceutical facility and producing the biopharmaceutical product. Since calibration is a significant cost of operating a biopharmaceutical production facility, a system and method for scheduling and modeling the calibration of process equipment, solution preparation equipment and preparation equipment would allow the biopharmaceutical facility designer to predict and minimize the cost of equipment calibration. Additionally, scheduling and modeling equipment calibration of a biopharmaceutical production process would allow for more reliable calibration programs to insure the adequate and consistent performance of all manufacturing systems.

Modeling and scheduling biopharmaceutical production equipment calibration is based on the functional specifications and usage of the biopharmaceutical production process equipment. Each piece of equipment has associated calibration points. These calibration points typically include pressure indicators and transmitters, temperature indicators and transmitters, level sensors, flow meters, etc. All of these calibration points are required for the reliable operation of these process systems. Given equipment functional specifications, equipment calibration requirements and production schedules for biopharmaceutical production process equipment, equipment calibration can be modeled and scheduled.

FIG. 55 illustrates the process of generating process equipment calibration table 5506. Process equipment calibration table 5506 includes calibration procedures, calibration duration (i.e., the amount of time required to perform the calibration), the calibration period (i.e., the amount of use before the equipment must be serviced), and the number of hours required to complete the calibration tasks for the equipment.

Step 5504 generates process equipment calibration table 5506 from process equipment list with functional specifications 4908 and process equipment calibration data 5502. Process equipment calibration data 5502 includes functional specifications for each piece of process equipment and their associated calibration information. Process equipment calibration data 5502 includes replaceables, reusables, labor, cycle life and the cost of the associated calibration item. As mentioned above, some examples of replaceables and reusables are: filters, gaskets, bearings, seals, belts, crank-shafts, lubricants and thermal media. Associated with each calibration item is the number and identifier for the item, the quantity, the cycle life (i.e., the amount of time or use before replacement), and the cost per cycle. Also included in process equipment calibration data 5502 are the amount of labor associated with each calibration item and the number of dollars per cycle for the labor.

Step 5504 matches process equipment list with functional specifications 4908 with process equipment calibration data 5502, to generate process equipment calibration table 5506. Process equipment list with functional specifications 4908 is matched with process equipment calibration data 5502 based on a comparison of functional specifications in the process equipment list 4908 and the process equipment calibration data 5502. Step 5504 copies the process equipment calibration data 5502 for each piece of process equipment in the process equipment list 4908, thereby creating process equipment calibration table 5506.

FIG 56 illustrates the process of generating the process equipment calibration time line 5604. Process equipment calibration time line 5604 is a

schedule calibration items or procedures for process equipment in the biopharmaceutical production process. Step 5602 generates process equipment calibration time line 5604 by applying the equipment scheduling data from the process equipment time line 906 data to the process equipment calibration table 5566. Step 5602 calculates the accumulated usage time for each piece of equipment and schedules calibration on the equipment at the times specified by the process equipment calibration table 5566. Process equipment calibration time line 5604 includes process equipment calibration data from process calibration data 5566 and the specific time and date when each piece of process equipment should be serviced. Step 5602, therefore, determines the number of unit operations or process cycles required to attain the cycle life rating on the calibration item in order to trigger the calibration processes.

FIG. 57 illustrates the process of generating solution preparation equipment calibration table 5706. Solution preparation equipment calibration table 5706 includes calibration procedures, calibration duration (i.e., the amount of time required to perform the calibration), reusables (i.e., those calibration items that must be replaced periodically), disposables (i.e., those calibration items that must be replaced after every use), the calibration period (i.e., the amount of use before the equipment must be serviced), and the number of hours required to complete the calibration tasks for the equipment.

Step 5704 generates solution preparation equipment calibration table 5706 from the solution preparation equipment list and functional specifications 5108 and solution preparation equipment calibration data 5702. Solution preparation equipment list 5108 is generated from preparation vessel identifier and associated volume list 1402. Preparation vessel identifier and associated volume list 1402 includes the solution preparation equipment associated with each solution preparation vessel. The solution preparation equipment list 5108, therefore, includes a list of solution preparation equipment from preparation vessel identifier and associated volume list 1402. Solution preparation equipment list 5108 also includes functional specifications associated with each piece of solution

preparation equipment in solution preparation equipment list 4809. The functional specifications for each solution preparation vessel and its associated solution preparation equipment are included in preparation vessel identifier and associated volume list 1402 when it is defined.

- 5 Step 5704 generates solution preparation equipment calibration table 5706 from solution preparation equipment list with functional specifications 5108 and solution preparation equipment calibration data 5702. Solution preparation equipment calibration data 5702 includes functional specifications for each piece of solution preparation equipment and their associated calibration data.
- 10 Step 5704 matches solution preparation equipment list and functional specifications 5108 with solution preparation equipment calibration data 5702 to generate solution preparation equipment calibration table 5706. Solution preparation equipment list with functional specifications 5108 is matched with solution preparation equipment calibration data 5702 based on a comparison of functional specifications in the solution preparation equipment list 5108 and the solution preparation equipment calibration data 5702. Step 5704 copies the solution preparation equipment calibration data 5702 for each piece of solution preparation equipment in the solution preparation equipment list 5108, thereby creating solution preparation equipment calibration table 5706.
- 15 FIG. 58 illustrates the process of generating the solution preparation equipment calibration time line 5804. Solution preparation equipment calibration time line 5804 is a schedule of calibration items and procedures for solution preparation equipment in the biopharmaceutical production process. Step 5802 generates process equipment calibration time line 5804 by applying the equipment scheduling data from the solution preparation equipment time line 3210 data to the solution preparation equipment calibration table 5706. Step 5802 calculates the accumulated usage time for each piece of equipment and schedules re-calibration on the equipment at the times specified by the solution preparation equipment calibration table 5706. Solution preparation equipment calibration time line 5804 include solution preparation equipment calibration data from process calibration
- 20
- 25
- 30

data 5706 and the specific time and date when each piece of solution preparation equipment should be calibrated. Step 5802, therefore, determines the number of unit operations or process cycles required to attain the cycle life rating on the calibration of the equipment in order to trigger re-calibration of the equipment.

5 FIG. 59 illustrates the process of generating preparation equipment calibration table 5906 Preparation equipment calibration table 5906 include calibration procedures, calibration duration (i.e., the amount of time required to perform the calibration), the calibration period (i.e., the amount of use before the equipment must be serviced), and the number of hours required to complete the calibration tasks for the equipment.

10 Step 5904 generates preparation equipment calibration table 5906 from preparation equipment list with functional specifications 4706 and preparation equipment calibration data 5902. Preparation equipment list 4706 also include functional specifications associated with each piece of preparation equipment as determined in step 3314. Preparation equipment calibration data 5902 include functional specifications for each piece of preparation equipment and their associated calibration data. Preparation equipment calibration data 5902 includes labor, and cycle life of the associated with calibration.

15 Step 5904 matches preparation equipment list and functional specifications 4706 with preparation equipment calibration data 5902, to generate preparation equipment calibration table 5906. Preparation equipment list with functional specifications 4706 is matched with preparation equipment calibration data 5902 based on a comparison of functional specifications in the preparation equipment list 4706 and the preparation equipment calibration data 5902. Step 5904 copies the preparation equipment calibration data 5902 for each piece of preparation equipment in the preparation equipment list 4706, thereby creating preparation equipment calibration table 5906.

20 FIG. 60 illustrates the process of generating the preparation equipment calibration time line 6004. Preparation equipment calibration time line 6004 is a calibration schedule calibration for preparation equipment in the biopharmaceutical

production process. Step 6002 generates process equipment calibration time line 6004 by applying the equipment scheduling data from the preparation equipment time line 4610 data to the preparation equipment calibration table 5906. Step 6002 calculates the accumulated usage time for each piece of equipment and schedules calibration on the equipment at the times specified by the preparation equipment calibration table 5906. Preparation equipment calibration time line 6004 include preparation equipment calibration data from process calibration data 5906 and the specific time and date when each piece of preparation equipment should be calibrated. Step 6002, therefore, determines the number of unit operations or process cycles required to attain the cycle life rating on the calibration item in order to trigger the calibration processes.

6.0 Quality Control Module

Quality control in a biopharmaceutical production facility is necessary to ensure the safety and quality of the biopharmaceutical product. Quality control sampling and testing, at various points in the biopharmaceutical production process ensures contamination-free product during the process, solution preparation and equipment preparation. The type and frequency of quality control sampling and testing required in a biopharmaceutical production process is a function of the particular equipment used in the process, the frequency and nature of the equipment use and the particular step or task in which the equipment is engaged. Often, quality control testing, frequency and cost are not planned prior to the design of a biopharmaceutical production facility. Quality control, sampling and testing, however, play a significant role in scheduling the operation of a biopharmaceutical facility. Modeling and scheduling quality control sampling and testing in a biopharmaceutical production facility is based on the definitions of the basic steps in the biopharmaceutical production process. Quality control testing and sampling steps are specified for the production process, the solution preparation process and equipment preparation protocols.

FIG. 61 illustrates the process for generating a master quality control protocol table 6110. Quality control protocols are assays and testing procedures associated with quality control sampling and testing. Quality control protocols 6102 are defined by the biopharmaceutical facility designer, determined through testing and experimentation or specified by the vendor of the equipment in the biopharmaceutical facility. Quality control protocols 6102 include quality control protocol parameters. Quality control parameters are values that define the quality control assays. Examples of quality control parameters are the category and title of the assay, the setup time for the assay, the time required to draw each sample, the time required to clean up after taking the sample(s) and the disposal material necessary to dispose of the samples after testing.

Step 6104 generates quality control protocol identifiers 6108 for each of quality control protocols 6102. Quality control protocol identifiers 6108 are tags or codes that identify individual quality control protocols 6102. Step 6106 assigns quality control protocol identifiers 6108 to the quality control protocols 6102 resulting in master quality control protocol table 6110. Master quality control protocol table 6110 includes quality control protocols 6102 and a unique quality control identifier 6108 associated with each of quality control protocols 6102.

FIG. 21 illustrates an exemplary master quality control protocol table 6110. Column 2102 illustrates three exemplary categories of quality control protocols including environmental, analytical, and *in vitro* biological quality control protocols. Column 2104 illustrates exemplary quality control protocol identifiers 6108. Column 2106 illustrates exemplary values for quality control protocol parameters. More specifically, column 2106 illustrates quality control protocol parameters for the number of man-hours required to setup, draw each sample and cleanup the sampling operations associated with each quality control protocol. Setup and cleanup parameters define the amount of time necessary to setup prior to and cleanup after quality control protocol sampling. The per sample quality control protocol parameter defines the amount of time required to draw each sample. For example, 10 samples of temperature (quality control protocol

identifier E-1) would require 0.5 man-hours to set up, 1.0 man-hours to sample (0.1 hours/sample × 10 samples) and 0.5 man-hours to clean up.

FIG 62 illustrates the process of generating master quality control sample table 6208. Master quality control sample table 6208 includes all of the tasks and quality control sampling protocols associated with the production of a biopharmaceutical product. Each task or step in the process time line, the solution preparation schedule or the preparation equipment time line that has an associated quality control protocol 6102 is included in master unit operation list 6206. Each task or step in master unit operation list 6206 also includes a quality control protocol. The quality control protocol parameters of master quality control protocol table 6110 is used to generate master quality control sample list in step 6202. The master quality control sample list 6202 lists all the codes of the quality control protocols from the master QC protocol table 6110. Step 6204 uses the master quality control sample list to assign sampling assays to each step in master unit operation list 6206 according to which quality control protocol is assigned to each step in master unit operation list 6206. The result of step 6204 is a master QC sample table 6208 which includes all of the steps in the biopharmaceutical production process, solution preparation and equipment preparation as well as their associated quality control protocol and sample list.

FIG. 63 illustrates the process for generating the process equipment quality control time line 6304. Quality control process equipment time line 6304 is a table of all the unit operations associated with process equipment time line 906 as well as the schedule of quality control assays and samples associated with each. Step 6302 generates the process equipment quality control time line 6304. Step 6302 matches the process steps of process equipment 906 with master unit operation list 6206 to determine which assays need to be assigned to the tasks in process equipment time line 906. Step 6302 assigns the quality control samples to be taken in each of the associated tasks from master quality control sample table 6208 to each of the tasks in process equipment time line 906, resulting in process equipment quality control time line 6304.

FIGS 45A-45I illustrate an exemplary process equipment quality control time line 6304. Fig. 45A illustrates unit operations 1A-6A in column 4502. Scheduling for each of the tasks in unit operations 1A-6A is illustrated in columns 4504. Columns 4506 of FIGS. 45A-45B illustrate the quality control assays from master quality control protocol table 6110. Although columns 4506 are empty, if quality control samples where scheduled for unit operations 1A-6A in column 4502, columns 4506 would contain the number of samples to be taken at the scheduled time, as defined in master quality control sample table 6208. FIGS. 45C-45I illustrate the balance of the tasks and unit operations for the process equipment quality control time line 6304.

FIG. 22 illustrates the process for generating the solution preparation equipment quality control time line 2204. Quality control solution preparation equipment time line 2204 is a table of all the tasks associated with solution preparation schedule 3210, as well as the schedule of quality control assays and samples associated with each task. Step 2202 generates the solution preparation equipment quality control time line 2204. Step 2202 matches the solution preparation tasks of solution preparation schedule 3210 with master unit operation list 6206 to determine which assays need to be assigned to the tasks in solution preparation schedule 3210. Step 2202 assigns the quality control samples to be taken in each of the associated tasks with from master quality control sample table 6208 to each of the tasks in process equipment time line 906, resulting in process equipment quality control time line 2204.

FIG. 23 illustrates the process for generating preparation equipment quality control time line 2304. Quality control preparation equipment time line 2304 is a table of all the tasks associated with preparation equipment time line 4610, as well as the schedule of quality control assays and samples associated with each task in the preparation equipment protocols. Step 2302 generates the preparation equipment quality control time line 2304. Step 2302 matches the equipment preparation tasks of preparation equipment time line 4610 with master unit operation list 6206 to determine which assays need to be assigned to the tasks

in preparation equipment time line 4610. Step 2302 assigns the quality control samples to be taken in each of the associated tasks from master quality control sample table 6208 to each of the tasks in process equipment time line 906, resulting in process equipment quality control time line 2304.

5 **7.0 *Environment***

The present invention may be implemented using hardware, software or a combination thereof and may be implemented in a computer system or other processing system. In fact, in one embodiment, the invention is directed toward a computer system capable of carrying out the functionality described herein. An example computer system 1901 is shown in FIG. 19. The computer system 1901 includes one or more processors, such as processor 1904. The processor 1904 is connected to a communication bus 1902. Various software embodiments are described in terms of this example computer system. After reading this description, it will become apparent to a person skilled in the relevant art how to implement the invention using other computer systems and/or computer architectures

Computer system 1902 also includes a main memory 1906, preferably random access memory (RAM), and can also include a secondary memory 1908. The secondary memory 1908 can include, for example, a hard disk drive 1910 and/or a removable storage drive 1912, representing a floppy disk drive, a magnetic tape drive, an optical disk drive, etc. The removable storage drive 1912 reads from and/or writes to a removable storage unit 1914 in a well known manner. Removable storage unit 1914, represents a floppy disk, magnetic tape, optical disk, etc. which is read by and written to by removable storage drive 1912.

As will be appreciated, the removable storage unit 1914 includes a computer usable storage medium having stored therein computer software and/or data.

In alternative embodiments, secondary memory 1908 may include other similar means for allowing computer programs or other instructions to be loaded

into computer system 1901. Such means can include, for example, a removable storage unit 1922 and an interface 1920. Examples of such can include a program cartridge and cartridge interface (such as that found in video game devices), a removable memory chip (such as an EPROM, or PROM) and associated socket, and other removable storage units 1922 and interfaces 1920 which allow software and data to be transferred from the removable storage unit 1922 to computer system 1901

Computer system 1901 can also include a communications interface 1924. Communications interface 1924 allows software and data to be transferred between computer system 1901 and external devices. Examples of communications interface 1924 can include a modem, a network interface (such as an Ethernet card), a communications port, a PCMCIA slot and card, etc. Software and data transferred via communications interface 1924 are in the form of signals which can be electronic, electromagnetic, optical or other signals capable of being received by communications interface 1924. These signals 1926 are provided to communications interface via a channel 1928. This channel 1928 carries signals 1926 and can be implemented using wire or cable, fiber optics, a phone line, a cellular phone link, an RF link and other communications channels.

In this document, the terms "computer program medium" and "computer usable medium" are used to generally refer to media such as removable storage device 1912, a hard disk installed in hard disk drive 1910, and signals 1926. These computer program products are means for providing software to computer system 1901.

Computer programs (also called computer control logic) are stored in main memory and/or secondary memory 1908. Computer programs can also be received via communications interface 1924. Such computer programs, when executed, enable the computer system 1901 to perform the features of the present invention as discussed herein. In particular, the computer programs, when executed, enable the processor 1904 to perform the features of the present

invention. Accordingly, such computer programs represent controllers of the computer system 1901.

In an embodiment where the invention is implemented using software, the software may be stored in a computer program product and loaded into computer system 1901 using removable storage drive 1912, hard drive 1910 or communications interface 1924. The control logic (software), when executed by the processor 1904, causes the processor 1904 to perform the functions of the invention as described herein.

In another embodiment, the invention is implemented primarily in hardware using, for example, hardware components such as application specific integrated circuits (ASICs). Implementation of the hardware state machine so as to perform the functions described herein will be apparent to persons skilled in the relevant art(s).

In yet another embodiment, the invention is implemented using a combination of both hardware and software.

8.0 Conclusion

While the invention has been particularly shown and described with reference to preferred embodiments thereof, it will be understood by those skilled in the relevant art that various changes in form and details may be made therein without departing from the spirit and scope of the invention.

What Is Claimed Is:

1 1 A method for scheduling and simulating solution preparation, said
2 solution for use in a biopharmaceutical production process, comprising the steps
3 of.

4 (1) identifying at least one solution for preparation and its associated
5 volume;

6 (2) identifying a predetermined start date for preparation of said at
7 least one solution and at least one successive start date for preparation of said at
8 least one solution;

9 (3) assigning said at least one solution to a to a preparation vessel; and

10 (4) determining the duration of the solution preparation procedure
11 based on said step of assigning said at least one solution to a preparation vessel.

1 2 The method of claim 1, wherein step (1) comprises the step of
2 calculating the total volume of said at least one solution needed for one process
3 cycle

1 3. The method of claim 1, wherein the step (2) comprises the step of
2 calculating the latest start date for preparation of said at least one solution
3 necessary for the preparation of said at least one solution to be prepared in time
4 for use in the biopharmaceutical process.

System and Method for Simulation, Modeling and Scheduling of Solution Preparation in Biopharmaceutical Batch Process Manufacturing Facilities

Abstract

5 A method and system for simulating, modeling and scheduling solution preparation in the biopharmaceutical production process is described herein. The system and method includes the steps of identifying a solution for preparation and its associated volume. After the solution for preparation is identified, a predetermined start date and one successive start date for solution preparation for the solution are identified. After the solution, start and successive start dates are identified, the solution is assigned to a preparation vessel. After the solution has been assigned to a preparation vessel, the duration of the solution preparation procedure is determined and assigned to the solution preparation vessel.

10

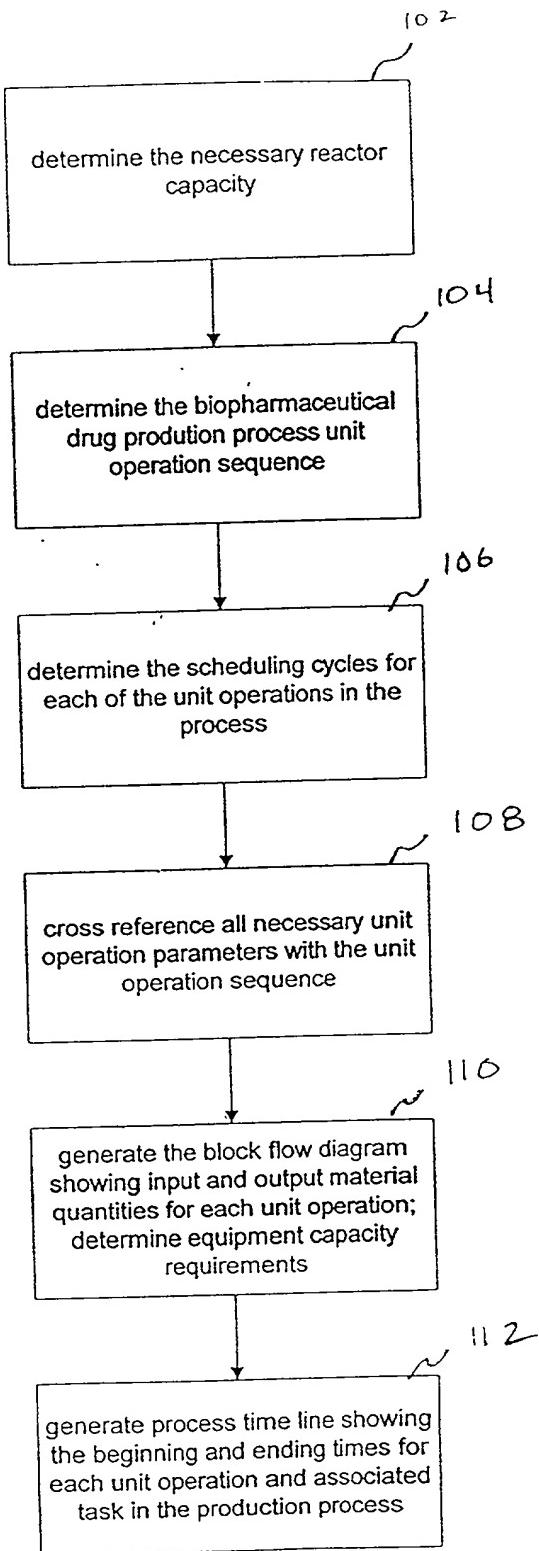


FIG. 7

102

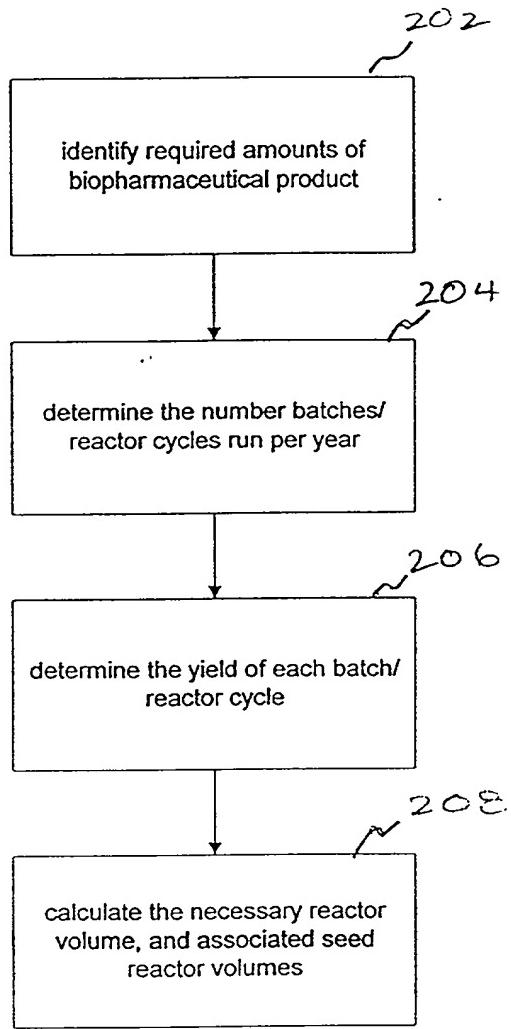


FIG. 2

Unit Operations List

Microbial Fermentation Process

UOP Seq. No.	Code	Unit Operation Type	Cycles per		Batch		Process		Recovery		Total Protein	
			UnOp Offset (Hrs)	Start	UnOp Start	UnOp End	Offset (Hrs)	UnOp Start	UnOp End	Offset (Hrs)	SWR	OAR
1	1	Inoculum Prep	1	3	1	6		1			100%	100%
2	2	Flask Growth	1	3	1	6		1			100%	100%
3	53	Seed Fermentation	1	3	1	6		1			95%	95%
4	3	Production Fermentation	1	3	1	6		1			95%	95%
5	51	Heat Exchange	1	3	1	6		1			100%	95%
6	28	Cont. Centrifugation/Whole Cell Harvest	1	3	1	6		1			100%	95%
7	48	Resuspend Cell Paste	1	1	1	1		1			100%	95%
8	51	Heat Exchange	1	3	8	10		1			80%	78%
9	31	Cell Disruption/ High Pressure	1	3	8	10		1			100%	78%
10	51	Heat Exchange	1	3	8	10		1			100%	100%
11	48	Resuspension/Surfactant	1	2	11	12		1			100%	78%
12	29	Cont. Centrifugation/Precipitate Harvest	1	2	11	12		1			95%	72%
13	48	Resuspension/Buffer	1	1	1	1		1			100%	72%
14	29	Ultrfiltration/Concentration/Dilution	1	1	1	1		1			95%	69%
15	48	Microfiltration/Tangential Flow	1	1	1	1		1			93%	64%
16	36	Product Adsorption MPLC	1	1	1	1		1			85%	54%
17	34	Product Adsorption MPLC	1	1	1	1		1			90%	49%
18	39	Ultrfiltration/Flow Dialysis	1	1	1	1		1			95%	46%
19	39	Product Adsorption MPLC	1	1	1	1		1			85%	39%
20	37	Ultrfiltration/Flow Dialysis	1	1	1	1		1			90%	35%
21	39	Product Adsorption MPLC	1	1	1	1		1			90%	32%
22	37	Microfiltration/Dead End	1	1	1	1		1			95%	30%
23	99	End	1	1	1	1		1			95%	30%
			306		308		312		314		316	
			304		318		320		324		328	
			322		326		328		330		332	

FIG. 3

Unit Operations List

Mammalian Cell Culture Process

UOP Seq. No.	Code	Unit Operation Type	Cycles per			Batch Offset (Hrs)	UnOp Start	UnOp End	Offset (Hrs)	Process Start	Process End	Recovery			
			UnOp	Offset (Hrs)	Batch							Product SWR	OAR	Total Protein SWR	OAR
1	4	Initial Seeding	1	1	1										
2	5	Culture Vessel Split	1	1	1										
3	5	Culture Vessel Split	1	1	1										
4	5	Culture Vessel Split	1	1	1										
5	6	Spinner Flask Split	1	1	1										
6	54	Spinner Flask Split	1	1	1										
7	13	Stirred Tank Reactor	1	1	1										
8	61	Harvest/Feed	7	24	1										
9	62	Harvest Pool	1	1	1										
10	34	MF/Tangential Flow	1	1	1										
11	36	UF/Concentration	1	1	1										
12	39	PAC/MPLC	1	1	1										
13	39	PAC/MPLC	1	1	1										
14	36	UF/Concentration	1	1	1										
15	39	PAC/MPLC	1	1	1										
16	37	UF/Flow Dialysis	1	1	1										
17	39	PAC/MPLC	1	1	1										
18	35	MF/Dead End	1	1	1										
19	99	End	1	1	1										

402 404 408 410 412 414 416 418 420 422 424

FIG. 4

112
=

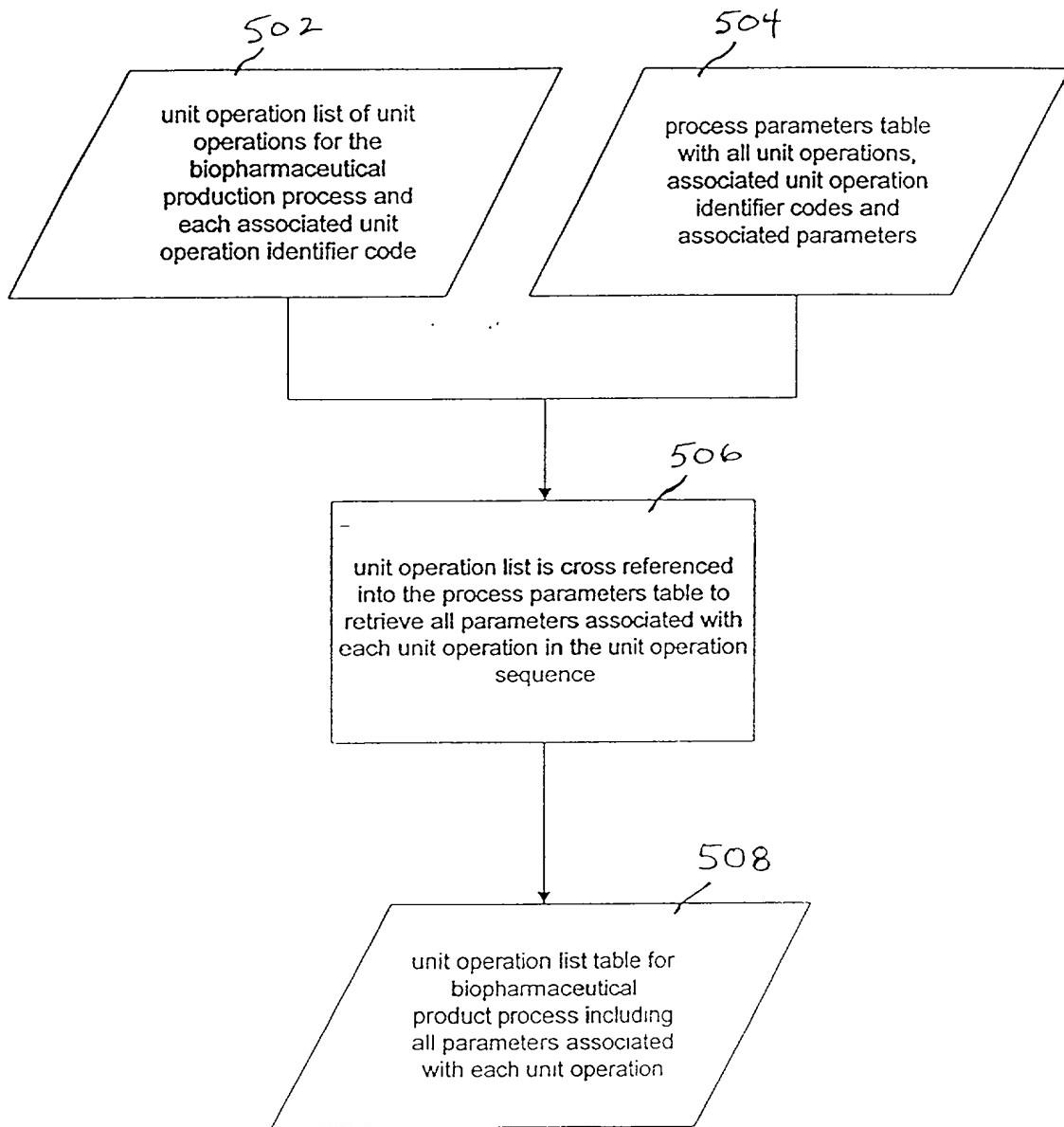


FIG. 5

504

Unit operation id code	Unit operation type	Parameters	solution type	tasks	task duration
1	inoculum prep	# of flasks, volume of flasks, temperature, agitation, duration, final OD	S-101	setup, preincubation, incubation, clean up	3, 3, 23, .3 Hrs
2	flask growth	scale up ratio, media volume, temperature, agitation, duration, final OD	S-101	setup, preincubation, incubation, clean up	1, 1, 23, .3 Hrs
3	fermentation seed	scale up ratio, fermentor working volume, antifoam, base acid, grow temperature, agitation, sparge rate, back pressure, total duration	S-101, 102, 103, 104, 105	setup, preincubation, fermentation, harvest, CIP, SIP, clean up	1, 1, 21, .5, 1, 1, 3 Hrs
4	fermentation production	scale up ratio, fermentor working volume, antifoam A, antifoam B, base, acid, grow temperature, agitation, sparge rate, back pressure, total duration, final OK, dry cell mass, product concentration, CIP, SIP	S-101, 102, 103, 104, 105	setup preincubation, fermentation, CIP, SIP, cleanup	.
5	heat exchange	process initial & final temp; utility initial & final temp; process specific heat; design type, step recovery of product, step recovery of T.P., temperature regulation, CIP, SIP		setup, transfer, CIP, SIP, cleanup	.
6	batch centrifugation	system void volume, RCF, time, volume reduction, wash volume, clean, rinse	S-106	setup, centrifugation, wash, CIP, SIP, cleanup	.
7	resolubilization resuspension	reagent/product ratio, titration solution, resolubilization, agitation, solution name, step recovery of the product, step recovery of T.P., temperature regulation, CIP, SIP	S-107	setup, dilution, agitate, CIP, SIP, clean up	.
8	Cell Disruption High Press, Homogenization	product temperature, utility temperature, void volume, number of passes, pressure, flow rate, temperature increase, wash, rinse, step recovery of product, step recovery of T.P., temperature regulation, CIP	S-107	setup, lysis, CIP, SIP, clean up	.
9	Dilute with Surfactant	reagent/product ratio, titration solution, dilution time, agitation, solution name, step recovery of product, step recovery of T.P., temperature regulation, CIP, SIP	S-108	setup, dilution, agitate, CIP, SIP, clean up	.
10	batch centrifugation precipitate harvest	system void volume, RCF, time, volume reduction, wash volume, clean, rinse, step recovery of product, step recovery of T.P., temperature regulation, CIP, SIP	S-108	setup, centrifugation, wash, CIP, SIP, clean up	.
11	resuspend with chaotrope	reagent/product ratio, titration solution, resolubilization, agitation, solution name, step recovery of product, step recovery to TP, temperature regulation, CIP, SIP	S-109	setup, flush, prime, concentration, dilution, wash, flush, store, CIP, SIP, cleanup	.
.
.
.
.

Fig. 6

108
==

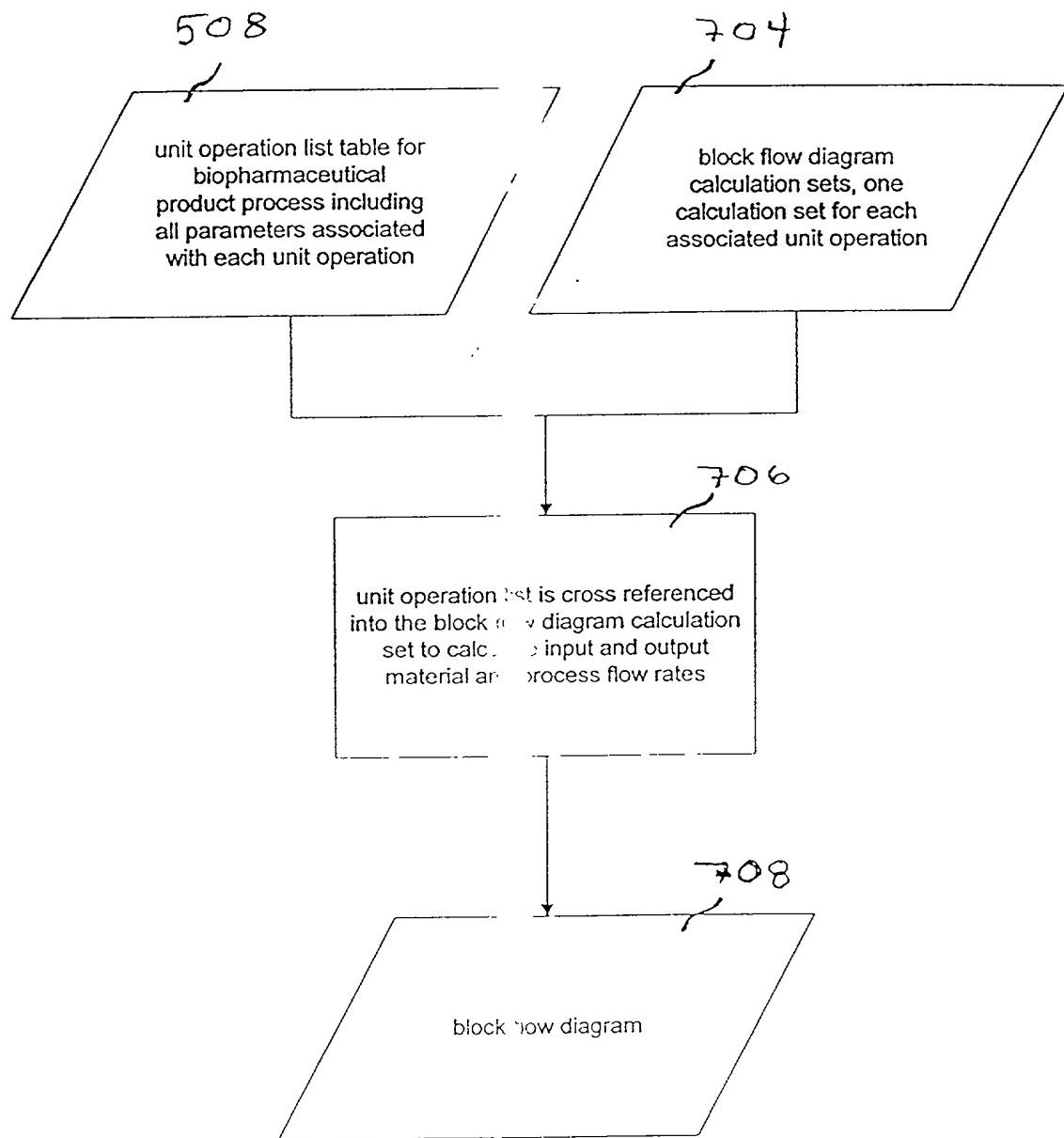
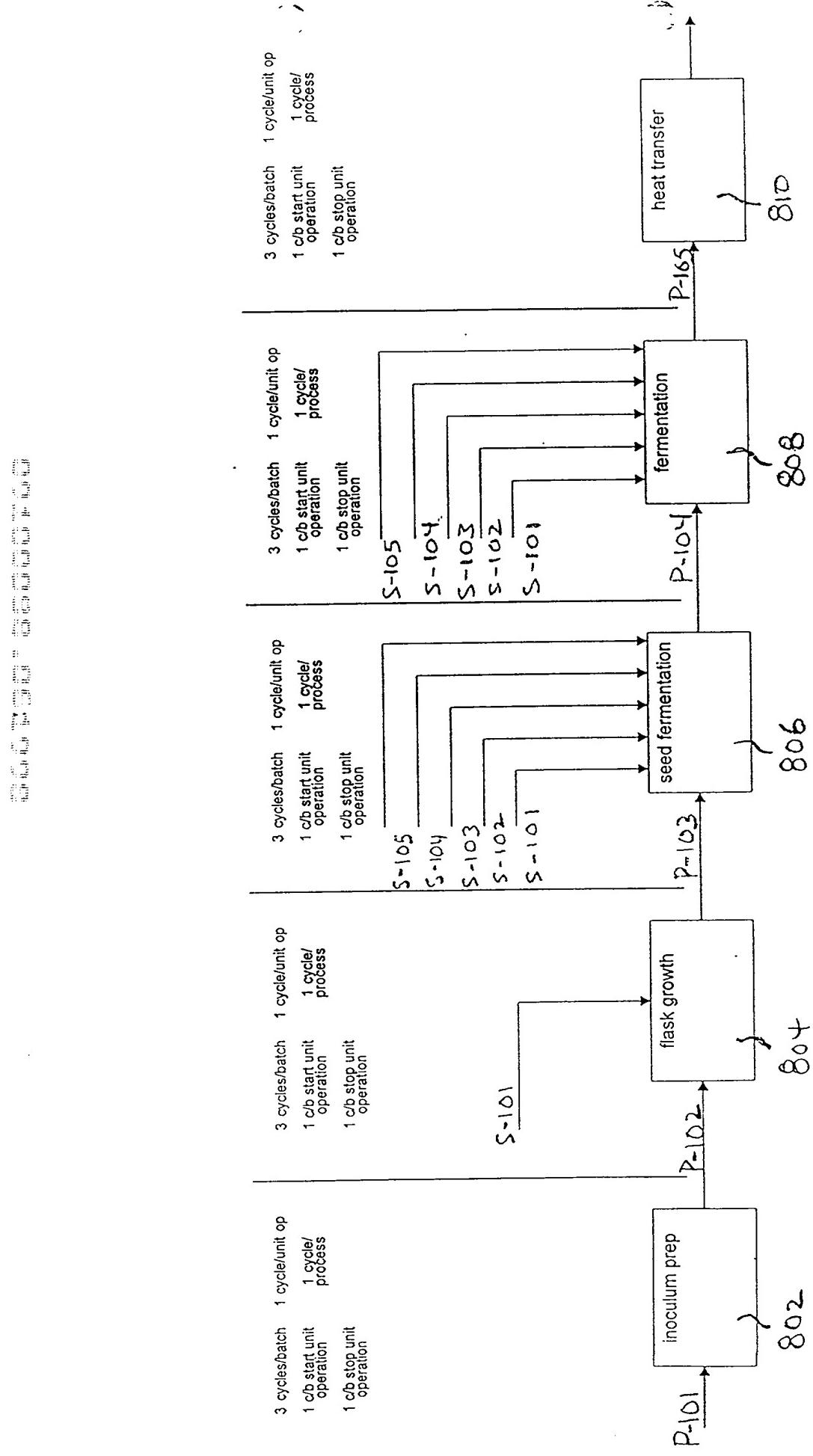


FIG. 7



۸۰

110
11

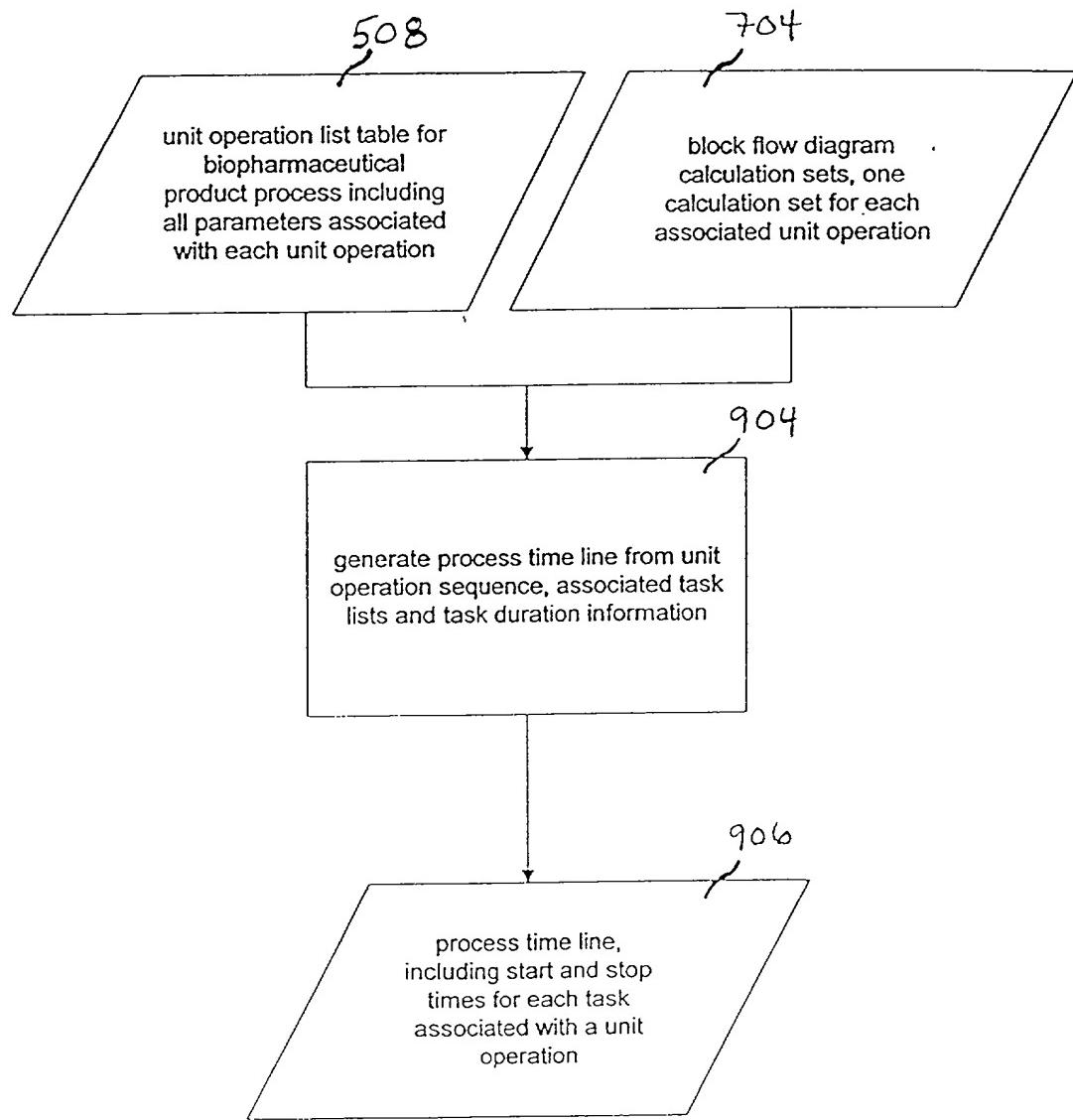


FIG- 9

Sample Application of Process Design Cycles in Process Scheduling

Microbial Fermentation Process (see unit operation list)

Duration	First Process Cycle		Second Process Cycle	
	Week	Day	Week	Day

Note: None of the unit operations in this process have more than 1 cycle per unit operation
 (see unit operation 8 in the mammalian cell culture process for an example of multiple cycles per unit operation)

Unit Operations 1-6 undergo three repetitive cycles per batch as a set before continuing with unit op 7
 This translates to three runs on a fermentor with each harvest (unit op 5 & 6) being stored for pooling at unit op 7
 Associated with each fermentor run (unit op 4) are the previous steps for inoculation prep (unit ops 1-3)

1/3 fermentation cycles per batch

1	Inoculum Prep	24 hrs	1	Fri - Sat	2	Fri - Sat
2	Flask Growth	24 hrs	2	Sat - Sun	3	Sat - Sun
3	Seed Fermentation	24 hrs	2	Sun - Mon	3	Sun - Mon
4	Production Fermentation	24 hrs	2	Mon - Tue	3	Mon - Tue
5	Heat Exchange	1 hr	2	Tue	3	Tue
6	Centrifugation	1hr	2	Tue	3	Tue

2/3 fermentation cycles per batch

1	Inoculum Prep	24 hrs	2	Sun - Mon	3	Sun - Mon
2	Flask Growth	24 hrs	2	Mon - Tue	3	Mon - Tue
3	Seed Fermentation	24 hrs	2	Tue - Wed	3	Tue - Wed
4	Production Fermentation	24 hrs	2	Wed - Thu	3	Wed - Thu
5	Heat Exchange	1 hr	2	Thu	3	Thu
6	Centrifugation	1hr	2	Thu	3	Thu

3/3 fermentation cycles per batch

1	Inoculum Prep	24 hrs	2	Tue - Wed	3	Tue - Wed
2	Flask Growth	24 hrs	2	Wed - Thu	3	Wed - Thu
3	Seed Fermentation	24 hrs	2	Thu - Fri	3	Thu - Fri
4	Production Fermentation	24 hrs	2	Fri - Sat	3	Fri - Sat
5	Heat Exchange	1 hr	2	Sat	3	Sat
6	Centrifugation	1hr	2	Sat	3	Sat

Unit Operation 7 pools the harvests from the three fermentation cycles above

7	Pool Harvests	3 hr	3	Mon	4	Mon
---	---------------	------	---	-----	---	-----

Unit Operations 8-9 undergo three repetitive cycles per batch as set before continuing with unit operation 11
 This translates to three consecutive passes through cell disruptor (unit op 9) with its associated heat exchangers
 (unit op 8 & 10) at the inlet and the outlet of the cell disruptor

1/3 disruption cycles per batch

8	Heat Exchange						
9	Cell Disruption						
10	Heat Exchange	0.5 hr		3	Mon	4	Mon

2/3 disruption cycles per batch

8	Heat Exchange						
9	Cell Disruption						
10	Heat Exchange	0.5 hr		3	Mon	4	Mon

3/3 disruption cycles per batch

8	Heat Exchange						
9	Cell Disruption						
10	Heat Exchange	0.5 hr		3	Mon	4	Mon

FIG. 10

Sample Application of Process Design Cycles in Process Scheduling

Microbial Fermentation Process (see unit operation list)

	First Process Cycle		Second Process Cycle	
	Duration	Week	Day	Week

Unit ops 11-12 undergo two repetitive cycles per batch as a set before continuing with unit op 13
 This translates to two cycles of resuspending the cell lysate from the cell disruptor in a mild surfactant and reconcentrating the insoluble product to a paste by centrifugation

1/2 product washing cycles per batch

11	Resuspension	0.5 hr	3 Mon	4 Mon
12	Centrifugation	1 hr	3 Mon	4 Mon

2/3 product washing cycles per batch

11	Resuspension	0.5 hr	3 Mon	4 Mon
12	Centrifugation	1 hr	3 Mon	4 Mon

Unit ops 13-22 undergo only one cycle per unit operation each to the end of the process

13	Resuspension	0.5 hr	3 Mon	4 Mon
14	Buffer Exchange	2 hr	3 Mon	4 Mon
15	Filtration	2 hr	3 Mon	4 Mon
16	Liquid Chromatography	16 hrs	3 Mon - Tue	4 Mon - Tue
17	Liquid Chromatography	4 hrs	3 Tue	4 Tue
18	Buffer Exchange	2 hrs	3 Tue	4 Tue
19	Liquid Chromatography	2 hrs	3 Wed	4 Wed
20	Buffer Exchange	2 hrs	3 Wed	4 Wed
21	Liquid Chromatography	2 hrs	3 Wed	4 Wed
22	Filtration	2 hrs	3 Wed	4 Wed

FIG. 11

Process Time Line									
Operation		Duration (hrs)		Rel. Time Scale (hrs)		Abs. Date		Start	
Cat.	ID	Adj.	Adj.	Prep.	Excl.	Contibl.	Start	End	Date
1	1 A	Inoculum Prep				16.5			06/03/98 08:00 AM
2	2	Set Up	3.0	0.0	3.0	Hrs	12.5	0.40	05/30/98 09:30 AM
3	3	Preliminary	3.0	0.0	21.0	Hrs	15.5	0.52	05/30/98 12:30 PM
4	4	Incubation	23.0	0.0	0.3	Hrs	28.5	0.65	05/30/98 03:30 PM
5	5	Clean Up	0.3	0.0	0.3	Hrs		1.81	05/04/98 02:30 PM
6	6	Subtotal	26.0		29.0	Hrs	38.8		05/04/98 02:45 PM
7	7	2 A	Flask Growth						
8	8	Set Up	1.0	0.0	1.0	Hrs	37.5	1.52	05/04/98 12:30 PM
9	9	Preliminary	1.0	0.0	1.0	Hrs	38.5	1.60	05/04/98 01:30 PM
10	10	Incubation	23.0	0.0	23.0	Hrs	61.5	1.60	05/04/98 02:30 PM
11	11	Clean Up	0.3	0.0	0.3	Hrs	61.8	2.57	05/05/98 01:30 PM
12	12	Subtotal	23.0		25.0	Hrs	61.5		05/05/98 01:45 PM
13	13	3 A	Seed Fermentation						
14	14	Set Up	1.0	0.0	1.0	Hrs	60.5	2.62	05/05/98 11:30 AM
15	15	Preliminary	1.0	0.0	1.0	Hrs	61.5	2.62	05/05/98 12:30 PM
16	16	Fermentation	21.0	0.0	21.0	Hrs	82.5	2.68	05/05/98 01:30 PM
17	17	Harvest	0.5	0.0	0.5	Hrs	83.0	3.44	05/05/98 02:30 AM
18	18	CIP	1.0	0.0	1.0	Hrs		3.46	05/06/98 10:30 AM
19	19	SIP	1.0	0.0	1.0	Hrs	63.5	3.44	05/06/98 11:30 AM
20	20	Clean Up	3.0	0.0	3.0	Hrs	64.5	3.48	05/06/98 12:30 AM
21	21	Subtotal	26.5		28.5	Hrs	87.5	3.52	05/06/98 12:30 PM
22	22	4 A	Production Fermentation						
23	23	Set Up	1.0	0.0	1.0	Hrs	82.0	3.38	05/06/98 09:00 AM
24	24	Preliminary	1.0	0.0	1.0	Hrs	83.0	3.42	05/06/98 10:00 AM
25	25	Fermentation	21.0	0.0	21.0	Hrs	104.0	3.46	05/06/98 11:00 AM
26	26	CIP	1.0	0.0	1.0	Hrs	105.0	4.33	05/07/98 08:00 AM
27	27	SIP	1.0	0.0	1.0	Hrs	106.0	4.33	05/07/98 09:00 AM
28	28	Clean Up	2.0	0.0	2.0	Hrs	108.0	4.42	05/07/98 10:00 AM
29	29	Subtotal	27.0		27.0	Hrs	104.0	4.50	05/07/98 10:00 AM
30	30	5 A	Heat Exchange						
31	31	Set Up	0.50	0.0	0.5	Hrs	104.5	4.33	05/07/98 08:00 AM
32	32	Transfer	1.00	0.0	1.0	Hrs	105.0	4.33	05/07/98 08:30 AM
33	33	CIP	1.0	0.0	1.0	Hrs	106.0	4.33	05/07/98 09:30 AM
34	34	SIP	1.0	0.0	1.0	Hrs	107.0	4.42	05/07/98 10:00 AM
35	35	Clean Up	2.0	0.0	2.0	Hrs	109.0	4.46	05/07/98 11:00 AM
36	36	Subtotal	5.0		5.0	Hrs	105.0		05/07/98 11:30 AM
37	37	6 A	Cont. Cont/Solids						
38	38	Set Up	1.00	0.0	1.0	Hrs	105.0	4.33	05/07/98 08:00 AM
39	39	Centrifugation	1.00	0.0	1.0	Hrs	108.0	4.33	05/07/98 08:30 AM
40	40	Wash	0.10	0.0	0.1	Hrs	108.1	4.39	05/07/98 09:30 AM
41	41	CIP	0.25	0.0	0.3	Hrs		4.42	05/07/98 10:00 AM
42	42	SIP	1.00	0.0	1.0	Hrs	108.4	4.42	05/07/98 10:08 AM
43	43	Clean Up	0.90	0.0	0.5	Hrs	107.4	4.43	05/07/98 10:21 AM
44	44	Sub Total	3.85		3.85	Hrs	106.1	4.47	05/07/98 11:21 AM
45	45	1 B	Inoculum Prep						
46	46	Set Up	1.0	0.0	1.0	Hrs	14.5	0.58	05/03/98 01:30 PM
47	47	Preliminary	1.0	0.0	1.0	Hrs	15.5	0.60	05/03/98 02:30 PM
48	48	Incubation	23.0	0.0	21.0	Hrs		0.65	05/03/98 03:30 PM
49	49	Clean Up	0.3	0.0	0.3	Hrs			
50	50	Subtotal	23.0		29.0	Hrs			
51	51	5 A	Heat Exchange						
52	52	Set Up	0.50	0.0	0.5	Hrs	104.5	4.33	05/07/98 08:00 AM
53	53	Transfer	1.00	0.0	1.0	Hrs	105.0	4.33	05/07/98 08:30 AM
54	54	CIP	1.0	0.0	1.0	Hrs	106.0	4.33	05/07/98 09:30 AM
55	55	SIP	1.0	0.0	1.0	Hrs	107.0	4.42	05/07/98 10:00 AM
56	56	Clean Up	2.0	0.0	2.0	Hrs	109.0	4.46	05/07/98 11:00 AM
57	57	Subtotal	5.0		5.0	Hrs	105.0		05/07/98 11:30 AM
58	58	6 B	Cont. Cont/Solids						
59	59	Set Up	1.00	0.0	1.0	Hrs	105.0	4.33	05/07/98 08:00 AM
60	60	Centrifugation	1.00	0.0	1.0	Hrs	108.0	4.39	05/07/98 08:30 AM
61	61	Wash	0.10	0.0	0.1	Hrs	108.1	4.42	05/07/98 09:30 AM
62	62	CIP	0.25	0.0	0.3	Hrs		4.42	05/07/98 10:00 AM
63	63	SIP	1.00	0.0	1.0	Hrs	108.4	4.42	05/07/98 10:08 AM
64	64	Clean Up	0.90	0.0	0.5	Hrs	107.4	4.43	05/07/98 10:21 AM
65	65	Sub Total	3.85		3.85	Hrs	106.1	4.47	05/07/98 11:21 AM
66	66	7 A	Inoculum Prep						
67	67	Set Up	1.0	0.0	1.0	Hrs	14.5	0.58	05/03/98 01:30 PM
68	68	Preliminary	1.0	0.0	1.0	Hrs	15.5	0.60	05/03/98 02:30 PM
69	69	Incubation	23.0	0.0	21.0	Hrs		0.65	05/03/98 03:30 PM
70	70	Clean Up	0.3	0.0	0.3	Hrs			
71	71	Subtotal	23.0		29.0	Hrs			
72	72	8 A	Heat Exchange						
73	73	Set Up	0.50	0.0	0.5	Hrs	104.5	4.33	05/07/98 08:00 AM
74	74	Transfer	1.00	0.0	1.0	Hrs	105.0	4.33	05/07/98 08:30 AM
75	75	CIP	1.0	0.0	1.0	Hrs	106.0	4.33	05/07/98 09:30 AM
76	76	SIP	1.0	0.0	1.0	Hrs	107.0	4.42	05/07/98 10:00 AM
77	77	Clean Up	2.0	0.0	2.0	Hrs	109.0	4.46	05/07/98 11:00 AM
78	78	Subtotal	5.0		5.0	Hrs	105.0		05/07/98 11:30 AM
79	79	9 A	Cont. Cont/Solids						
80	80	Set Up	1.00	0.0	1.0	Hrs	105.0	4.33	05/07/98 08:00 AM
81	81	Centrifugation	1.00	0.0	1.0	Hrs	108.0	4.39	05/07/98 08:30 AM
82	82	Wash	0.10	0.0	0.1	Hrs	108.1	4.42	05/07/98 09:30 AM
83	83	CIP	0.25	0.0	0.3	Hrs		4.42	05/07/98 10:00 AM
84	84	SIP	1.00	0.0	1.0	Hrs	108.4	4.42	05/07/98 10:08 AM
85	85	Clean Up	0.90	0.0	0.5	Hrs	107.4	4.43	05/07/98 10:21 AM
86	86	Subtotal	3.85		3.85	Hrs	106.1	4.47	05/07/98 11:21 AM
87	87	10 A	Inoculum Prep						
88	88	Set Up	1.0	0.0	1.0	Hrs	14.5	0.58	05/03/98 01:30 PM
89	89	Preliminary	1.0	0.0	1.0	Hrs	15.5	0.60	05/03/98 02:30 PM
90	90	Incubation	23.0	0.0	21.0	Hrs		0.65	05/03/98 03:30 PM
91	91	Clean Up	0.3	0.0	0.3	Hrs			
92	92	Subtotal	23.0		29.0	Hrs			
93	93	11 A	Heat Exchange						
94	94	Set Up	0.50	0.0	0.5	Hrs	104.5	4.33	05/07/98 08:00 AM
95	95	Transfer	1.00	0.0	1.0	Hrs	105.0	4.33	05/07/98 08:30 AM
96	96	CIP	1.0	0.0	1.0	Hrs	106.0	4.33	05/07/98 09:30 AM
97	97	SIP	1.00	0.0	1.0	Hrs	107.0	4.42	05/07/98 10:00 AM
98	98	Clean Up	2.0	0.0	2.0	Hrs	109.0	4.46	05/07/98 11:00 AM
99	99	Subtotal	5.0		5.0	Hrs	105.0		05/07/98 11:30 AM
100	100	12 A	Cont. Cont/Solids						
101	101	Set Up	1.0	0.0	1.0	Hrs	14.5	0.58	05/03/98 01:30 PM
102	102	Preliminary	1.0	0.0	1.0	Hrs	15.5	0.60	05/03/98 02:30 PM
103	103	Incubation	23.0	0.0	21.0	Hrs		0.65	05/03/98 03:30 PM
104	104	Clean Up	0.3	0.0	0.3	Hrs			
105	105	Subtotal	23.0		29.0	Hrs			
106	106	13 A	Heat Exchange						
107	107	Set Up	0.50	0.0	0.5	Hrs	104.5	4.33	05/07/98 08:00 AM
108	108	Transfer	1.00	0.0	1.0	Hrs	105.0	4.33	05/07/98 08:30 AM
109	109	CIP	1.0	0.0	1.0	Hrs	106.0	4.33	05/07/98 09:30 AM
110	110	SIP	1.00	0.0	1.0	Hrs	107.0	4.42	05/07/98 10:00 AM
111	111	Clean Up	2.0	0.0	2.0	Hrs	109.0	4.46	05/07/98 11:00 AM
112	112	Subtotal	5.0		5.0	Hrs	105.0		05/07/98 11:30 AM
113	113	14 A	Cont. Cont/Solids						
114	114	Set Up	1.0	0.0	1.0	Hrs	14.5	0.58	05/03/98 01:30 PM
115	115	Preliminary	1.0	0.0	1.0	Hrs	15.5	0.60	05/03/98 02:30 PM
116	116	Incubation	23.0	0.0	21.0	Hrs		0.65	05/03/98 03:30 PM
117	117	Clean Up	0.3	0.0	0.3	Hrs			
118	118	Subtotal	23.0		29.0	Hrs			

1

2

3

4

5

6

7

8

9

10

11

12

13

14

15

1

2

3

4

5

6

7

8

9

10

11

12

13

14

15

1

2

3

4

5

6

7

8

9

10

11

12

13

14

15

1

2

3

4

5

6

7

8

9

10

11

12

13

14

15

Process Time Line		Duration (Hrs)		Rel. Time Scale (Hrs)		Abs. Date		Start Date		Finish Date			
Operation	Code	A/D	Adj.	Prep	Exec.	Compl.	Start	End	Time	Date	Time	Date	Calculations
65 Incubation	23.0	0.0	23.0 Hrs	34.5	0.85	1.52	06/03/96	08:00 AM	06/04/96	01:30 PM	06/04/96	02:30 PM	
66 Clean Up	0.3	0.0	0.3 Hrs	38.5	1.55	1.60	06/04/96	01:30 PM	06/04/96	02:30 PM	06/04/96	02:45 PM	
67 Subtotal	25.0		25.0 Hrs	38.5	1.60	2.68	06/04/96	02:30 PM	06/04/96	02:30 PM	06/04/96	02:45 PM	
62 2 B Flask Growth													
63 Set Up	1.0	0.0	1.0 Hrs	37.5									
64 Preincubation	1.0	0.0	1.0 Hrs	38.5									
65 Incubation	23.0	0.0	23.0 Hrs	61.5									
66 Clean Up	0.3	0.0	0.3 Hrs	61.5									
67 Subtotal	25.0		25.0 Hrs	61.5									
68 3 B Seed Fermentation													
70 Set Up	1.0	0.0	1.0 Hrs	60.5									
71 Preincubation	1.0	0.0	1.0 Hrs	61.5									
72 Incubation	21.0	0.0	21.0 Hrs	82.5									
73 Fermentation	0.5	0.0	0.5 Hrs	83.0									
74 Harvest	1.0	0.0	1.0 Hrs	83.5									
75 CIP	1.0	0.0	1.0 Hrs	84.5									
76 SIP	1.0	0.0	1.0 Hrs	85.5									
77 Clean Up	2.0	0.0	2.0 Hrs	87.5									
78 Subtotal	28.5		28.5 Hrs	83.0									
79 4 B Production Fermentation													
80 Set Up	1.0	0.0	1.0 Hrs	82.0									
81 Preincubation	1.0	0.0	1.0 Hrs	83.0									
82 Incubation	21.0	0.0	21.0 Hrs	104.0									
83 Fermentation	1.0	0.0	1.0 Hrs	105.0									
84 CIP	1.0	0.0	1.0 Hrs	108.0									
85 SIP	1.0	0.0	1.0 Hrs	109.0									
86 Clean Up	2.0	0.0	2.0 Hrs	108.0									
87 Subtotal	27.0		27.0 Hrs	104.0									
88 5 B Heat Exchange													
89 Set Up	0.50	0.0	0.5 Hrs	104.5									
90 Transfer	1.0	0.0	1.0 Hrs	105.0									
91 CIP	1.0	0.0	1.0 Hrs	106.0									
92 SIP	1.0	0.0	1.0 Hrs	107.0									
93 Clean Up	2.0	0.0	2.0 Hrs	109.0									
94 Subtotal	5.0		5.0 Hrs	105.0									
95 6 B Cont. Cont/Solids													
96 Set Up	1.00	0.0	1.0 Hrs	105.0									
97 Centrifugation	1.00	0.0	1.0 Hrs	106.0									
98 Wash	0.10	0.0	0.1 Hrs	106.1									
99 CIP	0.25	0.0	0.3 Hrs	106.4									
100 SIP	1.00	0.0	1.0 Hrs	107.4									
101 Clean Up	0.50	0.0	0.5 Hrs	107.9									
102 Sub Total	3.85		3.85 Hrs	106.1									
103 1 C Inoculum Prop													
104 Set Up	1.0	0.0	1.0 Hrs	14.5									
105 Preincubation	1.0	0.0	1.0 Hrs	15.5									
106 Incubation	23.0	0.0	23.0 Hrs	36.5									
107 Clean Up	0.3	0.0	0.3 Hrs	36.6									
108 Subtotal	25.0		25.0 Hrs	36.5									
109 2 B													
110 Set Up	1.0	0.0	1.0 Hrs	1.50									
111 Transfer	1.0	0.0	1.0 Hrs	1.61									
112 CIP	2.0	0.0	2.0 Hrs	2.68									
113 SIP	0.3	0.0	0.3 Hrs	2.69									
114 Clean Up	0.3	0.0	0.3 Hrs	2.70									
115 Subtotal	25.0		25.0 Hrs	2.70									

Fig. 12 B

FIG. 12C

Process Time Line		Duration (Hrs.)		Rel. Time Scale (Hrs.)		Abs. Days		Start Date		Finish Time		Calculations	
	Operation	Calc.	Adj.	Prep	Exe.	Compl.	Start	End	Date	Initial	Final	Initial	Final
175	Set Up	0.90	0.0	0.5 Hrs	107.6		4.46	4.46	06/03/96 08:00 AM	06/07/96 11:06 AM	11:36 AM	06/07/96 11:36 AM	06/07/96 11:36 AM
176	Transfer	0.30	0.0	0.3 Hrs		107.9	4.48	4.50	06/07/96 11:36 AM	06/07/96 11:54 AM	11:54 AM	06/07/96 11:54 AM	06/07/96 11:54 AM
177	CIP	0.0	0.0	0.0 Hrs		107.9	4.50	4.50	06/07/96 11:54 AM	06/07/96 11:54 AM	11:54 AM	06/07/96 11:54 AM	06/07/96 11:54 AM
178	SIP	0.0	0.0	0.0 Hrs		107.9	4.50	4.50	06/07/96 11:54 AM	06/07/96 11:54 AM	11:54 AM	06/07/96 11:54 AM	06/07/96 11:54 AM
179	Clean Up	0.0	0.0	0.0 Hrs		107.9	4.50	4.50	06/07/96 11:54 AM	06/07/96 11:54 AM	11:54 AM	06/07/96 11:54 AM	06/07/96 11:54 AM
180	SubTotal	0.48	0.0	0.0 Hrs		107.9							
181													
182	9 A Homogenization												
183													
184	Set Up	0.25	0.0	0.3 Hrs	107.9		4.49	4.50	06/07/96 11:59 AM	06/07/96 12:04 PM	12:04 PM	06/07/96 12:04 PM	06/07/96 12:04 PM
185	Lysis	0.68	0.0	0.7 Hrs	108.6		4.50	4.52	06/07/96 11:54 AM	06/07/96 12:24 PM	12:24 PM	06/07/96 12:24 PM	06/07/96 12:24 PM
186	CIP	0.0	0.0	0.0 Hrs		108.6	4.52	4.52	06/07/96 12:24 PM	06/07/96 12:34 PM	12:34 PM	06/07/96 12:34 PM	06/07/96 12:34 PM
187	SIP	0.0	0.0	0.0 Hrs		108.6	4.52	4.52	06/07/96 12:34 PM	06/07/96 12:44 PM	12:44 PM	06/07/96 12:44 PM	06/07/96 12:44 PM
188	Clean Up	0.0	0.0	0.0 Hrs		108.6	4.52	4.52	06/07/96 12:44 PM	06/07/96 12:54 PM	12:54 PM	06/07/96 12:54 PM	06/07/96 12:54 PM
189	Sub Total	0.9	0.0	0.9 Hrs		108.6							
190													
191	10 A Heat Exchange												
192													
193	Set Up	0.50	0.0	0.5 Hrs	108.6		4.50	4.52	06/07/96 12:34 PM	06/07/96 12:44 PM	12:44 PM	06/07/96 12:44 PM	06/07/96 12:44 PM
194	Transfer	0.30	0.0	0.3 Hrs		108.9	4.52	4.54	06/07/96 12:44 PM	06/07/96 12:54 PM	12:54 PM	06/07/96 12:54 PM	06/07/96 12:54 PM
195	CIP	0.0	0.0	0.0 Hrs		108.9	4.54	4.54	06/07/96 12:54 PM	06/07/96 12:52 PM	12:52 PM	06/07/96 12:52 PM	06/07/96 12:52 PM
196	SIP	0.0	0.0	0.0 Hrs		108.9	4.54	4.54	06/07/96 12:52 PM	06/07/96 12:52 PM	12:52 PM	06/07/96 12:52 PM	06/07/96 12:52 PM
197	Clean Up	0.0	0.0	0.0 Hrs		108.9	4.54	4.54	06/07/96 12:52 PM	06/07/96 12:52 PM	12:52 PM	06/07/96 12:52 PM	06/07/96 12:52 PM
198	SubTotal	0.3	0.0	0.3 Hrs		108.9							
199													
200	6 B Heat Exchange												
201													
202	Set Up	0.00	0.0	0.0 Hrs	108.9		4.54	4.54	06/07/96 12:52 PM	06/07/96 12:52 PM	12:52 PM	06/07/96 12:52 PM	06/07/96 12:52 PM
203	Transfer	0.30	0.0	0.3 Hrs		109.2	4.55	4.55	06/07/96 12:52 PM	06/07/96 12:52 PM	12:52 PM	06/07/96 12:52 PM	06/07/96 12:52 PM
204	CIP	0.0	0.0	0.0 Hrs		109.2	4.55	4.55	06/07/96 12:52 PM	06/07/96 12:52 PM	12:52 PM	06/07/96 12:52 PM	06/07/96 12:52 PM
205	SIP	0.0	0.0	0.0 Hrs		109.2	4.55	4.55	06/07/96 12:52 PM	06/07/96 12:52 PM	12:52 PM	06/07/96 12:52 PM	06/07/96 12:52 PM
206	Clean Up	0.0	0.0	0.0 Hrs		109.2	4.55	4.55	06/07/96 12:52 PM	06/07/96 12:52 PM	12:52 PM	06/07/96 12:52 PM	06/07/96 12:52 PM
207	SubTotal	0.3	0.0	0.3 Hrs		109.2							
208													
209	9 B Homogenization												
210													
211	Set Up	0.00	0.0	0.0 Hrs	109.2		4.55	4.55	06/07/96 12:52 PM	06/07/96 12:52 PM	12:52 PM	06/07/96 12:52 PM	06/07/96 12:52 PM
212	Lysis	0.60	0.0	0.7 Hrs		109.9	4.55	4.55	06/07/96 12:52 PM	06/07/96 12:52 PM	12:52 PM	06/07/96 12:52 PM	06/07/96 12:52 PM
213	CIP	0.0	0.0	0.0 Hrs		109.9	4.55	4.55	06/07/96 12:52 PM	06/07/96 12:52 PM	12:52 PM	06/07/96 12:52 PM	06/07/96 12:52 PM
214	SIP	0.0	0.0	0.0 Hrs		109.9	4.55	4.55	06/07/96 12:52 PM	06/07/96 12:52 PM	12:52 PM	06/07/96 12:52 PM	06/07/96 12:52 PM
215	Clean Up	0.0	0.0	0.0 Hrs		109.9	4.55	4.55	06/07/96 12:52 PM	06/07/96 12:52 PM	12:52 PM	06/07/96 12:52 PM	06/07/96 12:52 PM
216	SubTotal	0.7	0.0	0.7 Hrs		109.9							
217													
218	10 B Heat Exchange												
219													
220	Set Up	0.50	0.0	0.5 Hrs	109.9		4.56	4.56	06/07/96 12:52 PM	06/07/96 12:52 PM	12:52 PM	06/07/96 12:52 PM	06/07/96 12:52 PM
221	Transfer	0.30	0.0	0.3 Hrs		110.2	4.56	4.56	06/07/96 12:52 PM	06/07/96 12:52 PM	12:52 PM	06/07/96 12:52 PM	06/07/96 12:52 PM
222	CIP	0.0	0.0	0.0 Hrs		110.2	4.56	4.56	06/07/96 12:52 PM	06/07/96 12:52 PM	12:52 PM	06/07/96 12:52 PM	06/07/96 12:52 PM
223	SIP	0.0	0.0	0.0 Hrs		110.2	4.56	4.56	06/07/96 12:52 PM	06/07/96 12:52 PM	12:52 PM	06/07/96 12:52 PM	06/07/96 12:52 PM
224	Clean Up	0.0	0.0	0.0 Hrs		110.2	4.56	4.56	06/07/96 12:52 PM	06/07/96 12:52 PM	12:52 PM	06/07/96 12:52 PM	06/07/96 12:52 PM
225	SubTotal	0.3	0.0	0.3 Hrs		110.2							
226													
227	4 C Heat Exchange												
228													
229	Set Up	0.00	0.0	0.0 Hrs	110.2		4.59	4.59	06/07/96 12:52 PM	06/07/96 12:52 PM	12:52 PM	06/07/96 12:52 PM	06/07/96 12:52 PM
230	Transfer	0.30	0.0	0.3 Hrs		110.5	4.59	4.60	06/07/96 12:52 PM	06/07/96 12:52 PM	12:52 PM	06/07/96 12:52 PM	06/07/96 12:52 PM
231	CIP	1.0	0.0	1.0 Hrs		111.5	4.60	4.64	06/07/96 12:52 PM	06/07/96 12:52 PM	12:52 PM	06/07/96 12:52 PM	06/07/96 12:52 PM
232	SIP	1.0	0.0	1.0 Hrs		112.5	4.64	4.69	06/07/96 12:52 PM	06/07/96 12:52 PM	12:52 PM	06/07/96 12:52 PM	06/07/96 12:52 PM
233	Clean Up	1.0	0.0	1.0 Hrs		113.5	4.69	4.73	06/07/96 12:52 PM	06/07/96 12:52 PM	12:52 PM	06/07/96 12:52 PM	06/07/96 12:52 PM
234	SubTotal	3.3	0.0	3.3 Hrs		110.5							

FIG : 12 D

Process Timeline		Duration (Hrs.)		Rel. Time Scale (Hrs.)		Abs. Date		Start		Finish		Calculations		
Operation	Calc.	Act.	Adj.	Prep.	Exec.	Comp.	Start	End	Time	Date	Time	Date		
236 9 C Homogenization														
237 Set Up	0.00	0.0	0.0 Hrs	110.5			4.60	4.60	08/07/98	02:27 PM	08/07/98	02:27 PM		
238 Lysis	0.68	0.0	0.7 Hrs	111.1			4.60	4.63	08/07/98	02:27 PM	08/07/98	03:07 PM	68.5 L @	1.6 LPM
240 CIP	1.0	0.0	1.0 Hrs	112.1			4.63	4.67	08/07/98	03:07 PM	08/07/98	04:07 PM		0.68 Hrs
241 SIP	1.0	0.0	1.0 Hrs	113.1			4.67	4.71	08/07/98	04:07 PM	08/07/98	05:07 PM		
242 Clean Up	1.0	0.0	1.0 Hrs	114.1			4.71	4.76	08/07/98	05:07 PM	08/07/98	06:07 PM		
243 Sub Total	3.7		3.7 Hrs	111.1										
244														
245 10 C Heat Exchange														
246 Set Up	0.00	0.0	0.0 Hrs	111.1			4.63	4.63	08/07/98	03:07 PM	08/07/98	03:07 PM		
247 Transfer	0.30	0.0	0.3 Hrs	111.4			4.63	4.64	08/07/98	03:07 PM	08/07/98	03:25 PM		
248 CIP	1.0	0.0	1.0 Hrs	112.4			4.64	4.68	08/07/98	03:25 PM	08/07/98	04:25 PM		
249 SIP	1.0	0.0	1.0 Hrs	113.4			4.68	4.73	08/07/98	04:25 PM	08/07/98	05:25 PM		
250 Clean Up	1.0	0.0	1.0 Hrs	114.4			4.73	4.77	08/07/98	05:25 PM	08/07/98	06:25 PM		
251 Sub Total	3.3		3.3 Hrs	111.4										
252														
253														
254 11 A Resolubilization														
255 Set Up	1.0	0.0	1.0 Hrs	108.9			4.49	4.54	08/07/98	11:52 AM	08/07/98	12:52 PM		
256 Dilution	0.5	0.0	0.5 Hrs	109.4			4.54	4.56	08/07/98	12:52 PM	08/07/98	01:52 PM		
258 Agitate	0.5	0.0	0.5 Hrs	109.9			4.56	4.59	08/07/98	01:22 PM	08/07/98	01:52 PM		0.50 Hrs.
259 CIP	0.0	0.0	0.0 Hrs	109.9			4.58	4.58	08/07/98	01:52 PM	08/07/98	01:52 PM		0.50 Hrs.
260 SIP	0.0	0.0	0.0 Hrs	109.9			4.58	4.58	08/07/98	01:52 PM	08/07/98	01:52 PM		
261 Clean Up	0.0	0.0	0.0 Hrs	109.9			4.58	4.58	08/07/98	01:52 PM	08/07/98	01:52 PM		
262 Sub Total	2.0		2.0 Hrs	109.9										
263														
264 12 A Cont. Cont/Solids														
265 Set Up	1.0	0.0	1.0 Hrs	109.9			4.54	4.58	08/07/98	12:52 PM	08/07/98	01:52 PM		
266 Centrifugation	0.5	0.0	0.6 Hrs	110.4			4.58	4.60	08/07/98	01:52 PM	08/07/98	02:22 PM		
267 Wash	0.1	0.0	0.1 Hrs	110.5			4.60	4.60	08/07/98	02:22 PM	08/07/98	02:22 PM		
268 CIP	0.0	0.0	0.0 Hrs	110.5			4.60	4.60	08/07/98	02:22 PM	08/07/98	03:0 L @	0.5 LPM	0.50 Hrs.
269 SIP	0.0	0.0	0.0 Hrs	110.5			4.60	4.60	08/07/98	02:22 PM	08/07/98	03:0 L @	0.5 LPM	0.50 Hrs.
270 Clean Up	0.0	0.0	0.0 Hrs	110.5			4.60	4.60	08/07/98	02:22 PM	08/07/98	03:0 L @	0.5 LPM	0.25 Hrs.
271 Sub Total	1.6		1.6 Hrs	110.5										
272														
273														
274 11 B Resolubilization														
275 Set Up	0.0	0.0	0.0 Hrs	110.5			4.60	4.60	08/07/98	02:26 PM	08/07/98	02:26 PM		
276 Dilution	0.5	0.0	0.5 Hrs	111.0			4.60	4.62	08/07/98	02:26 PM	08/07/98	02:26 PM		
277 Agitate	0.3	0.0	0.3 Hrs	111.2			4.62	4.63	08/07/98	02:26 PM	08/07/98	03:13 PM		
278 CIP	1.0	0.0	1.0 Hrs	112.2			4.63	4.65	08/07/98	03:13 PM	08/07/98	04:13 PM		
279 SIP	1.0	0.0	1.0 Hrs	113.2			4.65	4.72	08/07/98	04:13 PM	08/07/98	05:13 PM		
280 Clean Up	1.0	0.0	1.0 Hrs	114.2			4.72	4.76	08/07/98	05:13 PM	08/07/98	06:13 PM		
281 Sub Total	3.8		3.8 Hrs	111.2										
282														
283														
284 12 B Cont. Cont/Solids														
285 Set Up	1.0	0.0	1.0 Hrs	111.2			4.59	4.63	08/07/98	02:13 PM	08/07/98	03:13 PM		
286 Centrifugation	0.5	0.0	0.5 Hrs	111.7			4.63	4.66	08/07/98	03:13 PM	08/07/98	04:43 PM		
287 Wash	0.1	0.0	0.1 Hrs	111.6			4.66	4.68	08/07/98	04:43 PM	08/07/98	05 L @	0.5 LPM	0.50 Hrs.
288 CIP	0.3	0.0	0.3 Hrs	112.1			4.68	4.68	08/07/98	05:43 PM	08/07/98	06 L @	0.5 LPM	0.10 Hrs.
289 SIP	1.0	0.0	1.0 Hrs	113.1			4.68	4.67	08/07/98	06:43 PM	08/07/98	08 L @	0.5 LPM	0.25 Hrs.
290 Clean Up	0.5	0.0	0.5 Hrs	113.1			4.67	4.71	08/07/98	08:04 PM	08/07/98	09:34 PM		
291 Sub Total	3.4		3.4 Hrs	111.6										
292														
293 13 A Resolubilization														

Fig. 12 E

Process Time Line		Duration (hrs.)		Rel. Time Scale (hrs.)		Actual Dura.		Start		Finish		Calculations		
Operation	Catc.	A/D	Adj.	Prep	Exec.	Compl.	Start	End	Date	Time	Date	Time		
295														
296	Set Up	1.0	0.0	1.0	110.5	4.56	4.60	00:07:08	01:28 PM	06/07/98	02:28 PM			
297	Dilution	0.5	0.0	0.5	111.0	4.60	4.62	00:07:08	02:28 PM	06/07/98	02:28 PM			
298	Agitate	1.0	0.0	1.0	129.0	4.62	5.37	00:07:08	02:28 PM	06/07/98	03:50 AM			
299	CIP	1.0	0.0	1.0	130.0	5.37	5.42	00:08:08	03:58 AM	06/08/98	04:58 AM			
300	SIP	1.0	0.0	1.0	131.0	5.42	5.46	00:08:08	03:58 AM	06/08/98	10:58 AM			
301	Clean Up	1.0	0.0	1.0	132.0	5.46	5.50	00:08:08	10:58 AM	06/08/98	11:58 AM			
302	SubTotal	22.5	22.5	22.5	123.0									
303														
304	14 A Concentration													
305	Set Up	1.0	0.0	1.0	127.6	5.28	5.32	00:08:08	06:38 AM	06/08/98	07:38 AM			
306	Flush	0.7	0.0	0.7	128.3	5.32	5.35	00:08:08	07:38 AM	06/08/98	08:18 AM	64.0 L	64.0 L	
308	Pump	0.7	0.0	0.7	129.0	5.35	5.37	00:08:08	08:18 AM	06/08/98	08:58 AM	64.0 L	64.0 L	
309	Concentration	1.0	0.0	1.0	130.0	5.37	5.42	00:08:08	08:58 AM	06/08/98	09:58 AM	3.0 LSF/Hr	3.0 LSF/Hr	
310	Dilution	0.4	0.0	0.4	130.4	5.42	5.43	00:08:08	09:58 AM	06/08/98	10:25 AM	3.0 LSF/Hr	3.0 LSF/Hr	
311	Wash	0.9	0.0	0.9	131.3	5.43	5.47	00:08:08	10:25 AM	06/08/98	11:19 AM	72.0 L	72.0 L	
312	Flush	0.3	0.0	0.3	131.7	5.47	5.49	00:08:08	11:19 AM	06/08/98	11:59 AM	3.0 LSF/Hr	3.0 LSF/Hr	
313	Store	0.7	0.0	0.7	132.3	5.49	5.51	00:08:08	11:59 AM	06/08/98	12:19 PM	64.0 L	64.0 L	
314	CIP	1.0	0.0	1.0	133.3	5.51	5.56	00:08:08	12:19 PM	06/08/98	9:19 PM	3.0 LSF/Hr	3.0 LSF/Hr	
315	SIP	1.0	0.0	1.0	134.3	5.56	5.60	00:08:08	9:19 PM	06/08/98	02:19 PM			
316	Clean Up	1.0	0.0	1.0	135.3	5.60	5.64	00:08:08	02:19 PM	06/08/98	03:19 PM			
317	Sub Total	8.7	8.7	8.7	131.3									
318														
319	15 A Microfiltration													
320	Set Up	1.0	0.0	1.0	131.1	5.42	5.46	00:08:08	10:03 AM	06/08/98	11:03 AM	25.2 L	25.2 L	
321	Flush	0.1	0.0	0.1	131.2	5.46	5.47	00:08:08	11:03 AM	06/08/98	11:11 AM	16.0 LSF/Hr	16.0 LSF/Hr	
322	Pump	0.1	0.0	0.1	131.3	5.47	5.47	00:08:08	11:11 AM	06/08/98	11:19 AM	15.0 L	15.0 L	
323	Filtration	0.5	0.0	0.5	131.6	5.47	5.49	00:08:08	11:19 AM	06/08/98	11:59 AM	3.15 LPM	3.15 LPM	
324	Wash	0.0	0.0	0.0	131.8	5.49	5.49	00:08:08	11:59 AM	06/08/98	11:59 AM	0.0 L	0.0 L	
325	Regenerate	0.0	0.0	0.0	131.9	5.49	5.49	00:08:08	11:59 AM	06/08/98	11:59 AM	15.0 LSF/Hr	15.0 LSF/Hr	
326	Store	0.1	0.0	0.1	131.9	5.49	5.50	00:08:08	11:59 AM	06/08/98	11:59 AM	6.3 L	6.3 L	
327	CIP	1.0	0.0	1.0	132.0	5.50	5.54	00:08:08	11:59 AM	06/08/98	12:55 PM	15.0 LSF/Hr	15.0 LSF/Hr	
328	SIP	1.0	0.0	1.0	133.9	5.54	5.58	00:08:08	12:55 PM	06/08/98	01:55 PM	3.15 LPM	3.15 LPM	
329	Clean Up	1.0	0.0	1.0	134.9	5.58	5.62	00:08:08	01:55 PM	06/08/98	02:55 PM			
330	Sub Total	4.9	4.9	4.9	131.8									
331														
332	16 A PIA MPIC													
333	Equilibration	1.1	0.0	1.1	131.4	5.43	5.48	00:08:08	10:17 AM	06/08/98	11:24 PM	63.8 L CV	63.8 L CV	
334	Load	0.7	0.0	0.7	132.5	5.49	5.52	00:08:08	11:49 AM	06/08/98	12:31 PM	100.0 CM/Hr	100.0 CM/Hr	
335	Wash	1.3	0.0	1.3	133.3	5.52	5.58	00:08:08	12:31 PM	06/08/98	01:52 PM	50.0 CM/Hr	50.0 CM/Hr	
336	Elute A	1.3	0.0	1.3	135.2	5.58	5.63	00:08:08	01:52 PM	06/08/98	02:12 PM	50.0 CM/Hr	50.0 CM/Hr	
337	Elute B	0.0	0.0	0.0	135.2	5.63	5.63	00:08:08	02:12 PM	06/08/98	02:12 PM	30.0 CM/Hr	30.0 CM/Hr	
338	Regenerate	0.2	0.0	0.2	135.4	5.63	5.64	00:08:08	02:12 PM	06/08/98	02:25 PM	63.8 L	63.8 L	
339	Store	0.4	0.0	0.4	135.9	5.64	5.66	00:08:08	02:25 PM	06/08/98	03:52 PM	100.0 CM/Hr	100.0 CM/Hr	
340	CIP	1.0	0.0	1.0	136.9	5.66	5.70	00:08:08	03:52 PM	06/08/98	04:52 PM			
341	SIP	1.0	0.0	1.0	137.9	5.70	5.74	00:08:08	04:52 PM	06/08/98	05:52 PM			
342	Clean Up	1.0	0.0	1.0	138.9	5.74	5.79	00:08:08	05:52 PM	06/08/98	06:52 PM			
343	Sub Total	6.2	6.2	6.2	135.2									
344														
345	17 A PIAMPIC													
346	Equilibration	0.8	0.0	0.8	135.6	5.62	5.65	00:08:08	02:59 PM	06/08/98	03:38 PM	12.2 L CV	12.2 L CV	
347	Load	1.1	0.0	1.1	136.3	5.68	5.71	00:08:08	03:12 PM	06/08/98	04:17 PM	61.0 L	61.0 L	
348	Wash	0.8	0.0	0.8	137.1	5.68	5.71	00:08:08	04:17 PM	06/08/98	05:03 PM	36.6 L	36.6 L	
349	Elute A	0.8	0.0	0.8	137.3	5.71	5.74	00:08:08	05:03 PM	06/08/98	05:39 PM	50.0 CM/Hr	50.0 CM/Hr	
350	Elute B	0.0	0.0	0.0	137.8	5.74	5.74	00:08:08	05:49 PM	06/08/98	06:49 PM	30.0 CM/Hr	30.0 CM/Hr	
351														
352														
353														
354														

FIG. 12F

26.89 SF

12.60 SF

Max FR

1.35 LPM

Process Time Line												
	Duration (Hrs.)		Rel. Time Scale (hrs.)		Abs. Dura.		Start Date		Finish Date			
Operation	Calc.	A/D	Adj.	Prep	Exc.	Compl.	Start	End	Time	Date	Time	
355 Regenerate	0.1	0.0	0.1 Hrs				138.0	6.74	6.75	06/08/98	05:49 AM	06/08/98 06:00 AM
356 Store	0.3	0.0	0.3 Hrs				138.2	5.75	5.76	06/08/98	05:57 PM	06/08/98 06:13 PM
357 CIP	1.0	0.0	1.0 Hrs				139.2	5.76	6.80	06/08/98	06:13 PM	06/08/98 07:13 PM
358 SIP	1.0	0.0	1.0 Hrs				140.2	6.80	6.84	06/08/98	07:13 PM	06/08/98 08:13 PM
359 Clean Up	1.0	0.0	1.0 Hrs				141.2	6.84	6.88	06/08/98	08:13 PM	06/08/98 09:13 PM
360 Sub Total	6.7	6.7	Hrs									Max FR 1.58 LPM
361 16 A Flow Dialysis												12:20 SF
362 Set Up	1.0	0.0	1.0 Hrs				139.5	5.65	5.69	06/08/98	03:29 PM	06/08/98 04:29 PM
364 Flush	0.7	0.0	0.7 Hrs				137.2	5.69	5.72	06/08/98	04:29 PM	06/08/98 05:09 PM
365 Prime	0.7	0.0	0.7 Hrs				137.8	5.72	5.74	06/08/98	05:09 PM	06/08/98 05:49 PM
366 Dialysis	1.0	0.0	1.0 Hrs				138.8	5.74	6.78	06/08/98	05:49 PM	06/08/98 06:49 PM
368 Wash	0.0	0.0	0.0 Hrs				138.4	6.78	6.78	06/08/98	06:49 PM	06/08/98 07:49 PM
369 Flush	0.3	0.0	0.3 Hrs				139.2	6.78	6.80	06/08/98	07:49 PM	06/08/98 08:49 PM
370 Store	0.7	0.0	0.7 Hrs				139.8	5.80	6.83	06/08/98	08:09 PM	06/08/98 09:09 PM
371 CIP	1.0	0.0	1.0 Hrs				140.8	5.83	5.87	06/08/98	09:49 PM	06/08/98 10:49 PM
372 SIP	1.0	0.0	1.0 Hrs				141.8	5.87	5.91	06/08/98	10:49 PM	06/08/98 11:49 PM
373 Clean Up	1.0	0.0	1.0 Hrs				142.8	5.91	5.95	06/08/98	11:49 PM	06/08/98 12:49 PM
374 Sub Total	7.3	7.3	Hrs				136.8					Max FR 0.61 LPM
375 19 A PIA MPIC												28:81 CM Dia.
376 Equilibration	0.5	0.0	0.5 Hrs				138.5	5.75	5.77	06/08/98	05:59 PM	06/08/98 06:59 PM
377 Load	0.2	0.0	0.2 Hrs				139.1	5.78	5.82	06/08/98	06:59 PM	06/08/98 07:59 PM
378 Wash	0.8	0.0	0.8 Hrs				139.7	5.82	6.85	06/08/98	07:59 PM	06/08/98 08:59 PM
380 Elute A	0.6	0.0	0.6 Hrs				140.3	5.85	6.85	06/08/98	08:59 PM	06/08/98 09:59 PM
381 Elute B	0.6	0.0	0.6 Hrs				140.3	5.85	6.85	06/08/98	09:59 PM	06/08/98 10:59 PM
382 Regenerate	0.1	0.0	0.1 Hrs				140.4	5.85	6.85	06/08/98	10:20 PM	06/08/98 10:26 PM
383 Store	0.2	0.0	0.2 Hrs				140.7	5.85	5.88	06/08/98	10:26 PM	06/08/98 10:39 PM
384 CIP	1.0	0.0	1.0 Hrs				141.7	5.85	5.90	06/08/98	10:39 PM	06/08/98 11:39 PM
385 SIP	1.0	0.0	1.0 Hrs				142.7	5.90	6.94	06/08/98	11:39 PM	06/08/98 12:39 PM
386 Clean Up	1.0	0.0	1.0 Hrs				143.7	5.94	5.99	06/08/98	12:39 PM	06/08/98 13:39 PM
387 Sub Total	5.4	5.4	Hrs				140.3					Max FR 1.09 LPM
388 20 A Flow Dialysis												2:43 SF
389 Set Up	0.0	0.0	0.0 Hrs				139.0	5.79	5.79	06/08/98	07:00 PM	06/08/98 07:00 PM
390 Flush	0.7	0.0	0.7 Hrs				139.7	5.82	5.82	06/08/98	07:00 PM	06/08/98 07:40 PM
391 Prime	0.7	0.0	0.7 Hrs				140.3	5.82	5.85	06/08/98	07:40 PM	06/08/98 08:20 PM
392 Dialysis	2.0	0.0	2.0 Hrs				142.3	5.85	5.93	06/08/98	08:20 PM	06/08/98 09:20 PM
393 Wash	0.0	0.0	0.0 Hrs				142.3	5.93	5.93	06/08/98	09:20 PM	06/08/98 10:20 PM
394 Flush	0.3	0.0	0.3 Hrs				142.7	5.93	5.94	06/08/98	10:20 PM	06/08/98 10:39 PM
395 Store	0.7	0.0	0.7 Hrs				143.3	5.94	5.94	06/08/98	10:39 PM	06/08/98 11:39 PM
396 CIP	0.0	0.0	0.0 Hrs				143.3	5.97	5.97	06/08/98	11:20 PM	06/08/98 11:20 PM
397 SIP	0.0	0.0	0.0 Hrs				143.3	5.97	5.97	06/08/98	11:20 PM	06/08/98 11:20 PM
398 Clean Up	0.0	0.0	0.0 Hrs				144.3	5.97	6.01	06/08/98	11:20 PM	06/08/98 12:20 AM
399 Sub Total	4.3	5.3	Hrs				142.3					Max FR 0.12 LPM
400 21 A PIA MPIC												26:35 CM Dia.
401 Equilibration	0.5	0.0	0.5 Hrs				142.0	5.89	5.91	06/08/98	09:28 PM	06/08/98 09:57 PM
402 Load	0.1	0.0	0.1 Hrs				142.4	5.93	5.94	06/08/98	10:20 PM	06/08/98 10:26 PM
403 Wash	0.8	0.0	0.8 Hrs				143.0	5.94	5.96	06/08/98	10:26 PM	06/08/98 11:01 PM
404 Elute A	0.8	0.0	0.8 Hrs				143.6	5.96	5.98	06/08/98	11:01 PM	06/08/98 11:38 PM
405 Elute B	0.0	0.0	0.0 Hrs				143.6	5.98	5.98	06/08/98	11:38 PM	06/08/98 11:38 PM
406 Regenerate	0.1	0.0	0.1 Hrs				143.7	5.98	5.99	06/08/98	11:38 PM	06/08/98 11:42 PM
407 Store	0.2	0.0	0.2 Hrs				143.9	5.99	6.00	06/08/98	11:42 PM	06/08/98 11:54 PM
408 CIP	0.0	0.0	0.0 Hrs				143.9	6.00	6.00	06/08/98	11:54 PM	06/08/98 11:54 PM
409 SIP	0.0	0.0	0.0 Hrs				143.9	6.00	6.00	06/08/98	11:54 PM	06/08/98 11:54 PM

FIG. 12 G

H-I(s). 12H

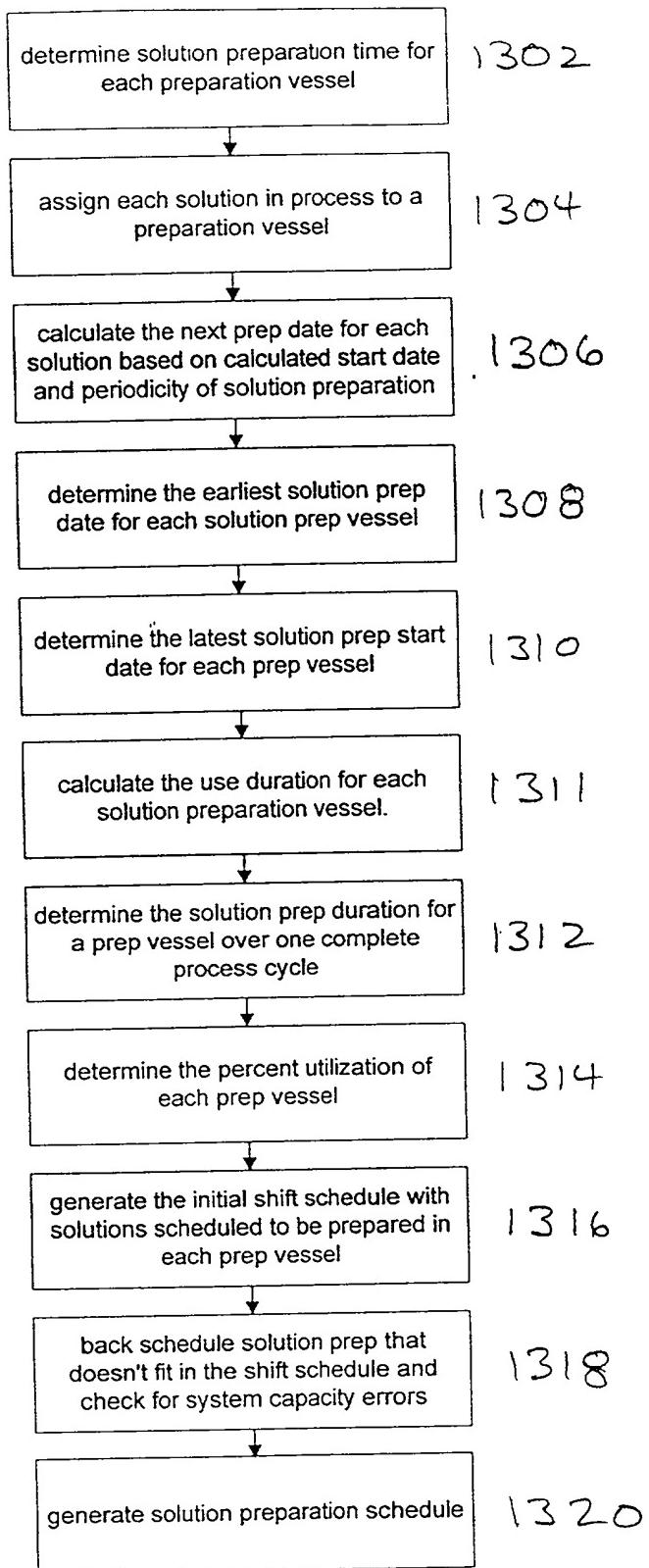


FIG.-13

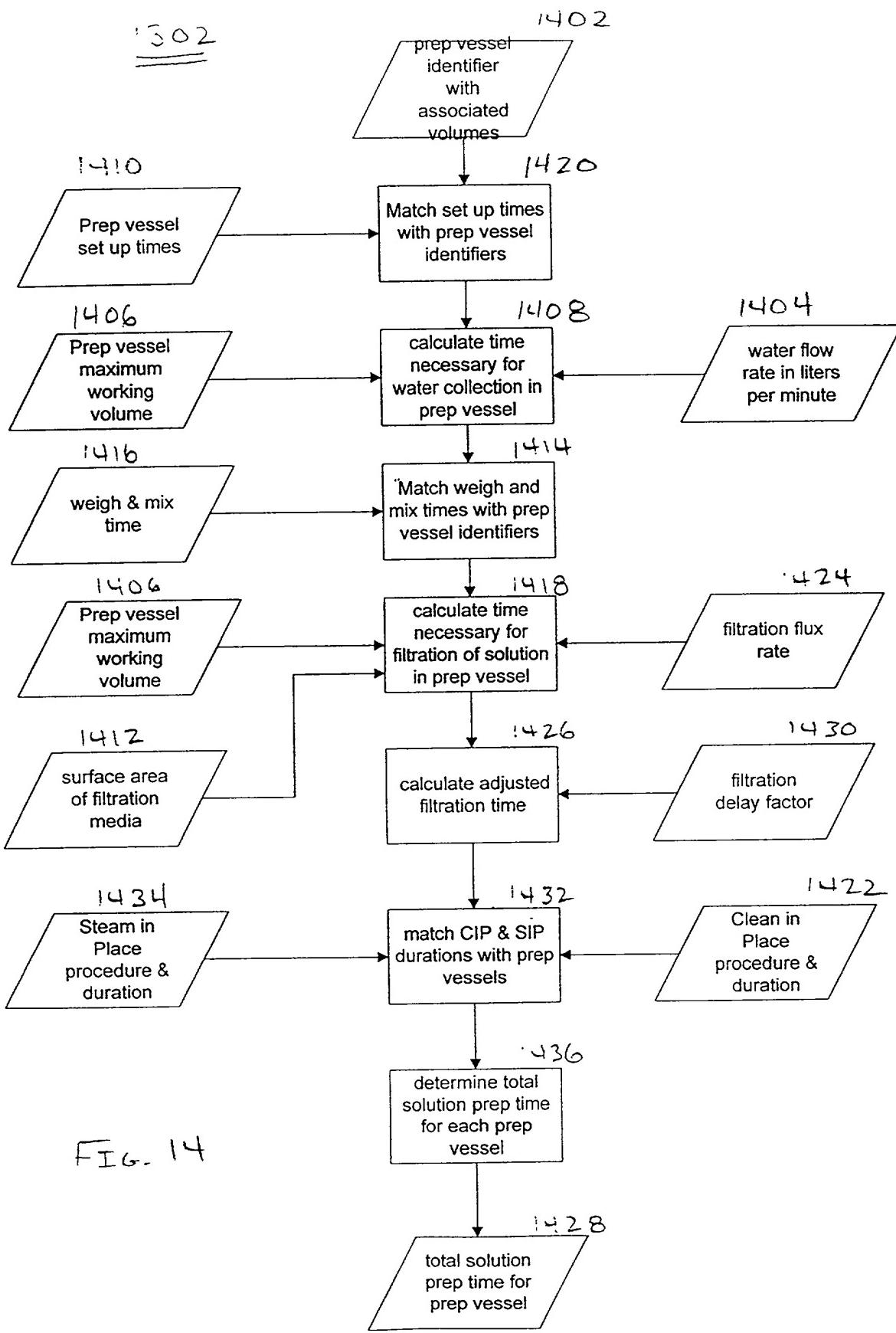


FIG. 14

Solution Prep Vessel List/Procedure

Batch Tank No.	Batch Tank			Water Collect.			Ultrafiltration/Microfiltration			CIP			Total			Perc. Util.	
	Min. L/WV	Max. L/WV	Min. L/WV	Max. L/WV	Set Up Min.	LPH	Min.	SF	USF/IHR	Min.	Delay Factor	Adj. Min.	Cycle	Min.	SIP	Min.	
101	0.5	101	0.5	1	10	1	15	0.5	25	4.8	1.2	5.76				31.76	0.5
102	1	102	1	2	10	2	15	1	25	4.8	1.2	5.76				31.76	0.5
103	2	103	2	4	20	2	30	1	25	9.6	1.2	11.52				63.52	1.1
104	4	104	4	10	20	10	30	2	25	12	1.2	14.4				65.4	1.1
105	10	105	10	20	20	10	30	2	25	24	1.2	28.8				80.8	1.3
106	20	106	20	50	20	10	5	30	10	25	12	14.4	CIP-1	60	40	109.4	1.8
107	50	107	50	100	20	10	10	30	10	25	24	1.2	CIP-1	60	40	128.8	2.1
108	100	108	100	250	0.5	50	5	30	30	25	20	1.2	CIP-1	60	40	99.5	1.7
109	250	109	250	500	0.5	50	10	30	30	25	40	1.2	CIP-1	60	40	128.5	2.1
110	500	110	500	1,500	1	50	30	60	30	60	120	1.2	CIP-1	60	40	173	2.9
111	1500	111	1500	3,000	1	50	60	30	60	120	1.2	144	CIP-1	60	40	276	4.6
																	16%

1402 1406 1410 1404 1408 1412 1410 1412 1424 1424 1422 1422 1428 1434
 1402 1406 1410 1404 1408 1412 1410 1412 1424 1424 1422 1422 1428 1434

Fig. 15

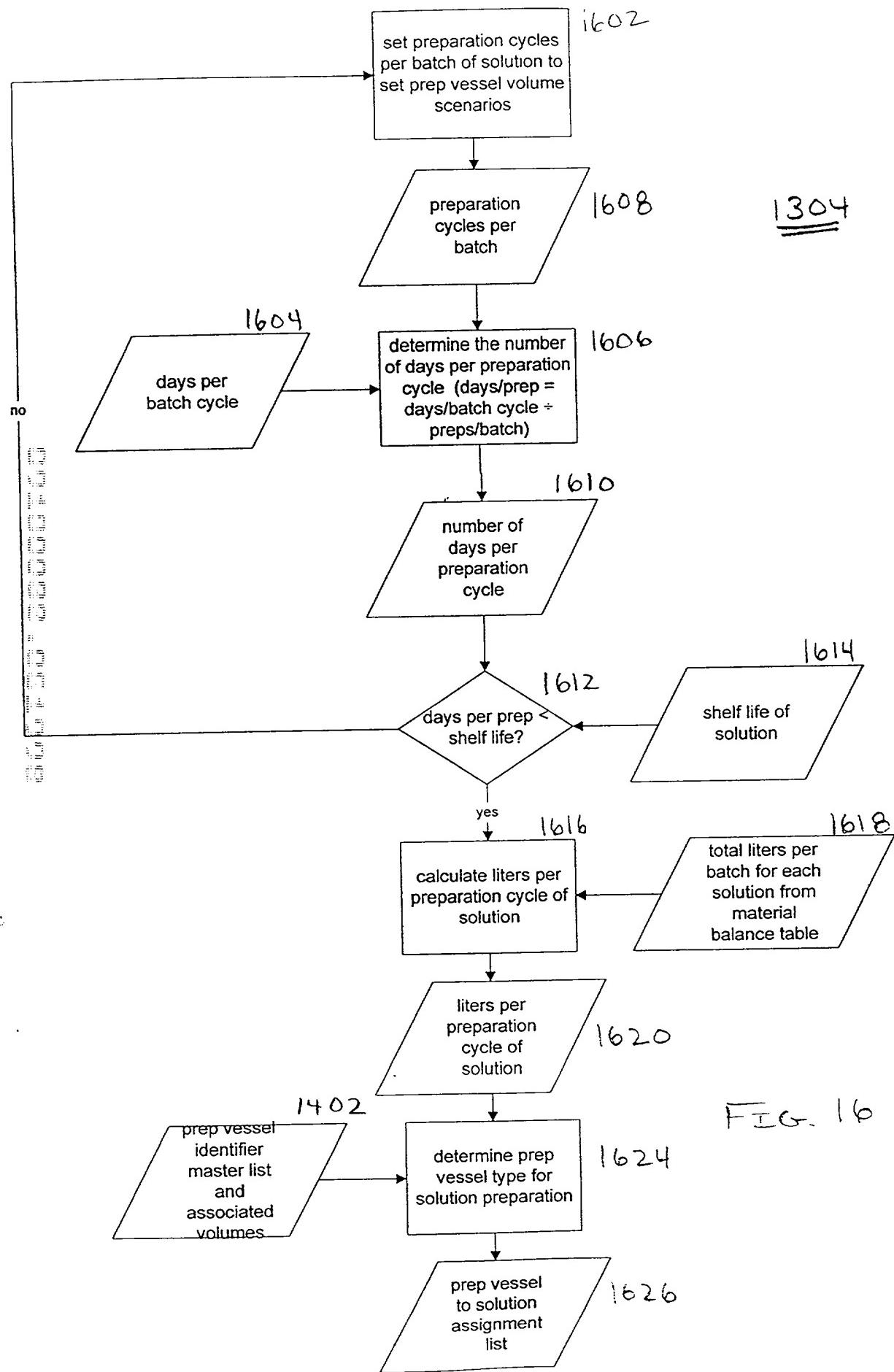


FIG. 16

Solution Prep Campaign Format

1626

Soh. ID	Storage Cond.			Soh. Prep Format			Solution Prep Cycles													
	RT	4C	XP	BOD	BIA		Liters/ Batch	Preps/ Batch	Liters/ Prep	Days/ Bat. Cy.	Days/ Prep	Shelf Days	Shelf Check	101	102	103	104	105	106	107
1 S-0101	X			0	x	0	1,666.50	1	1,666.50	7	7	56	OK							
2 S-0102	X			0	x	0	1.65	1	1.65	7	7	180	OK							
3 S-0103	X			0	x	0	1.65	1	1.65	7	7	56	OK							
4 S-0104	X			0	x	0	8.25	1	8.25	7	7	56	OK							
5 S-0105	X			0	x	0	8.25	1	8.25	7	7	56	OK							
6 S-0106	X			0	x	0	580.51	1	580.51	7	7	56	OK							
7 S-0107	X			0	x	0	125.93	1	125.93	7	7	56	OK							
8 S-0108	X			0	x	0	177.41	1	177.41	7	7	56	OK							
9 S-0109	X			0	x	0	22.18	1	22.18	7	7	56	OK							
10 S-0111	X			0	x	0	56.52	1	56.52	7	7	56	OK							
11 S-0112	X			0	x	0	113.03	1	113.03	7	7	56	OK							
12 S-0113	X			0	x	0	1,612.45	1	1,612.45	7	7	56	OK							
13 S-0114	X			0	x	0	574.10	1	574.10	7	7	56	OK							
14 S-0115	X			0	x	0	248.83	1	248.83	7	7	56	OK							
15 S-0116	X			0	x	0	497.65	1	497.65	7	7	56	OK							
16 S-0117	X			0	x	0	109.80	1	109.80	7	7	56	OK							
17 S-0118	X			0	x	0	497.85	1	497.85	7	7	56	OK							
18 S-0119	X			0	x	0	292.79	1	292.79	7	7	56	OK							
19 S-0120	X			0	x	0	109.80	1	109.80	7	7	56	OK							
20 S-0121	X			0	x	0	62.58	1	62.58	7	7	56	OK							
21 S-0122	X			0	x	0	0.00	1	0.00	7	7	56	OK							

1704

1608

1610

1614
1604
1610

107
106
107

Fig. 17

Solution Prep Campaign Format

1626

1-22 1-726 1-728

1724

0
0
0
0

05/29/98 08/14/96
Min

10

10
145

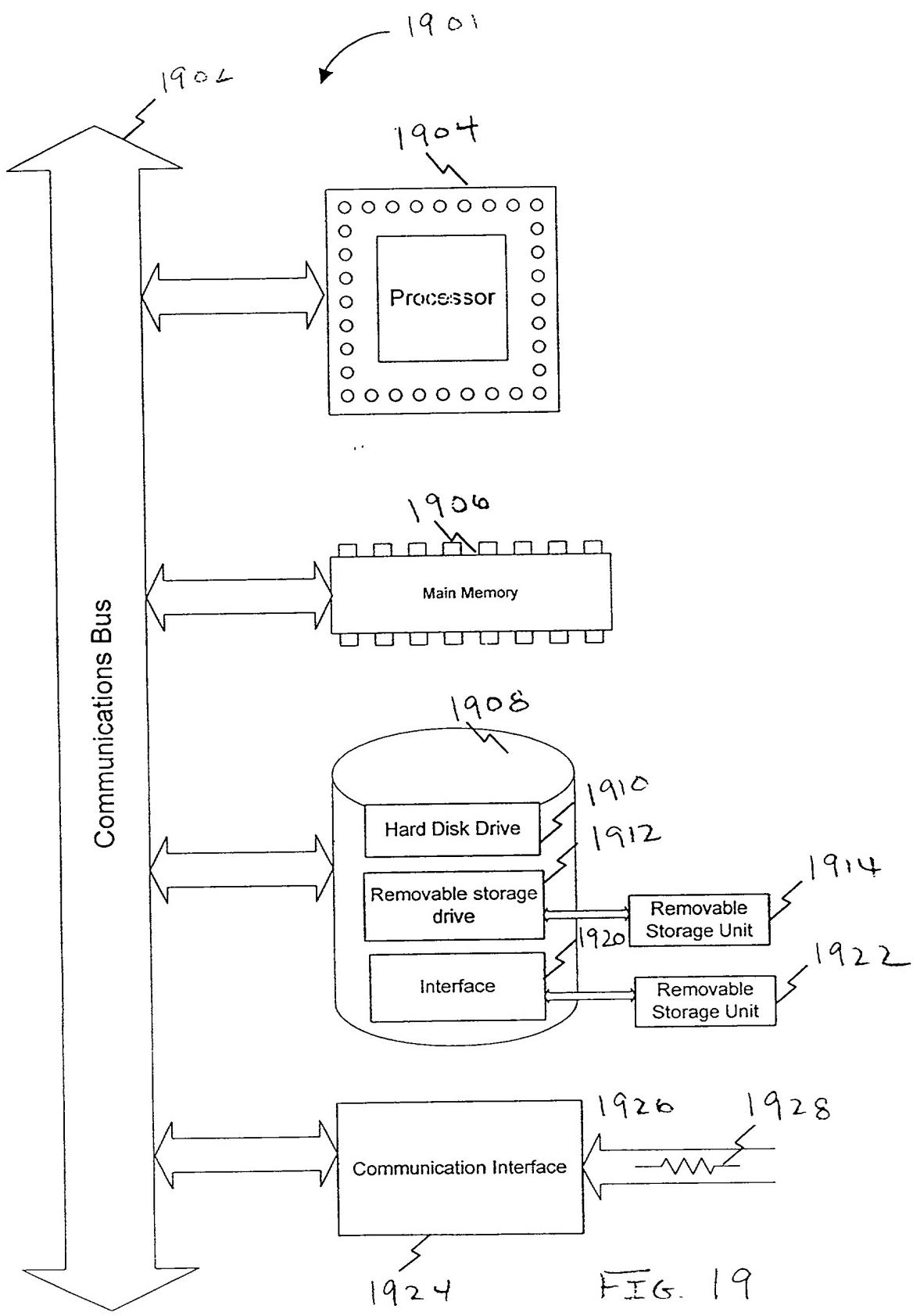
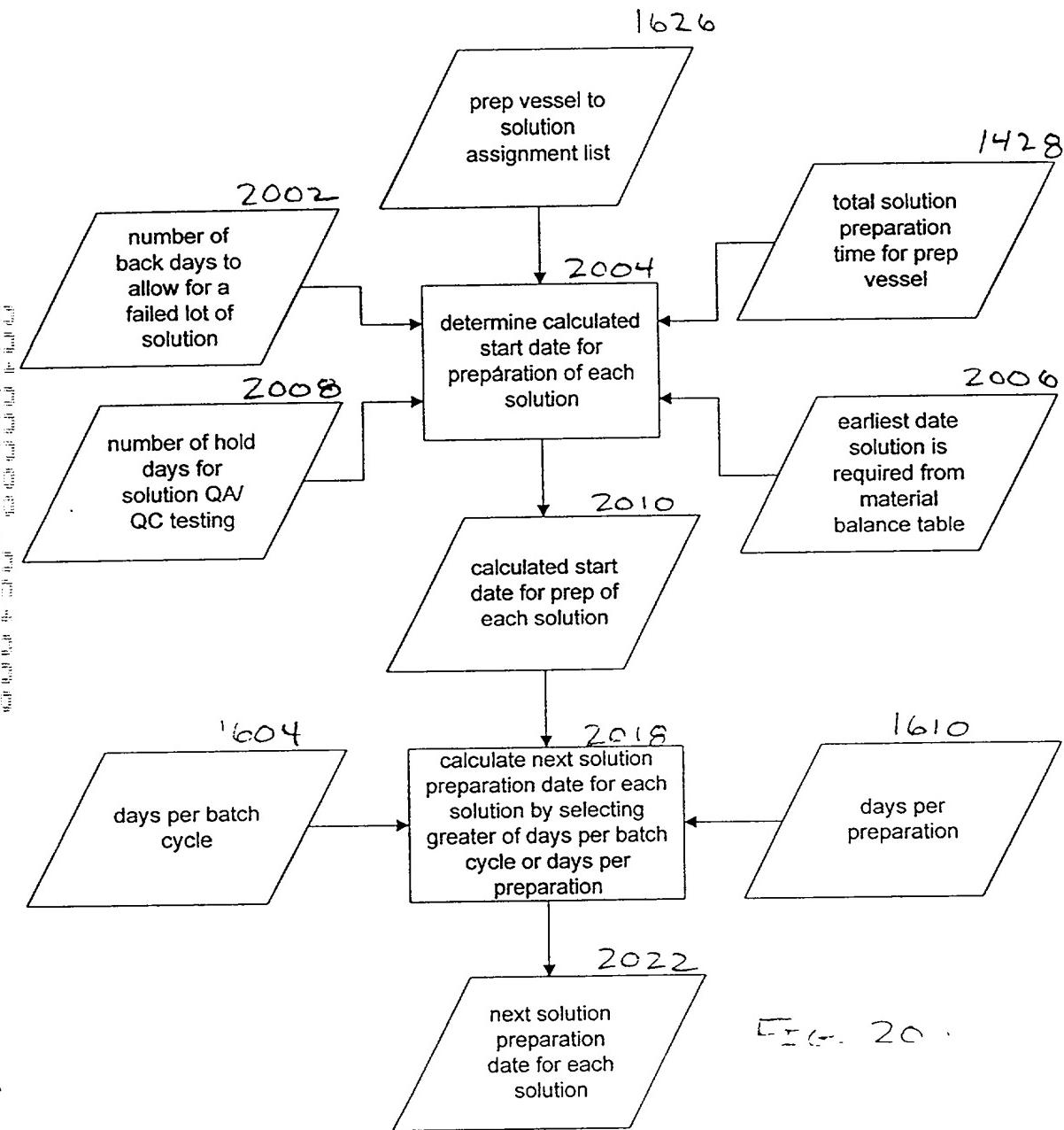


FIG. 19

306



Final 20

	Category/Assay	Code	Man Hour			Disp. Material
			Set Up	Per Sample	Clean Up	
1	Environmental					
2	Temperature	E-1	0.5	0.1	0.5	
3	Humidity	E-2	0.5	0.1	0.5	
4	Particle Count	E-3	0.5	0.2	0.5	
5						
6	Analytical					
7	Visual					
8	Certificate of Analysis	AV-1	0.25	0.2	0.5	
9	Appearance	AV-2	0.25	0.05	0.25	
10	Chemical					
11	Solubility	AC-1	0.5	0.1	0.5	
12	pH	AC-2	0.25	0.05	0.25	
13	Osmolality	AC-3	0.25	0.1	0.25	
14	Water Content (by Karl Fischer)	AC-4	0.5	0.2	0.5	
15	Key Element Analysis (by ICP Atomic Adsorption Spectroscopy)	AC-5	1	0.25	1	
16	GC/Mass Spec	AC-6	1	0.25	1	
17						
18	Biochemical					
19	DNA					
20	DNA Fluorochrome Stain	AB-1	0.5	0.1	0.5	
21	Protein					
22	Hemoglobin	AB-2	0.5	0.1	0.5	
23	Electrophoretic Profiles by SDS-PAGE	AB-3	1	0.2	1	
24	A280	AB-4	0.25	0.1	0.25	
25	Bradford Assay	AB-5	0.5	0.1	0.5	
26	Amino Acid Analysis by HPLC	AB-6	1	0.25	1	
27			0.5	0.1	0.5	
28	Endotoxin					
29	Gel Clot LAL	AB-7				
30						
31	Immunological					
32	ELISA	AI-1	1	0.1	1	
33	Western Blots	AI-2	1.5	0.2	1.5	
34	Activity					
35	Chromagenic Substrate Assays	AA-1	1	0.1	1	
36						
37	In Vitro Biological					
38	Microbiological	VB-1	0.5	0.2	0.5	
39	Mycoplasma (Barile Method)	VB-2	0.5	0.2	0.5	
40	Bacteriophage (Screened)	VB-3	0.5	0.2	0.5	
41	Cell Passage Test	VB-4	1	0.2	1	
42	Adventitious viral Agents		2	0.2	1	
43	CPE	VB-5	2	0.2	1	
44	BVD	VB-6	2	0.2	1	
45	P13	VB-7	2	0.2	1	
46	IBR	VB-8	2	0.2	1	
47	Virus Neutralization Titers (9CFR)					
48	BVD	VB-9	2	0.2	1	
49	P13	VB-10	2	0.2	1	
50	IBR	VB-11	2	0.2	1	
51	Tritiated Thymidine Uptake in Mouse Cells	VB-12	2	0.2	1	
	General Safety Test (Guinea Pigs)	VB-13	1	0.2	1	

FIG- 21

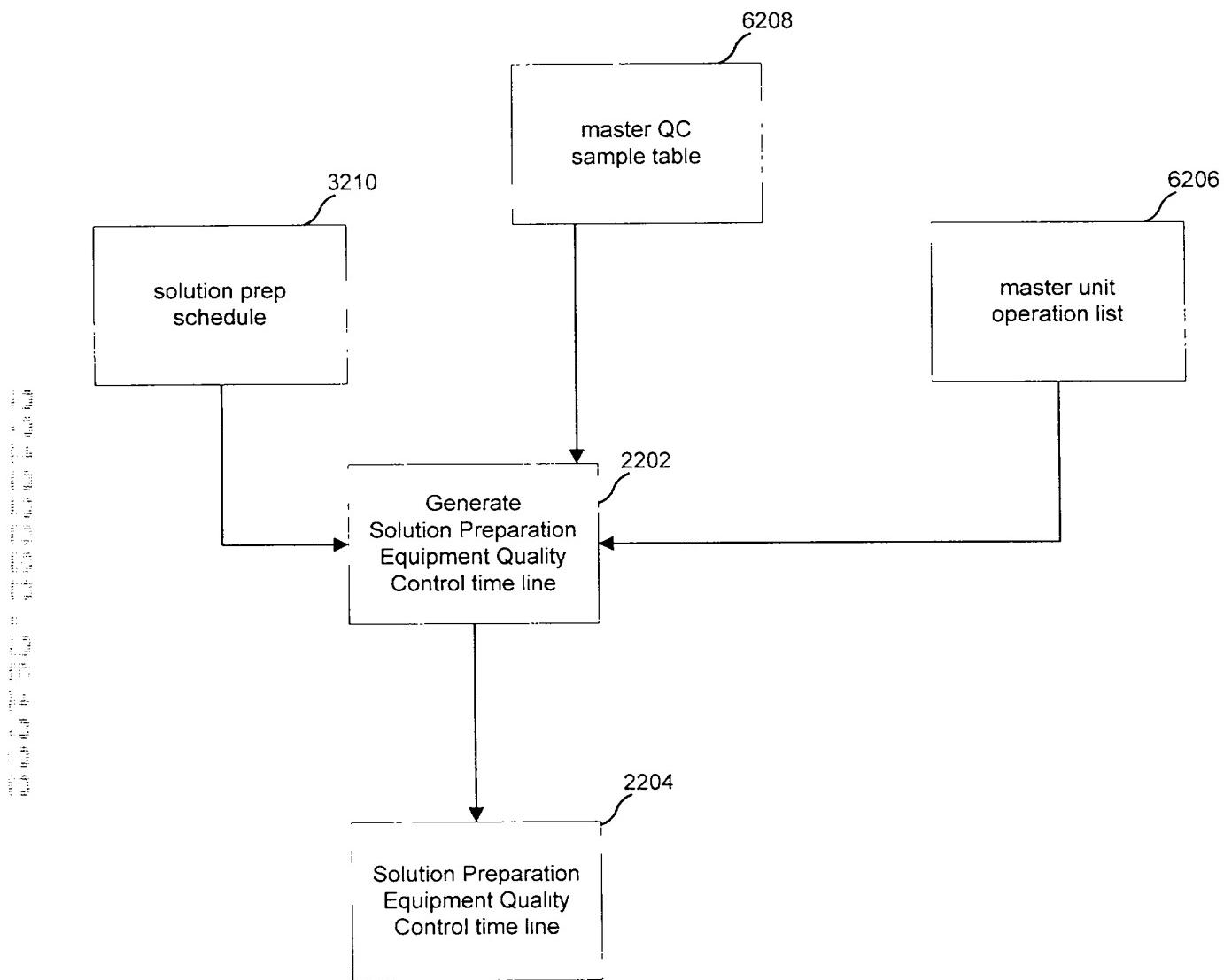


FIG. 22

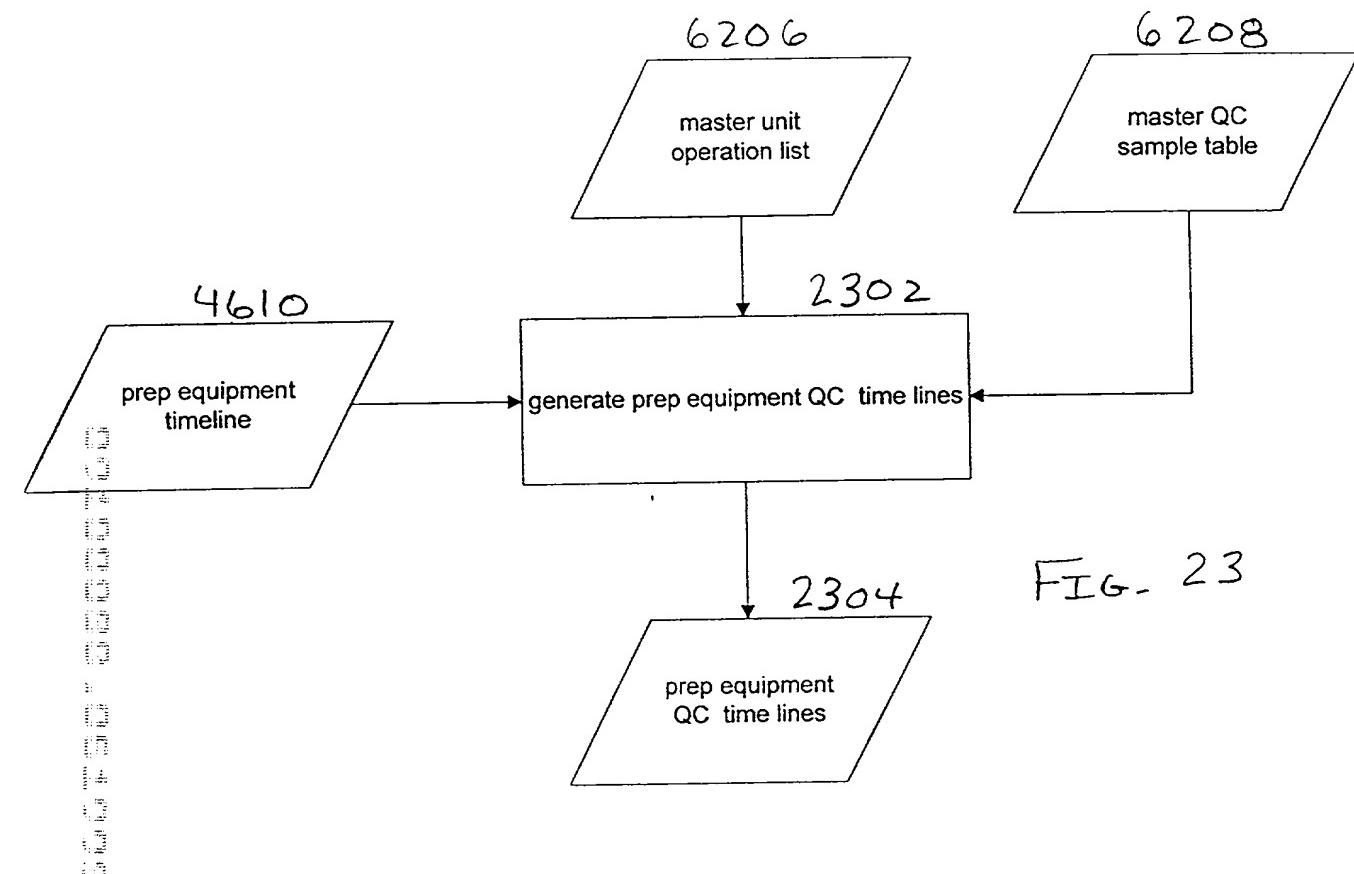


FIG- 23

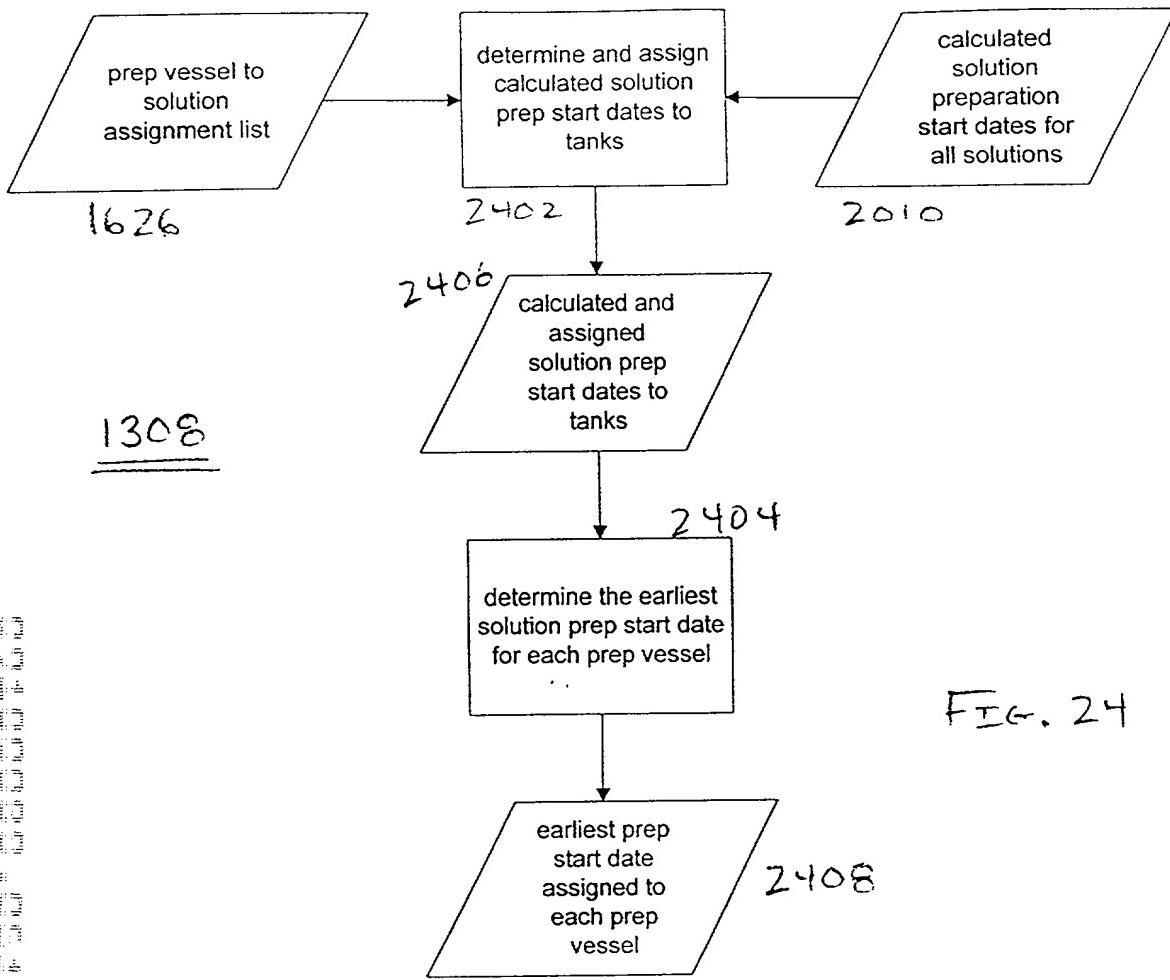


FIG. 24

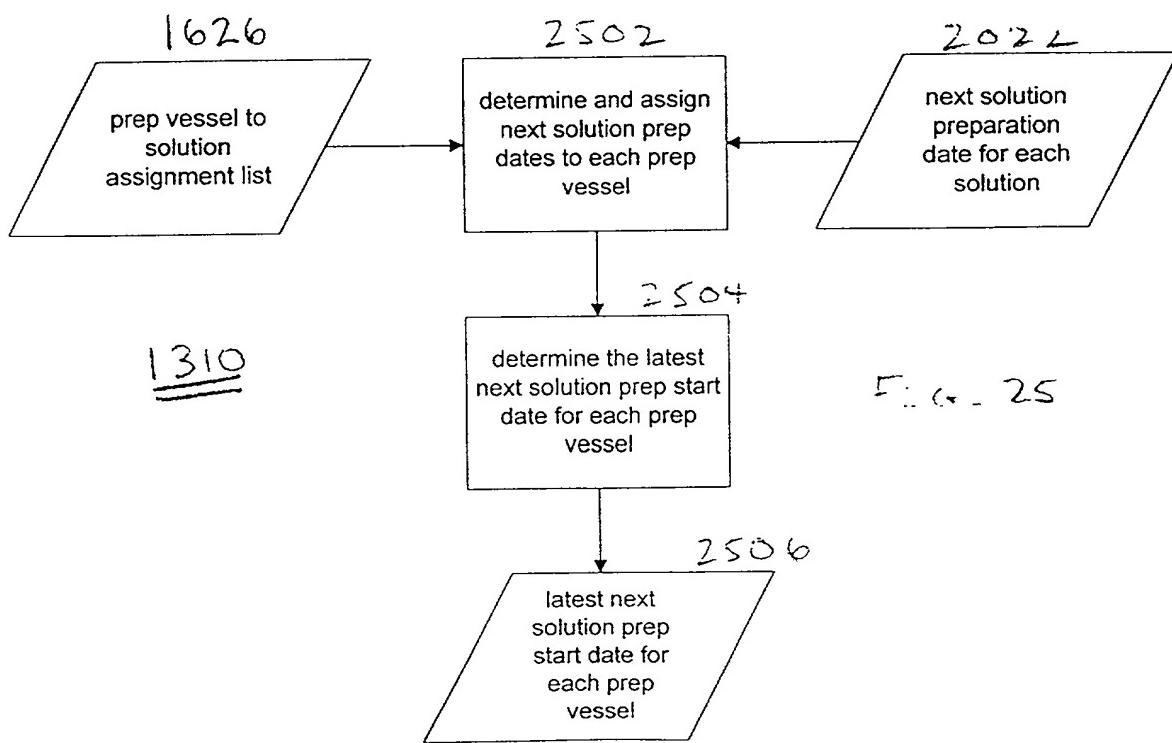


FIG. 25

312

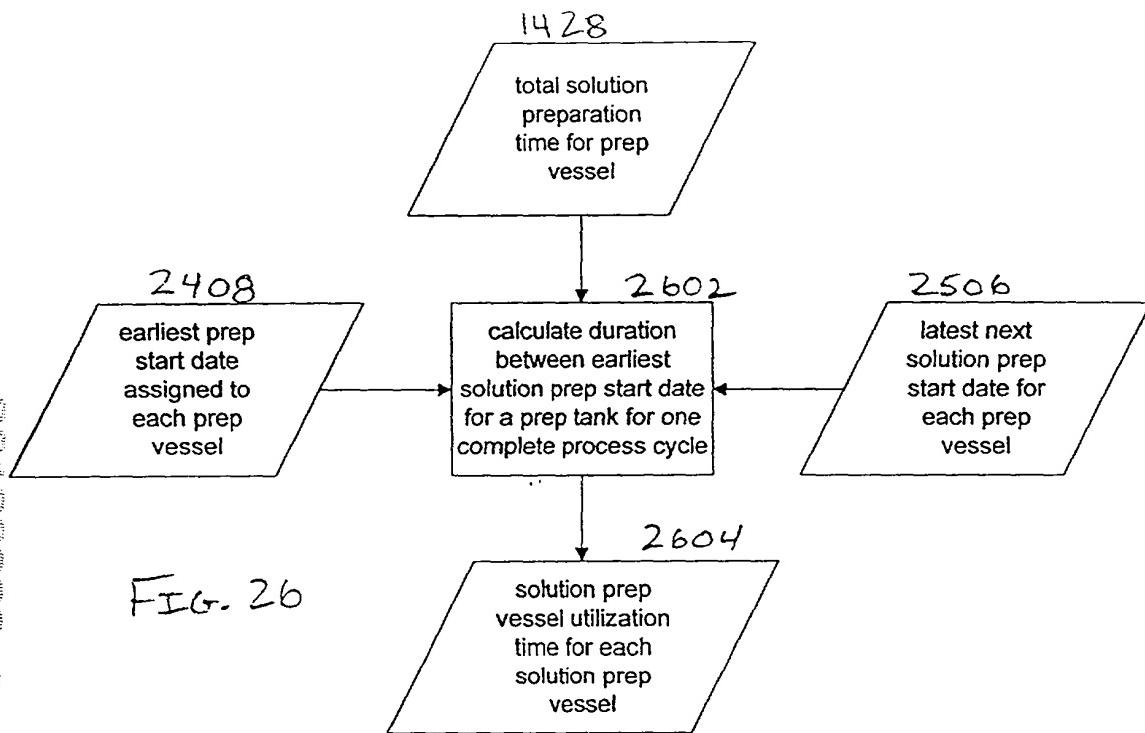
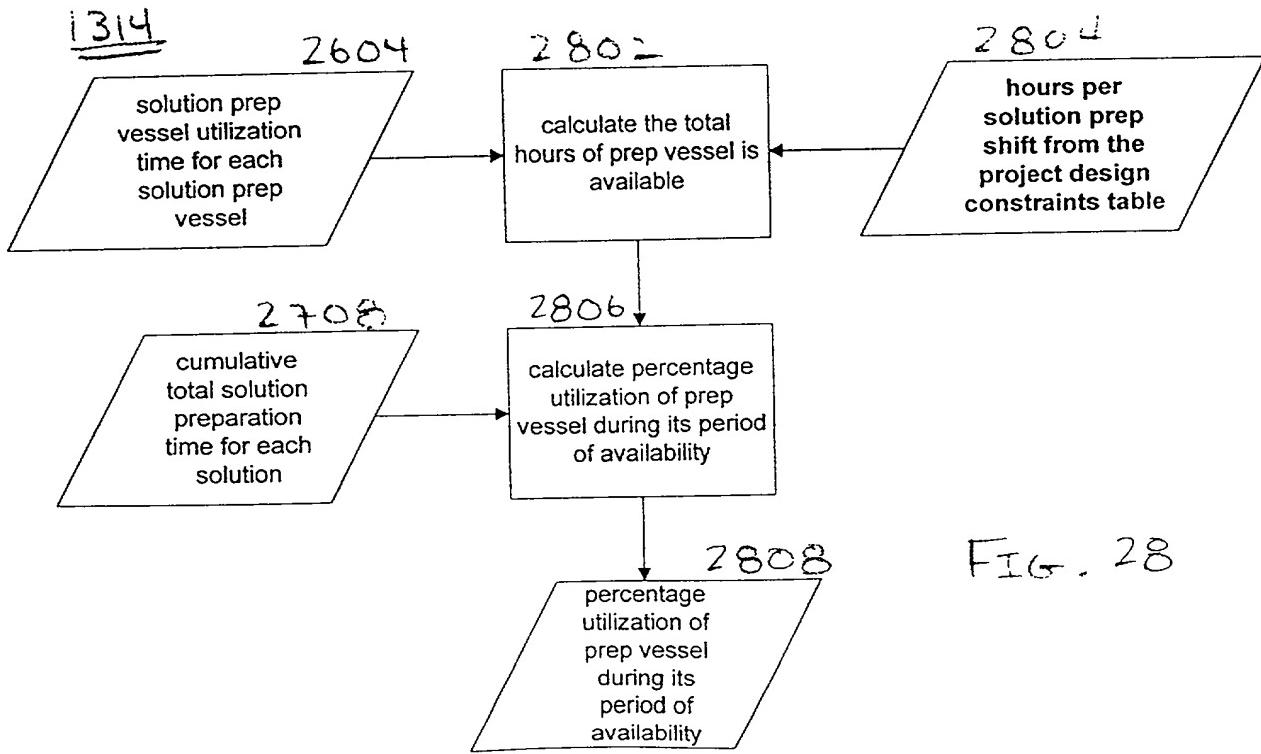
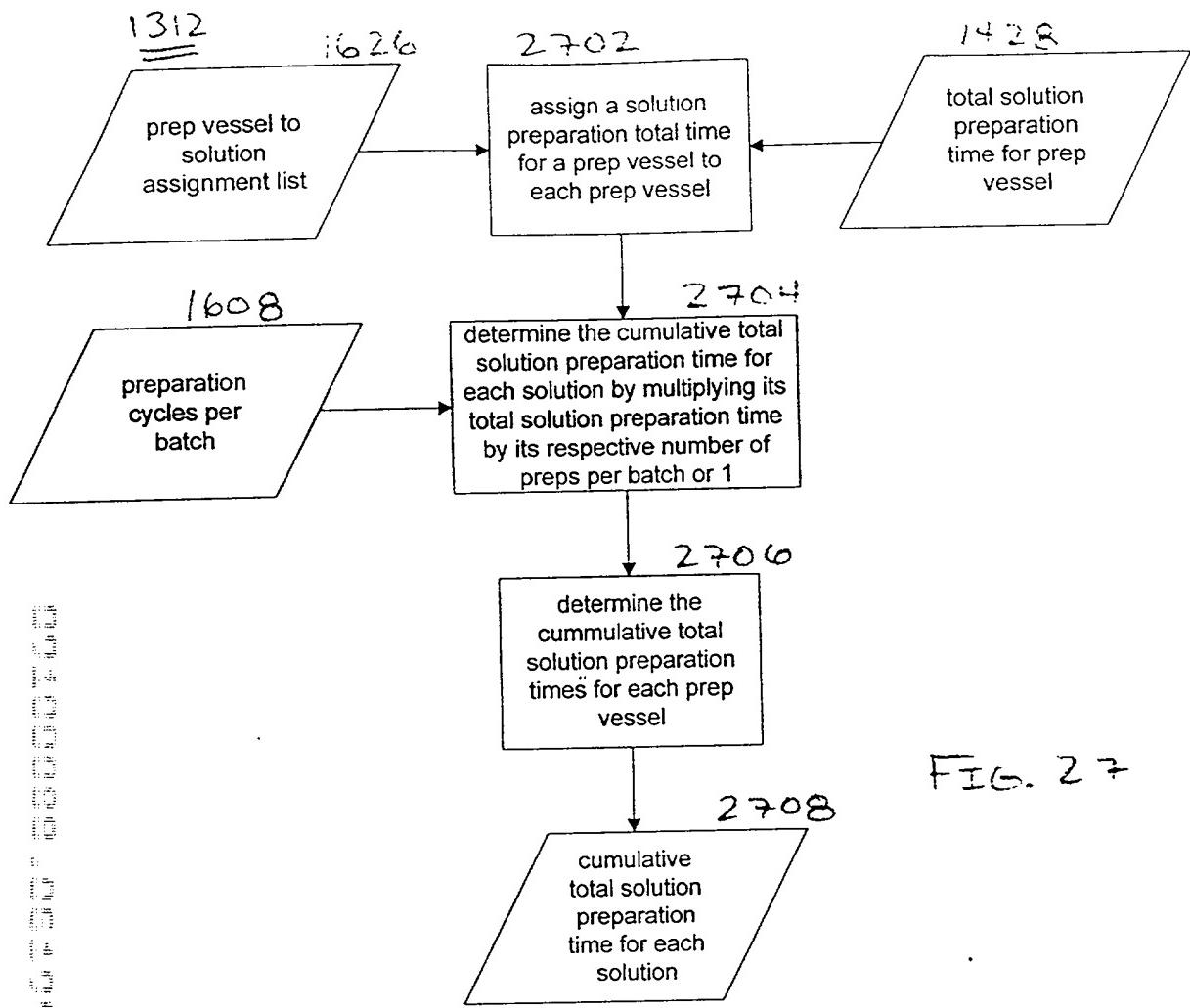


FIG. 26



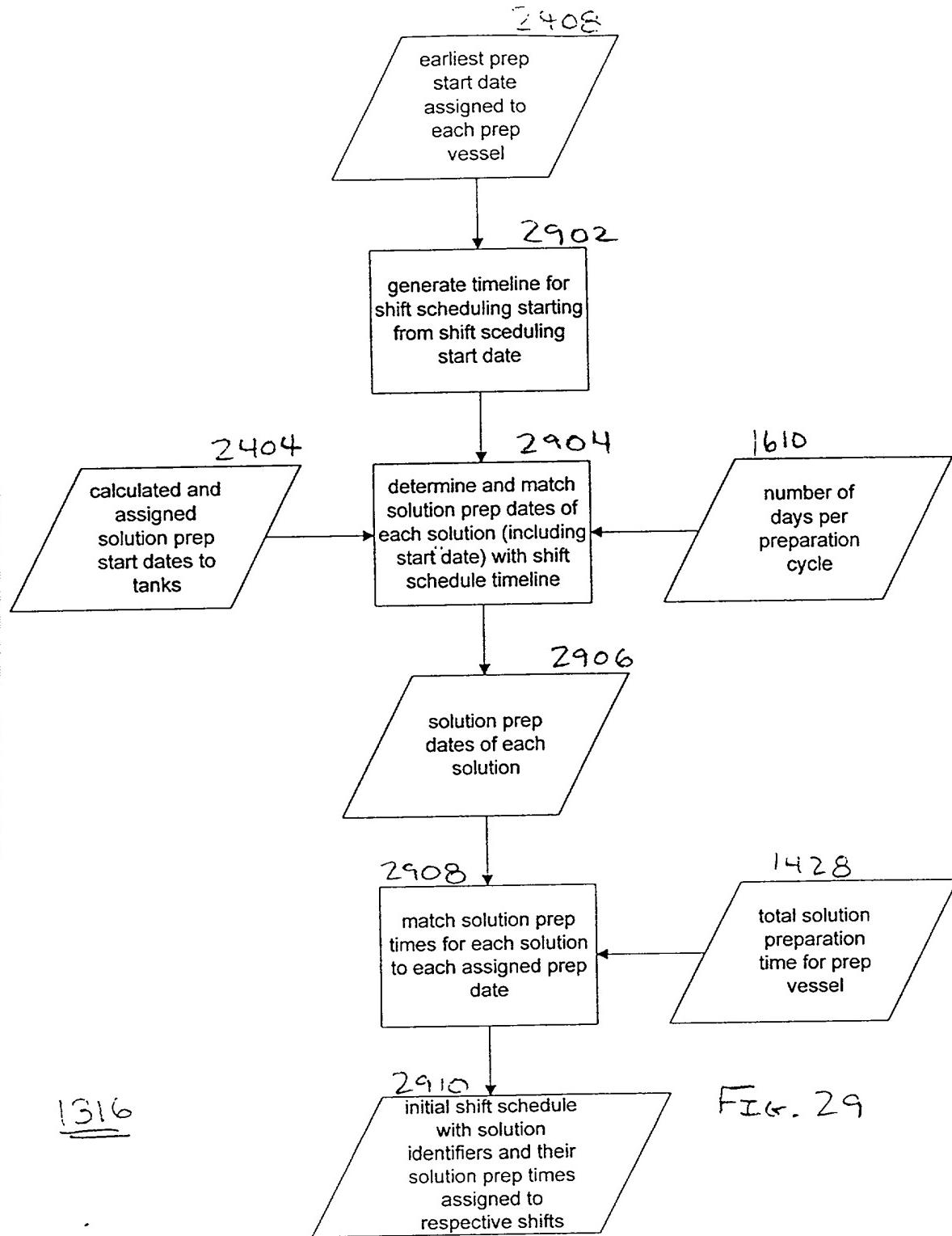
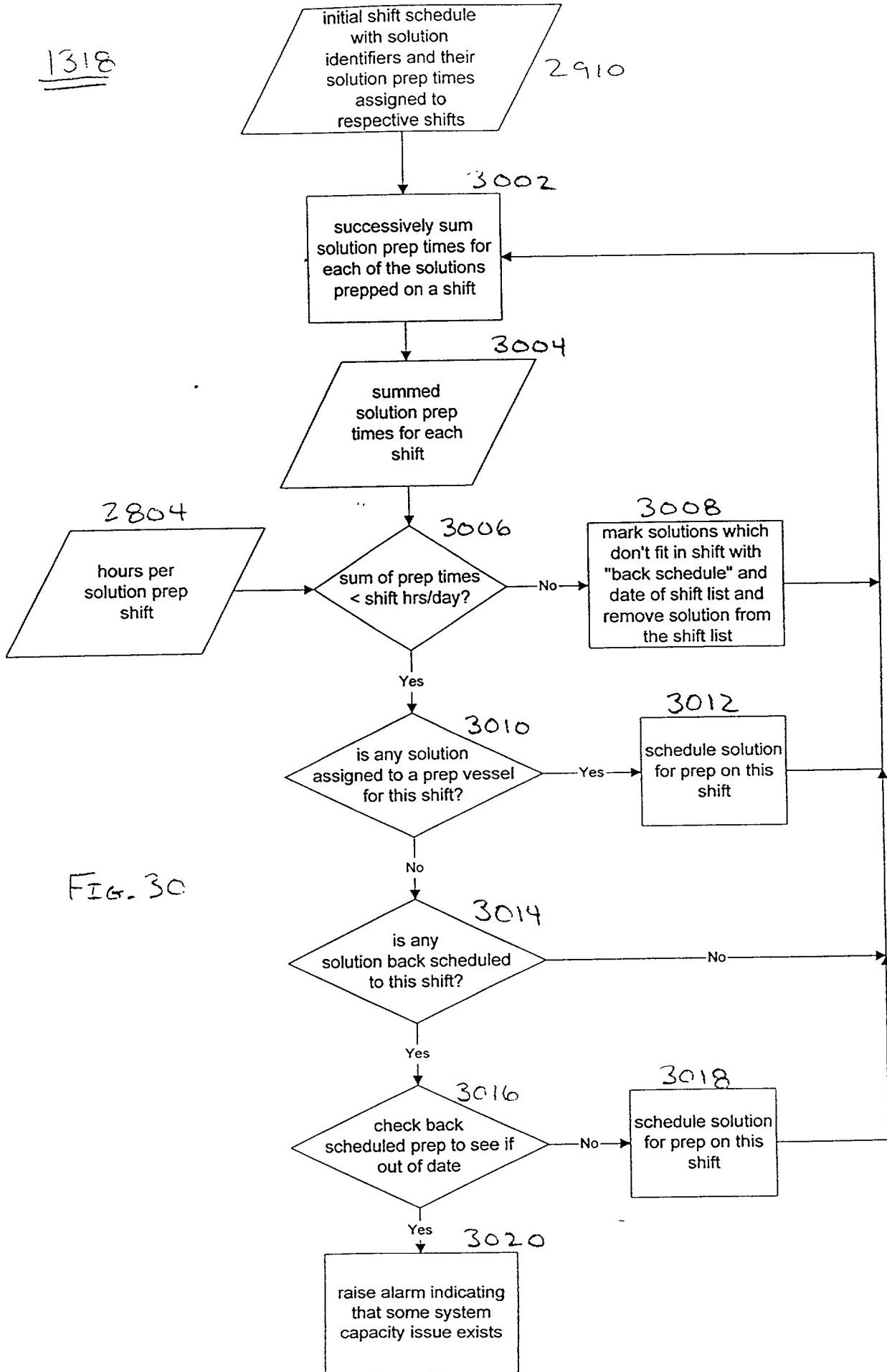


FIG. 29



Solution Prep Shift Schedule - Solution Prep Vessel 101

2804

Seqn.	Period	8 Hrs/Day		69		60		61		62		63		64		65		66		67		68	
		3.5	08/11/96	08/16/96	08/17/96	08/18/96	08/19/96	08/20/96	08/21/96	08/22/96	08/23/96	08/24/96	08/25/96	08/26/96	08/27/96	08/28/96	08/29/96	08/30/96	08/31/96	08/31/96	08/12/96		
S-0101																							
S-0102	13.2	56	02/14/96	04/10/96	04/10/96	04/10/96	04/10/96	04/10/96	04/10/96	04/10/96	04/10/96	04/10/96	04/10/96	04/10/96	04/10/96	04/10/96	04/10/96	04/10/96	04/10/96	04/10/96	04/10/96		
S-0103	1.7	7	05/22/96	05/22/96	05/22/96	05/22/96	05/22/96	05/22/96	05/22/96	05/22/96	05/22/96	05/22/96	05/22/96	05/22/96	05/22/96	05/22/96	05/22/96	05/22/96	05/22/96	05/22/96	05/22/96		
S-0104	8.1	7	05/22/96	05/22/96	05/22/96	05/22/96	05/22/96	05/22/96	05/22/96	05/22/96	05/22/96	05/22/96	05/22/96	05/22/96	05/22/96	05/22/96	05/22/96	05/22/96	05/22/96	05/22/96	05/22/96		
S-0105	8.3	7	05/22/96	05/22/96	05/22/96	05/22/96	05/22/96	05/22/96	05/22/96	05/22/96	05/22/96	05/22/96	05/22/96	05/22/96	05/22/96	05/22/96	05/22/96	05/22/96	05/22/96	05/22/96	05/22/96	05/22/96	
S-0106																							
S-0107																							
S-0108																							
S-0109	22.2	7	05/29/96	05/29/96	05/29/96	05/29/96	05/29/96	05/29/96	05/29/96	05/29/96	05/29/96	05/29/96	05/29/96	05/29/96	05/29/96	05/29/96	05/29/96	05/29/96	05/29/96	05/29/96	05/29/96	05/29/96	
S-0110																							
S-0111																							
S-0112																							
S-0113																							
S-0114																							
S-0115																							
S-0116																							
S-0117																							
S-0118																							
S-0119																							
S-0120																							
S-0121	0.0	7	05/29/96	05/29/96	05/29/96	05/29/96	05/29/96	05/29/96	05/29/96	05/29/96	05/29/96	05/29/96	05/29/96	05/29/96	05/29/96	05/29/96	05/29/96	05/29/96	05/29/96	05/29/96	05/29/96	05/29/96	
S-0122																							

1:10 7906

2:10 2

15 31

1320

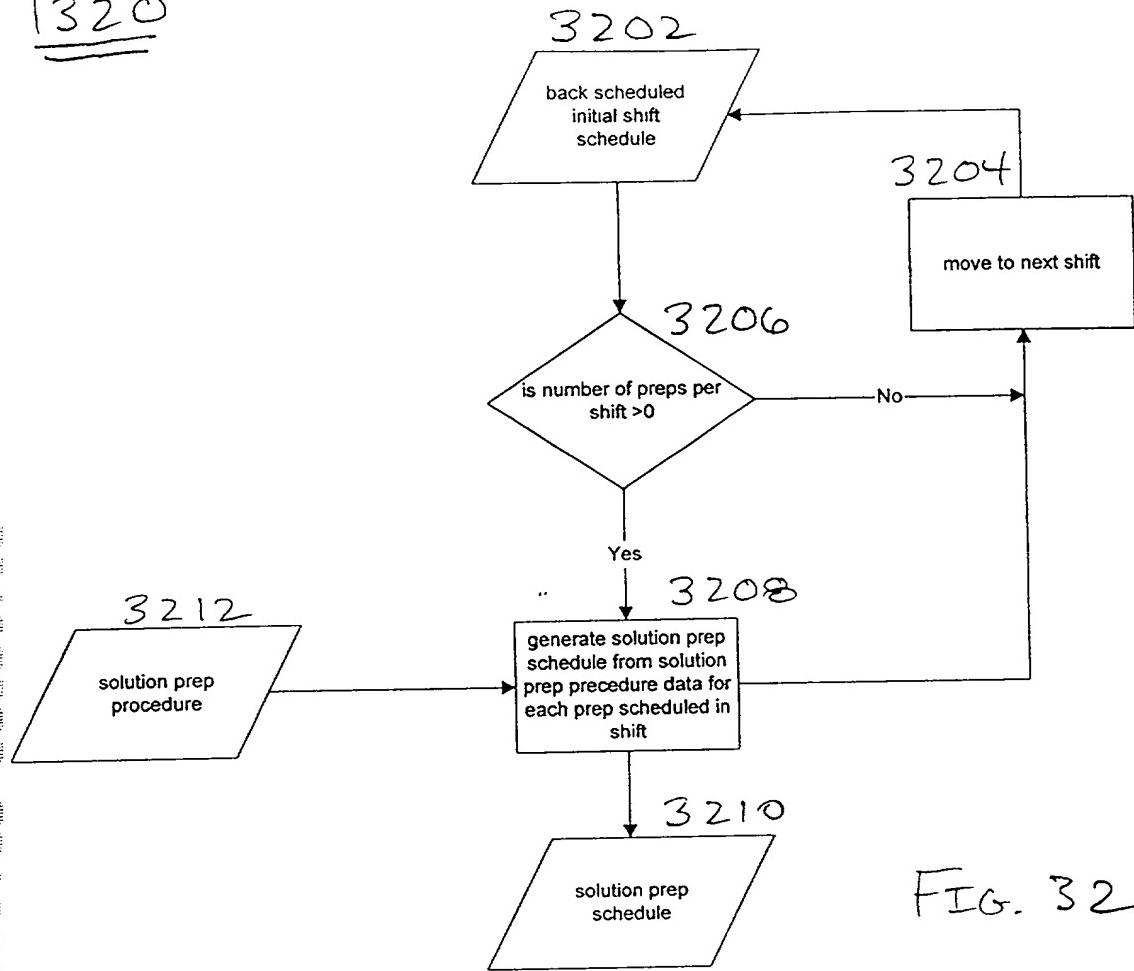
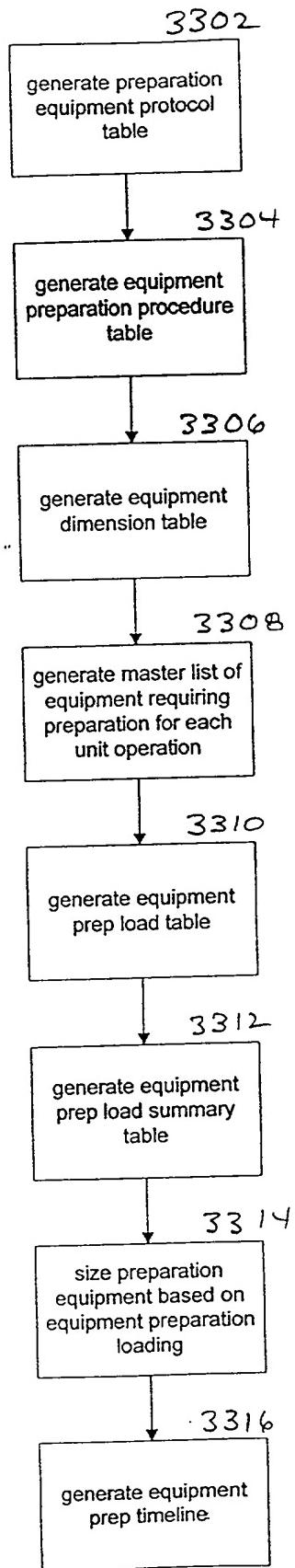
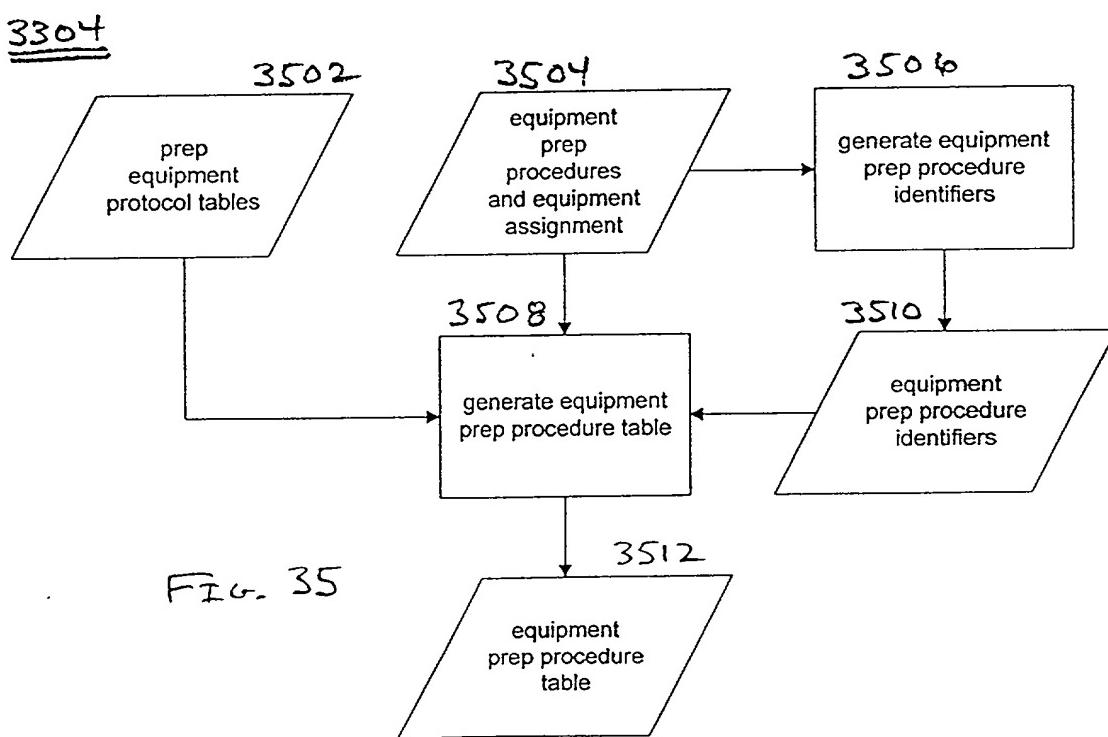
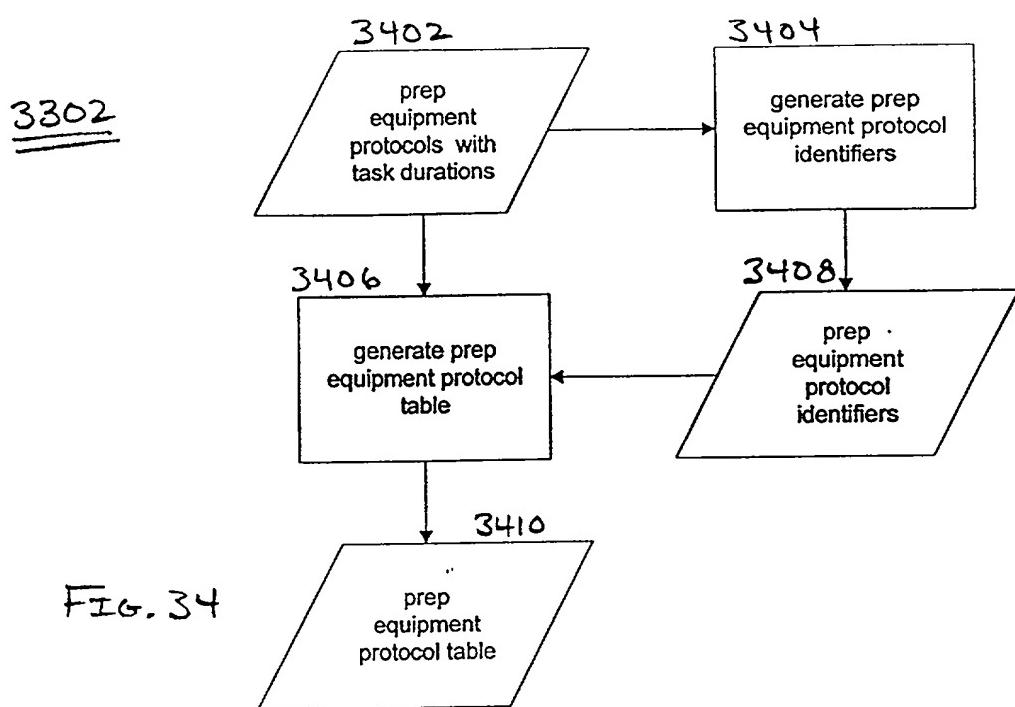


FIG. 32

FIG. 33





Prep Equipment Protocol - Bench Sink

3602 3604

Cycle Code	Load	Minutes/Cycle								Total
		Pre Wash Rinse		Detergent Wash			Post Wash Rinse		Final Rinse	
		NPHW	NPCW	Minutes	Reagent	Gm/CF	NPHW	NPCW		
1 BS-1	5	2	2	5	Alconox	0.5	2	2	2	20
2 BS-2	5	2	2	5	Alconox	0.5	2	2	2	20
3 BS-3	5	2	2	5	Alconox	0.5	2	2	2	20
4 BS-4	6	2	2	5	Alconox	0.5	2	2	2	20
5 BS-5	5	2	2	6	Alconox	0.5	2	2	2	20

Fig. 36A

Prep Equipment Protocol - Wash Station

3408

Protocol Cycle Code	Load	Minutes/Cycle						Final Rinse	Total
		Pre Wash Rinse		Detergent Wash			Post Wash Rinse		
		NPHW	NPCW	Minutes	Reagent	Gm/CF	NPHW	NPCW	
1 WS-1	5	2	2	5	Alconox	0.5	2	2	2 15
2 WS-2	5	2	2	5	Alconox	0.5	2	2	2 15
3 WS-3	5	2	2	5	Alconox	0.5	2	2	2 15
4 WS-4	5	2	2	5	Alconox	0.5	2	2	2 15
5 WS-5	5	2	2	5	Alconox	0.5	2	2	2 15

FIG. 36B

Prep Equipment Protocol - Glassware Washer

3408

Cycle Code	Load	Minutes/Cycle								Total	
		Pre Wash Rinse		Detergent Wash			Post Wash Rinse		Final Rinse		
		NPHW	NPCW	Minutes	Reagent	Gm/CF	NPHW	NPCW			
1	GW-1	15	2	2	5 Alconox	0.5	2	2	2	10	40
2	GW-2	15	2	2	6 Alconox	0.5	2	2	2	10	40
3	GW-3	15	2	2	5 Alconox	0.5	2	2	2	10	40
4	GW-4	15	2	2	5 Alconox	0.5	2	2	2	10	40
5	GW-5	15	2	2	5 Alconox	0.5	2	2	2	10	40

FIG. 36C

Prep Equipment Protocol - Glassware Dryer

	Cycle Code	Load	Heat Up Minutes	Dry		Cool Minutes	Unload	Total
				Temp (C)	Minutes			
1	DO-1	10	30	250	40	30	10	120
2	DO-2	10	30	250	25	30	10	105
3	DO-3	10	30	250	25	30	10	105
4	DO-4	10	30	250	25	30	10	105
5	DO-5	10	30	250	25	30	10	105

3618 3620 3622 3624 3626 3628

FIG. 36D

Prep Equipment Protocol - Carboy Washer

15 min
15 min

Load	Minutes/Cycle					Final Rinse	Unload	Total
	Pre Wash Rinse		Detergent		Post Wash Rinse			
	NPHW	NPCW	Minutes	Reagent	Gm/CF	NPHW	NPCW	
15	2	2	5	Alconox	0.5	2	2	15
15	2	2	5	Alconox	0.5	2	2	15
15	2	2	5	Alconox	0.5	2	2	15
15	2	2	5	Alconox	0.5	2	2	15
15	2	2	5	Alconox	0.5	2	2	15
15	2	2	5	Alconox	0.5	2	2	15

FIG. 36 E

Prep Equipment Protocol - Carboy Dryer

3400

	Cycle Code	Load	Heat Up Minutes	Dry		Cool Minutes	Unload	Total
				Temp (C)	Minutes			
1	CD-1	10	30	250	40	30	10	100
2	CD-2	10	30	250	25	30	10	85
3	CD-3	10	30	250	25	30	10	85
4	CD-4	10	30	250	25	30	10	85
5	CD-5	10	30	250	25	30	10	85

FIG. 36F

Prep Equipment Protocol - Steam Sterilizer

Cycles	SS-1						SS-2						SS-3						
	Press. (Bar)	Minutes To Ach.	Minutes To Hold	No. of Cycles	Subt.	Press. (Bar)	Minutes To Ach.	Minutes To Hold	No. of Cycles	Subt.	Press. (Bar)	Minutes To Ach.	Minutes To Hold	No. of Cycles	Subt.	Press. (Bar)	Minutes To Ach.	Minutes To Hold	
1 Load						20					20								20
2																			
3 Pre Sterilization																			
4 Deep Vacuum																			
5 Vacuum/Steam Pulse																			
6 Vacuum																			
7 Steam																			
8 Subtotal																			
9																			
10 Sterilization																			
11 Steam																			
12 Steam/Air																			
13 Subtotal																			
14																			
15 Cooling																			
16 Direct Air Cooling																			
17 Indirect Jacket Cooling																			
18 Overpressure																			
19 Subtotal																			
20																			
21 Drying																			
22 Fast Exhaust																			
23 Slow Exhaust																			
24 Deep Vacuum																			
25 Vacuum Pulse																			
26 Heat																			
27 Heated Pressure																			
28 Subtotal																			
29																			
30 Unload																			
31																			
32 Total Minutes																			
33 Total Hours																			

Fig. 365

Prep Equipment Protocol - Dry Heat Sterilizer

	Cycle Code	Load	Heat Up Minutes	Sterilization		Cool Minutes	Unload	Total
				Temp (C)	Minutes			
1	SO-1	15	30	250	40	30	15	130
2	SO-2	15	30	250	25	30	15	115
3	SO-3	15	30	250	25	30	15	115
4	SO-4	15	30	250	25	30	15	115
5	SO-5	15	30	250	25	30	15	115

340°

FIG. 36 H

Prep-Equipment Protocol - Equipment Prep Procedures

			EPC1	EPC2	EPC3	EPC4	EPC5	EPC6	EPC7
1	Initial Rinse								
2	Bench Sink - 1	Procedure Protocol							
3	Duration	PHrs.	BS-1 0.33	BS-1 0.33	BS-2 0.33	BS-1 0.33			
4	Hold/Dry	PHrs.	0	0	0				
5	Subtotal	PHrs.	0.33	0.33	0.33	0.33	0.00	0.00	0.00
6	Cumulative	PHrs.	0.33	0.33	0.33	0.33	0.00	0.00	0.00
10	Wash Station - 1	Procedure Protocol					WS-1 0.25	WS-1 0.25	
11	Duration	PHrs.	0.00	0.00	0.00	0.00	0.25	0.25	
12	Hold/Dry	PHrs.							
13	Subtotal	PHrs.	0.33333	0.33333	0.33333	0.33333	0.25	0.25	0.00
14	Cumulative	PHrs.					0	0	0
17	Cleaning								
19	Bench Sink - 1	Procedure Protocol							
20	Duration	PHrs.	BS-3 0.33	BS-3 0.33	BS-4 0.33				
21	Hold/Dry	PHrs.							
22	Subtotal	PHrs.	0.33	0.33	0.33	0.00	0.00	0.00	0.00
23	Cumulative	PHrs.	0.66667	0.66667	0.66667	0.33333	0	0	0
26	Glassware Washer - 1	Procedure Protocol					GW-1 0.67		
27	Duration	PHrs.	0.00	0.00	0.00	0.67	0.00	0.00	0.00
28	Hold/Dry	PHrs.							
29	Subtotal	PHrs.	0.66667	0.66667	0.66667	1	0	0	0
31	Cumulative	PHrs.					0	0	0
33	Glassware Dryer - 1	Procedure Protocol							
34	Duration	PHrs.	GD-1 2.00	GD-1 2.00	GD-2 1.75	GD-3 1.75			
35	Hold/Dry	PHrs.							
36	Subtotal	PHrs.	2.00	2.00	1.75	1.75	0.00	0.00	0.00
38	Cumulative	PHrs.	2.66667	2.66667	2.41667	2.75	0	0	0
40	Carboy Washer - 1	Procedure Protocol					CW-1 0.25	CW-1 0.25	
41	Duration	PHrs.	0.00	0.00	0.00	0.00	0.25	0.25	
42	Hold/Dry	PHrs.							
43	Subtotal	PHrs.	2.66667	2.66667	2.41667	2.75	0.25	0.25	0.00
45	Cumulative	PHrs.					0.25	0.25	0
47	Carboy Dryer - 1	Procedure Protocol					CD-1 1.67	CD-1 1.67	
48	Duration	PHrs.	0.00	0.00	0.00	0.00	1.67	1.67	
49	Hold/Dry	PHrs.							
50	Subtotal	PHrs.	2.66667	2.66667	2.41667	2.75	1.67	1.67	0.00
52	Cumulative	PHrs.					1.91667	1.91667	0
54	Prep								
55	Staffing		2	2	2	2	2	2	2
56	Preassembly								
57	Man Hours	MHrs.	1	0.5	.				
58	Procedure Hours								
59									
60									

FIG. 37-A

Prep Equipment Protocol - Equipment Prep Procedures

			EPC1	EPC2	EPC3	EPC4	EPC5	EPC6	EPC7
61	Cummulative	PHrs.	2.66667	3.16667	2.41667	2.75	1.91667	1.91667	0
62									
63	Wrap								
64	Man Hours	MHrs.	1.5	1.5	1.5	1.5	1.5	1.5	1.5
65	Procedure Hours		0.75	0.75	0.75	0.75	0.75	0.75	0.75
66	Cummulative	PHrs.	3.41667	3.91667	3.18667	3.5	2.66667	2.68667	0.75
67									
68	Sterilization								
69									
70	Autoclave - 1								
71	Procedure		SS-1	SS-1	SS-1	SS-1	SS-2		SS-3
72	Duration	PHrs.	2.68	2.68	2.68	2.68	3.25		3.83
73	Hold/Dry	PHrs.							
74	Subtotal	PHrs.	2.68	2.68	2.68	2.68	3.25	0.00	3.83
75	Cummulative	PHrs.	6.10	6.60	5.85	6.18	5.92	2.67	4.58
76									
77	Dry Heat - 1								
78	Procedure						SO-1		
79	Hours/Load	PHrs.					2.17		
80	Hold/Dry	PHrs.							
81	Subtotal	PHrs.	0.00	0.00	0.00	0.00	0.00	2.17	0.00
82	Cummulative	PHrs.	6.10	6.60	5.85	6.18	5.92	4.83	4.58
83									
84	Total		6.10	6.60	5.85	6.18	6.17	5.08	4.58
85									
86	Max		2.68	2.68	2.68	2.68	3.25	2.17	3.83

FIG. 37B

3306

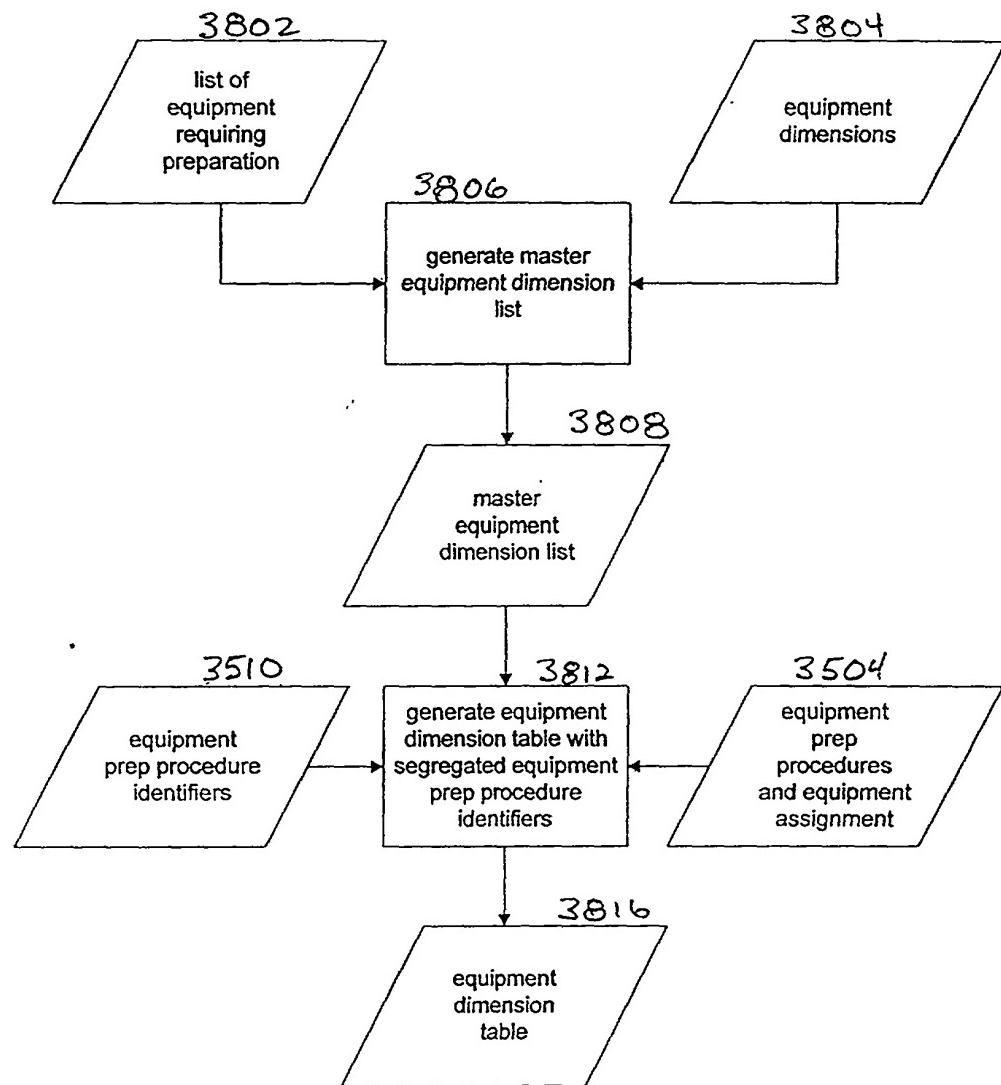


FIG. 38

Lead Configuration Table - General

3902

	EPIC-1	EPIC-2	EPIC-3	EPIC-4	EPIC-5	EPIC-6
Specimen Glass						
Spiral Tubes						
1 RFL needles	4	1	1	1	1	1
2 FIB needles	2	2	2	2	2	2
3 TMA needles	12	12	12	12	12	12
4	6	6	6	6	6	6
5	6	6	6	6	6	6
6	6	6	6	6	6	6
7	6	6	6	6	6	6
8	6	6	6	6	6	6
9	6	6	6	6	6	6
10	6	6	6	6	6	6
11	6	6	6	6	6	6
12	6	6	6	6	6	6
13	6	6	6	6	6	6
14	6	6	6	6	6	6
15	6	6	6	6	6	6
16	6	6	6	6	6	6
17	6	6	6	6	6	6
18	6	6	6	6	6	6
19	6	6	6	6	6	6
20	6	6	6	6	6	6
21	6	6	6	6	6	6
22	6	6	6	6	6	6
23	6	6	6	6	6	6
24	6	6	6	6	6	6
25	6	6	6	6	6	6
26	6	6	6	6	6	6
27	6	6	6	6	6	6
28	6	6	6	6	6	6
29	6	6	6	6	6	6
30	6	6	6	6	6	6
31	6	6	6	6	6	6
32	6	6	6	6	6	6
33	6	6	6	6	6	6
34	6	6	6	6	6	6
35	6	6	6	6	6	6
36	6	6	6	6	6	6
37	6	6	6	6	6	6
38	6	6	6	6	6	6
39	6	6	6	6	6	6
40	6	6	6	6	6	6
41	6	6	6	6	6	6
42	6	6	6	6	6	6
43	6	6	6	6	6	6
44	6	6	6	6	6	6
45	6	6	6	6	6	6
46	6	6	6	6	6	6
47	6	6	6	6	6	6
48	6	6	6	6	6	6
49	6	6	6	6	6	6
50	6	6	6	6	6	6
51	6	6	6	6	6	6
52	6	6	6	6	6	6
53	6	6	6	6	6	6
54	6	6	6	6	6	6
55	6	6	6	6	6	6
56	6	6	6	6	6	6
57	6	6	6	6	6	6
58	6	6	6	6	6	6
59	6	6	6	6	6	6
60	6	6	6	6	6	6
61	6	6	6	6	6	6
62	6	6	6	6	6	6
63	6	6	6	6	6	6
64	6	6	6	6	6	6
65	6	6	6	6	6	6
66	6	6	6	6	6	6
67	6	6	6	6	6	6
68	6	6	6	6	6	6
69	6	6	6	6	6	6
70	6	6	6	6	6	6
71	6	6	6	6	6	6
72	6	6	6	6	6	6
73	6	6	6	6	6	6
74	6	6	6	6	6	6
75	6	6	6	6	6	6
76	6	6	6	6	6	6
77	6	6	6	6	6	6
78	6	6	6	6	6	6
79	6	6	6	6	6	6
80	6	6	6	6	6	6
81	6	6	6	6	6	6
82	6	6	6	6	6	6
83	6	6	6	6	6	6
84	6	6	6	6	6	6
85	6	6	6	6	6	6
86	6	6	6	6	6	6
87	6	6	6	6	6	6
88	6	6	6	6	6	6
89	6	6	6	6	6	6
90	6	6	6	6	6	6
91	6	6	6	6	6	6
92	6	6	6	6	6	6
93	6	6	6	6	6	6
94	6	6	6	6	6	6
95	6	6	6	6	6	6
96	6	6	6	6	6	6
97	6	6	6	6	6	6
98	6	6	6	6	6	6
99	6	6	6	6	6	6
100	6	6	6	6	6	6
101	6	6	6	6	6	6
102	6	6	6	6	6	6
103	6	6	6	6	6	6
104	6	6	6	6	6	6
105	6	6	6	6	6	6
106	6	6	6	6	6	6
107	6	6	6	6	6	6
108	6	6	6	6	6	6
109	6	6	6	6	6	6
110	6	6	6	6	6	6
111	6	6	6	6	6	6
112	6	6	6	6	6	6
113	6	6	6	6	6	6
114	6	6	6	6	6	6
115	6	6	6	6	6	6
116	6	6	6	6	6	6
117	6	6	6	6	6	6
118	6	6	6	6	6	6
119	6	6	6	6	6	6
120	6	6	6	6	6	6
121	6	6	6	6	6	6
122	6	6	6	6	6	6
123	6	6	6	6	6	6
124	6	6	6	6	6	6
125	6	6	6	6	6	6
126	6	6	6	6	6	6
127	6	6	6	6	6	6
128	6	6	6	6	6	6
129	6	6	6	6	6	6
130	6	6	6	6	6	6
131	6	6	6	6	6	6
132	6	6	6	6	6	6
133	6	6	6	6	6	6
134	6	6	6	6	6	6
135	6	6	6	6	6	6
136	6	6	6	6	6	6
137	6	6	6	6	6	6
138	6	6	6	6	6	6
139	6	6	6	6	6	6
140	6	6	6	6	6	6
141	6	6	6	6	6	6
142	6	6	6	6	6	6
143	6	6	6	6	6	6
144	6	6	6	6	6	6
145	6	6	6	6	6	6
146	6	6	6	6	6	6
147	6	6	6	6	6	6
148	6	6	6	6	6	6
149	6	6	6	6	6	6
150	6	6	6	6	6	6
151	6	6	6	6	6	6
152	6	6	6	6	6	6
153	6	6	6	6	6	6
154	6	6	6	6	6	6
155	6	6	6	6	6	6
156	6	6	6	6	6	6
157	6	6	6	6	6	6
158	6	6	6	6	6	6
159	6	6	6	6	6	6
160	6	6	6	6	6	6
161	6	6	6	6	6	6
162	6	6	6	6	6	6
163	6	6	6	6	6	6
164	6	6	6	6	6	6
165	6	6	6	6	6	6
166	6	6	6	6	6	6
167	6	6	6	6	6	6
168	6	6	6	6	6	6
169	6	6	6	6	6	6
170	6	6	6	6	6	6
171	6	6	6	6	6	6
172	6	6	6	6	6	6
173	6	6	6	6	6	6
174	6	6	6	6	6	6
175	6	6	6	6	6	6
176	6	6	6	6	6	6
177	6	6	6	6	6	6
178	6	6	6	6	6	6
179	6	6	6	6	6	6
180	6	6	6	6	6	6
181	6	6	6	6	6	6
182	6	6	6	6	6	6
183	6	6	6	6	6	6
184	6	6	6	6	6	6
185	6	6	6	6	6	6
186	6	6	6	6	6	6
187	6	6	6	6	6	6
188	6	6	6	6	6	6
189	6	6	6	6	6	6
190	6	6	6	6	6	6
191	6	6	6	6	6	6
192	6	6	6	6	6	6
193	6	6	6	6	6	6
194	6	6	6	6	6	6
195	6	6	6	6	6	6
196	6	6	6	6	6	6
197	6	6	6	6	6	6
198	6	6	6	6	6	6
199	6	6	6	6	6	6
200	6	6	6	6	6	6
201	6	6	6	6	6	6
202	6	6	6	6	6	6
203	6	6	6	6	6	6
204	6	6	6	6	6	6
205	6	6	6	6	6	6
206	6	6	6	6	6	6
207	6	6	6	6	6	6
208	6	6	6	6	6	6
209	6	6	6	6	6	6
210	6	6	6	6	6	6
211	6	6	6	6	6	6
212	6	6	6	6	6	6
213	6	6	6	6	6	6
214	6	6	6	6	6	6
215	6	6	6	6	6	6
216	6	6	6	6	6	6
217	6	6	6	6	6	6
218	6	6	6	6	6	6
219	6	6	6	6	6	6
220	6	6	6	6	6	6
221	6	6	6	6	6	6
222	6	6	6	6	6	6
223	6	6	6	6	6	6
224	6	6	6	6	6	6
225	6	6	6	6	6	6
226	6	6	6	6	6	6
227	6	6	6	6	6	6
228	6	6	6	6	6	6
229	6</					

3308

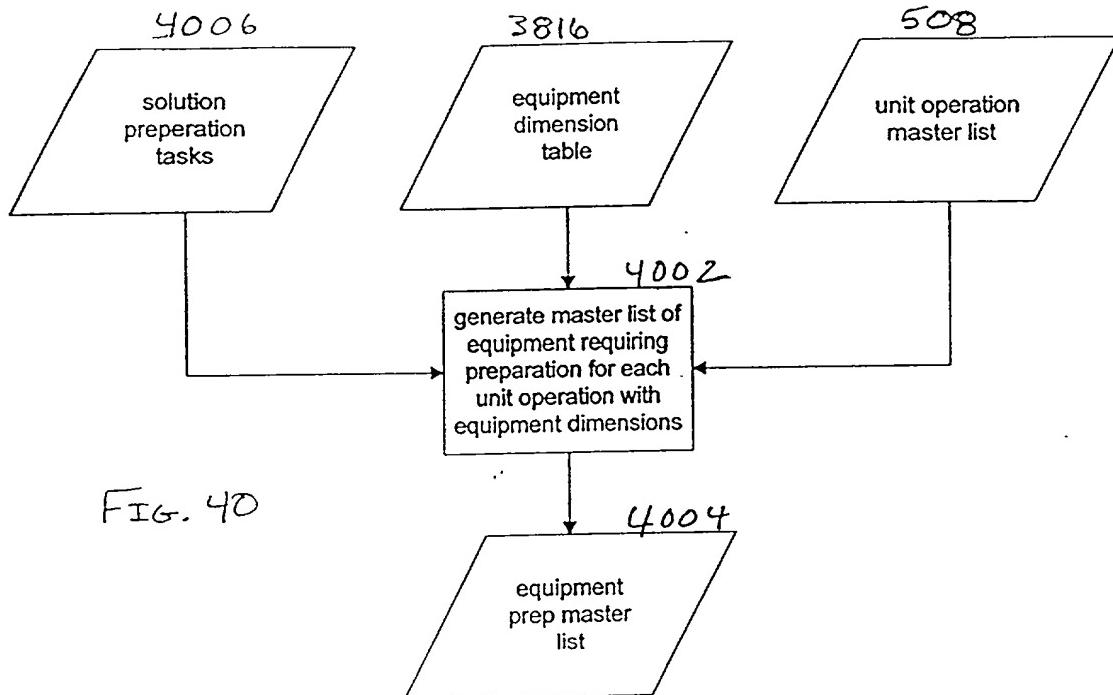


FIG. 40

3310

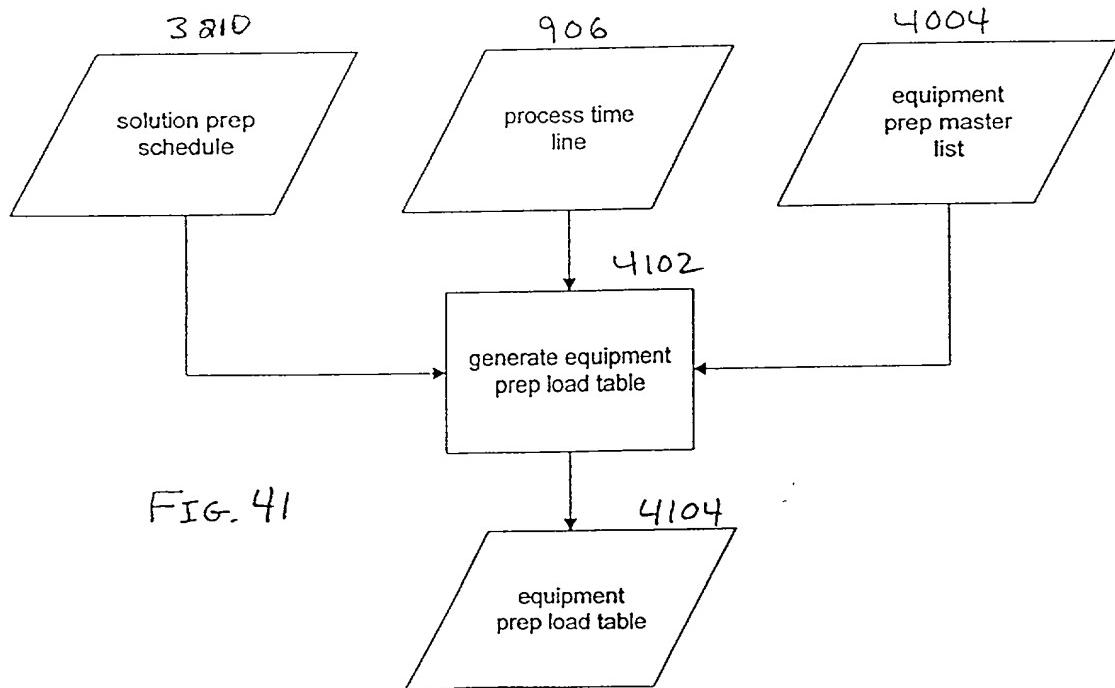


FIG. 41

4202 4204 4206 Equipment Prep Load Table 4208

Task	Equipment Item	EPC-1		EPC-2		EPC-3	
		Unit Date	Open Time	Specially Glass Siphon Tubes	Instruments	Fittings	Total
				Total	Pi DO Probe pH Probe	Tees Elbows Crosses Reducers	Plasticware Beakers
					0.03 0.08	0.03 0.02 0.06 0.01	0.03
1 Inoculum Prep	06/04/96	02:30 PM		0			
2 Flask Growth	06/05/96	01:30 PM		0			
3 Seed Fermentation	06/06/96	03:30 PM		0			
4 Fermentation	06/07/96	12:00 PM		0 4		2 4	
5 Heat Exchange	06/07/96	01:00 PM		0 3	0.111	0.17 0.03	0.00
6 Cont. Cent/Solids	06/07/96	11:51 AM		0 3	4	4 4	0.00
1 Inoculum Prep	06/06/96	02:30 PM		0 0.083	0.111	0.03	
2 Flask Growth	06/07/96	01:30 PM		0			
3 Seed Fermentation	06/08/96	03:30 PM		0			
4 Fermentation	08/09/96	09:00 AM		0 4		2 4	
5 Heat Exchange	06/09/96	10:00 AM		0 0.111	0.17	0.03 0.03	0.50
6 Cont. Cent/Solids	06/09/96	08:51 AM		0 3	4	4 4	0.22
1 Inoculum Prep	06/09/96	02:30 PM		0 0.083	0.111	0.03 0.03	0.31
2 Flask Growth	06/09/96	01:30 PM		0			
3 Seed Fermentation	06/10/96	03:30 PM		0			
4 Fermentation	06/03/96	10:00 AM		0 4		2 4	
5 Heat Exchange	06/11/96	08:00 AM		0 3	0.111	0.17 0.03	0.50
6 Cont. Cent/Solids	06/11/96	08:51 AM		0 0.083	0.111	4 4	0.31
7 Cell Resuspension	06/11/96	12:15 PM		0 3	4	0.03 0.03	0.31
8 Heat Exchange	06/11/96	09:33 AM		0	0.111	4 4	0.08
9 Cell Disruption	06/11/96	08:51 AM		0			0.00
10 Heat Exchange	06/11/96	10:09 AM		0			0.00

Fr. 4/7 A

4210 4212

4214

4216

Equipment Items	Unit Oper Date	End Time	EPC-4			EPC-5			EPC-6				
			Flasks 0.25	Rubber Stoppers Silicone 0.00	Flexible Tubing Butyl 0.03	Total CF 3.33	Small Glassware Beakers 0.03125	Total CF 0.25	PP Carboys 10L 1.3333	BSG Carboys 20L 4.88	Total CF 10.7	BSG Carboys 10L 1.3333	Total CF 20L 4.88
1 Inoculum Prep	06/04/96	02:30 PM											
2 Flask Growth	06/05/96	01:30 PM											
3 Seed Fermentation	06/06/96	03:30 PM	4	4	1.33	1.35	1.00	1	4	0			
4 Fermentation	06/07/96	12:00 PM	4	4	1.33	1.35			5.33		5.33		
5 Heat Exchange	06/07/96	01:00 PM				0.00		0			0.00		
6 Cont. Cent/Solids	06/07/96	11:51 AM				0.00							
1 Inoculum Prep	06/06/96	02:30 PM				0.00			0		0.00		
2 Flask Growth	06/07/96	01:30 PM				0.00			1.25	1.25	0.00		
3 Seed Fermentation	06/08/96	03:30 PM				0.00			5	0	0.00		
4 Fermentation	06/09/96	08:00 AM				0.00			1.25	1.25	0.00		
5 Heat Exchange	06/09/96	10:00 AM				0.00			0	0.00	0.00		
6 Cont. Cent/Solids	06/09/96	08:51 AM				0.00			0	0.00	0.00		
1 Inoculum Prep	06/08/96	02:30 PM				0.00			5	0	0.00		
2 Flask Growth	06/09/96	01:30 PM				0.00			1.25	1.25	0.00		
3 Seed Fermentation	06/10/96	03:30 PM				0.00			6	0	0.00		
4 Fermentation	06/03/96	10:00 AM				0.00			1.25	1.25	0.00		
5 Heat Exchange	06/11/96	09:51 AM				0.00			0	0.00	0.00		
6 Cont. Cent/Solids	06/11/96	08:51 AM				0.00			0	0.00	0.00		
7 Cell Resuspension	06/11/96	12:15 PM				0.00			0	0.00	0.00		
8 Heat Exchange	06/11/96	09:33 AM				0.00			0	0.00	0.00		
9 Cell Disruption	06/11/96	09:51 AM				0.00			0	0.00	0.00		
10 Heat Exchange	06/11/96	10:08 AM				0.00			6	1.25	1.25	0.00	0.00

Fig. 42B

4718

Equipment Prep Load Table

4220

Equipment Items	Unit Open Date	End Time	EPC-1			EPC-2			EPC-3								
			Specialty Glass	Siphon Tubes	Total	Instruments	Pi 0.03	DO Probe 0.06	pH Probe 0.06	Fittings	Tees 0.03	Elbows 0.02	Crosses 0.06	Reducers 0.01	Hose Barb 0.01	Clamps 0.01	Total CF
8 Heat Exchange	06/11/96	10:27 AM			0												0.00
9 Cell Disruption	06/11/96	10:46 AM			0												0.00
10 Heat Exchange	06/11/96	12:00 AM			0												0.00
8 Heat Exchange	06/11/96	02:21 PM			0												0.00
9 Cell Disruption	06/11/96	02:39 PM			0												0.00
10 Heat Exchange	06/11/96	02:57 PM			0												0.00
11 IB Resuspension	06/11/96	10:57 AM			0												0.00
12 Centrifugation	06/11/96	11:33 AM			0												0.00
11 IB Resuspension	06/11/96	03:06 PM			0												0.00
12 Centrifugation	06/11/96	03:12 PM			0												0.00
13 Renaturation	06/12/96	08:43 AM			0												0.00
14 Buffer Exchange	06/12/96	11:47 AM			0												0.00
15 Clarification	06/12/96	11:03 AM			0												0.00
16 Chromatography 1	06/12/96	03:59 PM			0												0.00
17 Chromatography 2	06/12/96	06:59 PM			0												0.00
18 Buffer Exchange	06/12/96	03:27 PM			0												0.00
19 Chromatography 3	06/12/96	10:07 PM			0												0.00
20 Buffer Exchange	06/12/96	10:38 PM			0												0.00
21 Chromatography 4	06/13/96	12:14 AM			0												0.00
22 Sterile Filtration	06/13/96	12:48 AM			0												0.00
Totals																	3.26

Fig. 42C.

Equipment Top Load Table

4228

4226

Equipment Item	Unit Open Date	End Time	EPC-4			EPC-5			EPC-6			
			Flasks	Rubber Stoppers	Flexible Tubing	Total Small Glassware	Beakers	Flasks	Total PP Cartboys	10L CF	20L CF	Total BSG Cartboys
8 Heat Exchange	06/11/96	10:27 AM	0.25	0.00	0.03	0.33	Neoprene	3.33	0.03125	0.25	1.35333	4.88
9 Cell Disruption	06/11/96	10:45 AM										
10 Heat Exchange	06/11/96	12:00 AM										
8 Heat Exchange	06/11/96	02:21 PM										
9 Cell Disruption	06/11/96	02:39 PM										
10 Heat Exchange	06/11/96	02:57 PM										
11 IB Resuspension	06/11/96	10:57 AM										
12 Centrifugation	06/11/96	11:33 AM										
11 IB Resuspension	06/11/96	03:06 PM										
12 Centrifugation	06/11/96	03:12 PM										
13 Renaturation	06/12/96	08:43 AM										
14 Buffer Exchange	06/12/96	11:47 AM										
15 Clarification	06/12/96	11:03 AM										
16 Chromatography 1	06/12/96	03:59 PM										
17 Chromatography 2	06/12/96	06:59 PM										
18 Buffer Exchange	06/12/96	08:27 PM										
19 Chromatography 3	06/12/96	10:07 PM										
20 Buffer Exchange	06/12/96	10:38 PM										
21 Chromatography 4	06/13/96	12:14 AM										
22 Sterile Filtration	06/13/96	12:48 AM										
Totals												

Fig. 42D

3312

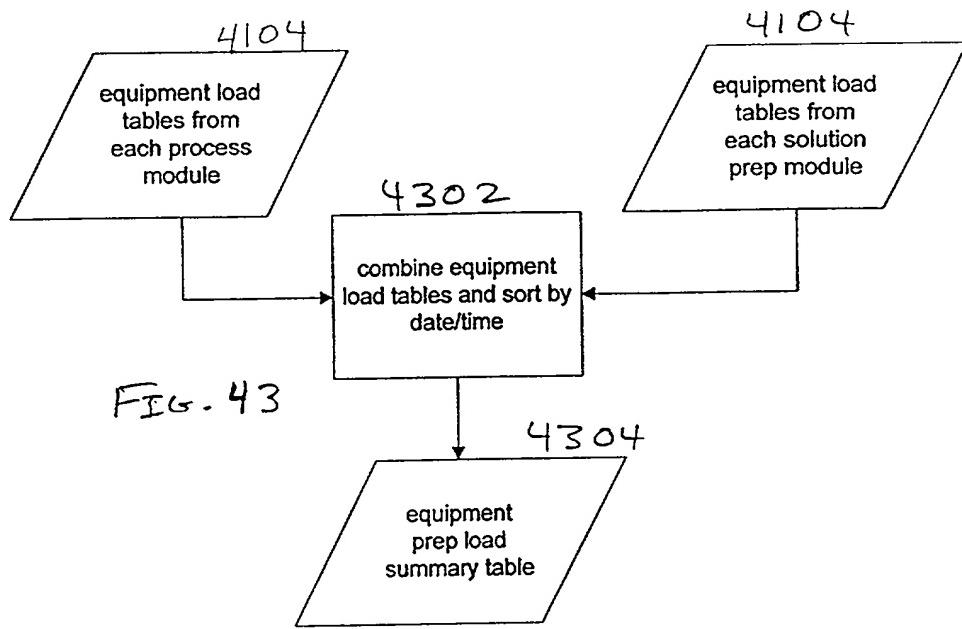


FIG. 43

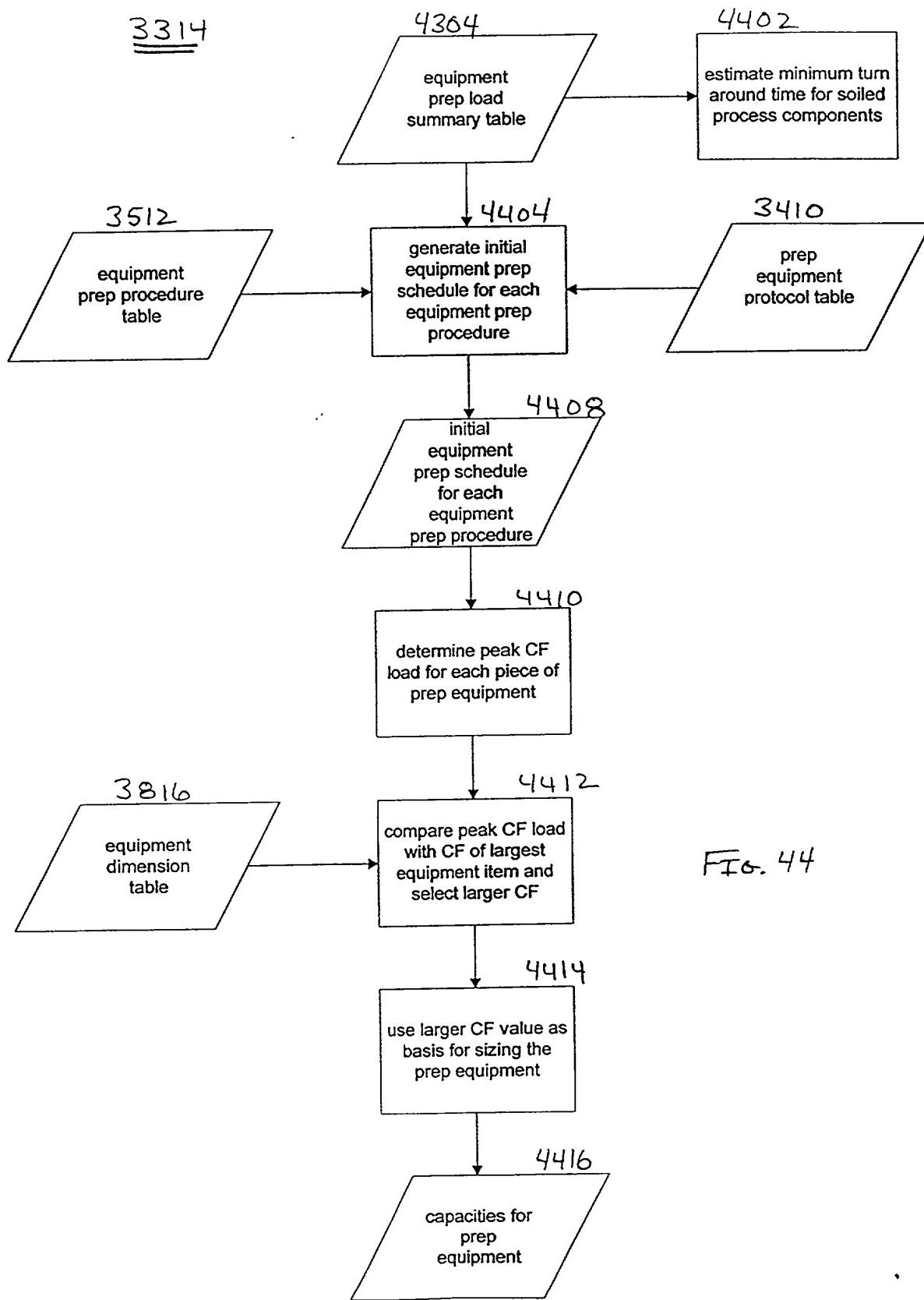


FIG. 44

四百五

QC Load Table - PE Module

丁
四
五
丁

4502

Fig. 45A.

QC Load Table - PE Module

4564

	Operation	QA/QC Samples												Immunochemical	Act.									
		Start		Finish		Visual		Chemical		Biochemical														
		Start	Date	Start	Date	Time	AV-1	AV-2	AC-1	AC-2	AC-3	AC-4	AC-5	AC-6	AB-1	AB-2	AB-3	AB-4	AB-5	AB-6	AB-7	AI-1	AI-2	AA-1
48	Centrifugation	06/03/96	08:00 AM	06/03/96	09:00 AM	06/07/96	10:00 AM																	
49	Wash	06/07/96	10:00 AM	06/07/96	10:00 AM	06/07/96	10:06 AM																	
50	CIP	06/07/96	10:06 AM	06/07/96	10:21 AM	06/07/96	10:21 AM																	
51	SIP	06/07/96	10:21 AM	06/07/96	11:21 AM	06/07/96	11:51 AM																	
52	Clean Up																							
53	Sub Total																							
54																								
55	1 B Inoculum Prop																							
56																								
57	Set Up	06/03/96	01:30 PM	06/03/96	02:30 PM	06/03/96	03:30 PM	06/04/96	04:30 PM	06/04/96	05:30 PM	06/04/96	06:30 PM	06/04/96	07:30 PM	06/04/96	08:30 PM	06/04/96	09:30 PM	06/04/96	10:30 PM	06/04/96		
58	Preincubation	06/03/96	06/03/96	06/03/96	06/03/96	06/04/96	06/04/96	06/04/96	06/04/96	06/04/96	06/04/96	06/04/96	06/04/96	06/04/96	06/04/96	06/04/96	06/04/96	06/04/96	06/04/96	06/04/96	06/04/96	06/04/96		
59	Incubation																							
60	Clean Up																							
61	Subtotal																							
62	2 B Flask Growth																							
63																								
64	Set Up	06/04/96	12:30 PM	06/04/96	01:30 PM	06/04/96	02:30 PM	06/04/96	03:30 PM	06/04/96	04:30 PM	06/04/96	05:30 PM	06/04/96	06:30 PM	06/04/96	07:30 PM	06/04/96	08:30 PM	06/04/96	09:30 PM	06/04/96		
65	Preincubation	06/04/96	06/04/96	06/04/96	06/04/96	06/04/96	06/04/96	06/04/96	06/04/96	06/04/96	06/04/96	06/04/96	06/04/96	06/04/96	06/04/96	06/04/96	06/04/96	06/04/96	06/04/96	06/04/96	06/04/96	06/04/96		
66	Incubation																							
67	Clean Up																							
68	Subtotal																							
69	3 B Seed Fermentation																							
70																								
71	Set Up	06/05/96	11:30 AM	06/05/96	12:30 PM	06/05/96	01:30 PM	06/05/96	02:30 PM	06/05/96	03:30 PM	06/05/96	04:30 PM	06/05/96	05:30 PM	06/05/96	06:30 PM	06/05/96	07:30 PM	06/05/96	08:30 PM	06/05/96		
72	Preincubation	06/05/96	06/05/96	06/05/96	06/05/96	06/05/96	06/05/96	06/05/96	06/05/96	06/05/96	06/05/96	06/05/96	06/05/96	06/05/96	06/05/96	06/05/96	06/05/96	06/05/96	06/05/96	06/05/96	06/05/96	06/05/96		
73	Fermentation																							
74	Harvest																							
75	CIP																							
76	SIP																							
77	Clean Up																							
78	Subtotal																							
79																								
80	4 B Production Fermentation																							
81																								
82	Set Up	06/06/96	09:00 AM	06/06/96	10:00 AM	06/06/96	11:00 AM	06/06/96	12:00 PM	06/06/96	01:00 PM	06/06/96	02:00 PM	06/06/96	03:00 PM	06/06/96	04:00 PM	06/06/96	05:00 PM	06/06/96	06:00 PM	06/06/96		
83	Preincubation	06/06/96	11:00 AM	06/06/96	08:00 AM	06/06/96	09:00 AM	06/06/96	10:00 AM	06/06/96	11:00 AM	06/06/96	12:00 PM	06/06/96	01:00 PM	06/06/96	02:00 PM	06/06/96	03:00 PM	06/06/96	04:00 PM	06/06/96		
84	Fermentation																							
85	CIP																							
86	SIP																							
87	Clean Up																							
88	Subtotal																							
89																								
90	5 B Heat Exchange																							
91																								
92	Set Up	06/07/96	08:00 AM	06/07/96	09:00 AM	06/07/96	10:00 AM	06/07/96	11:00 AM	06/07/96	12:00 PM	06/07/96	01:00 PM	06/07/96	02:00 PM	06/07/96	03:00 PM	06/07/96	04:00 PM	06/07/96	05:00 PM	06/07/96		
93	Transfer																							
94	CIP																							

FIG. 45B

3

2

1

0

QC Load Table - PE Module

Operation	QA/QC Samples												Immunological Act.																																
	Start Date			Finish Date			Visual Time			Chemical Time			Biochemical			AB-1			AB-2			AB-3			AB-4			AB-5			AB-6			AB-7			AI-1			AI-2			AA-1		
							AV-1	AV-2	AC-1	AC-2	AC-3	AC-4	AC-5	AC-6	AB-1	AB-2	AB-3	AB-4	AB-5	AB-6	AB-7	AI-1	AI-2	AA-1																					
95 SIP		06/03/96	08:00 AM																																										
96 Clean Up		06/07/96	10:00 AM	06/07/96	11:00 AM	06/07/96																																							
97 Subtotal																																													
98 6 B Cont. Cent./Solids																																													
100 Set Up		06/07/96	08:00 AM																																										
101 Centrifugation		06/07/96	08:00 AM	06/07/96	10:00 AM	06/07/96																																							
102 Wash		06/07/96	10:00 AM	06/07/96	10:06 AM	06/07/96																																							
103 CIP		06/07/96	10:21 AM	06/07/96	11:21 AM	06/07/96																																							
104 SIP		06/07/96	11:21 AM	06/07/96	11:51 AM	06/07/96																																							
105 Clean Up																																													
106 Subtotal																																													
107 Total																																													
108																																													
109 1 C Inoculum Prep																																													
110 Set Up		06/03/96	01:30 PM	06/03/96	02:30 PM	06/03/96																																							
111 Preincubation		06/03/96	03:30 PM	06/03/96	02:30 PM	06/03/96																																							
112 Incubation		06/04/96	01:30 PM	06/04/96	02:30 PM	06/04/96																																							
113 Clean Up		06/04/96	02:30 PM	06/04/96	01:30 PM	06/04/96																																							
114 Subtotal																																													
115 2 C Flask Growth																																													
116 Set Up		06/04/96	12:30 PM	06/04/96	01:30 PM	06/04/96																																							
117 Preincubation		06/04/96	01:30 PM	06/04/96	02:30 PM	06/04/96																																							
118 Incubation		06/04/96	02:30 PM	06/04/96	01:30 PM	06/04/96																																							
119 Clean Up		06/05/96	01:30 PM	06/05/96	02:30 PM	06/05/96																																							
120 Subtotal																																													
121 3 C Seed Fermentation																																													
122 Set Up		06/05/96	11:30 AM	06/05/96	12:30 PM	06/05/96																																							
123 Preincubation		06/05/96	12:30 PM	06/05/96	01:30 PM	06/05/96																																							
124 Fermentation		06/05/96	01:30 PM	06/05/96	10:30 AM	06/05/96																																							
125 Harvest		06/05/96	10:30 AM	06/05/96	11:30 AM	06/05/96																																							
126 CIP		06/05/96	11:30 AM	06/05/96	12:30 PM	06/05/96																																							
127 SIP		06/05/96	12:30 PM	06/05/96	01:30 PM	06/05/96																																							
128 Clean Up		06/05/96	01:30 PM	06/05/96	02:30 PM	06/05/96																																							
129 Subtotal																																													
130 4 C Production Fermentation																																													
131 Set Up		06/06/96	09:00 AM	06/06/96	10:00 AM	06/06/96																																							
132 Preincubation		06/06/96	10:00 AM	06/06/96	11:00 AM	06/06/96																																							
133 Fermentation		06/06/96	11:00 AM	06/06/96	08:00 AM	06/06/96																																							
134 Subtotal																																													
135 1 C Production Fermentation																																													
136 Set Up		06/06/96	10:00 AM	06/06/96	11:00 AM	06/06/96																																							
137 Preincubation		06/06/96	11:00 AM	06/06/96	08:00 AM	06/06/96																																							
138 Fermentation		06/06/96	08:00 AM	06/06/96	09:00 AM	06/06/96																																							
139 CIP		06/07/96	08:00 AM	06/07/96	09:00 AM	06/07/96																																							
140 SIP		06/07/96	09:00 AM	06/07/96	10:00 AM	06/07/96																																							
141 Clean Up		06/07/96	10:00 AM	06/07/96	12:00 PM	06/07/96																																							

Fig. 45C

QC Load Table - PE Module

四五〇

QC Load Table - PE Module

	Operation	Start		Finish		QA/QC Samples										Biochemical				Immunological				Act.	
		Date	Time	Date	Time	AV-1	AV-2	AC-1	AC-2	AC-3	AC-4	AC-5	AC-6	AB-1	AB-2	AB-3	AB-4	AB-5	AB-6	AB-7	AI-1	AI-2	AA-1		
191	10 A Heat Exchange			06/03/96	08:00 AM																				
192	Set Up			06/07/96	12:04 PM	06/07/96	12:34 PM	06/07/96	12:52 PM	06/07/96	12:52 PM	06/07/96	12:52 PM												
193	Transfer			06/07/96	12:34 PM	06/07/96	12:52 PM	06/07/96	12:52 PM	06/07/96	12:52 PM	06/07/96	12:52 PM												
194	CIP			06/07/96	12:52 PM	06/07/96	12:52 PM	06/07/96	12:52 PM	06/07/96	12:52 PM	06/07/96	12:52 PM												
195	SIP			06/07/96	12:52 PM	06/07/96	12:52 PM	06/07/96	12:52 PM	06/07/96	12:52 PM	06/07/96	12:52 PM												
196	Clean Up			06/07/96	12:52 PM	06/07/96	12:52 PM	06/07/96	12:52 PM	06/07/96	12:52 PM	06/07/96	12:52 PM												
197	Subtotal																								
198																									
199	8 B Heat Exchange																								
200																									
201	Set Up			06/07/96	12:52 PM	06/07/96	12:52 PM	06/07/96	12:52 PM	06/07/96	12:52 PM	06/07/96	12:52 PM												
202	Transfer			06/07/96	12:52 PM	06/07/96	12:52 PM	06/07/96	12:52 PM	06/07/96	12:52 PM	06/07/96	12:52 PM												
203	CIP			06/07/96	01:10 PM	06/07/96	01:10 PM	06/07/96	01:10 PM	06/07/96	01:10 PM	06/07/96	01:10 PM												
204	SIP			06/07/96	01:10 PM	06/07/96	01:10 PM	06/07/96	01:10 PM	06/07/96	01:10 PM	06/07/96	01:10 PM												
205	Clean Up			06/07/96	01:10 PM	06/07/96	01:10 PM	06/07/96	01:10 PM	06/07/96	01:10 PM	06/07/96	01:10 PM												
206	Subtotal																								
207																									
208	9 B Homogenization																								
209																									
210	Set Up			06/07/96	01:10 PM	06/07/96	01:10 PM	06/07/96	01:10 PM	06/07/96	01:10 PM	06/07/96	01:10 PM												
211	Lysis			06/07/96	01:51 PM	06/07/96	01:51 PM	06/07/96	01:51 PM	06/07/96	01:51 PM	06/07/96	01:51 PM												
212	CIP			06/07/96	01:51 PM	06/07/96	01:51 PM	06/07/96	01:51 PM	06/07/96	01:51 PM	06/07/96	01:51 PM												
213	SIP			06/07/96	01:51 PM	06/07/96	01:51 PM	06/07/96	01:51 PM	06/07/96	01:51 PM	06/07/96	01:51 PM												
214	Clean Up			06/07/96	01:51 PM	06/07/96	01:51 PM	06/07/96	01:51 PM	06/07/96	01:51 PM	06/07/96	01:51 PM												
215	Sub Total																								
216																									
217	10 B Heat Exchange																								
218																									
219	Set Up			06/07/96	01:21 PM	06/07/96	01:21 PM	06/07/96	01:21 PM	06/07/96	01:21 PM	06/07/96	01:21 PM												
220	Transfer			06/07/96	02:09 PM	06/07/96	02:09 PM	06/07/96	02:09 PM	06/07/96	02:09 PM	06/07/96	02:09 PM												
221	CIP			06/07/96	02:09 PM	06/07/96	02:09 PM	06/07/96	02:09 PM	06/07/96	02:09 PM	06/07/96	02:09 PM												
222	SIP			06/07/96	02:09 PM	06/07/96	02:09 PM	06/07/96	02:09 PM	06/07/96	02:09 PM	06/07/96	02:09 PM												
223	Clean Up			06/07/96	02:09 PM	06/07/96	02:09 PM	06/07/96	02:09 PM	06/07/96	02:09 PM	06/07/96	02:09 PM												
224	Subtotal																								
225																									
226	8 C Heat Exchange																								
227																									
228	Set Up			06/07/96	02:09 PM	06/07/96	02:09 PM	06/07/96	02:09 PM	06/07/96	02:09 PM	06/07/96	02:09 PM												
229	Transfer			06/07/96	02:09 PM	06/07/96	02:09 PM	06/07/96	02:09 PM	06/07/96	02:09 PM	06/07/96	02:09 PM												
230	CIP			06/07/96	02:27 PM	06/07/96	02:27 PM	06/07/96	02:27 PM	06/07/96	02:27 PM	06/07/96	02:27 PM												
231	SIP			06/07/96	03:27 PM	06/07/96	03:27 PM	06/07/96	03:27 PM	06/07/96	03:27 PM	06/07/96	03:27 PM												
232	Clean Up			06/07/96	04:27 PM	06/07/96	04:27 PM	06/07/96	04:27 PM	06/07/96	04:27 PM	06/07/96	04:27 PM												
233	Subtotal																								
234																									
235	9 C Homogenization			06/07/96	02:27 PM	06/07/96	02:27 PM	06/07/96	02:27 PM	06/07/96	02:27 PM	06/07/96	02:27 PM												
236																									
237	Set Up			06/07/96	02:27 PM	06/07/96	02:27 PM	06/07/96	02:27 PM	06/07/96	02:27 PM	06/07/96	02:27 PM												
238	Lysis			06/07/96	03:07 PM	06/07/96	03:07 PM	06/07/96	03:07 PM	06/07/96	03:07 PM	06/07/96	03:07 PM												
239																									

FIG. 45E

QC Load Table - PE Module

454

QC Load Table - PE Module

		QA/QC Samples												Immunochemical	Act.								
		Visual			Chemical			Biochemical															
Operation	Start Date	Finish Date	Time	Time	AV-1	AV-2	AC-1	AC-2	AC-3	AC-4	AC-5	AC-6	AB-1	AB-2	AB-3	AB-4	AB-5	AB-6	AB-7	A-1	A-2	AA-1	
289	CIP		06/03/96	03:00 AM																			
290	SIP		06/07/96	03:49 PM	04:04 PM	04:04 PM	06/07/96	05:04 PM	06/07/96	05:34 PM													
291	Clean Up		06/07/96	05:04 PM																			
292	Sub Total																						
293																							
294	13 A Resolubilization																						
295	Set Up		06/07/96	01:28 PM	06/07/96	02:28 PM	06/07/96	02:58 PM	06/07/96	08:58 AM	06/08/96	08:58 AM	06/08/96	10:58 AM	06/08/96	11:58 AM	06/08/96	11:58 AM					
296	Dilution		06/07/96	02:28 PM	06/07/96	02:58 PM	06/07/96	08:58 AM	06/08/96	08:58 AM	06/08/96	10:58 AM	06/08/96	11:58 AM	06/08/96	11:58 AM	06/08/96	11:58 AM					
297	Agitate		06/07/96	02:58 PM	06/08/96	08:58 AM	06/08/96	08:58 AM	06/08/96	08:58 AM	06/08/96	10:58 AM	06/08/96	11:58 AM	06/08/96	11:58 AM	06/08/96	11:58 AM					
298	CIP																						
299	SIP																						
300	Clean Up																						
301	Subtotal																						
302																							
303																							
304	14 A Concentration																						
305	Set Up		06/08/96	06:38 AM	06/08/96	07:38 AM	06/08/96	08:18 AM	06/08/96	08:58 AM	06/08/96	09:58 AM	06/08/96	10:28 AM	06/08/96	11:19 AM	06/08/96	11:38 AM	06/08/96	11:58 AM	06/08/96	11:58 AM	
306	Flush		06/08/96	07:38 AM	06/08/96	08:18 AM	06/08/96	08:58 AM	06/08/96	09:58 AM	06/08/96	10:28 AM	06/08/96	11:19 AM	06/08/96	11:38 AM	06/08/96	11:58 AM	06/08/96	11:58 AM	06/08/96	11:58 AM	
307	Prime		06/08/96	08:18 AM	06/08/96	08:58 AM	06/08/96	09:58 AM	06/08/96	10:28 AM	06/08/96	11:19 AM	06/08/96	11:38 AM	06/08/96	11:58 AM	06/08/96	11:58 AM	06/08/96	11:58 AM	06/08/96	11:58 AM	
308	Concentration																						
309	Dilution																						
310	311 Wash																						
311	Wash		06/08/96	10:25 AM	06/08/96	11:19 AM	06/08/96	11:39 AM	06/08/96	12:19 PM	06/08/96	01:19 PM	06/08/96	02:19 PM	06/08/96	03:19 PM	06/08/96	03:19 PM	06/08/96	03:19 PM	06/08/96	03:19 PM	
312	Flush																						
313	Store																						
314	CIP																						
315	SIP																						
316	Clean Up																						
317	Sub Total																						
318																							
319	16 A Microfiltration																						
320	Set Up		06/08/96	10:03 AM	06/08/96	11:03 AM	06/08/96	11:11 AM	06/08/96	11:19 AM	06/08/96	11:49 AM	06/08/96	11:49 AM	06/08/96	11:51 AM	06/08/96	11:55 AM	06/08/96	12:55 PM	06/08/96	01:55 PM	
321	Flush		06/08/96	11:03 AM	06/08/96	11:11 AM	06/08/96	11:19 AM	06/08/96	11:49 AM	06/08/96	11:49 AM	06/08/96	11:51 AM	06/08/96	11:55 AM	06/08/96	12:19 PM	06/08/96	12:31 PM	06/08/96	01:52 PM	
322	Prime																						
323	Filtration																						
324	Wash																						
325	Regenerate																						
326	Store																						
327	CIP																						
328	SIP																						
329	Clean Up																						
330	Sub Total																						
331																							
332	16 A PIA MPLC																						
333																							
334																							
335	Equilibration																						
336	Load																						
337	Wash																						

F1 & 45G

QC Load Table - PE Module

		QA/QC Samples										Immunochemical						Act.													
		Start			Finish			Date			Time			AV-1	AV-2		AC-1	AC-2		AC-3	AC-4		AC-5	AC-6		AB-1	AB-2		AI-1	AI-2	AA-1
		Date	Time		AV-1	AV-2		AC-1	AC-2		AC-3	AC-4		AC-5	AC-6		AB-1	AB-2		AB-3	AB-4		AB-5	AB-6		AB-7	AI-1	AI-2	AA-1		
	Operation																														
338	Elute A		06/03/96	08:00 AM	06/08/96	01:32 PM		06/08/96	03:12 PM		06/08/96	03:12 PM		06/08/96	03:25 PM		06/08/96	03:52 PM		06/08/96	04:52 PM		06/08/96	05:52 PM		06/08/96	06:52 PM				
339	Elute B		06/08/96	06:12 PM	06/08/96	03:12 PM		06/08/96	03:12 PM		06/08/96	03:12 PM		06/08/96	03:25 PM		06/08/96	03:52 PM		06/08/96	04:52 PM		06/08/96	05:52 PM		06/08/96	06:52 PM				
340	Regenerate		06/08/96	03:25 PM	06/08/96	03:52 PM		06/08/96	03:52 PM		06/08/96	03:52 PM		06/08/96	04:52 PM		06/08/96	04:52 PM		06/08/96	05:52 PM		06/08/96	06:52 PM		06/08/96	06:52 PM				
341	Store		06/08/96	06:52 PM	06/08/96	06:52 PM		06/08/96	06:52 PM		06/08/96	06:52 PM		06/08/96	06:52 PM		06/08/96	06:52 PM		06/08/96	06:52 PM		06/08/96	06:52 PM		06/08/96	06:52 PM				
342	CIP		06/08/96	06:52 PM	06/08/96	06:52 PM		06/08/96	06:52 PM		06/08/96	06:52 PM		06/08/96	06:52 PM		06/08/96	06:52 PM		06/08/96	06:52 PM		06/08/96	06:52 PM		06/08/96	06:52 PM				
343	SIP		06/08/96	06:52 PM	06/08/96	06:52 PM		06/08/96	06:52 PM		06/08/96	06:52 PM		06/08/96	06:52 PM		06/08/96	06:52 PM		06/08/96	06:52 PM		06/08/96	06:52 PM		06/08/96	06:52 PM				
344	Clean Up		06/08/96	06:52 PM	06/08/96	06:52 PM		06/08/96	06:52 PM		06/08/96	06:52 PM		06/08/96	06:52 PM		06/08/96	06:52 PM		06/08/96	06:52 PM		06/08/96	06:52 PM		06/08/96	06:52 PM				
345	Sub Total																														
346																															
347																															
348	17 A PIA MPLC																														
349	Equilibration		06/08/96	02:59 PM	06/08/96	03:12 PM		06/08/96	03:12 PM		06/08/96	03:12 PM		06/08/96	03:25 PM		06/08/96	03:52 PM		06/08/96	04:52 PM		06/08/96	05:52 PM		06/08/96	06:52 PM				
350	Load		06/08/96	03:12 PM	06/08/96	04:17 PM		06/08/96	04:17 PM		06/08/96	04:17 PM		06/08/96	05:03 PM		06/08/96	05:49 PM													
351	Wash		06/08/96	05:03 PM	06/08/96	05:49 PM		06/08/96	05:49 PM		06/08/96	05:49 PM		06/08/96	05:49 PM		06/08/96	05:49 PM		06/08/96	05:49 PM		06/08/96	05:49 PM		06/08/96	05:49 PM				
352	Elute A		06/08/96	05:49 PM	06/08/96	06:49 PM		06/08/96	06:49 PM		06/08/96	06:49 PM		06/08/96	06:49 PM		06/08/96	06:49 PM		06/08/96	06:49 PM		06/08/96	06:49 PM		06/08/96	06:49 PM				
353	Elute B		06/08/96	06:49 PM	06/08/96	07:13 PM		06/08/96	07:13 PM		06/08/96	07:13 PM		06/08/96	07:13 PM		06/08/96	07:13 PM		06/08/96	07:13 PM		06/08/96	07:13 PM		06/08/96	07:13 PM				
354	Regenerate		06/08/96	07:13 PM	06/08/96	08:13 PM		06/08/96	08:13 PM		06/08/96	08:13 PM		06/08/96	08:13 PM		06/08/96	08:13 PM		06/08/96	08:13 PM		06/08/96	08:13 PM		06/08/96	08:13 PM				
355	Store		06/08/96	08:13 PM	06/08/96	09:13 PM		06/08/96	09:13 PM		06/08/96	09:13 PM		06/08/96	09:13 PM		06/08/96	09:13 PM		06/08/96	09:13 PM		06/08/96	09:13 PM		06/08/96	09:13 PM				
356	CIP		06/08/96	09:13 PM	06/08/96	09:49 PM		06/08/96	09:49 PM		06/08/96	09:49 PM		06/08/96	09:49 PM		06/08/96	09:49 PM		06/08/96	09:49 PM		06/08/96	09:49 PM		06/08/96	09:49 PM				
357	SIP		06/08/96	09:49 PM	06/08/96	09:49 PM		06/08/96	09:49 PM		06/08/96	09:49 PM		06/08/96	09:49 PM		06/08/96	09:49 PM		06/08/96	09:49 PM		06/08/96	09:49 PM		06/08/96	09:49 PM				
358	Clean Up		06/08/96	09:49 PM	06/08/96	09:49 PM		06/08/96	09:49 PM		06/08/96	09:49 PM		06/08/96	09:49 PM		06/08/96	09:49 PM		06/08/96	09:49 PM		06/08/96	09:49 PM		06/08/96	09:49 PM				
359	Sub Total																														
360																															
361	18 A Flow Dialysis																														
362	Set Up		06/08/96	03:29 PM	06/08/96	04:29 PM		06/08/96	04:29 PM		06/08/96	04:29 PM		06/08/96	05:09 PM		06/08/96	05:09 PM		06/08/96	05:09 PM		06/08/96	05:09 PM		06/08/96	05:09 PM				
363	Flush		06/08/96	04:29 PM	06/08/96	05:49 PM		06/08/96	05:49 PM		06/08/96	05:49 PM		06/08/96	05:49 PM		06/08/96	05:49 PM		06/08/96	05:49 PM		06/08/96	05:49 PM		06/08/96	05:49 PM				
364	Purge		06/08/96	05:49 PM	06/08/96	06:49 PM		06/08/96	06:49 PM		06/08/96	06:49 PM		06/08/96	06:49 PM		06/08/96	06:49 PM		06/08/96	06:49 PM		06/08/96	06:49 PM		06/08/96	06:49 PM				
365	Dialysis		06/08/96	06:49 PM	06/08/96	07:09 PM		06/08/96	07:09 PM		06/08/96	07:09 PM		06/08/96	07:09 PM		06/08/96	07:09 PM		06/08/96	07:09 PM		06/08/96	07:09 PM		06/08/96	07:09 PM				
366	Wash		06/08/96	07:09 PM	06/08/96	07:49 PM		06/08/96	07:49 PM		06/08/96	07:49 PM		06/08/96	07:49 PM		06/08/96	07:49 PM		06/08/96	07:49 PM		06/08/96	07:49 PM		06/08/96	07:49 PM				
367	Flush		06/08/96	07:49 PM	06/08/96	08:49 PM		06/08/96	08:49 PM		06/08/96	08:49 PM		06/08/96	08:49 PM		06/08/96	08:49 PM		06/08/96	08:49 PM		06/08/96	08:49 PM		06/08/96	08:49 PM				
368	Store		06/08/96	08:49 PM	06/08/96	09:49 PM		06/08/96	09:49 PM		06/08/96	09:49 PM		06/08/96	09:49 PM		06/08/96	09:49 PM		06/08/96	09:49 PM		06/08/96	09:49 PM		06/08/96	09:49 PM				
369	CIP		06/08/96	09:49 PM	06/08/96	09:49 PM		06/08/96	09:49 PM		06/08/96	09:49 PM		06/08/96	09:49 PM		06/08/96	09:49 PM		06/08/96	09:49 PM		06/08/96	09:49 PM		06/08/96	09:49 PM				
370	SIP		06/08/96	09:49 PM	06/08/96	09:49 PM		06/08/96	09:49 PM		06/08/96	09:49 PM		06/08/96	09:49 PM		06/08/96	09:49 PM		06/08/96	09:49 PM		06/08/96	09:49 PM		06/08/96	09:49 PM				
371	Clean Up		06/08/96	09:49 PM	06/08/96	09:49 PM		06/08/96	09:49 PM		06/08/96	09:49 PM		06/08/96	09:49 PM		06/08/96	09:49 PM		06/08/96	09:49 PM		06/08/96	09:49 PM		06/08/96	09:49 PM				
372	Sub Total																														
373																															
374																															
375	19 A PIA MPLC																														
376	Equilibration		06/08/96	05:59 PM	06/08/96	06:31 PM		06/08/96	06:31 PM		06/08/96	06:31 PM		06/08/96	07:03 PM		06/08/96	07:41 PM		06/08/96	08:20 PM		06/08/96	08:20 PM		06/08/96	08:20 PM				
377	Load		06/08/96	06:39 PM	06/08/96	07:03 PM		06/08/96	07:03 PM		06/08/96	07:03 PM		06/08/96	07:03 PM		06/08/96	07:03 PM		06/08/96	07:03 PM		06/08/96	07:03 PM		06/08/96	07:03 PM				
378	Wash		06/08/96	07:03 PM	06/08/96	07:41 PM		06/08/96	07:41 PM		06/08/96	07:41 PM		06/08/96	08:19 PM		06/08/96	08:19 PM		06/08/96	08:19 PM		06/08/96	08:19 PM		06/08/96	08:19 PM				
379	Elute A		06/08/96	07:41 PM	06/08/96	08:20 PM		06/08/96	08:20 PM		06/08/96	08:20 PM		06/08/96	08:20 PM		06/08/96	08:20 PM		06/08/96	08:20 PM		06/08/96	08:20 PM		06/08/96	08:20 PM				
380	Elute B		06/08/96	0																											

QC Load Table - PE Module

Fig. 45 π

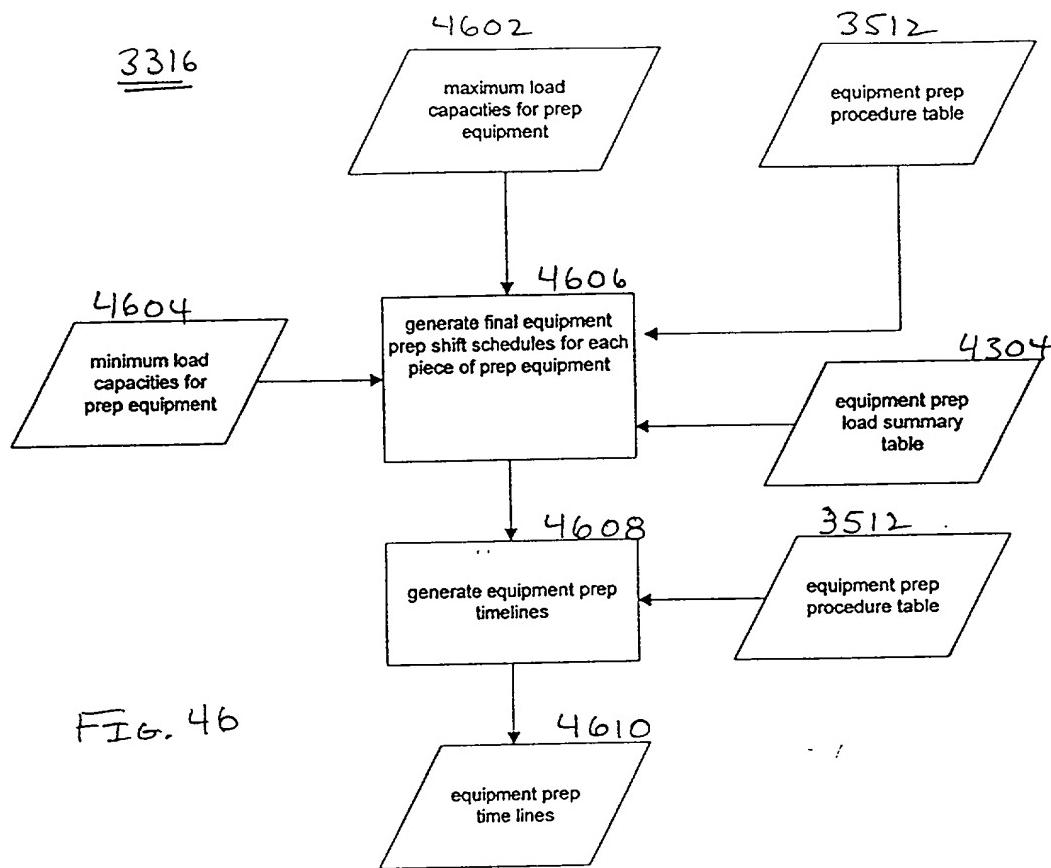


FIG. 46

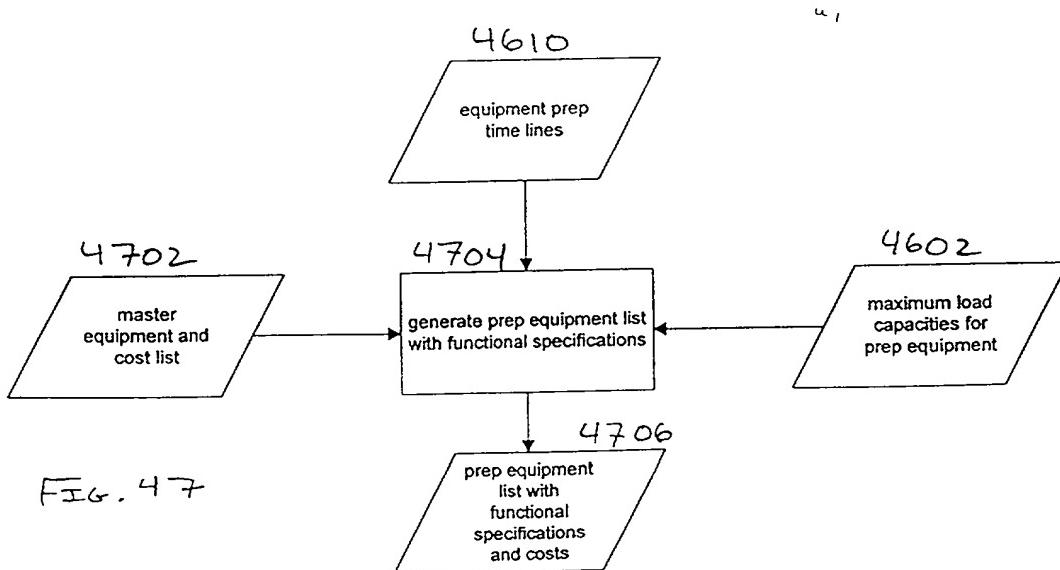


FIG. 47

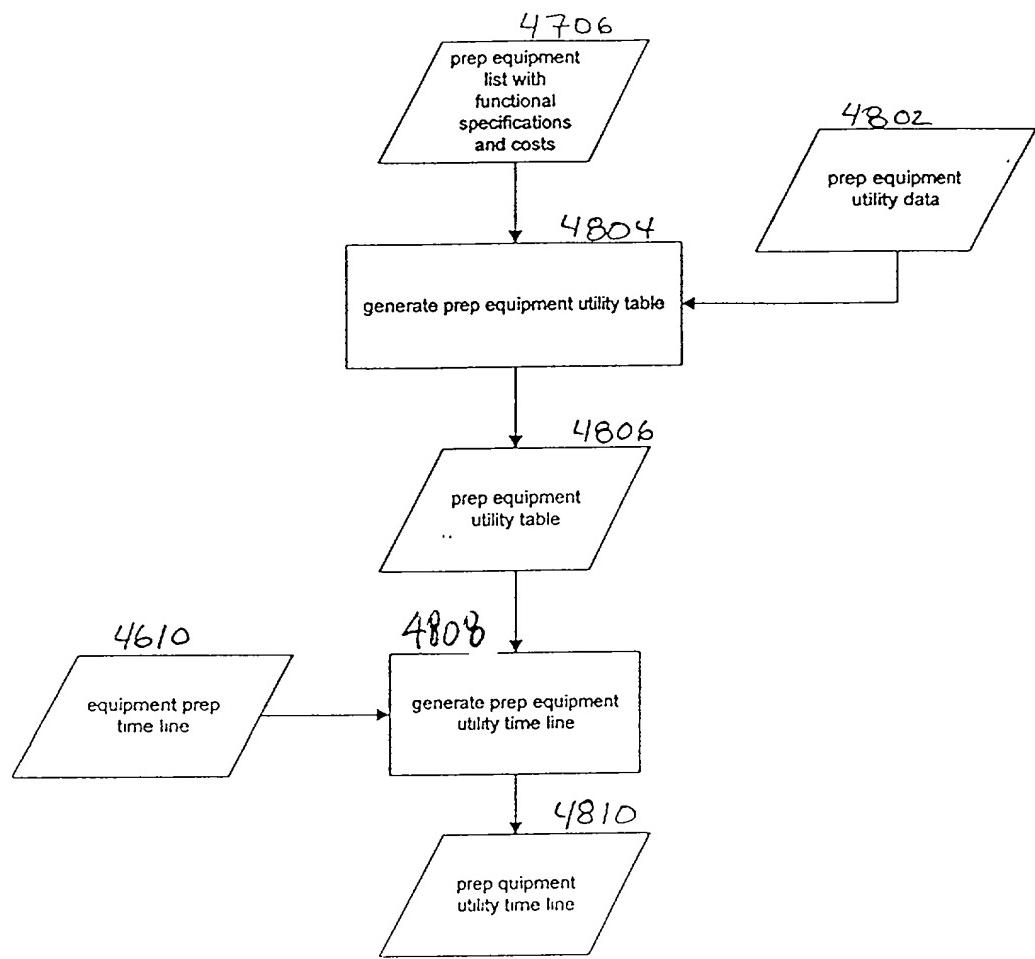


Fig. 48

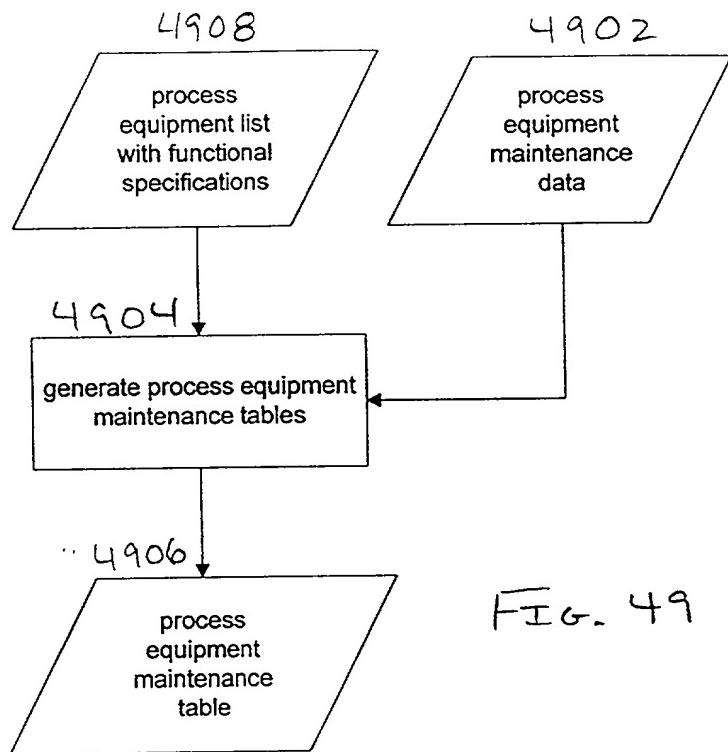


FIG. 49

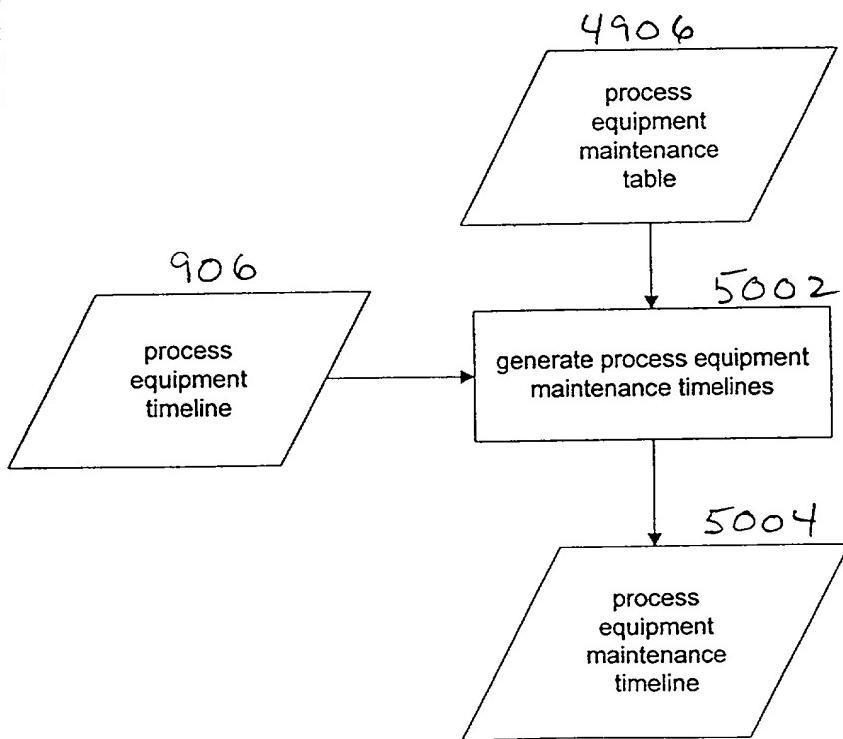


FIG. 50

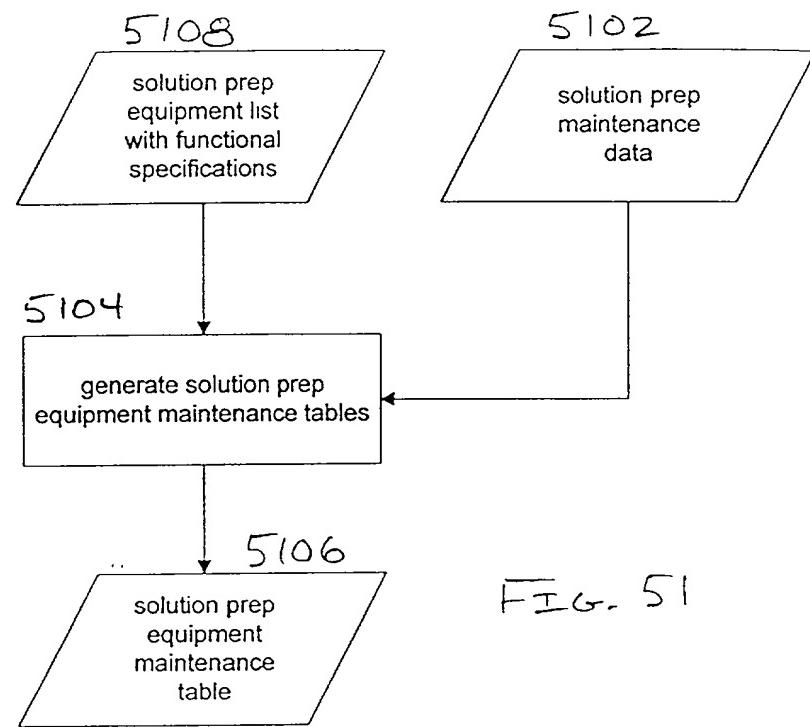


FIG. 51

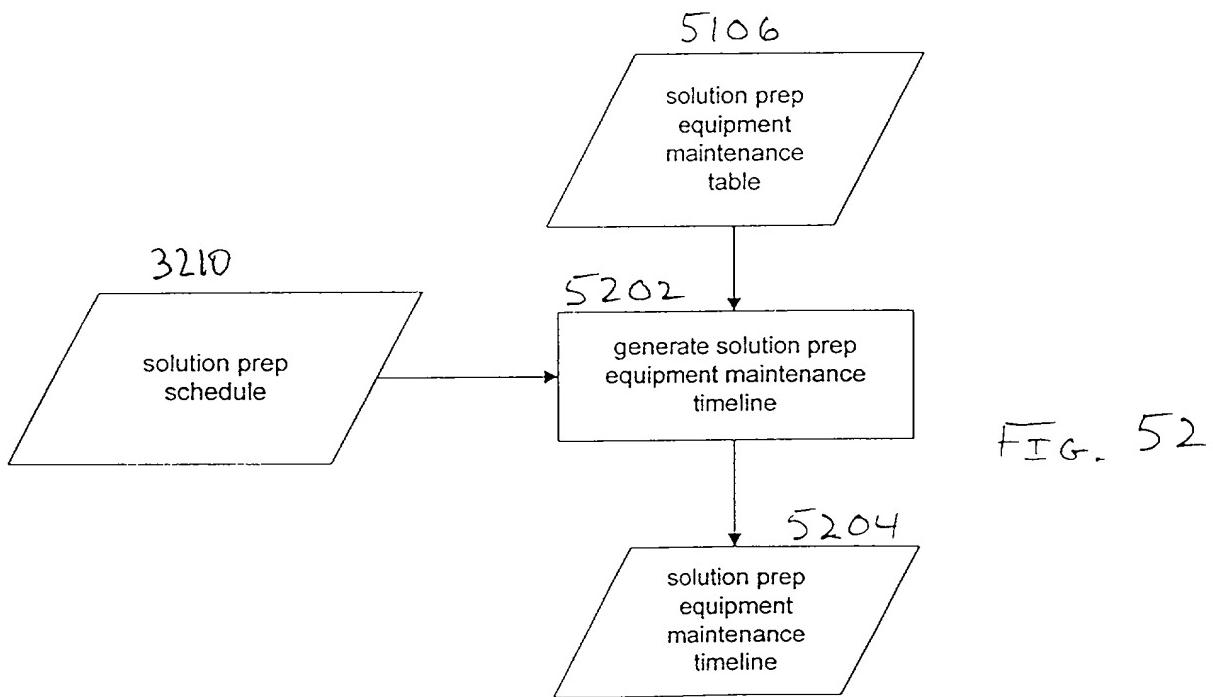
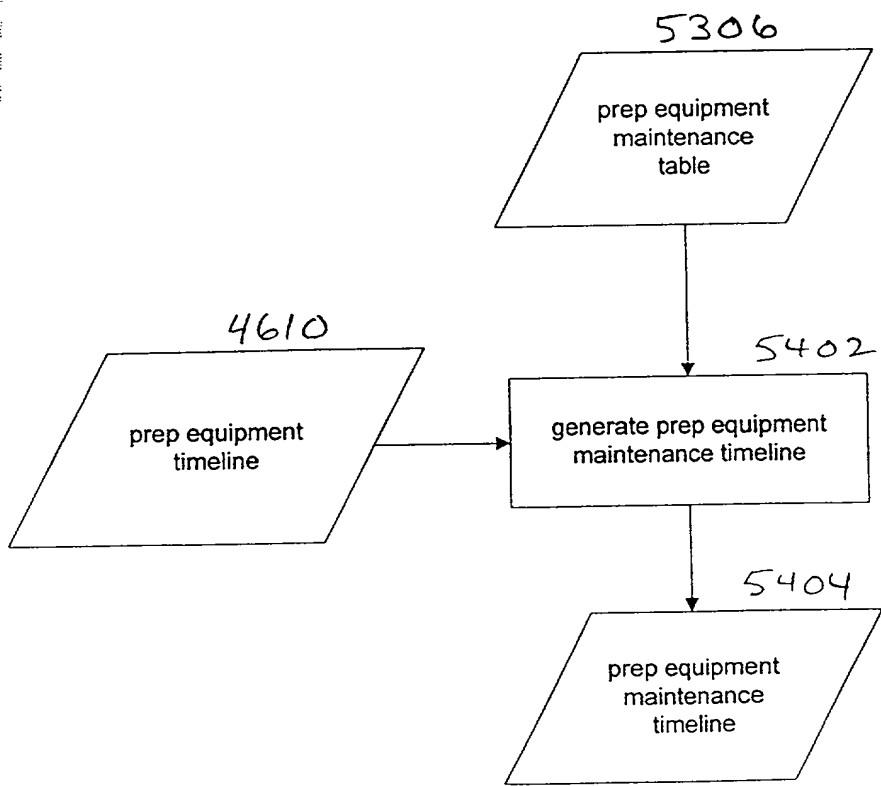
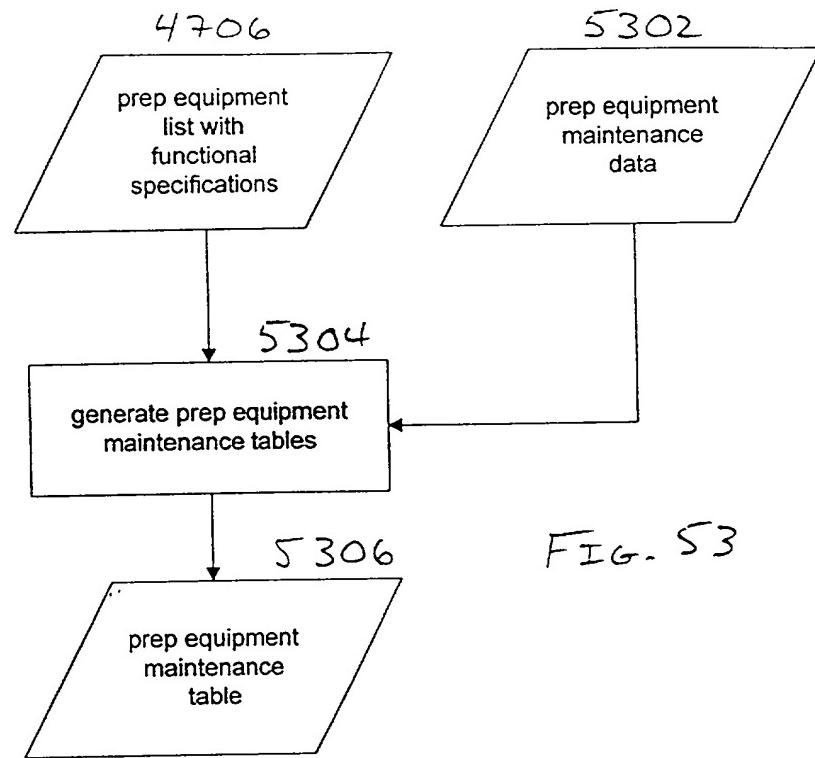


FIG. 52



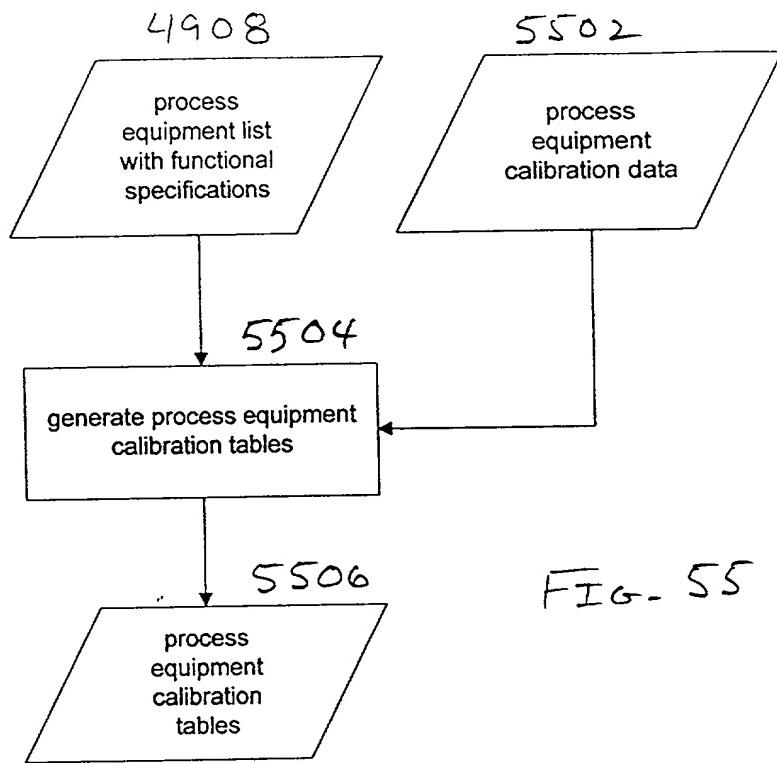


FIG- 55

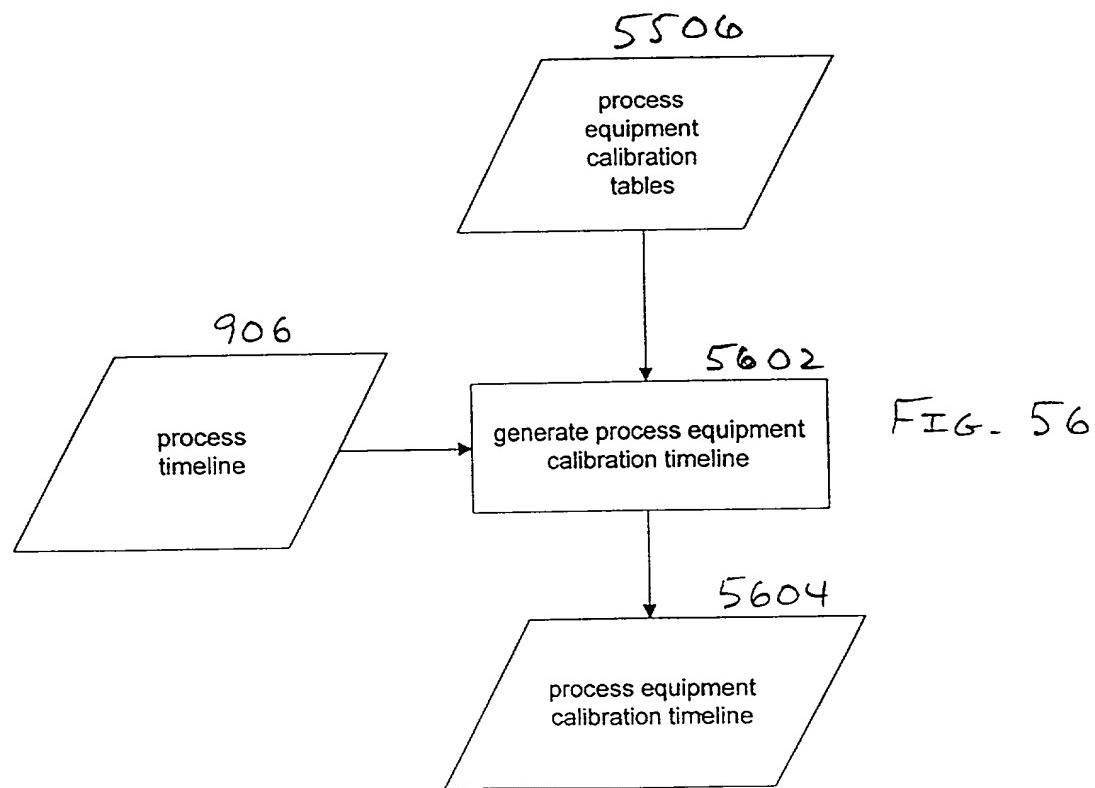


FIG- 56

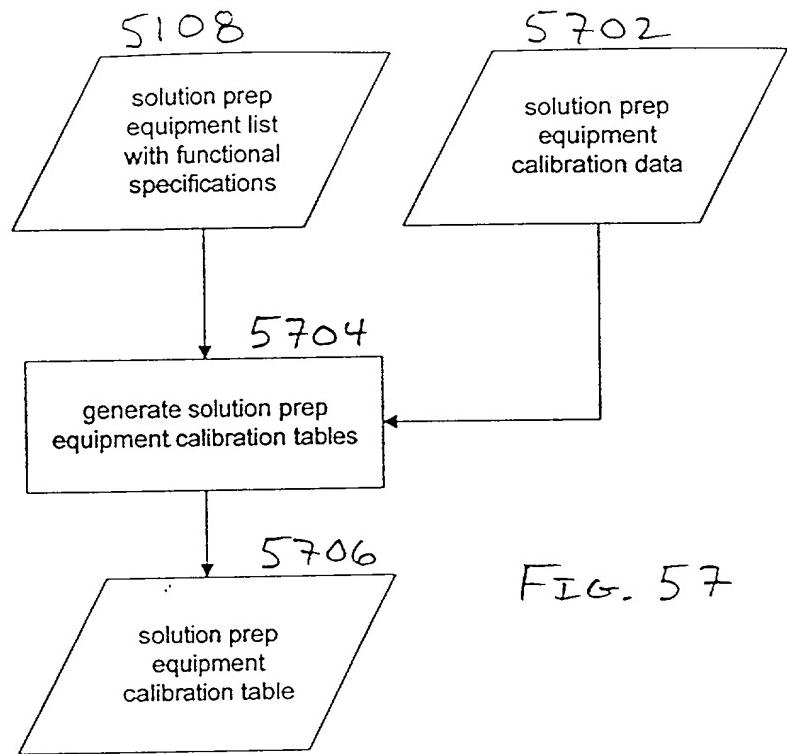


FIG. 57

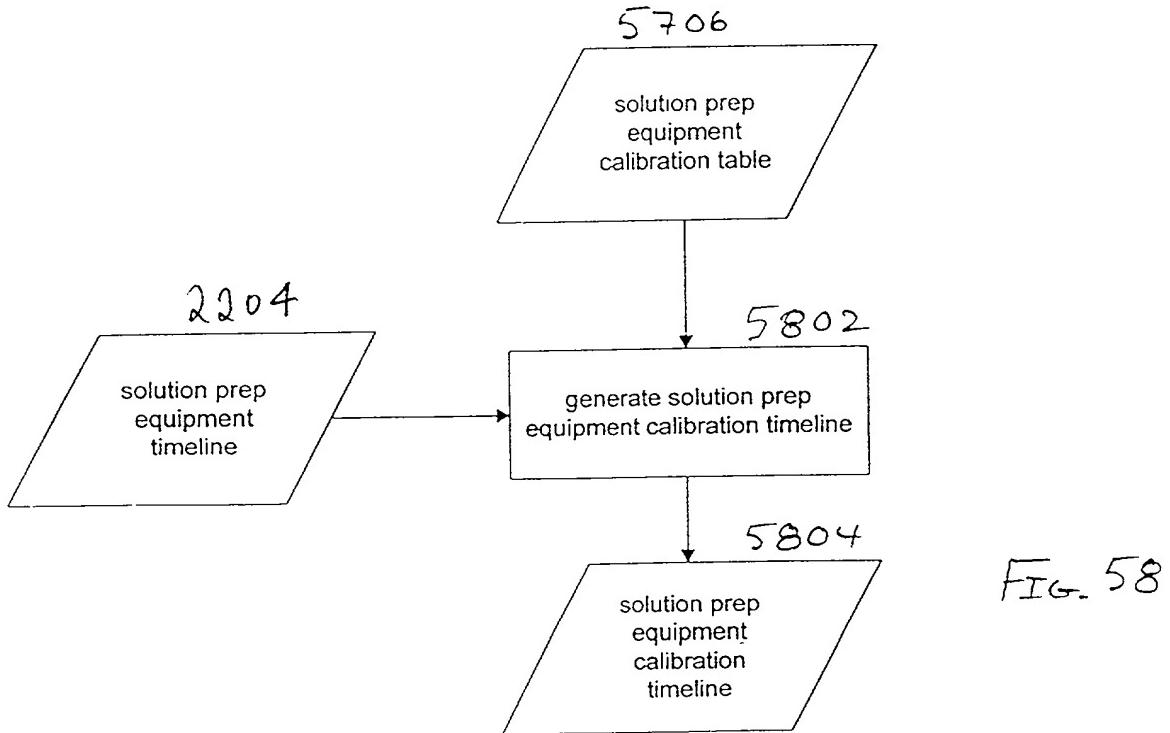
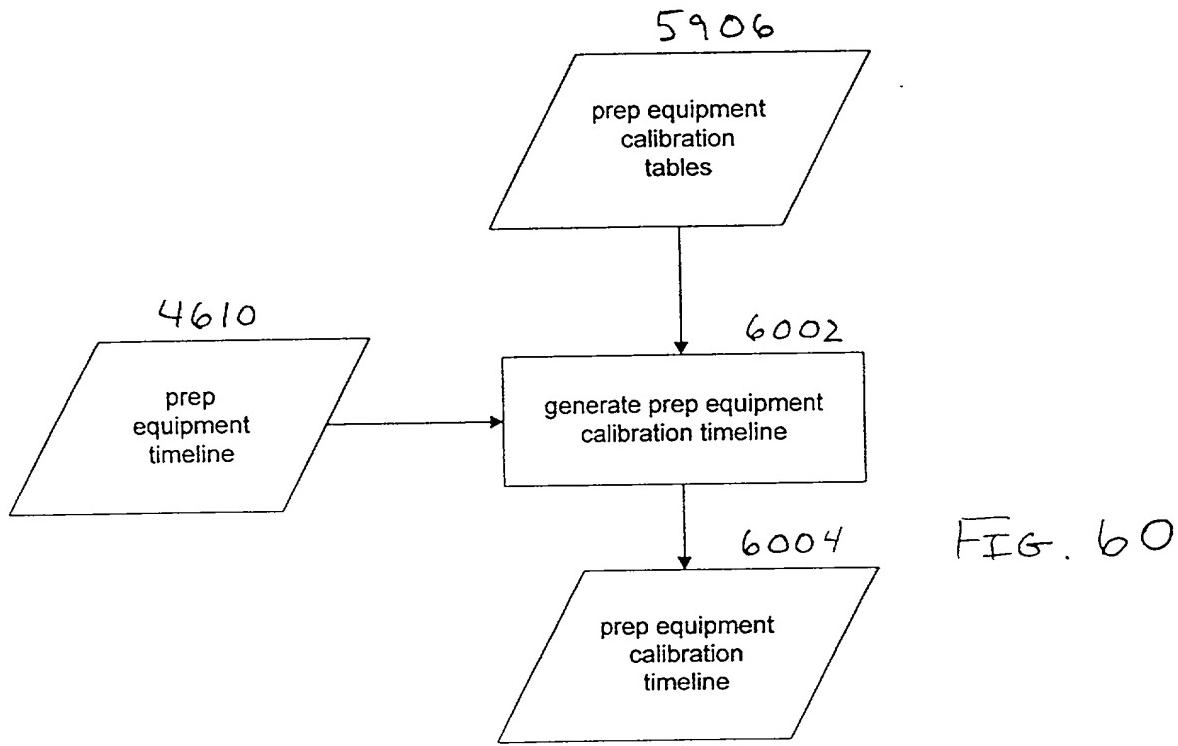
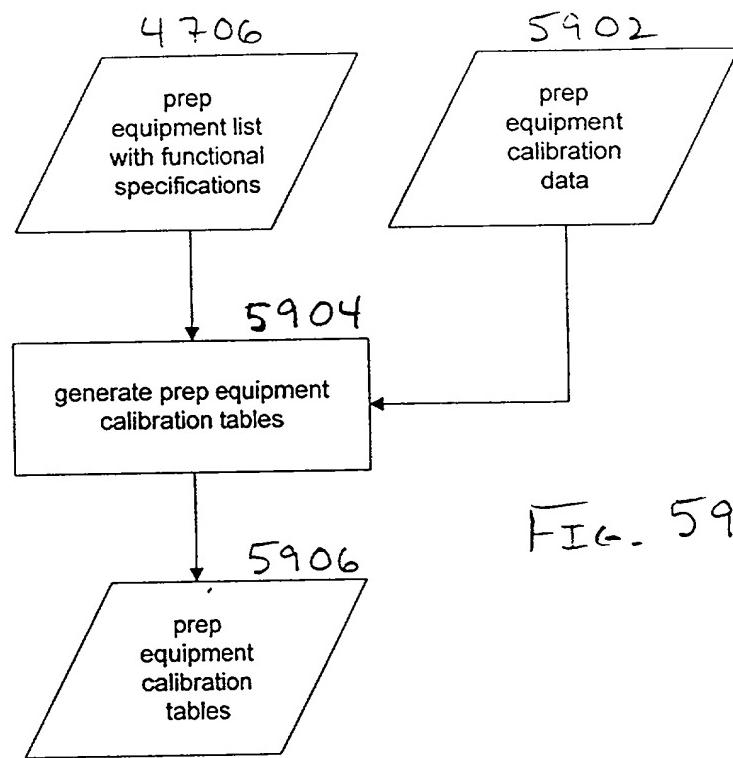


FIG. 58



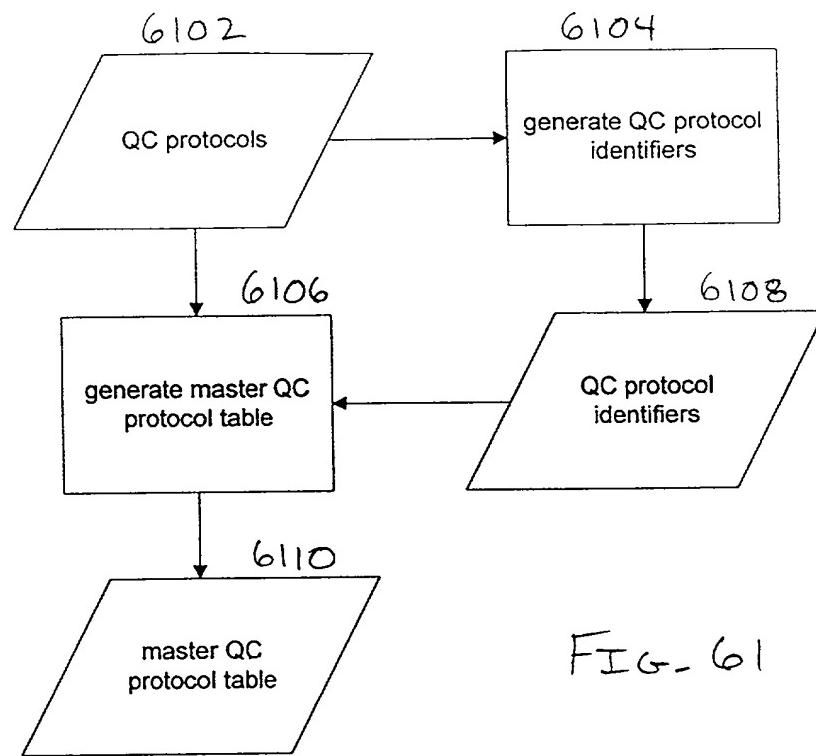


FIG- 61

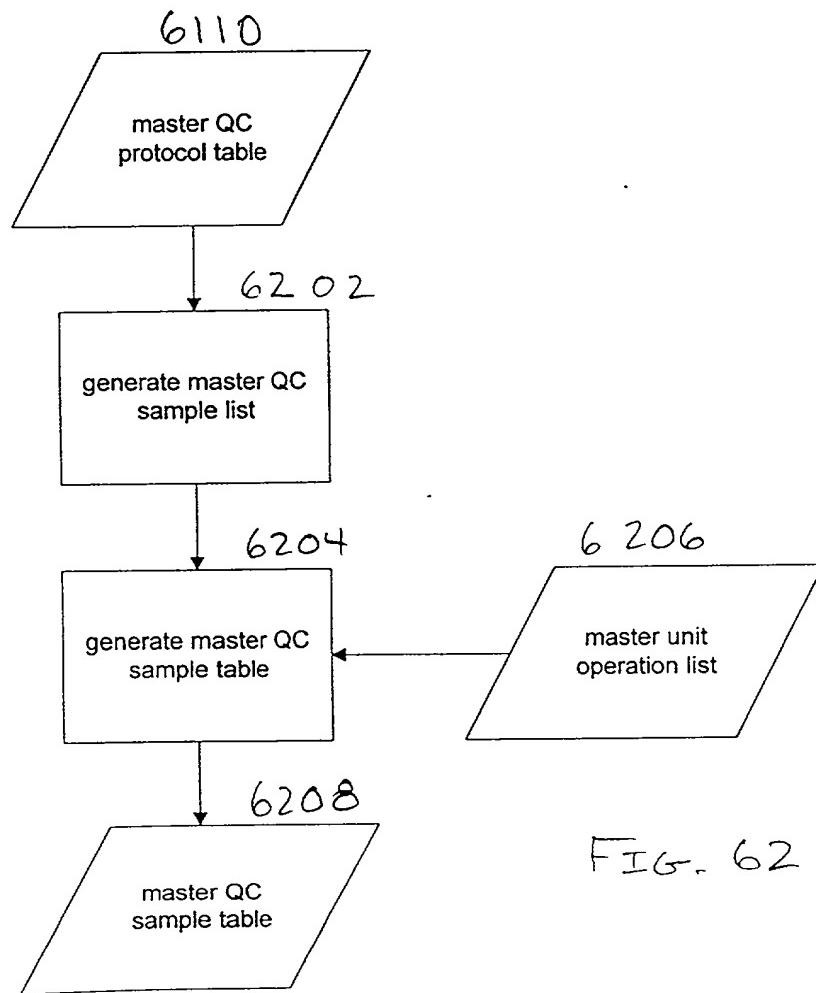


FIG- 62

6402

Equipment Maintenance Table - Microbial Fermentation

6404

6406

6408

	Filters				Gaskets				Bearings							
	Materials		Labor		Materials		Labor		Materials		Labor		Materials		Labor	
Equipment Items	Item No.	Qty	Cycle Life	Unit Cost	\$/Cycle	Hours	\$/Cycle	Item No.	City	Cycle Life	Unit Cost	\$/Cycle	Hours	\$/Cycle	Item No.	
Media Inoculum Dispenser																
-80 C Stock Freezer																
Shaking Water Bath																
Media Glass Growth Jars																
Floor Incubator-Shaker																
Microscope																
Seed Fermentation																
Seed Bioreactor																
Production Bioreactor	75868	1	100	55	.55	.5	.0875	48914	1	500	55	.11	1	.035		
Whole Cell Harvest																
Harvest Heat Exchanger																
Harvest Vessel																
Agitator																
Concentration																
Pump																
Filter Holder																
Manifolding																
Instrumentation																
MF Flush Vessel																
MF Prime Vessel																
MF Filtrate Vessel																
Agitator																
MF Wash Vessel																
MF Regeneration Vessel																
MF Storage Vessel																

FIG. 64A

Equipment Maintenance Table - Microbial Fermentation

6408

6410

6412

Equipment Items	Seals						Belts											
	Qty	Cycle Life	Unit Cost	\$/Cycle	Hours	\$/Cycle	Materials	Item No.	Qty	Cycle Life	Unit Cost	\$/Cycle	Labor	Hours	\$/Cycle	Materials	Item No.	Qty
1.1 Incubator-Shaker																		
-80 C Stock Freezer																		
Shaking Water Bath																		
1.2.1 Haskett Stocker																		
Floor Incubator-Shaker																		
Microscope																		
1.3 Seed Fermentation																		
Seed Bioreactor																		
1.4 Fermentation																		
Production Bioreactor																		
1.5 Harvest Leaves																		
Harvest Heat Exchanger																		
Harvest Vessel																		
Agitator																		
1.6 Cell Concentration																		
Pump																		
Filter Holder																		
Manifolding																		
Instrumentation																		
MF Flush Vessel																		
MF Prime Vessel																		
MF Filtrate Vessel																		
Agitator																		
MF Wash Vessel																		
MF Regeneration Vessel																		
MF Storage Vessel																		

Fig. 64B

Equipment Maintenance Table - Microbial Fermentation

6416

6418

Equipment Items	Shafts						Lubricant			
	Cycle Life	Unit Cost	\$/Cycle	Labor	Hours	\$/Cycle	Materials	Item No.	Qty	Cycle Life
1. Inoculation & Growth										
-80 C Stock Freezer										
Shaking Water Bath										
2. Flask Growth										
Floor Incubator-Shaker										
Microscope										
3. Seed Fermentation										
Seed Bioreactor										
4. Production Fermentation										
Production Bioreactor	500	25	.05	1	.035					
5. Harvesting										
Harvest Heat Exchanger										
Harvest Vessel										
6. Agitator										
Pump										
Filter Holder										
Manifolding										
Instrumentation										
MF Flush Vessel										
MF Prime Vessel										
MF Filtrate Vessel										
Agitator										
MF Wash Vessel										
MF Regeneration Vessel										
MF Storage Vessel										

Fig. 64C

Equipment Maintenance Table - Microbial Fermentation

6420

6418

Equipment Items	Thermal Media						Labor					
	Unit Cost	\$/Cycle	Hours	\$/Cycle	Item No.	Qty	Cycle Life	Unit Cost	\$/Cycle	Hours	\$/Cycle	
1. Introduction Equipment												
-80 C Stock Freezer												
Shaking Water Bath												
2. Harvesting Equipment												
Floor Incubator-Shaker												
Microscope												
3. Seed Fermentation												
Seed Bioreactor	1.5	.03	.5	.175								
4. Fermentation Equipment												
Production Bioreactor					56258	5	500.	.85	425	1	17.5	
5. Whole Cell Harvesting												
Harvest Heat Exchanger												
Harvest Vessel												
6. Cell Concentration												
Agitator												
Pump												
Filter Holder												
Manifolding												
Instrumentation												
MF Flush Vessel												
MF Prime Vessel												
MF Filtrate Vessel												
Agitator												
MF Wash Vessel												
MF Regeneration Vessel												
MF Storage Vessel												

F2 Cr. 64 D

Equipment Maintenance Table - Microbial Fermentation

Equipment Items	Filters			Gaskets			Bearings			Materials						
	Materials	Item No.	Qty	Cycle Life	Unit Cost	\$/Cycle	Labor	Material	Item No.	Hours	\$/Cycle	Unit Cost	Cycle Life	Unit	Hours	\$/Cycle
MF Concentration Vessel																
MF Wash Vessel																
Pump																
Filter Holder																
Manifolding																
Instrumentation																
MF Flush Vessel																
MF Prime Vessel																
MF Filtrate Vessel																
MF Wash Vessel																
MF Regeneration Vessel																
MF Storage Vessel																
MF Resuspension Vessel																
Stir Plate																
Cell Disruptor																
Lysate Vessel																
MF Resuspension Vessel																
Stir Plate																
MF Concentration Vessel																
MF Wash Vessel																
Pump																
Filter Holder																

FIG. 64E

Equipment Maintenance Table - Microbial Fermentation

Equipment Items	Seals						Belts		
	Qty	Cycle Life	Unit Cost	\$/Cycle	Hours	\$/Cycle	Materials	Labor	Materials
MF Concentration									
MF Wash Vessel									
Pump									
Filter Holder									
Manifolding									
Instrumentation									
MF Flush Vessel									
MF Prime Vessel									
MF Filtrate Vessel									
MF Wash Vessel									
MF Regeneration Vessel									
MF Storage Vessel									
MF Cell Resuspension									
Resuspension Vessel									
Stir Plate									
Cell Disruption									
Cell Disruptor									
Lysate Vessel									
MF Resuspension									
Resuspension Vessel									
Stir Plate									
MF Concentration 1 & 2									
MF Wash Vessel									
Pump									
Filter Holder									

Fig. 64F

Equipment Maintenance Table Microbial Fermentation

Equipment Items	Shafts						Lubricant			
	Cycle Life	Unit Cost	\$/Cycle	Labor Hours	Materials \$/Cycle	Unit Cost	Material Qty	Item No.	Qty	Materials
MF Wash Vessel										
Pump										
Filter Holder										
Manifolding										
Instrumentation										
MF Flush Vessel										
MF Prime Vessel										
MF Filtrate Vessel										
MF Wash Vessel										
MF Regeneration Vessel										
MF Storage Vessel										
10% Cell Resuspension										
Resuspension Vessel										
Stir Plate										
90% Cell Disruption										
Cell Disruptor										
Lysate Vessel										
10% B Cell Resuspension										
Resuspension Vessel										
Stir Plate										
10% B Cell Concentration										
MF Wash Vessel										
Pump										
Filter Holder										

FIG. 616

Equipment Maintenance Table - Microbial Fermentation

Equipment Items	Thermal Media						Labor				
	Unit Cost	\$/Cycle	Labor Hours	\$/Cycle	Materials Item No.	Qty	Cycle Life	Unit Cost	\$/Cycle	Hours	\$/Cycle
Cell Concentration											
MF Wash Vessel											
Pump											
Filter Holder											
Manifolding											
Instrumentation											
MF Flush Vessel											
MF Prime Vessel											
MF Filtrate Vessel											
MF Wash Vessel											
MF Regeneration Vessel											
MF Storage Vessel											
Cell Resuspension											
Resuspension Vessel											
Stir Plate											
Cell Disruption											
Lysate Vessel											
Cell Resuspension											
Resuspension Vessel											
Stir Plate											
Cell Concentration											
MF Wash Vessel											
Pump											
Filter Holder											

FIG. 6-14

Equipment Maintenance Table - Microbial Fermentation

Equipment Items	Filters			Gaskets			Bearings			
	Materials	Item No.	Qty	Cycle Life	Unit Cost	\$/Cycle	Labor	Materials	Item No.	Materials
Manifolding										
Instrumentation										
MF Flush Vessel										
MF Prime Vessel										
MF Filtrate Vessel										
MF Dilute Vessel										
MF Wash Vessel										
MF Regeneration Vessel										
MF Storage Vessel										
14% Renaturant										
Renaturant Vessel										
Stir Plate										
15% Buffer Exchange										
Pump										
Filter Holder										
Manifolding										
Instrumentation										
UF Flush Vessel										
UF Prime Vessel										
UF Filtrate Vessel										
UF Wash Vessel										
UF Diluent Vessel										
UF Regeneration Vessel										
UF Storage Vessel										

FIG. 64 I

Equipment Maintenance Table - Microbial Fermentation

Equipment Items	Seals						Belts										
	Qty	Cycle Life	Unit Cost	\$/Cycle	Hours	\$/Cycle	Item No.	Qty	Cycle Life	Unit Cost	\$/Cycle	Hours	\$/Cycle	Labor	Materials	Item No.	Qty
Manifolding																	
Instrumentation																	
MF Flush Vessel																	
MF Prime Vessel																	
MF Filtrate Vessel																	
MF Dilute Vessel																	
MF Wash Vessel																	
MF Regeneration Vessel																	
MF Storage Vessel																	
<hr/>																	
Stir Plate																	
Spare Buffer Exchange																	
Pump																	
Filter Holder																	
Manifolding																	
Instrumentation																	
UF Flush Vessel																	
UF Prime Vessel																	
UF Filtrate Vessel																	
UF Wash Vessel																	
UF Diluent Vessel																	
UF Regeneration Vessel																	
UF Storage Vessel																	

FIG- 64J

Equipment Maintenance Table - Microbial Fermentation

Equipment Items	Shafts						Lubricant				
	Labor		Materials		Labor		Item No.	Qty	Cycle Life	Unit Cost	
Cycle Life	Unit Cost	\$/Cycle	Hours	\$/Cycle	Hours	\$/Cycle	Hours	\$/Cycle	Item No.	Qty	Cycle Life
Manifolding											
Instrumentation											
MF Flush Vessel											
MF Prime Vessel											
MF Filtrate Vessel											
MF Dilute Vessel											
MF Wash Vessel											
MF Regeneration Vessel											
MF Storage Vessel											
UF Buffer Exchange											
Pump											
Filter Holder											
Manifolding											
Instrumentation											
UF Flush Vessel											
UF Prime Vessel											
UF Filtrate Vessel											
UF Wash Vessel											
UF Diluent Vessel											
UF Regeneration Vessel											
UF Storage Vessel											

Fig. 64 K

Equipment Maintenance Table - Microbial Fermentation

Equipment Items	Thermal Media						Labor
	Unit Cost	\$/Cycle	Labor	Hours	\$/Cycle	Materials	
Item No.	Qty	Cycle Life	Unit Cost	\$/Cycle	Hours	\$/Cycle	
Manifolding							
Instrumentation							
MF Flush Vessel							
MF Prime Vessel							
MF Filtrate Vessel							
MF Dilute Vessel							
MF Wash Vessel							
MF Regeneration Vessel							
MF Storage Vessel							
14. Renaturant Vessel							
Renaturant Vessel							
Stir Plate							
15. Buffer/Exchanger							
Pump							
Filter Holder							
Manifolding							
Instrumentation							
UF Flush Vessel							
UF Prime Vessel							
UF Filtrate Vessel							
UF Wash Vessel							
UF Diluent Vessel							
UF Regeneration Vessel							
UF Storage Vessel							

FIG. 64L

Equipment Maintenance Table - Microbial Fermentation

Equipment Items	Filters				Gaskets				Bearings								
	Materials	Item No.	Qty	Cycle Life	Unit Cost	\$/Cycle	Hours	\$/Cycle	Item No.	Qty	Cycle Life	Unit Cost	\$/Cycle	Hours	\$/Cycle	Material	Item No.
16. Chromatography	Chromatography Column																
	Pump																
	Inst. & Control System																
	Manifolding																
	Equilibration Vessel																
	Wash Vessel																
	Eluent Vessel																
	Regenerate Vessel																
	Storage Vessel																
	Waste Vessel (1)																
	Product Vessel																
	Waste Vessel (2)																
17. Chromatography	Chromatography Column																
	Pump																
	Inst. & Control System																
	Manifolding																
	Equilibration Vessel																
	Wash Vessel																
	Eluent Vessel																
	Regenerate Vessel																

Fig. 64 m

Equipment Maintenance Table - Microbial Fermentation

Equipment Items	Seals						Belts							
	Materials			Labor			Materials		Labor		Materials		Labor	
Qty	Cycle Life	Unit Cost	\$/Cycle	Hours	\$/Cycle	Item No.	Qty	Cycle Life	Unit Cost	\$/Cycle	Hours	\$/Cycle	Item No.	Qty
UF Waste Vessel														
16. Chromatography														
Chromatography Column														
Pump														
Inst. & Control System														
Manifolding														
Equilibration Vessel														
Wash Vessel														
Eluent Vessel														
Regenerate Vessel														
Storage Vessel														
Waste Vessel (1)														
Product Vessel														
Waste Vessel (2)														
17. Chromatography														
Chromatography Column														
Pump														
Inst. & Control System														
Manifolding														
Equilibration Vessel														
Wash Vessel														
Eluent Vessel														
Regenerate Vessel														

FIG. 64N

Equipment Maintenance Table - Microbial Fermentation

Equipment Items	Shafts			Materials			Labor			Materials			Lubricant		
	Cycle Life	Unit Cost	\$/Cycle	Hours	\$/Cycle	Item No.	Qty	Cycle Life	Unit Cost	\$/Cycle	Hours	\$/Cycle	Item No.	Qty	Cycle Life
UF Waste Vessel															
16. Chromatography 1															
Chromatography Column															
Pump															
Inst. & Control System															
Manifolding															
Equilibration Vessel															
Wash Vessel															
Eluent Vessel															
Regenerate Vessel															
Storage Vessel															
Waste Vessel (1)															
Product Vessel															
Waste Vessel (2)															
17. Chromatography 2															
Chromatography Column															
Pump															
Inst. & Control System															
Manifolding															
Equilibration Vessel															
Wash Vessel															
Eluent Vessel															
Regenerate Vessel															

Fig. 640

Equipment Maintenance Table - Microbial Fermentation

Equipment Items	Thermal Media						Labor
	Unit Cost	\$/Cycle	Hours	\$/Cycle	Item No.	Qty	
UF Waste Vessel							
F6. Chromatography 1							
Chromatography Column							
Pump							
Inst. & Control System							
Manifolding							
Equilibration Vessel							
Wash Vessel							
Eluent Vessel							
Regenerate Vessel							
Storage Vessel							
Waste Vessel (1)							
Product Vessel							
Waste Vessel (2)							
F7. Chromatography 2							
Chromatography Column							
Pump							
Inst. & Control System							
Manifolding							
Equilibration Vessel							
Wash Vessel							
Eluent Vessel							
Regenerate Vessel							

FIG. 64 P

Equipment Maintenance Table - Microbial Fermentation

Equipment Items	Filters			Gaskets			Bearings		Materials							
	Materials	Item No.	Qty	Cycle Life	Unit Cost	\$/Cycle	Labor	Material	Item No.	Qty	Cycle Life	Unit Cost	\$/Cycle	Labor	Material	Item No.
Storage Vessel																
Waste Vessel (1)																
Product Vessel																
Waste Vessel (2)																
18A Buffer Exchange																
Pump																
Filter Holder																
Manifolding																
Instrumentation																
UF Flush Vessel																
UF Prime Vessel																
UF Filtrate Vessel																
UF Wash Vessel																
UF Diluent Vessel																
UF Regeneration Vessel																
UF Storage Vessel																
UF Waste Vessel																
19A Chromatography	3															
Chromatography Column																
Pump																
Inst. & Control System																
Manifolding																
Equilibration Vessel																

FIG. 64 Q

Equipment Maintenance Table - Microbial Fermentation

Equipment Items	Seals			Materials			Labor			Bells		Materials Item No.	Qty	
	Qty	Cycle Life	Unit Cost	\$/Cycle	Hours	\$/Cycle	Item No.	Qty	Cycle Life	Unit Cost	\$/Cycle	Hours		
Storage Vessel														
Waste Vessel (1)														
Product Vessel														
Waste Vessel (2)														
8. Buffer Exchange														
Pump														
Filter Holder														
Manifolding														
Instrumentation														
UF Flush Vessel														
UF Prime Vessel														
UF Filtrate Vessel														
UF Wash Vessel														
UF Diluent Vessel														
UF Regeneration Vessel														
UF Storage Vessel														
UF Waste Vessel														
9. Chromatography														
Chromatography Column														
Pump														
Inst. & Control System														
Manifolding														
Equilibration Vessel														

Fig. 64 R

Equipment Maintenance Table - Microbial Fermentation

Equipment Items	Shafts			Materials			Labor			Lubricant		
	Cycle Life	Unit Cost	\$/Cycle	Hours	\$/Cycle	Item No.	Qty	Cycle Life	Unit Cost	\$/Cycle	Hours	\$/Cycle
Storage Vessel												
Waste Vessel (1)												
Product Vessel												
Waste Vessel (2)												
8. Buffer Exchange												
Pump												
Filter Holder												
Manifolding												
Instrumentation												
UF Flush Vessel												
UF Prime Vessel												
UF Filtrate Vessel												
UF Wash Vessel												
UF Diluent Vessel												
UF Regeneration Vessel												
9. Chromatography												
Chromatography Column												
Pump												
Inst. & Control System												
Manifolding												
Equilibration Vessel												

FIG. 64 S

Equipment Maintenance Table - Microbial Fermentation

Equipment Items	Thermal Media						Labor			
	Unit Cost	\$/Cycle	Labor Hours	\$/Cycle	Item No.	Cycle Life	Unit Cost	\$/Cycle	Hours	\$/Cycle
Storage Vessel										
Waste Vessel (1)										
Product Vessel										
Waste Vessel (2)										
UF Buffer Exchange										
Pump										
Filter Holder										
Manifolding										
Instrumentation										
UF Flush Vessel										
UF Prime Vessel										
UF Filtrate Vessel										
UF Wash Vessel										
UF Diluent Vessel										
UF Regeneration Vessel										
UF Storage Vessel										
UF Waste Vessel										
Chromatography										
Chromatography Column										
Pump										
Inst. & Control System										
Manifolding										
Equilibration Vessel										

FIG. 64 T

Equipment Maintenance Table - Microbial Fermentation

Equipment Items	Filters			Gaskets			Bearings			Materials Item No.				
	Materials			Materials			Labor							
	Item No.	Qty	Cycle Life	Unit Cost	\$/Cycle	Hours	\$/Cycle	Item No.	Qty	Cycle Life	Unit Cost	\$/Cycle	Hours	\$/Cycle
Wash Vessel														
Eluent Vessel														
Regenerate Vessel														
Storage Vessel														
Waste Vessel (1)														
Product Vessel														
Waste Vessel (2)														
20L Buffer Exchanger														
Pump														
Filter Holder														
Manifolding														
Instrumentation														
UF Flush Vessel														
UF Prime Vessel														
UF Filtrate Vessel														
UF Wash Vessel														
UF Diluent Vessel														
UF Regeneration Vessel														
UF Storage Vessel														
UF Waste Vessel														
Chromatography Column														
Pump														

FIG. 64U

Equipment Maintenance Table - Microbial Fermentation

Equipment Items	Seals						Belts								
	Qty	Cycle Life	Unit Cost	\$/Cycle	Labor	Materials	Item No.	Qty	Unit Cost	\$/Cycle	Labor	Hours	\$/Cycle	Item No.	Qty
Wash Vessel															
Eluent Vessel															
Regenerate Vessel															
Storage Vessel															
Waste Vessel (1)															
Product Vessel															
Waste Vessel (2)															
20. Buffer Exchangers															
Pump															
Filler Holder															
Manifolding															
Instrumentation															
UF Flush Vessel															
UF Prime Vessel															
UF Filtrate Vessel															
UF Wash Vessel															
UF Diluent Vessel															
UF Regeneration Vessel															
UF Storage Vessel															
UF Waste Vessel															
21. Chromatography															
Chromatography Column															
Pump															

Fig. 64V

Equipment Maintenance Table - Microbial Fermentation

Equipment Items	Shafts			Materials			Labor			Lubricant				
	Cycle Life	Unit Cost	\$/Cycle	Hours	\$/Cycle	Qty	Cycle Life	Unit Cost	\$/Cycle	Hours	\$/Cycle	Item No.	Qty	Cycle Life
Wash Vessel														
Eluent Vessel														
Regenerate Vessel														
Storage Vessel														
Waste Vessel (1)														
Product Vessel														
Waste Vessel (2)														
20. Buffer Exchange														
Pump														
Filter Holder														
Manifolding														
Instrumentation														
UF Flush Vessel														
UF Prime Vessel														
UF Filtrate Vessel														
UF Wash Vessel														
UF Diluent Vessel														
UF Regeneration Vessel														
UF Storage Vessel														
UF Waste Vessel														
21. Chromatography														
Chromatography Column														
Pump														

F Gr. 64 W

Equipment Maintenance Table - Microbial Fermentation

Equipment Items	Thermal Media						Labor				
	Unit Cost	\$/Cycle	Labor Hours	\$/Cycle	Materials Item No.	Qty	Cycle Life	Unit Cost	\$/Cycle	Hours	\$/Cycle
Wash Vessel											
Eluent Vessel											
Regenerate Vessel											
Storage Vessel											
Waste Vessel (1)											
Product Vessel											
Waste Vessel (2)											
20. Buffer Exchange											
Pump											
Filter Holder											
Manifolding											
Instrumentation											
UF Flush Vessel											
UF Prime Vessel											
UF Filtrate Vessel											
UF Wash Vessel											
UF Diluent Vessel											
UF Regeneration Vessel											
UF Storage Vessel											
UF Waste Vessel											
21. Chromatography											
Chromatography Column											
Pump											

Fig. 61 X

Equipment Maintenance Table - Microbial Fermentation

Equipment Items	Filters				Gaskets				Bearings					
	Materials			Labor	Materials			Labor	Materials					
	Item No.	Qty	Cycle Life	Unit Cost	\$/Cycle	Hours	\$/Cycle	Item No.	Qty	Cycle Life	Unit Cost	\$/Cycle	Hours	\$/Cycle
Inst. & Control System														
Manifolding														
Equilibration Vessel														
Wash Vessel														
Eluent Vessel														
Regenerate Vessel														
Storage Vessel														
Waste Vessel (1)														
Product Vessel														
Waste Vessel (2)														
2.2.4 Sterile Filtration														
MF Wash Vessel														
Pump														
Filter Holder														
Manifolding														
Instrumentation														
MF Flush Vessel														
MF Prime Vessel														
MF Filtrate Vessel														
MF Wash Vessel														

Equipment Maintenance Table - Microbial Fermentation

Equipment Items	Seals						Belts								
	Qty	Cycle Life	Unit Cost	\$/Cycle	Hours	\$/Cycle	Item No.	Qty	Cycle Life	Unit Cost	\$/Cycle	Hours	\$/Cycle	Item No.	Qty
Inst. & Control System															
Manifolding															
Equilibration Vessel															
Wash Vessel															
Eluent Vessel															
Regenerate Vessel															
Storage Vessel															
Waste Vessel (1)															
Product Vessel															
Waste Vessel (2)															
22% Sterile Filtration															
MF Wash Vessel															
Pump															
Filter Holder															
Manifolding															
Instrumentation															
MF Flush Vessel															
MF Prime Vessel															
MF Filtrate Vessel															
MF Wash Vessel															

Equipment Maintenance Table - Microbial Fermentation

Equipment Items	Shafts						Lubricant							
	Labor			Materials			Labor			Materials				
Cycle Life	Unit Cost	\$/Cycle	Hours	\$/Cycle	Item No.	Qty	Cycle Life	Unit Cost	\$/Cycle	Hours	\$/Cycle	Item No.	Qty	Cycle Life
Inst. & Control System														
Manifolding														
Equilibration Vessel														
Wash Vessel														
Eluent Vessel														
Regenerate Vessel														
Storage Vessel														
Waste Vessel (1)														
Product Vessel														
Waste Vessel (2)														
12.2 Sterile Filtration														
MF Wash Vessel														
Pump														
Filter Holder														
Manifolding														
Instrumentation														
MF Flush Vessel														
MF Prime Vessel														
MF Filtrate Vessel														
MF Wash Vessel														

Equipment Maintenance Table - Microbial Fermentation

Equipment Items	Thermal Media										
	Unit Cost	\$/Cycle	Hours	\$/Cycle	Item No.	Qty	Cycle Life	Unit Cost	\$/Cycle	Hours	\$/Cycle
Inst & Control System											
Manifolding											
Equilibration Vessel											
Wash Vessel											
Eluent Vessel											
Regenerate Vessel											
Storage Vessel											
Waste Vessel (1)											
Product Vessel											
Waste Vessel (2)											
224 Sterile Filtration											
MF Wash Vessel											
Pump											
Filter Holder											
Manifolding											
Instrumentation											
MF Flush Vessel											
MF Prime Vessel											
MF Filtrate Vessel											
MF Wash Vessel											

FEB 6 4 AB

Master Process Parameters Table - Biopharmaceutical

Unit Operation Type	Parameter	Group 1		Group 2		Group 3	
		Scin.	Parameter	Scin.	Parameter	Scin.	Parameter
T1 Inoculum Prep	Number of Flasks	2	Temperature	37 °C	Final OD	12	
	Media Volume/flask	0.25 L/mL	Agitation Duration	200 RPM 18 Hours			
T2 Flask Growth	Scale Up Ratio	10 Fold	Temperature	37 °C	Final OD	12	
	Media Volume/Flask	1.25 L	Agitation Duration	200 RPM 18 Hours			
T3 Fermentation Production	Scale Up Ratio	10 Fold	Growth Temperature	37 Hours	Final OD	12	
	Fermentor Working Volume	500 Liters	Agitation Sparge Rate	1 HPM/L	Dry Cell Mass	0.06 Gms TDM/L	
	Antifoam A	1 mL	Back Pressure	15 VFM	Product Concentration	0.3 Gms Product/L	
	Antifoam B	5 mL	Total Duration	5 PSIG 21 Hrs	CIP		
	Beta Acid	5 mL					
T4 Initial seeding	Number of Ampules	2	Serum Content	20%	Final Bovine Serum		
	Volume Per Ampule	2 mL	Feed Rate	1 Feed per vessel per			
	Starting Cell Density	300,000 Cells/mL	Days to Confluence	2 Days	2 Days		
	Ampule Split Ratio	1 Vessel/1 Ampule		2 Days			
	Culture Vessel Type	Roll Bot.		2 Days			
	Feed Volume	100 mL		2 Days			
T5 Culture Vessel Split	Vessel Split Ratio	2	Feed Rate	0	1 Feed per vessel per		
	New Vessel Type	R8	Days to Confluence	2	2 Days		
	Feed Volume	100 mL		2 Days			
	Serum Content	20% Final Bovine Serum		2 Days			
T6 Spinner Flask Seeding	Flask Feed Volume	4 Liters	Serum Content	20%	Final Bovine Serum		
	Vessel/Flask Ratio	0.1 L Cell/L Flask	Feed Rate	1 Feed per vessel per			
	Cellular Density	5 mL/Liter	Days to Confluence	2 Days	2 Days		
	Number of PBS Washes	2					
	Number of Media Washes	1					
	No of Media/Sem Washes	2					
T7 Biosynthesis Bioreactor Preparation (Stirred Tank Reactor)	Reactor Feed Volume	500 Liters	Serum Content	20%	Final Bovine Serum		
	Spinner/Reactor Ratio	6.3	Feed Rate	1 Feed per vessel per			
	Cell Density	5 g/mLiter	Days to Confluence	2 Days	2 Days		
	Number of PBS Washes	2	Serum Free Media Washes				
	Number of Media Washes	1					
	No of Media/Sem Washes	2					
T8 Biosynthesis Bioreactor Preparation (Hollow Fiber Reactor)	Reactor Feed Volume	100 Liters	Number of Reactions	1	Harvest Volume		
	Number of PBS Washes	2	Feed Rate	1 Feed per vessel per	Product Concentration		
	Number of Media Washes	2	Days to Confluence	1 Days	Total Protein Concentn		
	No of Media/Sem Washes	2		10 Days			
	Serum Content	20% Final Bovine Serum					
T9 Biosynthesis Bioreactor Preparation (Fluidized Bed Reactor)	Reactor Feed Volume	Liters	Number of Reactions	1	Product Concentration		
	Cell Density	0.1 mL	Feed Rate	1 Feed per vessel per	Total Protein Concentn.		
	Number of PBS Washes		Days to Confluence	1 Days			
	Number of Media Washes			10 Days			
	No of Media/Sem Washes						
	Serum Content						
T10 Initial seeding	Number of Ampules	2	Serum Content	20% Final Bovine Serum			
	Volume Per Ampule	2 mL	Feed Rate	1 Feed per vessel per			
	Starting Cell Density	300,000 Cells/mL	Days to Confluence	2 Days			
	Ampule Split Ratio	1 Vessel/1 Ampule		2 Days			

A 1

Master Process Parameters Table • Biopharmaceutical

Unit Operation Type	Group 1		Group 2		Group 3	
	Parameter	Soln.	Parameter	Soln.	Parameter	Soln.
T11 Culture Vessel Split	Culture Vessel Type Feed Volume	Roll Bot 100 Mi	PBS Washes Tryptin Wash	200 Mi 100 Mi	Feed Rate Days to Confluence PBS Washes Tryptin Wash	1 Feed per vessel per 2 Days 2 Days 200 Mi 100 Mi
T12 Spinner Flask Split	Vessel/Split Ratio New Vessel Type Feed Volume Serum Content	RB 2 100 Mi 20% Fetal Bovine Serum	Serum Content Feed Rate Days to Confluence	2.0% Fetal Bovine Serum 1 Feed per vessel per 2 Days 2 Days	Amplification Factor	100%
T13 Biosynthesis Bioreactor Preparation (Stirred Tank Reactor)	Flask Feed Volume Vessel/Reactor Ratio uCarrier Density Number of PBS Washes Number of Media Washes No. of Media/Serum Washes	4 Liters 0.1 L Cell/L Flask 5 Gm/Liter 2 1 2	Serum Content Feed Rate Days to Confluence Serum Free Media Washes	2.0% Fetal Bovine Serum 1 Feed per vessel per 2 Days 10 Days 2	Product Concentration Total Protein Concen.	100%
T14 Biosynthesis Bioractor Preparation (Fluidized Bed Reactor)	Reactor Feed Volume uCarrier Density Number of PBS Washes Number of Media Washes No. of Media/Serum Washes	500 Liters 8.3 5 Gm/Liter 2 1 2	Number of Reactors Feed Rate Days to Confluence	1 1 Feed per vessel per 1 Days 10 Days	Product Concentration Total Protein Concen.	2500% Mg Prod. 0.125 Mg TPA/Mi
T15 Initial Coupling	Flask Feed Volume Vessel/Reactor Ratio uCarrier Density Number of PBS Washes Number of Media Washes No. of Media/Serum Washes	4 Liters 0.1 L Cell/L Flask 5 Gm/Liter 2 1 2 FBS	Serum Content Feed Rate Days to Confluence Serum Free Media Washes	2.0% Fetal Bovine Serum 1 Feed per vessel per 2 Days 2 Days	Amplification Factor	100%
T16 Additional Coupling	Reactor Feed Volume Spinner/Reactor Ratio uCarrier Density Number of PBS Washes Number of Media Washes No. of Media/Serum Washes	500 Liters 8.3 5 Gm/Liter 2 1 2	Serum Content Feed Rate Days to Confluence Serum Free Media Washes	2.0% Fetal Bovine Serum 1 Feed per vessel per 2 Days 10 Days 2	Product Concentration Total Protein Concen.	2500% Mg Prod. 0.125 Mg TPA/Mi
T17 Peptide Cleavage	Reactor Feed Volume Number of PBS Washes Number of Media Washes No. of Media/Serum Washes Serum Content	100 Liters 2 2 2 2	Number of Reactors Feed Rate Days to Confluence	1 1 Feed per vessel per 1 Days 10 Days	Harvest Volume Product Concentration Total Protein Concen.	500% Liters 25 Mg Prod. 0.125 Mg TPA/Mi
T18 Tissue Thawing	Crude Product Yield Environmental Temperature Thaw Duration	25 Gm Crude Prod./kg Tissue 25 C 16 Hours	Contaminant Protein Conc	100 Gm/L	Temperature Regulation CIP SIP	Y Y Y Y
T19 Homogenization	Crude Product Yield Liquid/Solid Ratio Homogenizer Temp Homogenizer Type Energy Input Duration	25 Gm Crude Prod./kg Tissue 10 L Solution/kg Tissue 4 C RS 200 HP/100UL/Hr 4 Hours	Contaminant Protein Conc	100 Gm/L	Temperature Regulation CIP SIP	Y Y Y Y
T20 Liquid Thawing					Amplification Factor	100%

A 2

Master Process Parameters Table • Biopharmaceutical

Unit Operation Type	Group 1			Group 2			Group 3		
	Parameter	Soln.	Parameter	Soln.	Parameter	Soln.	Parameter	Soln.	Parameter
T21 Product Ppt by Solids	Reagent Concentration	1 M	Kgms of Reagent/Liters Prod	0.25 Kg/L	Step Recovery of Product	95%	Step Recovery of T.P.	95%	Step Recovery of T.P.
			Temperature Addition Time	4 C	Temperature Regulation	Y	Temperature Regulation	Y	Temperature Regulation
			Additional Mix Time	0.5 Hours	CIP	Y	CIP	Y	CIP
				2 Hours	SIP	Y	SIP	Y	SIP
T22 Product Ppt by Liquids	Reagent Concentration	1 M	Liters Reagent/Liters Product	0.25 L/L	Step Recovery of Product	95%	Step Recovery of T.P.	95%	Step Recovery of T.P.
			Temperature Addition Time	4 C	Temperature Regulation	Y	Temperature Regulation	Y	Temperature Regulation
			Additional Mix Time	0.5 Hours	CIP	Y	CIP	Y	CIP
				2 Hours	SIP	Y	SIP	Y	SIP
T23 Contaminant Ppt by Solids	Reagent Concentration	1 M	Liters Reagent/Liters Product	0.25 L/L	Step Recovery of Product	95%	Step Recovery of T.P.	95%	Step Recovery of T.P.
			Temperature Addition Time	4 C	Temperature Regulation	Y	Temperature Regulation	Y	Temperature Regulation
			Additional Mix Time	0.5 Hours	CIP	Y	CIP	Y	CIP
				2 Hours	SIP	Y	SIP	Y	SIP
T24 Contaminant Ppt by Liquids	Reagent Concentration	1 M	Liters Reagent/Liters Product	0.25 L/L	Step Recovery of Product	95%	Step Recovery of T.P.	95%	Step Recovery of T.P.
			Temperature Addition Time	4 C	Temperature Regulation	Y	Temperature Regulation	Y	Temperature Regulation
			Additional Mix Time	0.5 Hours	CIP	Y	CIP	Y	CIP
				2 Hours	SIP	Y	SIP	Y	SIP
T25 Solids Harvest Tangential Flow MF	Porosity Average Flux Rate	0.2 Micron 11 LSF/HR at 40 Psi at 4 C 400 Liters/SF 1 HR	Flush Prime Concentration Factor Wash Regenerate Store	2 LSF 2 LSF 0.5 USF 1 LSF 2 LSF	Step Recovery of Product	95%	Step Recovery of T.P.	95%	Step Recovery of T.P.
				10 Fold	Temperature Regulation	Y	Temperature Regulation	Y	Temperature Regulation
			Total Throughput Filtration Time	0.5 USF	CIP	Y	CIP	Y	CIP
				2 LSF	SIP	Y	SIP	Y	SIP
T26 Continuous Centrifugation Solids Harvest	System Void Volume	5 Liters	RCF Time Volume Reduction Wash Volume	10,000 X G 60 Minutes 30 X Vol Reduction 0.2 X System Void Volume	Step Recovery of Product	95%	Step Recovery of T.P.	95%	Step Recovery of T.P.
				0.062 Vol. Reduction	Temperature Regulation	Y	Temperature Regulation	Y	Temperature Regulation
			System Void Volume	15 X System Void Volume	CIP	Y	CIP	Y	CIP
					SIP	Y	SIP	Y	SIP
T27 Continuous Centrifugation Supernatant Harvest	System Void Volume	6 Liters	RCF Time Volume Reduction Wash Volume	10,000 X G 30 Minutes 16 X Vol Reduction 1.6 X System Void Volume	Step Recovery of Product	95%	Step Recovery of T.P.	0.95	Step Recovery of T.P.
				0.062 Vol. Reduction	Temperature Regulation	Y	Temperature Regulation	Y	Temperature Regulation
			System Void Volume	16 X System Void Volume	CIP	Y	CIP	Y	CIP
					SIP	Y	SIP	Y	SIP
T28 Dilution	System Void Volume	6 Liters	RCF Time Volume Reduction Wash Volume	10,000 X G 30 Minutes 16 X Vol Reduction 1.6 X System Void Volume	Step Recovery of Product	95%	Step Recovery of T.P.	0.95	Step Recovery of T.P.
				0.062 Vol. Reduction	Temperature Regulation	Y	Temperature Regulation	Y	Temperature Regulation
			System Void Volume	16 X System Void Volume	CIP	Y	CIP	Y	CIP
					SIP	Y	SIP	Y	SIP
T29 Batch Centrifugation Solids Harvest	System Void Volume	6 Liters	RCF Time Volume Reduction Wash Volume	10,000 X G 30 Minutes 16 X Vol Reduction 1.6 X System Void Volume	Step Recovery of Product	95%	Step Recovery of T.P.	0.95	Step Recovery of T.P.
				0.062 Vol. Reduction	Temperature Regulation	Y	Temperature Regulation	Y	Temperature Regulation
			System Void Volume	16 X System Void Volume	CIP	Y	CIP	Y	CIP
					SIP	Y	SIP	Y	SIP

A3

Master Process Parameters Table - Biopharmaceutical

Unit Operation Type	Group 1			Group 2			Group 3		
	Parameter	Soln.	Parameter	Soln.	Parameter	Soln.	Parameter	Soln.	Parameter
T20 Batch Centrifugation Supernatent Harvest	System Void Volume	8 Litres	RCF	10000 X G	30 Minutes	Step Recovery of Product	95%	Y	Y
			Volume Reduction	10 X Vol Reduction	Step Recovery of T.P.	0.95			
			Wash Volume	1.5 X System Void Volume	Temperature Regulation				
					CIP				
					SIP				
T31 Cell Disruption High Press Homogen	Product Temperature	8 C	Number of Passes	0 Times	Rinses	500% Void Volumes			
	Utility Temperature	2 C	Pressure	12,000 PSI	Step Recovery of Product	95%			
	Void Volume	5 Litres	Flow Rate	5 LPM	Step Recovery of T.P.	95%			
			Temperature Increase	1.8 Degrees C/1,000 PSI	Temperature Regulation				
					CIP				
					SIP				
T32 Cell Disruption Bead Mill	Number of Passes	2							
	Reagent Void Volume	0.5 LPM							
	Flow Rate								
T33 Cell Disruption Chemical Lysis	Regent Temperature	0.5 M NaOH	Urea Reagent/Gm Product	0.4 LGm	Step Recovery of Product	95%			
	Exposure Time	4 C	Turnaround	0 MMiller	Step Recovery of T.P.				
		2 Hours			Temperature Regulation				
					CIP				
					SIP				
T34 Microfiltration Tangential Flow	Porosity	0.2 Micron	Flush	2.00 LSF	Step Recovery of Product	95%			
	Average Flux Rate	50 LSF/HR at	Prime	2.00 LSF	Step Recovery of T.P.	95%			
		40 Pfg at	Wash	0.60 LSF	Temperature Regulation				
		4 C	Solids	0.30% Of Product Solution	CIP				
		400 Liters/SF	Regenerate	1.00 LSF	SIP				
		2 HR	Store	2.00 LSF					
T35 Microfiltration Dead End	Porosity	0.2 Micron	Flush	0 LSF					
	Average Flux Rate	50 LSF/HR at	Prime	0 LSF					
		40 Pfg at	Wash	0.5 LSF					
		4 C	Solids	0.003 Of Product Solution					
		400 Liters/SF	Regenerate	1 LSF					
		0.5 HR	Store	2 LSF					
T36 Ultrafiltration Concentration/Dilution	Porosity	60 KNMWL	Flush	2.00 LSF	Step Recovery of Product	95%			
	Average Flux Rate	3 LSF/HR at	Prime	2.00 LSF	Step Recovery of T.P.	95%			
		40 Pfg at	Dilute Concentrate	0.60 LSF	Temperature Regulation				
		4 C	Solids	0.30% Of Product Solution	CIP				
		2 HR	Regenerate	1.00 LSF	SIP				
T37 Ultrafiltration Flow Dialysis	Porosity	60 KNMWL	Flush	2 LSF	Step Recovery of Product	95%			
	Average Flux Rate	3 LSF/HR at	Prime	2.00 LSF	Step Recovery of T.P.	95%			
		40 Pfg at	Dialysis Buffer	5.0 X Feed Stream Volume	Temperature Regulation				
		4 C	Wash	0.60 LSF	CIP				
		2 HR	Solids	0.30% Of Product Solution	SIP				
			Regenerate	1.00 LSF					
T38 Prod Ads Chromatography HPLC	Column Capacity	10 MG Prod/Ml Of Packing	Column Equilibration	5 Column Volumes	Prod. Edition Volume	80%			
	Column Over-size Factor	1.5 Fold	Column Wash	3 Column Volumes	Step Recovery of Product	95%			
	Column Aspect Ratio	0.37 HO	Column Elite A	3 Column Volumes	Step Recovery of T.P.	95%			
	Max. Linear Velocity	100 Cm/hr at	Column Elite B	0 Column Volumes	Temperature Regulation				
		45 Pfg and	Column Regenerate	1 Column Volume	CIP				
		4 C	Column Store	2 Column Volumes	SIP				
T39 Prod Ads Chromatography	Column Capacity	10 MG Prod/Ml Of Packing	Column Equilibration	5 Column Volumes	Prod. Edition Volume	80%			
	Column Over-size Factor	1.5 Fold	Column Wash	3 Column Volumes	Step Recovery of Product	95%			

A4

Master Process Parameters Table - Biopharmaceutical

Unit Operation Type	Group 1		Group 2		Group 3	
	Parameter	Sohn.	Parameter	Sohn.	Parameter	Sohn.
T40 Prod Ads Chromatography LPLC	Column Aspect Ratio Column Ovate Factor Column Specific Ratio Max Linear Velocity	0.37 HD 100 Cm/Hr at 45 Psig and 4 C	Column Elite A Column Elite B Column Regenerate Column Store	3 Column Volumes 0 Column Volumes 1 Column Volumes 2 Column Volumes	Step Recovery of T.P. Temperature Regulation CIP SIP	95% N Y Y
T41 Cont Ads Chromatography HPLC	Column Capacity Column Ovate Factor Column Specific Ratio Max Linear Velocity	10 MG Prod/Ml Of Packing 1.5 Fold 0.37 HD 100 Cm/Hr at 45 Psig and 4 C	Column Equilibration Column Wash Column Elite A Column Elite B Column Regenerate Column Store	5 Column Volumes 3 Column Volumes 3 Column Volumes 2 Column Volumes 1 Column Volumes 2 Column Volumes	Prod. Elution Volume Step Recovery of Product Step Recovery of T.P. Temperature Regulation CIP SIP	42% 95% 95% N Y Y
T42 Cont Ads Chromatography MPIC	Column Capacity Column Ovate Factor Column Specific Ratio Max Linear Velocity	30 MG Cont/Ml Of Packing 1.5 Fold 0.37 HD 100 Cm/Hr at 45 Psig and 4 C	Column Equilibration Column Wash Column Elite A Column Elite B Column Regenerate Column Store	6 Column Volumes 3 Column Volumes 3 Column Volumes 2 Column Volumes 1 Column Volumes 2 Column Volumes	Prod. Elution Volume Step Recovery of Product Step Recovery of T.P. Temperature Regulation CIP SIP	42% 95% 95% N Y Y
T43 Cont Ads Chromatography LPLC	Column Capacity Column Ovate Factor Column Specific Ratio Max Linear Velocity	10 MG Cont/Ml Of Packing 1.5 Fold 0.37 HD 100 Cm/Hr at 45 Psig and 400% C	Column Equilibration Column Wash Column Elite A Column Elite B Column Regenerate Column Store	5 Column Volumes 3 Column Volumes 3 Column Volumes 2 Column Volumes 1 Column Volumes 2 Column Volumes	Prod. Elution Volume Step Recovery of Product Step Recovery of T.P. Temperature Regulation CIP SIP	42% 95% 95% N Y Y
T44 Size Excl Chromatography HPLC	Load Capacity Length Max Linear Velocity	10 MG Cont/Ml Of Packing 1.5 Fold 0.37 HD 100 Cm/Hr at 45 Psig and 4 C	Column Equilibration Column Wash Column Regenerate Column Store	6 Column Volumes 3 Column Volumes 3 Column Volumes 2 Column Volumes	Prod. Elution Volume Step Recovery of Product Step Recovery of T.P. Temperature Regulation CIP SIP	42% 95% 95% N Y Y
T45 Size Excl Chromatography MPIC	Load Capacity Length Max Linear Velocity	5% of Total Column Volume 100 Cm 100 Cm/Hr at 45 Psig and 4 C	Column Equilibration Column Wash Column Regenerate Column Store	4 Column Volumes 1 Column Volumes 1 Column Volumes 2 Column Volumes	Prod. Elution Volume Step Recovery of Product Step Recovery of T.P. Temperature Regulation CIP SIP	42% 95% 95% N Y Y
T46 Size Excl Chromatography LPLC	Load Capacity Length Max Linear Velocity	5% of Total Column Volume 100 Cm 100 Cm/Hr at 45 Psig and 4 C	Column Equilibration Column Wash Column Regenerate Column Store	4 Column Volumes 1 Column Volumes 1 Column Volumes 2 Column Volumes	Prod. Elution Volume Step Recovery of Product Step Recovery of T.P. Temperature Regulation CIP SIP	42% 95% 95% N Y Y
T47 Dilution	Dilution Factor	3 Liters/Liter	Dilution Time Additional Mix Time	0.5 Hours 1 Hours	Step Recovery of Product Step Recovery of T.P. Temperature Regulation CIP SIP	95% 95% Y Y Y
T48 Resublimation	Reagent/Product Ratio Dissolution Time Additional Mix Time	0 L/kg Product 0.50 Hours	Reagent 1 Concentration Water Dist.	Step Recovery of Product Step Recovery of T.P. Temperature Regulation CIP SIP	95% 95% Y Y Y	

A5

Master Process Parameters Table - Biopharmaceutical

Master Process Parameters Table - Biopharmaceutical

Unit Operation Type	Group 1		Group 2		Group 3	
	Parameter	Soln.	Parameter	Soln.	Parameter	Soln.
55 Liquid-Liquid Extraction	Utility Final Temp Process Specific Heat Design Type (P.T.C.)	5 Degrees C 12 K BTU/Hr P	1 L Extraction/L Product 4 C 0.5 Hours 4 Hours 0.3 HP/100 L	Phase Separation Time Product Phase (Top/Bottom) Harvest Time	1800% Hours Top 0.5 Hours	Step Recovery of Product Step Recovery of T.P. Temperature Regulation CIP SIP
60 Solid-Liquid Extraction	Liquid/Liquid Ratio Extraction Temperature Duration Mix Energy	1 L Extraction/L Product 4 C 0.5 Hours 4 Hours 0.3 HP/100 L	Phase Separation Time Product Phase (Top/Bottom) Harvest Time	1800% Hours Top 0.5 Hours	Step Recovery of Product Step Recovery of T.P. Temperature Regulation CIP SIP	

A7

Combined Declaration and Power of Attorney for Patent Application

Docket Number: 1606.0020001

As a below named inventor, I hereby declare that:

My residence, post office address and citizenship are as stated below next to my name.

I believe I am the original, first and sole inventor (if only one name is listed below) or an original, first and joint inventor (if plural names are listed below) of the subject matter that is claimed and for which a patent is sought on the invention entitled System and Method for Simulation, Modeling and Scheduling of Solution Preparation in Biopharmaceutical Batch Process Manufacturing Facilities, the specification of which is attached hereto unless the following box is checked:

- was filed on _____;
as United States Application Number or PCT International Application Number _____; and
was amended on _____ (if applicable).

I hereby state that I have reviewed and understand the contents of the above identified specification, including the claims, as amended by any amendment referred to above.

I acknowledge the duty to disclose information that is material to patentability as defined in 37 C.F.R. § 1.56.

I hereby claim foreign priority benefits under 35 U.S.C. § 119(a)-(d) or § 365(b) of any foreign application(s) for patent or inventor's certificate, or § 365(a) of any PCT international application, which designated at least one country other than the United States listed below, and have also identified below any foreign application for patent or inventor's certificate, or PCT international application having a filing date before that of the application on which priority is claimed.

Prior Foreign Application(s)	Priority Claimed		
(Application No.)	(Country)	(Day/Month/Year Filed)	<input type="checkbox"/> Yes <input type="checkbox"/> No
(Application No.)	(Country)	(Day/Month/Year Filed)	<input type="checkbox"/> Yes <input type="checkbox"/> No

I hereby claim the benefit under 35 U.S.C. § 119(e) of any United States provisional application(s) listed below.

<u>60/050,294</u> (Application No.)	<u>June 20, 1997</u> (Filing Date)
_____	_____

I hereby claim the benefit under 35 U.S.C. § 120 of any United States application(s), or under § 365(c) of any PCT international application designating the United States, listed below and, insofar as the subject matter of each of the claims of this application is not disclosed in the prior United States or PCT international application in the manner provided by the first paragraph of 35 U.S.C. § 112, I acknowledge the duty to disclose information that is material to patentability as defined in 37 C.F.R. § 1.56 that became available between the filing date of the prior application and the national or PCT international filing date of this application.

<u>_____</u> (Application No.) abandoned	<u>_____</u> (Filing Date)	<u>_____</u> (Status - patented, pending,
<u>_____</u> (Application No.) abandoned	<u>_____</u> (Filing Date)	<u>_____</u> (Status - patented, pending,

**Appl. No. To be assigned
Docket No. 1606.0020001**

I hereby appoint the following attorney(s) and/or agent(s) to prosecute this application and to transact all business in the Patent and Trademark Office connected therewith:

Robert G. Sterne, Esq., Reg. No. 28,912; Edward J. Kessler, Esq., Reg. No. 25,688; Jorge A. Goldstein, Esq., Reg. No. 29,021; Samuel L. Fox, Esq., Reg. No. 30,353; David K.S. Cornwell, Esq., Reg. No. 31,944; Robert W. Esmond, Esq., Reg. No. 32,893; Tracy-Gene G. Durkin, Esq., Reg. No. 32,831; Michele A. Cimbala, Esq., Reg. No. 33,851; Michael B. Ray, Esq., Reg. No. 33,997; Robert E. Sokohl, Esq., Reg. No. 36,013; Eric K. Steffe, Esq., Reg. No. 36,688; and Michael Q. Lee, Esq., Reg. No. 35,239.

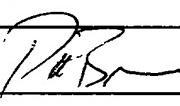
Send Correspondence to:

STERNE, KESSLER, GOLDSTEIN & FOX P.L.L.C.
1100 New York Avenue, N.W.
Suite 600
Washington, D.C. 20005-3934

Direct Telephone Calls to:

(202) 371-2600

I hereby declare that all statements made herein of my own knowledge are true and that all statements made on information and belief are believed to be true; and further that these statements were made with the knowledge that willful false statements and the like so made are punishable by fine or imprisonment, or both, under Section 1001 of Title 18 of the United States Code and that such willful false statements may jeopardize the validity of the application or any patent issued thereon.

Full name of sole or first inventor Peter G. BROWN	
Inventor's signature 	<i>6/17/53</i> Date
Residence 63 Clearwater Road, Newton, MA 02162	
Citizenship U.S.A.	
Post Office Address Same as above	

P:\USERS\VBLADES\RMILLIEN\16060020001.dcc
SKOF Rev 1/3/1998

(Supply similar information and signature for subsequent joint inventors, if any)